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August 12, 2016

The Board of Commissioners of Public Utilities Prince Charles Building 120 Torbay Road, P.O. Box 21040 St. John's, NL A1A 5B2

Attention: Ms. Cheryl Blundon Director Corporate Services & Board Secretary

Dear Ms. Blundon:

Re: The Board's Investigation and Hearing into Supply Issues and Power Outages on the Island Interconnected System – Phase Two – Filing of AMEC Report

In January and February of 2016, Hydro experienced tube ruptures in the re-heater sections of Units 1 and 2 at the Holyrood Thermal Generating Station (Holyrood). Emergency repairs were completed immediately with more extensive tube replacements planned as part of the 2016 summer annual outage.

To mitigate the risk of further boiler tube failures over the remaining operating period of the Plant, Hydro determined that it would operate the boilers at lower pressures and therefore proposed that the units be de-rated while undertaking a further review. Hydro engaged engineering specialty firm, AMEC Foster Wheeler, to review the technical basis for this de-rate assessment and to apply alternative assessment methods to maximize unit load capability while maintaining acceptable reliability.

Because of the planned tube replacements, AMEC recommends continued normal operation of Unit 1 and 2 with regular monitoring. Based upon their calculations for Unit 3, AMEC recommends operating at 90% of the operating pressure and replacement of some tubes within the next year. Hydro has completed some preliminary non-destructive testing and to date has not observed deterioration of a level that would cause concern. Hydro intends to carry out further testing in the coming year when the opportunity arises. The report notes that a 10% de-rate in operating pressure will provide additional assurance for reliable operation in the short-term. In the event of a forced outage during the 2016/2017 winter season, Hydro will replace Unit 3 lost generation with existing emergency back-up generation while immediate repairs are made using in-stock spare tube materials.

Hydro is corresponding with its boiler regulator, Government Services Center, on this matter. Hydro accepts AMEC's recommendations with the earliest opportunity for planned tube replacement being Summer of 2017, after the 2016/2017 high demand winter season.

Should you have any questions, please contact the undersigned.

Yours truly,

NEWFOUNDLAND AND LABRADOR HYDRO

Geoffrey P. Young

Senior Legal Counsel

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August 8, 2016

Mr. Nelson Seymour Nalcor Energy PO Box 12400 Hydro Place, 500 Columbus Drive St. John's, NL A1B 4K7

Dear Mr. Seymour,

RE: HOLYROOD TGS BOILER TUBE THINNING ASSESSMENT

Nalcor has a need to potentially operate the three generating units at Holyrood TGS to 2021 with a high degree of reliability. A risk assessment conducted by Nalcor has identified boiler tube failures due to tube thinning as a reliability risk and has proposed de-rating the units as a means of mitigating this risk over the remaining operating period. Amec Foster Wheeler Nuclear Canada has been engaged to review the technical basis for this de-rate assessment, and to apply alternative assessment methods to maximise unit load capability while maintaining acceptable reliability. The initial Nalcor assessment was provided as a basis [1].

Following this review, Amec Foster Wheeler concurs with the overall approach taken in the original Nalcor de-rate technical basis. However, there were issues with the process for establishing the normal and emergency operating loads that created uncertainty in the outcomes and assessment of continued reliability.

Using design and operational data provided by Nalcor [2][3] (also tabulated in Appendix 1), ASME [4] code calculations were revisited while also exploring alternative assessment methods. Amec Foster Wheeler recommends a fitness-for-service approach be taken using B&W Plant Service Bulletin PSB-26 [5] for water-touched components and API 579-1/ASME FFS-1 [6] creep rupture calculations for steam-touched components. From the analysis, it is concluded that with planned replacements completed there is a low risk of boiler tube failures due to wall thinning on Units 1 and 2, operating at current pressures, with no de-rate, to 2021.

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The assessment for Unit 3 has concluded there is a high risk of tube failures due to wall thinning within the next year. A 10% de-rate in operating pressure is recommended in addition to monitoring and tube replacement.

If it is assumed that there is a linear relationship between operating pressure and unit load for load ranges being considered, the target loads for Units 1 and 2 are 175 MW (gross), and 135MW (gross) for Unit 3. Additional recommendations are provided below.

It needs to be noted that the above assessment is based on calculations conducted with the current ASME code allowable stress values and therefore represents a variance from the registered design. Concurrence from the boiler and pressure vessel jurisdictional authority is recommended. These conclusions also consider only boiler tube wall thinning, and do not address other potential reliability risks.

1.0 BACKGROUND

Holyrood TGS consists of three oil-fired conventional steam cycle generating units. The units have a maximum output rating of 175 MW for Units 1 and 2, and 150 MW for Unit 3. Units 1 and 2 (Stage 1) were commissioned in 1969/70, and Unit 3 (Stage 2) was commissioned in 1979. Units 1 and 2 were uprated in 1987 with modifications. Unit 3 has not been uprated but the material changes have been made and the reheater surface was modified (tubes removed) in 2001 to improve boiler performance.

The boiler tubing on all three units has experienced various forms of degradation that presents a reliability risk. The primary concerns were oil ash corrosion in the high temperature sections of the tubing and fireside corrosion and erosion in the low temperature tubing. A change in fuel is considered to have mitigated the impact of these degradation mechanisms. Pad-weld repairs or replacement of tube sections have been completed in all three units to address tube failures. Wall thickness surveys are also being conducted annually to monitor tube wall loss.

2.0 ASSESSMENT METHOD

The original assessment consisted of a re-calculation of design pressure for the lowest measured wall thickness observed over the period of 2010 to 2016, using ASME BPVC Section I rules (para PG-27.2.1) [4]. The original ASME minimum wall thickness was used to back-calculate the allowable stress. Where the original ASME minimum wall thickness was not available the supplied wall thickness was used.

The assessment was based on ASME code of construction allowable stresses (1968 for Units 1 and 2, and 1977 for Unit 3), and assumed uniform wall thickness. No other tube failure mechanisms were considered. In addition, adoption of the analysis results assumed no further wall thickness reductions over the remaining operating period.

The original assessment identified a new design pressure for each inspection location where the lowest measured thickness was less than the original ASME wall thickness. A revised load was estimated for locations where the new allowable pressure was less than the original operating pressure. The revised load reflected the percentage reduction in pressure adjusted for

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measurement at the turbine stop valve, assuming a linear relationship between steam pressure and unit load.

In the original assessment the average load for the target sections of tubing was identified as the Emergency Maximum Load. The Normal Maximum Load was based on the Emergency Maximum reduced by a further 10 MW to derive a target operating load.

Following the original assessment, Nalcor contracted Babcock & Wilcox (B&W) to evaluate the Unit 3 boiler superheater, reheater, and economizer tube metal temperatures. B&W generated ASME wall thickness and temperature maps for each tube length in the Unit 3 boiler, for an equivalent fuel and using the code of construction allowable stress values. The results of this study were documented in a report [3]. This action was undertaken to address potentially significant limitations in the original work where supplied wall thicknesses were used as the minimum. Note that the results presented in this letter are based on the materials and temperatures stated in the Revision 02 of this B&W report. If significant changes are made to this evaluation, or if any undocumented field modifications are identified, the analysis presented here should be revisited and revised if necessary.

The present analysis considers four alternative methods for evaluating Maximum Allowable Working Pressure (MAWP) as listed below. For Unit 3, the B&W analysis was used to identify tube metal temperatures and materials. The B&W analysis considered the impact of the reheater surface removal in 2001. For Units 1 and 2, the post up-rate conditions were used [2].

1) Application of the B&W Plant Service Bulletin PSB-26 [5]

This bulletin provides guidance on limits for boiler tube wall loss tolerance based on supplied wall thickness, and takes advantage of manufacturing tolerances and design tolerances. For tubes satisfying this criteria, no change in operating pressure will be proposed.

2) Application of the current (2015) ASME code (Section I, PG-27.2.1) [4]

The allowable stresses for ASME materials was increased in 1999 by reducing the factor of safety. This increase in allowable stress permits an increase in the allowable pressure for a given tube wall thickness. The MAWP is derived for each section for the lowest measured wall thickness using the same method applied in the initial analysis. The margin (difference) between the calculated MAWP and original operating pressure, and the margins for incremental pressure reductions are provided.

3) Application of the current (2015) ASME code (Section I, Appendix A, para A-317.2.1) [4]

In addition to the increases in allowable stress in the current code, Appendix A, para A-317 provides a non-mandatory alternative for calculating wall thickness for boiler tubes and piping that further reduces the required tube wall thickness for a given pressure. Calculations similar to the method described above were completed to determine MAWP.

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4) Assessment of Tubing Operating in Creep Range (API 579-1/ASME FFS-1) [6]

For high temperature components, the creep life evaluation methods identified in API 579-1/ASME FFS-1 were applied. These methods are used for fitness-for-service assessments and are accepted in the National Board Inspection Code (NBIC) [7]. These evaluations result in estimated total life in operating hours for a given wall thickness, operating pressure, material, and temperature.

Assumptions

For the purpose of this wall thinning failure risk assessment, the following assumptions were applied. If any of these assumptions change, this assessment should be revisited.

- The station is required to operate in a manner consistent with current operations until 2021 in terms of cycles, hours, and operating temperatures.
- Over the next five years, the units will accumulate approximately 35,000 operating hours each (~80% operating factor per year).
- Currently, Unit 1 has approximately 193,000 total operating hours, Unit 2 has approximately 186,000 total operating hours, and Unit 3 has approximately 149,000 total operating hours.
- Wall thickness is uniform around the circumference and there is no further wall thinning.
- All tubing has been in-service since unit commissioning without accommodation for replaced tubing.
- The lowest wall thickness is representative of the tube bank for the respective area.
- Data supplied by the boiler manufacturer is correct; materials, minimum and supplied tube dimensions and temperatures.
- Allowable stresses and methods from the 2015 versions of the ASME Boiler and Pressure Vessel Code, Section I are applicable.
- Creep life calculations using lower bound Larson-Miller Parameter material properties are applicable.
- The set pressures for the closest upstream safety valves are taken as the maximum expected operating pressure for a given region.

3.0 RESULTS

The outcomes for the fitness-for-service methods described above are summarized in Table 1 and all analysis results are presented in detail in Appendix 1. These results provide a snapshot of current condition based on the inspection results and design documentation available at the time of this assessment.

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Note that for Units 1 and 2, results in Appendix 1 are presented for the reheater section being replaced in 2016. Appendix 1 also presents the results for the boiler floor tubes on Unit 3 that are planned to be restored in 2016. Discussion of these tubes are excluded from the comments below.

Acceptance Criteria

The following acceptance criteria were applied when evaluating the analysis results:

- B&W Plant Service Bulletin PSB-26: Current measured thickness greater than criteria is considered acceptable.
- ASME Code: Safety valve set pressure less than the code calculated MAWP using current tube wall thicknesses is considered acceptable.
- Creep Rupture: Calculated minimum creep life greater than 2x desired total life (projected total operating hours at 2021) is considered acceptable.
 - Unit 1 target: 456,000 hours
 - o Unit 2 target: 442,000 hours
 - o Unit 3 target: 368,000 hours
 - Tubes with calculated minimum creep life between the current number of operating hours and target number of operating hours are considered marginal and at medium risk of failure. Tubes with current operating hours exceeding the calculated minimum creep life are considered to be at high risk of failure.

3.1 Waterwall and Economiser Tubing

The waterwall and economiser tubing in all three units pass the PSB-26 criteria. This result indicates current operating pressures should not challenge the integrity of these tubes.

In Units 1 and 2, integrity of the economiser overhead bends at the 5th floor, and the Unit 3 economiser 6th floor lower tube wall bends are challenging ASME minimum wall thickness. Additionally, the waterwall upper rear tubes in Unit 2 were also found to be challenging ASME minimum wall thickness. However, these tubes currently still satisfy the PSB-26 criteria and are not anticipated to challenge creep life before end of operations. It is concluded these sections of tubing in all three units represents a low risk of failure due to tube wall thinning. Greater attention is required at these locations going forward to confirm and monitor wall thickness.

3.2 Superheater and Reheater Tubing

The steam tubing was assessed against the PSB-26 criteria, current ASME BPVC Section I (2015) code requirements, and evaluated for creep rupture life in accordance with API 579-1/ASME FFS-1.

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Page 5 of 19

<u>Unit 1</u>

The steam tubing in Unit 1 does not satisfy the PSB-26 criteria in all cases, but satisfies all ASME Section I criteria using the current code and original operating pressure. Therefore the risk of tube failure due to thinning is considered low.

<u>Unit 2</u>

The limiting location for Unit 2 is the primary superheater 8th floor bend. This location fails both the PSB-26 criteria and the current code ASME requirements at original operating pressure. The lower bound creep rupture life at the assumed operating pressure is approximately 2.6 million hours. The major factors leading to this result are extensive wall loss and a material (SA-210 A1) operating at the upper end of the acceptable range.

The results indicate this section of the primary superheater would require dropping operating pressure by approximately 10% to satisfy the current ASME code criteria. However, since the creep rupture life is shown to be extensive, it is concluded that the boiler can be operated for an additional five years at full operating pressure with low risk of tube failure due to thinning. Re-inspection of the area can confirm wall thickness, and replacement can be considered if the most severe damage is localised.

<u>Unit 3</u>

The Unit 3 steam tubing fails to satisfy the PSB-26 criteria and the ASME code requirements in several locations within the secondary superheater and reheater sections. Additional metallurgical concerns have also been identified with respect to the use of SA-213 T11 and T2 in the primary superheater.

The limiting locations are in the 9th floor cavity in the reheater. With only 64% remaining wall thickness, the 9th floor overhead reheater bends do not satisfy the PSB-26 criteria for steam tubing, do not meet the current ASME code requirements at full pressure (or with a 20% pressure de-rate), and do not meet the remaining creep life criteria. Creep life exhaustion is also predicted for the SA-213 T11 tubing below feet. Although there may be some life remaining before creep rupture based on available inspection results (currently no evidence of creep damage), it should be noted that predicted creep life is on the same order of magnitude as the reheater tubing that failed in Unit 1 earlier in 2016. To provide additional assurance in the short-term (1 year), a 10% pressure de-rate is recommended until additional targeted inspections/repairs can be conducted.

The main issue with the 9th floor cavity reheater tubes, in addition to wall thinning, is predicted metal temperatures at the upper limits of the allowable range. In this temperature range the ASME allowable stresses begin to drop significantly. Creep life is also highly dependent on temperature. This is illustrated where, although passing the PSB-26 thickness criteria, the SA-213 T11 spans are now challenging predicted creep life.

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Similarly, high predicted metal temperatures at the 10th floor primary superheater tubes are challenging predicted creep life, although still satisfying the PSB-26 criteria for wall thickness. This concern of elevated metal temperatures has also been identified in the B&W study [3]. Longer-term operation without mitigation (either through tube replacement or measures to decrease local temperatures) represents a reliability risk.

The Unit 3 reheater tubing at the 9th floor overhead south side bends and the 9th floor reheater T11 tubing below feet present a high risk of tube failure if mitigating action is not taken. The compromised primary superheating tubes should also be closely monitored. A 10% de-rate will provide additional assurance in the short-term (1 year), but selective, or bulk replacement of these tubes should be considered at the earliest opportunity followed by annual monitoring and replacement to ensure longer-term reliability.

4.0 SUMMARY AND RECOMMENDATIONS

The methods applied in the initial assessment by Nalcor for assessing boiler tube reliability associated with tube wall thinning are consistent with industry practice. Reductions in pressure for boiler component integrity management is common but acceptance from the local jurisdictional authority is typically required when operating outside of the original design configuration. Operating parameter changes to be applied over an extended period are consistent with direction in NBIC Section 3.4.1 "Re-Rating". The action can address the need to de-rate for integrity management, redefine ASME limitations using a more recent code, or uprating.

The revised analysis completed by Amec Foster Wheeler presents options for establishing a load limit for the remaining operating period (2016 to 2021) that would mitigate boiler tube reliability concerns due to tube wall thinning.

The results of the analysis indicate that Nalcor has two options:

- Base the target loads on the 2015 ASME BPVC Section I Code para. A-317.2.1 requirements.
- Base the target loads on the B&W PSB-26 for water-touched tubing where the failure mechanism is controlled by overload, and based on creep rupture where failure is controlled by creep life (steam-touched tubing).

The first option is more consistent with the re-rate alteration process. The second approach is a fitness-for-service case. Margins on safety for the ASME case are based on limits on allowable stress. In the fitness-for-service case, the margins are based on extended life well in-excess of the requirements for creep, and manufacturing and design margins for PSB-26. It is also noted that PSB-26 is consistent with the recommended practice for erosion corrosion (FAC) in ASME B31.1 Appendix IV.

To support extended life, Amec Foster Wheeler recommends adoption of the fitness-for-service approach.

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Through application of the PSB-26 criteria and predicted remaining creep life calculations, the analysis performed using currently available data suggests that Units 1 and 2 can continue to operate at full pressure with low risk of boiler tube failures due to wall thinning, to 2021. Target loads can therefore be maintained at 175 MW (gross). This conclusion assumes minimal future wall loss, with ongoing monitoring and repair.

For Unit 3, creep life is exhausted for the 9th floor cavity reheater tubing, where predicted creep life values are now in the same order of magnitude as the reheater tubing that required replacement on Units 1 and 2. Creep life is also being challenged for tubing in the primary superheater (10th floor). A 10% de-rate will provide additional assurance for reliable operation in the short-term, but corrective action is recommended at the earliest opportunity (within 1 year) to avoid tube failures. Assuming a linear relationship between pressure and load, a target load of 135 MW (gross) is recommended.

A summary of the tubes challenging ASME minimum allowable wall thickness and/or creep life, with recommended actions (for 1- and 5-year time horizons) assuming adoption of the fitness-for-service approach, is provided in Table 1 below.

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Unit	Appendix 1		Criteria at	Service Evaluation 100% Operating ressure ¹	Immediate (1 Year of Contin		Longer-Term (5 Years of Contin	
Unit	Row #	Compromised Tube Location	B&W PSB- 26	Creep Life (Larson-Miller Parameter)	Recommended Action	Recommended Unit De-Rate	Recommended Action	Recommended Unit De-Rate
1	21	Economizer, 5th Floor, Overhead (Bends)	PASS	EXTENSIVE REMAINING LIFE	Continue monitoring tube wall thinning.	None Required	Continue monitoring tube wall thinning.	None Required
	8	Primary Superheater, 8th Floor (Bends)	FAIL	EXTENSIVE REMAINING LIFE				
2	22	Water Wall Upper Rear Tubes	PASS	EXTENSIVE REMAINING LIFE	Continue monitoring tube wall thinning.	None Required	Continue monitoring tube wall thinning.	None Required
	23	Economizer, 5th Floor, Overhead (Bends)	PASS	EXTENSIVE REMAINING LIFE				
	1, 2	Economizer Tubes, 6th Floor, Lower Tube Wall (North and South Bends)	PASS	EXTENSIVE REMAINING LIFE				
	16, 17	Low Temperature Superheater, 10 th Floor, Below Feet (Boller Side) (Bends and Tubes)	PASS	MARGINAL - MEDIUM RISK				
	18	Low Temperature Superheater, 10 th Floor, Below Feet (Economizer Side) (Bends)	PASS	HIGH RISK	Identify a suitable wall		Proactively replace	10% (15 MW) (risk of creep
	19	Low Temperature Superheater, 10 th Floor, Below Feet (Economizer Side) (Tubes)	PASS	MARGINAL – MEDIUM RISK	thickness for each zone and conduct inspection and	10% (15 MW) (risk of creep rupture may be	tubing at or near end of creep life at the earliest opportunity,	rupture may be reduced, but not eliminated with a
3	20	High Temperature Superheater, 8th Floor, Overhead (Bends)	FAIL	EXTENSIVE REMAINING LIFE	selective replacement at the earliest	reduced, but not eliminated with a	placing priority on the highest-risk tubing.	reduced operating pressure)
	25, 26	High Temperature Superheater, 8.5 Floor, Below Feet (Tubes and Bends)	PASS	EXTENSIVE REMAINING LIFE	opportunity (within 1 year).	reduced operating pressure)	Continue monitoring tube wall thinning on	Re-assess based on inspection and
	29	Reheater Tubes, 9 th Floor, Overhead (Bends)	FAIL	HEGH RESK			other tubing.	replacement results.
	30	Reheater Tubes, 9th Floor, Overhead (Tubes)	FAIL	MARGINAL - MEDIUM RISK				results.
	31	Reheater Tubes, 9 th Floor, Below Feet (Tubes, SA-213 T11)	PASS	HIGH RISK				
	32	Reheater Tubes, 9 th Floor, Below Feet (Tubes, SA-213 T22)	PASS	MARGINAL – MEDIUM RISK				

Table 1: Recommendations for Boiler Tubes of Concern

¹Most relevant evaluation criteria for a given tube (based on metal temperatures) are **bold**. AM212/015/000001 R01 Uncontrolled if copied or printed from AMEC NSS Ltd. Intranet

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Page 9 of 19

Recommendations

The following recommendations are provided to support Nalcor in optimising load capability and mitigate the outage risk associated with boiler tube wall thinning:

- 1. It is recommended a fitness-for-service approach be applied to manage boiler tube integrity related to tube wall thinning. Limits for water-touched tubes should be based on the PSB-26 criteria, and for the steam-touched (high-temperature) tubes, based on predicted creep rupture life.
- 2. The results of this analysis should be reviewed with the local jurisdictional authority to assess regulatory requirements associated with implementation. It is expected that this discussion will confirm the feasibility of adopting the fitness-for-service approach.
- 3. It is recommended additional tube replacements be completed in the Unit 3 primary superheater and reheater at the earliest opportunity. The creep life analysis has determined that the primary superheater tubing on the 10th floor (below feet) and reheater tubing in the 9th floor cavity are approaching end of life. Creep life is predicted to be in the same order of magnitude as the reheater tubing in Units 1 and 2 that required replacement in 2016. A 10% (15 MW) de-rate is recommended in the interim period in order to regain margin and reduce the risk of creep rupture.
- 4. An assessment should be performed to determine minimum acceptable wall thickness for compromised areas to support inspection and selective replacement.
- 5. Conduct follow-up inspections in 2016 to confirm materials and wall thickness in limiting locations (extent of damage).
- 6. Continue with annual boiler tube wall thickness surveys to monitor damage accumulation rates and locations. If there is evidence of additional wall thinning, the rerating needs to be revisited. The cause(s) of tube thinning on Unit 3 should be investigated and mitigated where possible in order to reduce the risk of early tube failure.
- 7. Other failure mechanisms beyond wall thinning, such as fatigue cracking, are outside this scope of this thickness-based analysis. Fatigue failures are due to pressure/temperature cycles, therefore it is recommended that stops/starts and load cycling be limited when possible.
- Use of pressure for control of generator output is recommended over load control, due to potential non-linearity in the translation between the pressure and load at higher pressure reductions (i.e. >10%). Additionally, if a long-term de-rate is applied, a boiler performance assessment is recommended to evaluate other impacts.

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REFERENCES

- [1] Correspondence, "Holyrood TGS Condition Re-Rate Assessment Review", AmecFW File No. AM212/011/000001 R00, 2016-04-27.
- [2] Report, "Uprating Holyrood Units 1 and 2 from 150 MW to 175 MW", File No. TIS 8536, 1990-10-01.
- [3] Report, "Thermal Study Superheater and Reheater Metal" B&W File No. TP900932 R02, 2016-07-05.
- [4] ASME Boiler and Pressure Vessel Code Section I, 2015-07-01.
- [5] B&W Plant Service Bulletin, "Tube Thickness Evaluation Repair or Replacement Guide", B&W File No. PSB-26, 1994-06-01.
- [6] API 579-1/ASME FFS-1, "Fitness for Service", 2007-06-05.
- [7] National Board Inspection Code (NBIC), Part 3 "Repairs and Alterations", NB-23 (2015).

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Page 12 of 19

Analysis Results

														Uni	t 1														
			Physi	cal Propert	ies		B&W	Plant Ser	vice Bul	letin PSI	3-26		MAWF	(ASME)	BPVC Sec	tion I, Pi	G-27.2.1)		MAWF	(ASME	BPVC Ser	ction I, A	-317.2.1)	at 1 Oper	n-Miller 00% rating isure	at ! Oper	n-Miller 90% rating ssure
#	Inspection Location	Lowest Massiered Wall Thickness Jinch)	Assumed Jacos Operating Pressure [pui]	Melerial	Temp. (71	Tebe DD (inches)	P18-25 Requirement (1 - specified wall)	Percent Remaining from Driginal	Hequired Well [inches]	Margin at Dwign Pressure (Inches)	Criteria Satisfied?	MAWP [pil]	Max. Dperating Pressure Margin (pel)	Margin with 25 pressure reduction [pii]	Margin with 5% pressure reduction (s4)	Margin with 12% pressure reduction (psi)	Margin with 15N pressure reduction (pul)	Mergin with 20% pressure reduction [pvi]	RAAWP (p+l)	Mas. Operating Protoco Margin (pril)	Margin with 255 pressure reduction [mil]	Margin with 3% pressure reduction [pul]	Margin with 10% pressure reduction [psi]	Margin with 13% pressure reduction [gol]	Margin with 205- pressure reduction [psi]	Minimum Predicted Life (hours)	Mran Predicted Life (hours)	Malmum Produced Life (hours)	Merer Predicted Life (hours)
1	Weter Wall Tubes at Bunars	0.254	2205	14210A1	701	2.1	7054	182%	8.345	8.684	YES	2580	375	419	425	\$83	705	415	1770	\$65	429	675	736	296	1006	1.005+08	A.352+60	2.517+08	2.022+00
2	Economizer, Sth Floor, Beliow Feet	0.202	2205	\$A152	794	1	70%4	10245	0.340	2.052	725	2505	800	444	310	620	750	44	2767	342	606	873	783	83	1005	8.255 +027	2.767+68	2.076+08	Lastria
3	Boller Flaur Tubes	0.174	4		1.141	1.4	70%4	\$75.	0.140	E 634	TES	04.1	1000		1 a	12	3/253	14	141	2	1	102.0			1 4	*	-		- 141
4	Frimary Superhisater, 10th Fluor, Selow Fest	0.206	2015	\$4213711	814	÷	\$354	1148	8.333	1.033	755	2894	***	680	741	ш	\$47	3050	2859	804	846	807	1010	щи	1215	2.252+06	1.248+07	8.246404	2.036+07
3	Frimary Superfreater, 5th Floor, Overhead	0.19	2023	3A310A1	758	2	8354	1084	s.111	8.037	115	2413	360	403	463	343	***	m	2572	\$17	35¥	620	723	326	82ž	2.825+87	1.310144	4,488+07	2.725+08
4	Frimery SuperVester, 5th Fibor, Balow Fast	0.183	2033	SATIOAL	732	1	83%e	111%	8.340	6.043	123	2624	334	621	687	780	872	595	2017	762	tot	M	957	1010	3123	9.485+01	4.852+00	2.228+08	1.462+09
1	Frimary Superfreater, 8th Hour (Bend)	0.111	2055	SAZIDAL	732	2	A174	\$375	0.140	8 0 13	725	2145	-15	112	394	297	400	saz	2314	259	300	362	461	367	670	1.872+07	3.365+05	4.592+07	3.495+03
	Frimary Superheater, Sth Riccr (Tube)	8.173	2053	\$4210A1	732	2	#35%4	303.6	0.140	8.635	725	2473	-	459	321	621	726	829	2647	582	411	623	793	900	tant	3.046+07	4,231+02	3.376+08	0.306+08
1	Secondary Superhester, 7th Floor, Overheed	0.192	2055	14213TP323H	993	1	85%t	1167.	6.345	8.053	101	1241	1154	1295	1397	1400	2502	1001	3460	1405	3418	2507	3430	1711	3836	1.816+87	2.428+08	2.468+02	4.505+08
10	Secondary Superheater, 7th Ficor, Balow Feet	0.213	2013	\$A215722	875	2	8354	235	0.221	-0.005	NO	2147			193	294	400	Jai	2275	238	262	m	428	529	411	8.432+05	1.791+04	2.632+08	7.262+08
n	Secondary Seperheater, 8th Ficor, Below Feet	0.137	2055	\$421317347H	1160	3	£5%	825	8.204	-0.001	NO	2059		a	107	209	312	415	2130	134	116	257	340	413	348	8.002+01	2.272+05	2.345+05	J.778+05
12	Secondary Superheater, 5th Hoor (Overhead from Scaffold)	2.193	2055	\$A213722	959	2	854	825	8.202	40.09	NO	2076	10	ø	111	224	117	430	2208	131	194	254	358	451	364	7.38E485	J.astros	T-434+08	£.825+06
13	Reheater, Sth. Floor, Deethead	130.2	312	54213771044	1125	2.125	#3%;	41%	311.6	-0.065	NO	318	-224	411	-187	-441	-1534	-103	117	145	-114	418	41	-45	dif	1.218+05	1.305+06	2.368+05	2.028+06
24	Roheater, 9th floor, Bolow Feet (North Bend)	0.14	532	\$A213722	3060	2.125	4374	926	0.125	8.014	755	670	110	268	.284	221	211	264	712	220	200	246	m	295	226	2.825+06	7,452+08	4,485+08	1.085+07
15	Reheater, Bth Fizor, Below Fest [North Bend]	0.141	532	54213722	1060	2.115	85%4	1235	0.326	0.074	YES	===	401	411	428	415	481	504	1000	468	478	894	\$23	547	574	8.715+06	1.868+07	1.212+07	2.426+07
38	Rehester, Sth Floor, Below Feet (South Section of Tube)	0.214	533	1421319	11.00	2.125	8374	305%	0371	#041	YES	-	367	177	181	220	346	m	742	310	ш	217	263	290	317	3.568+06	1.715-07	4.172+08	2.786+07

² Tubes to be replaced in 2016.

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Page 13 of 19

Analysis Results

														Uni	t 1														
			Physic	al Propert	ties		B&W	Plant Ser	vice Bull	letin PSI	B-26		MAWP	(ASME	BPVC Sec	tion I, Po	3-27.2.1)		MAWE	(ASME	BPVC Sec	tion I, A	-317.2.1)	at 1	ating	at 9 Oper	n-Miller 90% rating ssure
#	Inspection Location	Lowest Measured Wall Thickness Jinch)	Assumed 100% Operating Frances [pui]	Material	Temp. [7]	Tube DD (inches)	P58-26 Requirement (1= specified wealt)	Persent Remaining from Drigtmal	Required Wat (inches)	Margin et Design Prassure [Inches]	Coltonia Satisfied?	MAWP (2H)	Mas. Operating Pressure Alargin (pul)	Alwrgin with 1% pressure reskution [pul]	Margin with 55 pressure reduction [sel]	Margin with 10% pressure reduction [psi]	Margin with 11% pressure reduction [p4]	Margin with 20% pressure reduction [pu]	Mawy ip=1	Mas. Dporating Pressure Margin (pul)	Margin with 2% pressure (reduction (pul)	Margin with SA. pressure reduction [col]	Margin with 10% pressure reduction [psi]	Margin with 11% pressure reduction [pul]	Margin with 20% pressure (selection (pul)	Minimum Predicted Life (haurs)	Mean Producted Life (howers)	Minimum Predicted Ule [heurs]	Mean Produced Life (hears)
17	Reheater, 3th Floor, Selow Fest (North Section of Tube)	0.254	112	5A113722	1060	1.125	8554	304K	0.126	0.014	113	770	211	248	364	жı	110		#11	301	112	ш	354	л	407	4.432+06	3.886+07	\$.728+05	1.308+07
15	Reheuter, 3th Figur, Overhead	0.185	\$12	\$4213722	1063	2.5	1354	1115	0.325	0.019	115	611	159	170	334	212	239	254	751	321	232	348	276	321	128	2.64(+04	7.515+06	4.325+06	1.011+07
19	Ashauter, 10th Finar, Selaw Feet	0.137	112	\$420971	730	2.5	8552	3025	6.154	0.003	163	1646	1114	2124	1340	1167	1193	1220	1821	1291	1101	1111	1344	1370	1333	1.480+12	3.768+12	1.736-11	9.405+12
20	Weter Wall Kowe Regard	0.215	2225	TATION	701	2.5	70%4	104.6	8.340	8.671	785	2582	477	\$21	387	687	101	\$18	2875	\$70	714	780	890	1000	1111	1,19(+08	1.146+01	8.428+08	2.685+29
n	Economizer, 3th Ficur, Overhead (Bend)	0.143	12.05	\$4193	704	1	70%e	72%	0.140	6.003	765	1747	-454	-414	-547	-237	-127	-17	1891	-122	-268	-202	-92	38	129	1.111-05	7.452+06	8.952+08	1.872+07
11	Economizer, 3th Floor, Overhead (Tube)	0.183	22.05	5A192	704	2	70%e	925	Ø.149	8.041	765	2323	- 114	142	238	334	444	259	2475	378	114	384	454	63	113	3.496+07	2.362+07	8.718-07	2.708+02

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AM212/015/000001 R01

Page 14 of 19

Form 111 R15

Analysis Results

														Uni	t 2														
			Physic	cal Propert	ies T		B&W	Plant Ser	vice Bul	letin PSI	3-25		MAWF	(ASME	BPVC Sec	tion I, Pe	G-27.2.1)		MAWF	(ASME	BPVC Sec	tion I, A	-317.2.1				at s Oper	n-Miller 90% rating isure
#	Inspection Location	Lowest Measured Wall Thickness Jinch)	Assumed Jacob Operating Pressure (pu)	Material	Temp. 171	Tube DD (inches)	P53-25 Requirement (t = specified well)	Percent Remaining from Driginal	Required Wal (Insthes)	Margin at Design Pressure [Inshes]	Criteria Satisfied?	Mawp (pu)	Mas. Operating Pressure Margin (pul)	Margin with 2% pressure reduction (pul)	Margin with 3% pressure reduction (pci)	Margin with 12% pressure reduction [pai]	Margin with 15% pressure reduction [pul]	Margin with ION pressure reduction (pu)	Mawr Iow]	Mas. Operating Pressure Margin (pol)	Margin with 1% pressure reduction [mil]	Margie with 5% presence reduction [polj	Alargin with 10% protocre reduction [god]	Margin wrth 15% pressure (pol)	Margin with 10% pressure reduction [ps]	Minimum Predicted Life (hours)	Mean Predicted Life (bours)	Minimum Fredicted Life [hours]	Mean Predicted Life (Incors)
1	Water Well Tubet at Buners	0.171	2205	14210A1	701	2.5	70%4	867.	0.148	8211	YES	2105	-100	-34	10	120	211	341	2287	81	126	252	301	413	113	1.485+07	Lazérda	4.376+07	4.395+08
1	Economicer, 4th Finor, Below Feet	0.209	2205	SALES	704	2	70%4	303.6	0.240	1.043	YES	2710	505	548	#15	726	#16	944	2875	sta	714	781	<i>e</i> 11	imi	2111	1.255+08	2.375+08	2.772+08	5.256+08
3	Roler Floor Tubes	0.177	1.10	10.00	DE SO	10.00	70%4	195.	0.340	0.037	TES	18400	12.2014	+	1	1		1000	11200	1.	-	1			100		1000		+
4	Frimary Superheater, 20th Floor, Balow Feet (Bend)	0.163	2015	54213723	914	1	85%	916	£.153	8310	¥15	2054	-4	80	101	204	307	410	2204	154	101	253	358	459	362	5,632+65	a.suffici	1.035+04	6.412+05
5	Primary Superheater, 10th Floor, Below Feat (Tube)	0.188	1055	54213713	114	3	15%	304%	8.153	0.725	res	2422	547	453	#70	\$73	675	m	2342	\$27	368	629	111	8 35	311	1.312+06	8.345+04	2.075+06	1.306+07
	Frenaty Superheater, 3th Floor, Overhead	0.151	2053	SAZIDAL	768	2	8554	3068	0.195	10.015	YES	2410	375	426	477	340	643	786	25.86	344	374	633	738	841	944	2.121+07	2.572+02	4.886+07	2.835+08
7	Frimary Superheater, 9th Floor, Balow Feet Frimary	0.142	2033	SA210A1	712	2	#354	130%	(0.140)	0.341	YES	2623	\$10/	63	\$70	m	276	\$79	2800	745	784	843	\$10	1053	1156	\$ 225+07	8.552+08	2.228+08	1.405+09
1	Frimary Superheater, 8th Floor (Bend) Frimary	0.125	3055	54210A1	712	1	#3%e	78.5	0.145	-0.915	NO .	1700	-358	-915	-252	140	-48	(66)	1861	-194	-153	-91	-11	114	217	3.552+05	2.685407	6.862+06	6.392+07
1	Superheater, Sth Finer (Tube) Secondary	0.175	2055	\$#210#1	732	1	159	19876	8.143	8.016	πι	2573	534	328	620	729	826	121	2743	898)	725	296	229	1003	5045 E	7.341497	3.722+08	1.442+08	1.234+09
10	Superheater, 7th Floor, Divertiged	0.192	2055	\$A31377321H	993	;	1350	1368	8.340	0.052	725	\$243	1154	1215	1297	1400	1502	1625	3440	3405	3446	1507	2620	1713	1826	1.810+07	2-422108	3.462+07	4.605+03
===	Superheater, 7th Floor, Below Fest Secondary	5.12	2055	\$A213722	875	2	8594	155	p 221	-8.381	NO	2106	181	191	293	\$56	459	562	2316	281	.122	341	485	520	482	3,252+05	4.882+06	1.942+06	8.315+06
12	Superheater, 8th Floor, Below Feet Secondary	0.192	2033	\$4213TF347H	1160	2	1152	80%	8.204	-6.011	980	1958	-47	-16	46	349	251	394	2118	78	334	325	278	381	484	7,012+05	Lateios	1.172+06	3.282+04
13	Superheater, 6th Floor (Dverheed from Scatfield)	0.213	2035	14111731	373	2	13%	29%	8.291	8.011	YES.	2326	m	m	374	477	578	612	2445	411	452	114	817	718	822	1.542+06	7.272+06	3.045+08	1.378+07
34	Reheater, Sth Floor, Diverhead	0.05	525	14211771044	1116	2.125	25%2	3.4N	861.0	-0.076	MQ	247	-278	-167	-252	-325	-299	-173	315	-201	-289	-189	-117	-444	-104	4.035+04	3.616+05	2,455+64	6.552+05
11	Balteater, Sth Ficor, Balow Feet (South Band)	8.204	\$23	5421579	1100	2.125	85%	10256	0.575	0.033	113		341	154	170	295	222	244	711	185	. 197	112	239	265	291	2.342+06	1.502+07	3.648+04	2.438+07
16	Rahester, 9th Floor, Salow Feet (South Band)	8.203	525	14211179	1100	2.125	\$3%s	1005	0.171	8.029	YES	633	128	m	254	111	207	233	696	m	111	397	225	250	276	2.835+06	1.152+67	1,251+06	2.196467
17	Reheater, 3th Floor, Salow Feet (South Saction of Tube)	0.225	525	1411378	1100	2.115	4354	111%	6.173	8.093	YES	741	216	226	242	268	214	121	785	250	m	287	m	319	.363	1.518+06	2.366+07	5.735+04	3.425+07

³ Tubes to be replaced in 2016.

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Page 15 of 19

Analysis Results

									-					Uni	t 2														
			Physic	al Proper	ties	1-	B&W	Plant Ser	vice Bull	letin PSI	8-26		MAWP	(ASME I	3PVC Sec	tion I, P	G-27.2.1)		MAWF	(ASME	BPVC Sec	ction I, A	-317.2.1)	Larson at 1 Open Pres	00%	at 9 Oper	n-Miller 90% rating ssure
H	Inspection Location	Lawret Messured Wall Thiskness [inch]	Assumed 100% Operating Pressure (pu)	Material	Tamp. (*/	Tube DD (inches)	PSB-26 Requirement (t= specified well)	Percent Remaining frum Drigtnal	Required Wall Sothes)	Margin st Design Prossure (Inshei)	Critaria Satisfied?	MAWP {pe}	Maa. Operating Pressure Margin (pol)	Morgin with 2% pressure reduction [poi]	Margin with 5% pressure reduction (psi)	Margin with 10% presults reduction (psi)	Margin with 15% preserve reduction [pu]	Margin with 20% pressure reduction [pu]	MANUP Isul	Maa, Operating Pressure Margin [p:0]	Margin with 155 pressure reduction [psi]	Margin with 5% pressure reduction [poi]	Margin with 10% pressure reduction [pui]	Margin with 13% protects reduction [pol]	Margin with 20% pressure reduction [pul]	Minimum Predicted Life (hours)	Mean Predicted Life (Dawn)	Alfoimum Predicted U/a (hoves)	Mistr Predicted (Jav (Nours)
ш	Rahestar, 9th Floor, Balow Fast (North Section of Tube)	8.17	53	\$4213722	1060	2.129	83%4	1156	8.316	8.044	105	861	336	348	لهر	590	424	ш	121	405	411	459	455	483	tat	7.102+06	1.178+07	1.012+07	2.045+07
19	Reheater, 3th Figur, Dearhead	0.189	\$25	\$4213T22	1065	2.5	#3%e	154%	0.126	8.041	TES	711	185	296	212	234	264	291	775	248	25.8	274	300	327	313	1.110+05	8.675+06	\$.291+06	1.142+07
20	Rohaster, 10th Flatr, Baltry Feat	0.133	\$25	SA20973	703	2.5	4354	23%	6.134	8.928	YES	1530	1045	3076	1091	1118	2344	1170	1766	1241	1252	1267	1294	1320	1548	1.158+12	3.316+12	2.518+12	A.451+17
21	Water Wall Knee Region	0.216	2205	1A210A1	701	2.3	70%4	1014	0.344	0.578	YES	1756	311	593	661	m	441	\$92	2950	741	789	855	965	1075	1100	1.745+08	2.452+68	4.275+08	3.256+03
11	Water Wall Upper Acer Tuber	0.15	1105	SATION1	701	2.5	7094	79%	5 140	0.010	ITA	1810	-515	(881)	-245	-375	44	45	1388	-217	479	-107	3	111	234	4.0005+006	1.342+07	1.192+07	2.348+08
28	Economics, 5th Finat, Overhead (Send)	0.155	2205	\$4182	704	2	70%¢	78%	0.544	0.015	155	1917	-254	-344	-177	-47	45	257	2065	-345	-85	-29		282	301	7,625104	1.002+07	1 #28+07	1.522+07
24	Economicer, 5th Floor, Overhead (Tube)	0.183	2105	SAINI	704	3	70%4	346	8.340	0.044	765	2396	281	235	302	412	523	612	2354	347	161	459	\$70	680	750	4.725+07	9.361+07	1.302+08	2.348+08

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Page 16 of 19

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Analysis Results

														Uni	t 3														
			Physi	al Propert	ies	I	B&W	Plant Ser	rvice Bui	letin PSI	8-26		MAWF	(ASME	BPVC Sec	tion I, P	G-27.2.1)		MAWI	P (ASME	BPVC Se	tion I, A	-317.2.1		at 1	-Miller 00% ating sure	at : Ope	n-Miller 90% rating ssure
#	Inspection Location	Larwest Maasurud Wull Thiskness (Jinch)	Assumed 100% Diporating Prosure (pil)	Matarial	Tamp. (79)	Tube DD (Inches)	P38-24 Requirement (t = specified well)	Persant Remaining fram Griginal	Required Wal (Inches)	Margin at Design Pressure (Inches)	Enteria Satisfied?	Mawp [pu]	Maa. Operating Prasuurs Margin (pai)	Margin with 2% pressure reduction (pu)	Mergin with SN: pressure reduction (poi)	Margin with 10% pressure reduction [pel]	Margin with 13% pressure reduction [psi]	Margin with 20% pressure reduction [pei]	MANUF [24]	Maz, Djørreting Pressure Margin (pol)	Margin with 15, protoco reduction [pol]	Margin with Sts pressure reduction [p+1]	Margin with 10% pressure reduction [psi]	Margin with 15% pressure reduction [pol]	Margin with 20% pressure reduction [pol]	Moleum Predicted Ufe (beurs)	Mean Predicted Life (hours)	Minimum Predicted Life (hours)	Mean Predicted Life (beurs)
1	Economizer Tuber, Sth Floor, Lewer Tobe Well (South Rend)	0.151	1200	1A210A1	700	2.5	70%£	75%	9.141	5 811	TES	1858	-342	-208	-331	-122	-12	38	2017	-143	-419	-53	57	367	277	L495-94	K.#13+07	1.585+07	1.736+08
1	Economicer Tubes, 61h Floor, Lower Tube Wall (North Band)	0.155	2200	SAZIOAL	700	2.5	70%4	78%	0.342	0.013	185	1886	-454	-276	-304	-94	16	128	2065	-135	-ii	-25	et.	293	305	8.336+06	7.755+97	2.812+07	1.552+0.5
1	Economizer Tubez, 6th Floor, Lower Tube Well (Tube)	0.113	2100	1A230A1	700	2.5	70%2	83%	0.342	8347	715	3370	170	214	380	350	\$00	6 10	23.57	317	401	467	\$77	647	797	1.942+97	4.832+03	1.115+08	2.111+09
a.	Economizer Tubes, 21A Flass, Lower (Under Sotblower)	0.178	2200	SATIOAL	780	23	70%4	485	8,142	6 2 3 4	113	2111	μ	н	111	213	542	452	2196	196	240	305	416	\$26	635	1.752+07	2.835+54	7.225+07	6.342+08
3	Economicer Tubes, 8th Floor, Lower (North Bendl	0.318	2200	54230A1	700	2.5	72%4	307%	8.141	8.076	111	1754	554	631	704	214	#14	1034	2390	795	814	800	1010	3330	1210	1.052+08	2.092+09	1.025+08	1.796+09
3	Economicer Tubes, 8th Floor, Lower (North Bend)	0.185	2200	14210A1	700	25	70%4	825	8.341	2.044	111	2317	117	m	217	347	457	\$47	вu	313	117	40	111	643	753	4.315+07	4,356-64	1.136104	8.891+68
7	Economizer Tubes, Rth Floor, Upper (South Benel)	0.171	2200	\$421041	700	2.5	7054	445	0.342	8.025	113	nu	-ti	4	n	ш	242	152	2295	н	115	205	m	425	533	1.812+07	1.506+0.5	4.53E+07	4.742+08
1	Economizer Tubes, 815 Floor, Upper (Tube)	6.178	2200	SAZSUAS	700	25	70%4	/445	8.142	6.014	MES	un	#	36	122	212	342	412	2896	194	340	506	416	529	636	2.755+07	2.835+03	7.332+07	E.ME+08
3	Tubes, 8th Floot, Upper (North Bendi Law	0.178	2200	\$421041	700	23	7014	44%	0.141	0.036	TES	ա	и	и	ш	211	342	452	2135	195	240	305	436	526	836	2.152407	2.415+04	7.132+07	\$746+03
10	Temperature Superheater, Sth Floor, Overhead (Rand)	0.180	2010	1421041	636	u	45%	495	0.375	1102	715	2254	368	241	341	419	549	#50	2444	634	174	333	623	734	814	8.512+07	8.29(+04	2.295+08	1.921+01
11	Low Temperature Superheater, 8th Floor, Overhead (Tube)	0.154	2010	1421041	836	2.5	13%	\$175	0.175	9.031	YES	2481	452	41	5 53	652	713	853	2611	641	F #1	142	M2	EME	tera	1.852+08	2.31(101	A 602+08	1411-09
12	Low Tempereture Superheator, 3th Finor, Below Feet (Rend)	0.179	2010	SAZIOAS	741	2.5	\$354	485	0.171	0.005	113	1922	-44	ŧ	ü	223	203	314	2081	n	ш	m	372	111	473	7.582+06	6.328+07	1.882+07	2475+05
13	Low Temperature Superheater, 5th Floor, Below Feet (Tube)	0.215	2519	14210A1	741	n	83%6	1064	0.175	8.645	115	2347	177	417	ın	378	ini	779	2555	545	540	eu	746	м	\$47	4.252+67	3.046+04	8.818+07	6.605+0.8
14	Low Temperature Luperfreater, 9th Floor, Overhead (Bend)	0.170	2010	SALEFTIA	756	ы	45%4	415	0.173	-8:003	M	21.64	174	24	274	119	423	576	2374	368	404	485	543	666	768	2.712+00	£.728+08	4.378+08	2.175409

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Page 17 of 19

AP	PEN	DIX	1

Analysis Results

														Uni	t 3														
			Physic	al Propert	ies		B&W	Plant Ser	vice Bul	etin PSI	3-26		MAWP	(ASME	BPVC Sec	tion I, P	G-27.2.1)		MAWF	(ASME	BPVC Sec	tion I, A	-317.2.1	Î			at s Oper	n-Miller 90% rating isure
#	Inspection Location	Lowest Maasurid Wall Thickness (inch)	Assumed 100% Dipensing Protoco (pul)	Material	Tump. [7]	Tube 20 (inches)	PSB-26 Requirement (1+ specified well)	Persent Remeining from Original	Required Wat (Inches)	Margin at Design Pressore (aches)	Criteria Satirfical?	MANUP [psi]	Maa. Operating Processory Nargin (pri)	Margin with 25 pressure reduction (poi)	Margin with 335 pressure sreduction (pul)	Margin with 10% pressure reduction [pui]	Margin with 15% pressure reduction [cui]	Margin with 20% pressure reduction [pu]	Massir P [p-4]	Mar. Operating Pressure Margin (psi)	Alergin with 25 pressore reduction [psi]	Margin w(th.1% pressure reduction [psi]	Margin with 10% pressure reduction [pul]	Marga with 15% presente reduction (pul)	Margin with 15% pressure readertion [pv]	Minimum Prodicted U/a (hours)	Mean Predicted Life (hown)	Minimum Predicted Life (houri)	Mean Predicted Life (Invers)
13	Low Temperature Superheater, 3th Floor, Overhead (Tube)	0.210	2018	SA205TLA	756	23	\$5%2	301%	6.173	8.017	113	2005	711	***	84	gu	3093	tint	3005	995	3035	1096	1194	1297	1387	1.300+09	4,055+07	1.098+09	8.4521-09
15	Low Temperature Superheater, 12th Floor, Below Feet (Sciler Side) (Bend)	0.374	2010	SATISTI	1015	ы	E5 %¢	57 %	8,333	2.039	723	1863	-184	-118	ł.	84	112	232	1956	-54	-34	47	347	348	ш	1.742-05	8,755+05	2.845+05	1.588+06
17	Low Temperature Superheater, 10th Floor, Below Fest (Boller Side) (Tube)	9.430	2010	54213711	1019	2.5	1359	383%,	6.325	(e.mit)	113	2206	195	234	297	297	<i>a</i> 11	598	2120	21.0	250	410	523	623	712	3.468+05	2.562+06	1_30(+01	3.015+08
11	Law Temperature Superheater, 10th Flace, Below Feet (Economicer Side) (Bend)	8.310	2018	SATELLE I	823	2.5	ensi	82%	8.287	8.013	713	1719	-191	-381	-351	-90	10	ш	1013	-187	-557	-36		105	205	1.522+05	2.855+00	1.648+85	4.336+01
19	Low Temperature Superhaster, 10th Floor, Below Feet (Economicer Side) (Tube)	0.347	2010	54211772	55 3	23	E354	102%	8.287	0.010	TES	1945	45	4	58	256	297	117	2043	58	n	259	263	16 0	461	1,812+01	4.175-01	1.441-05	8.018+05
20	High Temperature Superheater, 8th Floor, Overhead (Send)	8.314	2010	ALTEDIAN	541	2.25	8354	62.76	0.378	-0.062	NG	1840	-170	.130	-43	n	ш	212	un	-91	111	50	220	ы	ш	3.255+65	a.756465	A.798+03	1.301+08
21	High Temperature Superheater, 8th Floor, Overhead (Tube)	0.228	2010	SAIOSTIA	ы	2.23	15%	70%	0.278	-0.052	MIT	1959	-81	-38	SU	350	29.1	311	2581	71	ш	172	m	m	m	4.052+05	2.305-06	6.008+05	1.618+06
22	High Temperature Superheater, 2th Floor, Selow Feet	9.223	3010	LAIDITLA	905	2.35	23 54	785	0.242	-0.021	NO	2704	894	754	754	205	995	1014	2875		808	967	1047	£164	1268	1.585+04	4.805+06	2.5121-05	7.006+04
13	High Temperature Superheater, S.S. Floor, Dyerhead (Bend)	0.275	2010	5A213732	1037	1	85%2	815	0.178	-0.003	NO	1924	-46	-44	я	ш	ш	334	2025	u	54	228	218	317	417	4.525+05	1.766+06	8.405+05	3.095+06
24	High Temperature Superfector, 8.3 Floor, Overhead (Tube)	0.243	2010	54213722	3034	1	45%4	87%	8.27k	8.007	113	2015	25	83	125	226	124	47	2141	m	m	ш	m	411	m	6.336+PS	2,396106	1.152+06	4.176+05
25	High Temperature Superheater, 8.3 Floor, Below Fest (Band)	0.179	2010	543111721	1073	133	8354	AIN	8 34E	8 837	TEA	1500	-110	-71	4		RI	21	2005	4	n	95	296	294	JU 7	4.125-05	1.705+06	7.802+05	3.105+05

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Page 18 of 19

Form 111 R15

Analysis Results

														Uni	it 3														
			Physic	cal Propert	les		B&W	Plant Ser	vice Bull	letin PS	B-26		MAWP	(ASME	BPVC Ser	tion I, Pi	G-27.2.1)		MAWF	(ASME	BPVC Set	tion I, A	-317.2.1		Oper	00%	at ! Open	n-Miller 90% rating isure
#	Inspection Location	Lawrest Massured Wall Thickness [inch]	Assumed 100% Operating Pressure Ipril	Material	Temp. (19)	Tulta DD (Inches)	PS8-26 Requirement [t=specified well]	Persont Remaining from Driginal	Required Well [inches]	Margin st Design Pressare (inches)	Criteria Setisfied7	MAWP [pu]	Maa. Operating Pressure Margin (pai)	Margin with 2% pressure reduction (pul)	Margin with 3% precure reduction (pai)	Margin with 10% pressure reduction (pul)	Margin with ISN pressure reduction [p4]	Margin with 20% pressure reduction {pol}	ыланур (g=4)	Mas. Operating Pressure Margin §pil]	Margin with 2% processors reduction [pul]	Margin with 5% pressure reduction (pul)	Margin with 10% pressure reduction [pu]	Atargin with 15% pressure restaction [pu]	Margin with 10% preserve reduction [psi]	Minimum Predicted Life [hours]	Advan Presidand Life (hown)	Minimum Pradicted Life (Issurs)	Aleur Predicted Life (Issues)
28	High Temperature Superheater, 8.3 Floor, Salow Feet (Tube)	0.273	2010	ננדנונאו	1071	2.25	\$57.0	R15	8.342	6233	753	1968	-941	-102	-41	57	96t	250	1972	-34	z	41	ut	261	341	1.722+05	1.546+64	7.042+05	2.828+08
27	Roheator Tubes. 7th Floor, Top of Scattold (Send)	Ø.113	600	1421317947H	1017	2.23	#17A	76%	0.326	-0.913	NO	1547	947	#1#	317	1007	3017	3067	1729	1120	1241	1234	1189	\$229	1248	1.325+01	3,765+00	2.135+09	6.5510-00
23	Rohestor Tuber. 7th Ficor, Top of Scattald (Tube)	0.129	600	\$A21317347H	1017	2.25	8574	ITS	0.135	0.003	TES	1804	1204	3236	1234	1264	1254	ant.	1989	1389	3403	3439	3449	3479	tiat	2.542+09	7.872-09	4.476+09	1.371+10
29	Anhestar Tubes, 9th Filter, Overhend (Send)	0.116	800	\$4113722	1107	2.15	8374	645	R 253	-0.037	ND	152	-048	-716	-218	-311	-199	-124	812	-208	-156	-278	344	-138	-48	6.53(+04	2.348+05	1.162+05	3.738+01
30	Reheater Tubes, 9th Floor, Overhead (Tube)	0.140	600	1111122	1107	2.23	#STM	785	0.153	-0.013	NU	417	-148	-191	-133	-123	-73	-44	479	-111	ises	-81	41	-14	-1	3.895+05	3.651+05	3.195+05	8,738+05
11	Reheater Tubes, 9th Floor, Balow Feat (54-215 Y11)	0.161	800	SADISTIN	1063	23	85%4	83%	8.155	azet.	ves	484	116	-104	-84	-14	-26		\$25	171	-57	-41	-11	39	41	9.062+04	4.892+05	1.171+05	7,425103
32	Auhratar Tubes. 9th Flatt, Selow Feet (SA-253 T22)	0.365	600	\$4313723	1011	23	8574	875.	0.353	¥ 801	165	485	-134	-101	-64	-54	-74		531	-69	-37	-11	-0.	21	31	3.05E+05	8.052+05	5-101+05	2.336+04
11	Boller Apol Tubes (Roller Side)	0.188	1.04	- A 13	4	24.0	70%4	785	8368	8.034	YES	2	H STE		÷		0 UT: -	1.21	-	24		1	+			0.2	•		1.000
ы	Weter Wall Knee Region	0.213	112	1003-11-1		1.45	70%4	101%	8.147	0.044	YES		+	100	1.14				1	1.1			÷.	1. H. K.			1		
25	Boiler Floor Tubes ⁴	0.210		12:00	-	1.0	70%2	52%	0.147	-0.031	ND	11:50				1.25.1	11216		1.0	0.20	S.F.		÷			14	1.2		HUE IS
35	Water Wall at Runars (Elevation 1)	0.159			4	14	70%4	80%	6.347	6.023	rts	1	4		1	1.18			4	+		-	4)		104	1		1	14
37	Water Wall at Buners (Elevation 2)	0.199			+	1	7054	435	8,347	9354	TES	T.	1 (e. 1)	+	÷		1	•	+				1						•
38	Water Wall at Runers (Elevetion 1)	0.183	•	-	+		70%4	135	0.147	0,044	TES	+	144	+	÷.			3+7	0	in e	+			+	1	-	-	•	

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⁴ Tubes to be restored in 2016.

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Page 19 of 19

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AM212/015/000001 R01