Newfoundland & Labrador Hydro



Hydro Plant Corrosion / Fouling Study 2002

Cat Arm Generating Station SERVICE WATER SYSTEM

Newfoundland & Labrador Hydro



Cat Arm Generating Station

SERVICE WATER SYSTEM

Piping
Strainer
Supply Pumps
Control Valves
Heat Exchangers

Prepared for:

Newfoundland & Labrador Hydro

Hydro Generation

Submitted to:

John Mallam, P.Eng

Mechanical Supervising Engineer

Submitted by:

Shane White, B.Eng

Mechanical Engineer

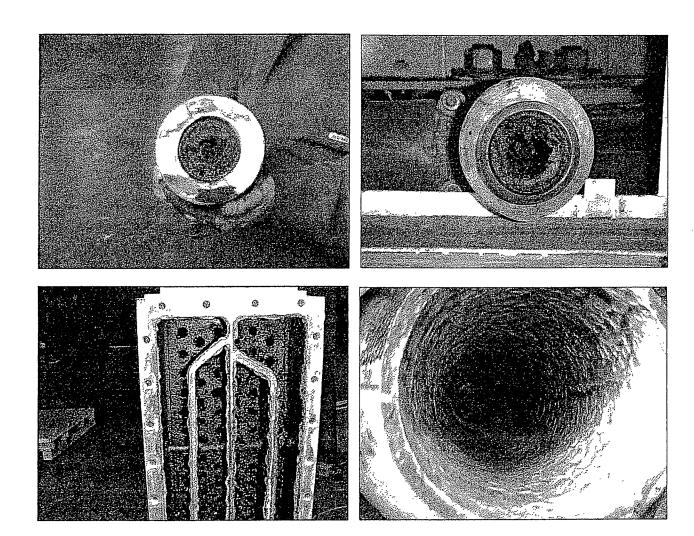
Date:

November 23, 2001

Newfoundland & Labrador Hydro



Cat Arm Generating Station



SERVICE WATER SYSTEM

Piping
Strainer
Supply Pumps
Control Valves
Heat Exchangers

TABLE OF CONTENTS

SERVICE WATER SYSTEM	. 3
General Information	3
Main Equipment	6
Primary Supply Pumps	6
Auxiliary Supply Pump	6
Flow Meter Orifices	. 6
Self-Cleaning Strainer	7
Surface Air Coolers	7
Generator Bearing Oil Coolers	8
Turbine Bearing Oil Cooler	8
Main Control Valves	9
Inlet Header Pressure Reducing Valve	9
SAC Temperature Control Valve	
Generator/Turbine Automatic Shut Off Valve	. 9
Penstock Emergency Automatic Shut Off Valve	10
Penstock Pressure Reducing Valve	10
Supply Pump Excess Pressure Release Valve	10
Sump Level Control Valve	11
Unit #1 in Operation	11
Unit #2 in Operation	
HISTORY OF SERVICE WATER SYSTEM	
General Information	
Review of Trend Monitoring Readings	
Test Samples	
Cost Analysis	
Maintenance Cost for Cleaning	
Total Cost to Clean SAC per Unit	30
Total Cost to Clean SAC Piping per Unit	30
Total Cost to Clean Generator Coolers per Unit	
Total Cost to Clean Generator Cooler Piping per Unit	
ALTERNATIVE SOLUTIONS	
General Information	
Mechanical Cleaning	
Chemical Cleaning	
Replace Piping	
Chemical Treatment of the Water	
Flushing Maintenance Program	
Organic Filters	
Closed System Operation	
VIABLE SOLUTIONS	
Continue to Maintain Current Operation	35
Replace Piping Inside of Generator Housing	
Generator Bearing Cooler Water Piping per Unit	
Replace Piping Outside of Generator Housing	39

Inlet Header Piping per Unit
Discharge Header Piping per Unit
Closed System Operation
Heat Exchanger Selection
Pump Selection
Chemical Injection
CONCULSIONS AND RECOMMENDATIONS
Appendix A
Flow Diagrams
Appendix B
BetzDearborn Water & Pipe Analysis
Appendix C
BetzDearborn Chemical Injection Proposal
Appendix D
Cat Arm Cooler Flushing Procedure
Appendix E
NPW Analysis
Appendix F
RSMeans Mechanical Cost Data
Appendix G
Design Flow Solution Analysis
Appendix H
Recirculation Pump Analysis

SUMMARY

It was determined that a hydro plant cooling water study was needed to determine the most effective solution to the cooling water fouling that is plaguing our hydro plants. The methodology for this study was planned out to include the following: prioritize plants and systems for review, review drawings, inspect coolers for extent of fouling, calculate actual flow rates, and determine the best solution for each hydro plant.

It was determined that Upper Salmon, Cat Arm, and Hinds Lake had the most problems with regards to cooling water.

In order to first determine which plant had the worse problems an in-depth analysis of each plants cooling water system had to be undertaken. Next a complete review of the plants work history had to be done. This was accomplished by reviewing all work orders related to the plants cooling water system in the J.D.Edwards. From this it can be determined which plant had the worse problems.

What was needed next was a review of how the plant's cooling water system has been operating. This was accomplished by using the Trend Monitoring Program that I designed. From the trend graphs one could see just how efficiently the plant has been operating and how the work on the cooling water system affects it. This gives us a time frame for cleaning components of the system so that we could set up a maintenance program for the cooling water system.

A cost analysis was done to determine the amount of money being spent on the current cooling water system in each plant. Also a cost analysis for replacing the piping was done using RSMeans Mechanical Cost Data for each plant.

Several solutions were presented to combat the fouling problem and they are; chemical cleaning of the system, replace the piping with corrosion resistant pipe, add a corrosion inhibitor to the water, use organic filters, or convert to a closed cooling water system.

From these solutions four were chosen for further investigation and they are; replace piping with corrosion resistant pipe, add a corrosion inhibitor to the water, convert the system to a closed system, and continue to operate as we have. Each solution was researched and a Net Present Worth calculation was done to determine the most economical solution. It was determine that replacing the piping with corrosion resistant pipe is the best solution, considering that the pipe has to be replaced in the next few years the other solutions did not seem economical.

The NPW of this solution for Cat Arm is \$420,252 for both units over the pipe life of 20 years. The NPW of continuing to operate as we have is \$434,640 for both units and this does not include replacing the existing piping which labour alone is \$42,000. The closed loop solution has a NPW of \$293,131 but again the existing piping has to be replaced. The closed loop solution can always be added on after the piping is replaced.

SERVICE WATER SYSTEM

The service water system in Cat Arm has had fouling problems since it's opening in 1985. At first this was though to be caused by the unsettled organic materials within the water reservoir and should be 'washed' through the system in three to four years. Every two or three years since the early 90's a scheduled outage is preformed on the units to clean the service water system. This maintenance is required to prevent the units from over heating during the summer months. The coolers are clogged with organic 'slim' and the piping is corroded with hardened organics attached to the walls.

The purpose of this report is to provide the reader with a complete review of the service water system along with an analysis of how the system has been operated. In conclusion to this information recommendations are provided that will help to improve the reliability and service of the cooling water system.

General Information

The service water systems primary supply of water is from the fresh water sump. A secondary supply is a direct feed from the penstock.

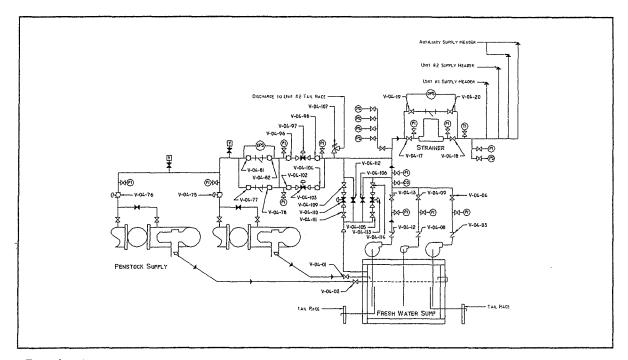
The freshwater sumps primary water supply is from a trough that is attached to the turbine pit's liner. The discharge water from the turbine is collected for the fresh water sump via these troughs.

The primary service water system consists of two main vertical turbine pumps taking water from the freshwater sump. A smaller capacity service water auxiliary pump is also incorporated into the system. When the main pumps are off, this smaller auxiliary pump operates providing service water for the fire protection system, compressed air water-cooled after-coolers and the air conditioning units water-cooled condensers.

The capacity and arrangement of each of the three service water pumps is as follows:

- The capacity of one main service water pump at or near peak pump operating efficiency is equal to the mean anticipated service water flow rate with both units operating.
- The capacity of one main service water pump together with the smaller service water auxiliary pump is equal to or greater than the maximum design service water flow with both units operating.
- The capacity of the smaller service water auxiliary pump is equal to or greater than the powerhouse miscellaneous service water requirements.

A separate supply line is provided, from the spherical valve bypass high pressure penstock water supply connections for each unit, as a secondary means of service water supply. This system is installed as a backup to the primary system and operates whenever there is a low freshwater sump level, a malfunction in the pump service water system or whenever both units are placed in the synchronous condenser mode of operation. The following is a flow diagram of both supply systems.



Drawing 1

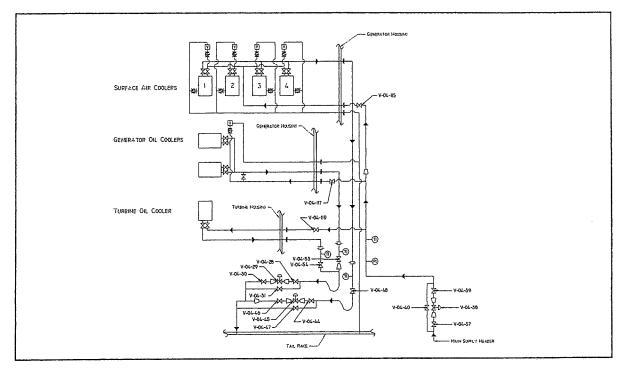
All flow diagrams can be found in Appendix A.

The following is the operating controls used to maintain the service water distribution header pressure together with set points and device.

Function	Set Point	Device
Operate service water auxiliary pump to augment main service water pump.	445 KPa ↓	PS-04-01
Operate lag main service water pump	385 KPa ↓	PS-04-02
Operate a main service water pump as standby when auxiliary pump is out of service.	400 KPa ↓	PS-04-03
Open high-pressure penstock lead PRV (V-04-97).	379 KPa ↓	V-04-97
Open high-pressure penstock lag PRV (V-04-103).	345 KPa ↓	V-04-103
Service water high-pressure alarm.	670 KPa ↑	PS-04-06
Service water low-pressure alarm.	310 KPa ↓	PS-04-07
Safety relief valve	690 KPa ↑	V-04-107

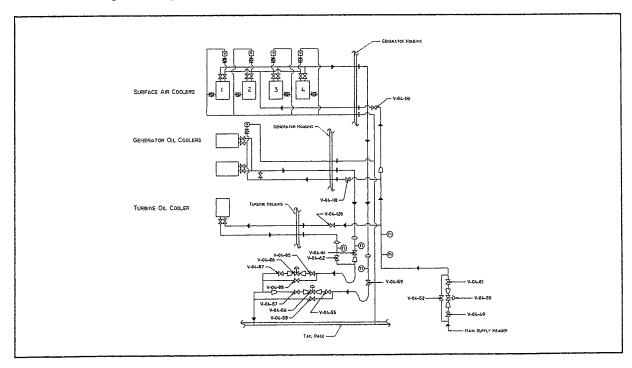
Table 1

The following drawing is the flow diagram for unit #1.



Drawing 2

The following drawing is the flow diagram for unit #2.



Drawing 3

Main Equipment

Primary Supply Pumps

There are two main vertical turbine supply pumps. Fairbanks Morse, model series 7000-12L-2 stage, manufactures both pumps. The following table lists the pump's technical specifications.

Lubrication	Water
Column Size	200mm
Discharge Connection	125mm
Type	Vertical Hollow Shaft
KW	37.3
Voltage	575V / 3Ph / 60Hz
RPM	1800
Capacity	57.4 L/s @ 441 KPa

Table 2

Auxiliary Supply Pump

There is only one auxiliary vertical turbine supply pump. Fairbanks Morse, model series 7000-6M-10 stage, manufactures the pump. The following table lists the pump's technical specifications.

Lubrication	Water	
Column Size	100mm	
Discharge Connection	100mm	
Type	Vertical Hollow Shaft	
KW	3.73	
Voltage	575V / 3Ph / 60Hz	
RPM	1800	
Capacity	5.16 L/s @ 441 KPa	

Table 3

Flow Meter Orifices

There are three flow meters located in the discharge lines of the coolers.

Discharge Line	Line size (sch 40)	Orifice size	
SAC	4 inches	3.0295 inches	
Generator	2 inches	1.1963 inches	
Turbine	1 ¼ inches	0.7111 inches	

Table 4

Self-Cleaning Strainer

Before the service water is supplied to the cooling water distribution header for each unit it is first passed through a self-cleaning strainer. This strainer's back wash system is set in automatic mode and a timer is used to control the backwash system. The timer is set for a 60 second back wash every hour. An inspection glass allows one to see the dirty side of the meshes and determine if they are in need of replacement. A conventional 200 mm Y strainer designed to handle the maximum anticipated water demand is also provided as a backup to the self-cleaning strainer. The following table lists the strainer's technical specifications.

Service	Water		
Serial number	8319V		
Design Pressure	150 psig @ 200 °F		
Working Pressure	100 psig		
Filter Media	60x60 s.s mesh with 10x10 s.s mesh		
Motor	³ / ₄ HP		
Voltage	120V / 1Ph / 60 Hz		
RPM	1800		

Table 5

Surface Air Coolers

There are four surface air coolers within the generator housing. These are aluminum-finned air to water heat exchangers with stainless steel tubes and carbon steel head covers. The following table lists the cooler's technical specifications.

MAWP	100 psig @ 200 °F
Water Pressure Drop Across Cooler	5.62 psi
Water Flow Rate per cooler	5.68 L/s
Number Tubes	186
Number Rows	6
Number Passes	6
Tube O.D	0.625 inches
Tube Wall Thickness	0.049 inches

Table 6

Design Velocity Calculations:

Flow Rate per tube $Q_t = 0.183$ L/s Area per tube $A_t = 0.218$ in² Velocity per tube $V_t = \frac{Qt}{At} = 4.27$ ft/s

Generator Bearing Oil Coolers

There are two generator thrust and guide bearing oil coolers within the generator housing. These are aluminum-finned oil to water heat exchangers with stainless steel tubes and carbon steel head covers. The following table lists the cooler's technical specifications.

MAWP	150 psig @ 200 °F
Water Pressure Drop Across Cooler	1.5 psi
Water Flow Rate per cooler	1.52 L/s
Number Tubes	24
Number Rows	6
Number Passes	6
Tube O.D	0.625 inches
Tube Wall Thickness	0.049 inches

Table 7

Design Velocity Calculations:

Flow Rate per tube $Q_t = 0.380 \text{ L/s}$ Area per tube $A_t = 0.218 \text{ in}^2$ Velocity per tube $V_t = \frac{Qt}{At} = 8.86 \text{ ft/s}$

Turbine Bearing Oil Cooler

There is one turbine bearing oil cooler made from 1 inch, sch 40, seamless, 304 stainless steel pipe. The piping is joined together to form two semicircles and is laid into the turbine oil pot. The following table lists the cooler's technical specifications.

MAWP	3521 psig @ 200 °F	
Water Flow Rate	1.1 L/s	
Tube O.D	1.315 inches	
Tube Wall Thickness	0.133 inches	

Table 8

Design Velocity Calculations:

Flow Rate per tube $Q_t = 1.1 \text{ L/s}$ Area per tube $A_t = 0.864 \text{ in}^2$ Velocity per tube $V_t = \frac{Qt}{At} = 6.475 \text{ ft/s}$

Main Control Valves

Inlet Header Pressure Reducing Valve

The inlet header pressure reducing valve V-04-38 unit #1 and V-04-50 unit #2 are a four inch Masoneilan Camflex II control valve model # 35-35102. The following table lists the valve's technical specifications.

Specifications	Minimum	Normal	Maximum
Inlet Pressure	346 KPa		540 KPa
Outlet Pressure		309 KPa	
Flow Rate	7.3 L/s	15.6 L/s	29.7 L/s
CF		0.85	
Required CV	203.4		81.35
Rated CV		230	
Diff. Pressure Size	37 KPa		231 KPa
Diff. Pressure shut off			620 KPa

Table 9

SAC Temperature Control Valve

The SAC temperature control valve V-04-45 unit #1 and V-04-56 unit #2 are a three inch Masoneilan control valve model # 47-21125. The following table lists the valve's technical specifications.

Specifications	Minimum	Normal	Maximum
Inlet Pressure	144 KPa		299 KPa
Outlet Pressure	0 KPa		7 KPa
Flow Rate	5.3 L/s		25.3 L/s
CF		0.9	
Required CV	12.8		88.6
Rated CV		110	
Diff. Pressure Size	137 KPa		292 KPa
Diff. Pressure shut off			1450 KPa

Table 10

Generator/Turbine Automatic Shut Off Valve

The generator/turbine automatic shut off valve V-04-29 unit #1 and V-04-86 unit #2 are two inch valves with Canadian Worcester Controls (model # 20-405). The valves them selves are wrapped in insulation making their identification not possible.

Penstock Emergency Automatic Shut Off Valve

The penstock automatic shut off valves V-04-75 and V-04-76 are six inch valves with Marks Controls (model #896). The valves themselves are wrapped in insulation making their identification not possible.

Penstock Pressure Reducing Valve

The penstock pressure reducing valves V-04-97 and V-04-103 are two inch Masoneilan control valves (model # 48-21734). The following table lists the valve's technical specifications.

Specifications	Minimum	Normal	Maximum
Inlet Pressure		3772 KPa	
Outlet Pressure		434 KPa	
Flow Rate	7.3 L/s	14.6 L/s	31.0 L/s
CF		0.95	
Required CV	5.26		22.3
Rated CV		30	
Diff. Pressure Size		3338 KPa	
Diff. Pressure shut off		6800 KPa	

Table 11

Supply Pump Excess Pressure Release Valve

The excess pressure release valve V-04-113 is a one & half inch Masoneilan control valve model # 48-21135. The following table lists the valve's technical specifications.

Specifications	Minimum	Normal	Maximum
Inlet Pressure		540 KPa	
Outlet Pressure		7 KPa	
Flow Rate		600 L/s	
CF		0.9	
Required CV		26.80	
Rated CV		35	
Diff. Pressure shut off			1450 KPa

Table 12

Sump Level Control Valve

The sump level control valve V-04-110 is a two-inch Masoneilan control valve model # 48-21135. The following table lists the valve's technical specifications.

Specifications	Minimum	Normal	Maximum
Inlet Pressure		427 KPa	
Outlet Pressure		0 KPa	
Flow Rate		18.5 L/s	
CF		0.93	
Required CV		37.4	
Rated CV		46	
Diff. Pressure Size		427 KPa	
Diff. Pressure shut off		434 KPa	1450 KPa

Table 13

Unit #1 in Operation

The service water pressure can fluctuate between 345 KPa (50 psi) and 550 KPa (80 psi), therefore a pressure-regulating valve V-04-38 has been installed to maintain pressure at 220 KPa (32 psi). A bypass valve V-04-40 is provided so that the pressure-regulating valve can be isolated for repairs. The pressure-regulating valve is located after the self-cleaning strainer at the start of unit #1 service water distribution header. All inlet header valves, V-04-115 SAC, V-04-117 generator, V-04-119 turbine, are in the full open position.

Approximately twelve (12) seconds after initiation of unit #1, the following occurs:

- 1. Pneumatically operated temperature control valve V-04-45 opens and water flow is established through the surface air coolers. A bypass valve V-04-47 is provided so that the control valve can be isolated for repairs.
- 2. Pneumatically operated automatic shut-off valve V-04-29 opens and water flow is established through the turbine guide bearing cooler and the generator thrust/guide bearing coolers. A bypass valve V-04-31 is provided so that the control valve can be isolated for repairs.

After the water flows have been established, the flow indicator switches Fi/s-04-01, Fi/s-04-02, Fi/s-04-03 pick up and start measuring flows through the surface air coolers, turbine guide bearing cooler, and the generator thrust/guide bearing coolers.

Water flow through the turbine guide bearing cooler is manually controlled by ball valve V-04-54. This ball valve is throttled to provide 1.20 L/s of water through the cooler at maximum flow and is located after the cooler. Temperature indicator Ti-04-02 together with the flow meter provided on the flow meter panel have been provided to help set the required maximum flow through the cooler. The turbine guide bearing cooler water flow should never be set less than 0.25 L/s.

Water flow through two generator thrust/guide bearing coolers is manually controlled by ball valve V-04-53. This ball valve is throttled to provide 3.50 L/s of water through the coolers at maximum flow and is located after the cooler. Temperature indicator Ti-04-03 together with the flow meter provided on the flow meter panel have been provided to help set the required maximum flow through the coolers. The generator thrust/guide bearing coolers water flow should never be set less than 0.7 L/s.

Water flow through four surface air coolers is controlled automatically by temperature control valve V-04-45. The integral controller for this valve remotely senses the temperature of the common cooling water leaving the surface air coolers. This valve is set to maintain a leaving water temperature of 35 C, which corresponds to a surface air cooler discharge air temperature of 40 C. The temperature control valve is equipped with a pneumatic minimum position relay to ensure that whenever the unit is operating, water flow is never allowed to fall below 4.0 L/s. The temperature control valve is also equipped with an electric solenoid to fully close the valve whenever the unit is shutdown.

Temperature indicator Ti-04-04 has been provided to facilitate the checking of the operation of the temperature control valve. Balancing valve V-04-48 on the surface air cooler return line should be set to provide a surface air cooler flow of 26.0 L/s when the temperature control valve is fully open.

Flow meter panel settings:

Flow Rates	Scale Range	Set Point
Turbine guide bearing cooler flow	0-1.20 L/s	0.20 L/s
Generator thrust/guide bearing coolers flow	0-3.50 L/s	0.60 L/s
Surface Air Coolers flow	0-26.0 L/s	3.50 L/s

Table 14

Unit #2 in Operation

The service water distribution header pressure can fluctuate between 345 KPa (50 psi) and 550 KPa (80 psi), therefore a pressure-regulating valve V-04-50 has been installed to maintain pressure at 220 KPa (32 psi). A bypass valve V-04-52 is provided so that the pressure-regulating valve can be isolated for repairs. The pressure-regulating valve is located after the self-cleaning strainer. All inlet header valves, V-04-116 SAC, V-04-118 generator, V-04-120 turbine, are in the full open position.

Approximately twelve (12) seconds after initiation of unit #1, the following occurs:

- 3. Pneumatically operated temperature control valve V-04-56 opens and water flow is established through the surface air coolers. A bypass valve V-04-58 is provided so that the control valve can be isolated for repairs.
- 4. Pneumatically operated automatic shut-off valve V-04-86 opens and water flow is established through the turbine guide bearing cooler and the generator thrust/guide bearing coolers. A bypass valve V-04-88 is provided so that the control valve can be isolated for repairs.

After the water flows have been established, the flow indicator switches Fi/s-04-04, Fi/s-04-05, Fi/s-04-06 pick up and start measuring flows through the surface air coolers, turbine guide bearing cooler, and the generator thrust/guide bearing coolers.

Water flow through the turbine guide bearing cooler is manually controlled by ball valve V-04-62. This ball valve is throttled to provide 1.20 L/s of water through the cooler at maximum flow and is located after the cooler. Temperature indicator Ti-04-07 together with the flow meter provided on the flow meter panel have been provided to help set the required maximum flow through the cooler. The turbine guide bearing cooler water flow should never be set less than 0.25 L/s.

Water flow through two generator thrust/guide bearing coolers is manually controlled by ball valve V-04-61. This ball valve is throttled to provide 3.50 L/s of water through the coolers at maximum flow and is located after the cooler. Temperature indicator Ti-04-06 together with the flow meter provided on the flow meter panel have been provided to help set the required maximum flow through the coolers. The generator thrust/guide bearing coolers water flow should never be set less than 0.7 L/s.

Water flow through four surface air coolers is controlled automatically by temperature control valve V-04-56. The integral controller for this valve remotely senses the temperature of the common cooling water leaving the surface air coolers. This valve is set to maintain a leaving water temperature of 35 C, which corresponds to a surface air cooler discharge air temperature of 40 C. The temperature control valve is equipped with a pneumatic minimum position relay to ensure that whenever the unit is operating, water flow is never allowed to fall below 4.0 L/s. The temperature control valve is also equipped with an electric solenoid to fully close the valve whenever the unit is shutdown.

Temperature indicator Ti-04-05 has been provided to facilitate the checking of the operation of the temperature control valve. Balancing valve V-04-59 on the surface air cooler return line should be set to provide a surface air cooler flow of 26.0 L/s when the temperature control valve is fully open.

Flow meter panel settings:

Flow Rates	Scale Range	Set Point
Turbine guide bearing cooler flow	0-1.20 L/s	0.20 L/s
Generator thrust/guide bearing coolers flow	0-3.50 L/s	0.60 L/s
Surface Air Coolers flow	0-26.0 L/s	3.50 L/s

Table 15

HISTORY OF SERVICE WATER SYSTEM

General Information

All work orders that are in the J.D.Edwards system since the fall of 1994 pertaining to the service water pumps, strainers, and heat exchangers have been reviewed to piece together an overview of the major work done on the service water system. All of the major work done on this system is listed below in the following table. It can be seen from table 16 that the SAC's are cleaned every second year since 1995. It can also be seen that the SAC piping has been cleaned every three years since 1997.

1.14	All Comments and the	CATAF	M. Work Order History:	DESCRIPTION OF THE PROPERTY.
	May	June	July	Oct
1995		Unit #1 Cleaned all SAC Unit #2 Cleaned all SAC		
1997		Technologies and American Commission (Commission Commission Commis	Secretarion of the Secretarion o	All four SAC were cleaned. 2.5" piping I.D = 2.0" - 2.3" scraped clean one section I.D = 2.467"
1998	Section 2019 to 1980 to	Note the Comment of t	Unit #1 Chemical Cleaning (TRAC 100) of generator coolers and turbine cooler. Unit #2 Chemial Cleaning (TRAC 100) of generator coolers and turbine cooler. Unit #2 leaked during flushing of coolers.	
1999		And the control of th	Unit #1 Flushed SAC and measured flows, 1: 7 l/s, 2: 13 l/s, 3: 10 l/s, 4: 4.5 l/s. Cleaned SAC 1, 3, & 4. Unit #2 Flushed SAC and measured flows, 1: 5 l/s, 2: 1 l/s, 3: 9.5 l/s, 4: 7 l/s Cleaned SAC 1,3, & 4, replaced 2.	
2000	strainer.	spare. Unit #2 Replaced SAC #1 with	3" pipe for SAC inside of generator housing.	housing. Unit

Table 16

Table 17 gives the dates when each unit was off line for maintenance since 1999.

		CATAF	RM UNIT O	UTAGES		
Month Unit #1		Unit #2				
WOTH	1999	2000	2001	1999	2000	2001
	537					edicularity Political
January		8,26	1,12,17	4	1,2,3,8,12,26	
February	13	8		9	8,18	
March	12			9	10	
April	13			9	11	
May	10			7,8,17		
June	14	14,19,23		12	23	13
July	2,7,8,9,14			6,14,16,20,21		
August	3,8	24		3,8	24	
September		18,25			18,20,26	
October		10				
November		25			30	
December	6,13-17,21	5,6,29		7,15-18,20,31		

Table 17

Review of Trend Monitoring Readings

Trend Monitoring readings are taken weekly by operations for all hydro generating stations except Snooks Arm and Venams Bight. With knowledge of the work history performed on the generating station coupled with the trend monitoring readings one can develop a picture of how the generating station has operated over the last few years.

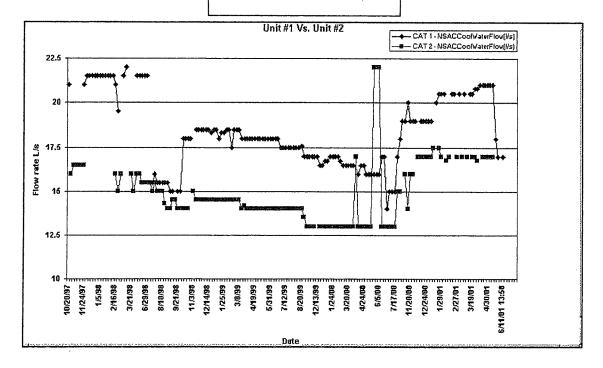
The Trend monitoring readings are now being stored into a database using Microsoft Access. A hard copy of the weekly readings is being kept on site for backup. The Microsoft Access Trend Monitoring program now allows quick graphing of operating parameters to help us determine the efficiency of the unit. The program is user friendly and allows operations to view the units operating parameters over an extended period of time.

Table 18 shows the missing trend monitoring readings for Cat Arm.

	UNIT #1		UNIT #2	
			1997/11/24 to 1998/02/16	Early Winter 1998
DATES	1998/03/09 to 1998/06/01	Spring 1998	1998/03/23 to 1998/06/01	Spring 1998
DATES	1999/08/20 to 1999/11/08	Fall 1999	1999/08/20 to 1999/11/08	Fall 1999
	2000/07/31 to 2000/10/30	Late Summer 2000	2000/07/31 to 2000/10/30	Late Summer 2000

Table 18

Graph 1 - SAC Flow Rates



Graph 1 shows the flow rates for the SAC's since October 1997. The recommended flow rates are 23 L/s during the summer months and 5 L/s during the winter months. One can see the increase in flow rate around July 2000 when the SAC piping was cleaned. Cleaning the SAC's in July 1999 did nothing to increase the flow rate because the problem was clogged piping. Cleaning the SAC's in October 1997 did maintain high flow rates up until the fall 1998 when both units SAC's started a steady decline until the piping was cleaned in July 2000. It is interesting to note that the flow rate through unit #2 has always been lower than unit #1, this warrants further investigation.

The SAC flow rate has also increased in the fall and decreased in the spring. This is believed to be caused by the spring run off carrying suspended particulates of organic matter. After these particulates flow through the SAC the heat causes them to solidify and fall out of the solution. Theses solid globes of matter then become caught along the inside of the pipe, especially if the pipe is corroded.

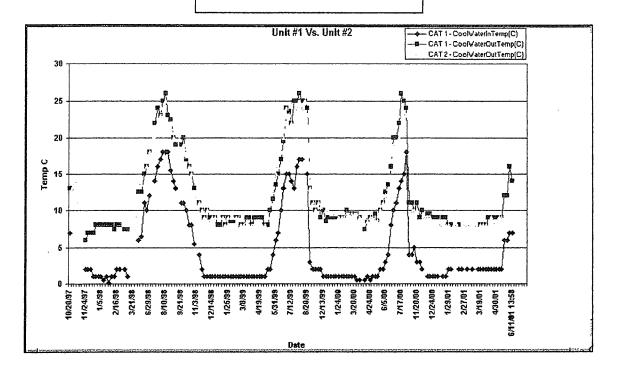
To combat this problem for the summer it was suggested that the 3-inch by-pass line also be fully opened. So both units by-pass lines where fully open along with their main 4inch discharge lines. Unit #1 increased its flow from 18 L/s to 20 L/s and unit #2 increased its flow from 15.5 L/s to 17L/s. The by-pass lines will remain open until the end of the warm season some time in September 2001.

Actual Velocity Calculations:

Unit #1 Flow Rate per tube $Q_t = 0.161 \text{ L/s}$ Area per tube $A_t = 0.218 \text{ in}^2$

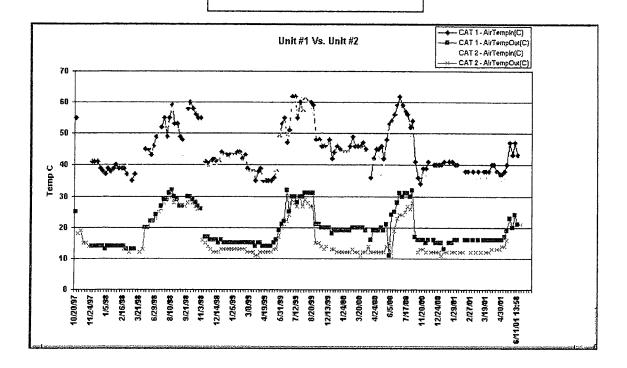
Unit #2 Flow Rate per tube $Q_t = 0.137 \text{ L/s}$ Area per tube $A_t = 0.218 \text{ in}^2$ Area per tube $A_t = 0.218$ in Area per tube $A_t = 0.218$ in Velocity per tube $V_t = \frac{Qt}{At} = 3.76$ ft/s Velocity per tube $V_t = \frac{Qt}{At} = 3.20$ ft/s

Graph 2 - SAC Water Temperature



Graph 2 shows the water temperature differential for the SAC's on both units since October 1997. This clearly shows how the water temperature fluctuates through out the year, with increased temperatures during the summer months and decreased temperatures during the winter months. Even though the temperature fluctuates the differential temperature between inlet and discharge remains constant around an average of 5 °C.

Graph 3 - SAC Air Temperatures



Graph 3 shows the air temperature differential for the SAC's on both units since October 1997. The air temperature into the SAC's is measured inside the stator frame and the air temperature out of the SAC's is measured inside the generator housing. Only one SAC air temperatures are measured, which is SAC #2 for unit #1 and SAC #3 for Unit #2. This graph clearly shows how the air temperature fluctuates through out the year, with increased temperatures during the summer months and decreased temperatures during the winter months. Even though the temperature fluctuates the differential temperature between inlet and outlet remains constantly around an average of 20 °C.

SAC Air Temperature Set Points:

Unit #1	Cold Air	Warm Air
Alarm	45 °C	70 °C
Trip Unit Off Line	52 °C	

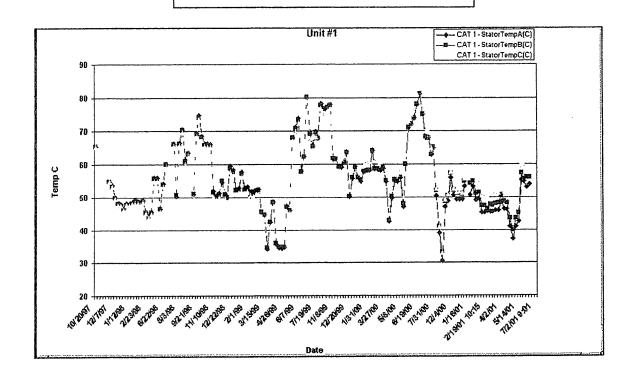
Table 19

Unit #2	Cold Air	Warm Air
Alarm	45 °C	68 °C
Trip Unit Off Line	50 °C	

Table 20

The air temperature out of the SAC's have never reached the alarm set point of 45 °C at least since October 1997.

Graph 4 - Unit #1 Stator Temperatures



Graph 4 shows the Stator temperatures for unit #1 since October 1997. This graph clearly shows how the stator temperature fluctuates through out the year, with increased temperatures during the summer months and decreased temperatures during the winter months.

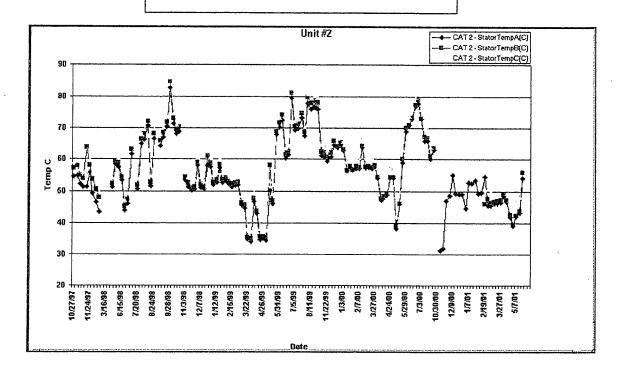
Stator Temperature Set Points:

Core Alarm	105 °C
Iron Alarm	90 °C

Table 21

The stator temperatures have never reached the iron alarm set point of 90 °C at least since October 1997.

Graph 5 - Unit #2 Stator Temperatures



Graph 5 shows the Stator temperatures for unit #2 since October 1997. This graph clearly shows how the stator temperature fluctuates through out the year, with increased temperatures during the summer months and decreased temperatures during the winter months.

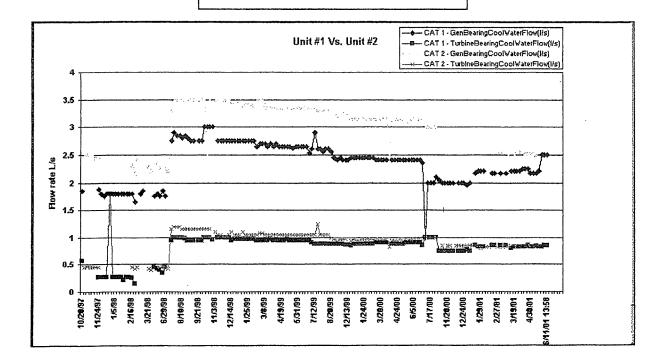
Stator Temperature Set Points:

Core Alarm	105 °C
Iron Alarm	90 °C

Table 22

During the summer of 1998 unit #2 stator temperatures climbed to 86 °C almost reaching the iron alarm temperature of 90 °C.

Graph 6 - Generator/Turbine Flow Rates



Graph 6 shows the flow rates for the generator and turbine coolers since October 1997. The recommended flow rates are 3.5 L/s for the generator coolers and 1.20 L/s for the turbine cooler. One can see how much the flow rate increased through the coolers in July 1998 after they where chemically cleaned with Trac 100.

To combat the problem of summer fouling it was also suggested that the 2-inch by-pass line also be fully opened. Only unit #1 by-pass line was fully open, unit #2 by-pass line was not opened due to the by-pass valve being seized closed. The flow rate through the generator and turbine coolers did not change. This seized by-pass valve will be fixed during the fall 2001 outage under work order # 230448.

Actual Velocity Calculations:

Generator Coolers:

Turbine Cooler:

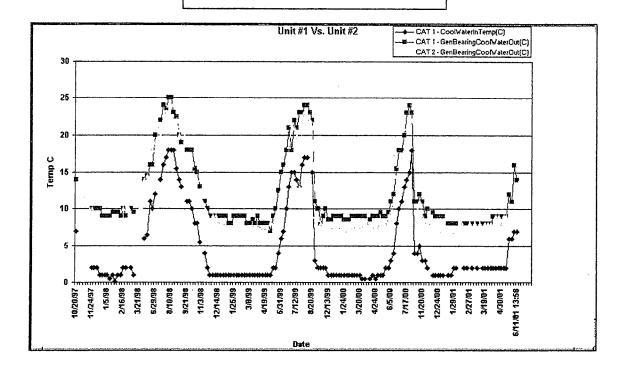
Flow Rate per tube $Q_t = 0.312 \text{ L/s}$ Area per tube $A_t = 0.218 \text{ in}^2$

Area per tube $A_t = 0.864 \text{ in}^2$

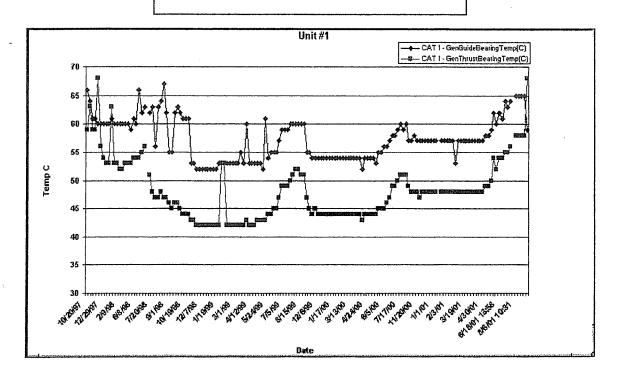
Flow Rate per tube $Q_t = 0.80 \text{ L/s}$

Velocity per tube $V_t = Qt/At = 7.29$ ft/s Velocity per tube $V_t = Qt/At = 4.71$ ft/s

Graph 7 - Generator Water Temperatures



Graph 7 shows the water temperature differential for the generator coolers on both units since October 1997. This graph clearly shows how the water temperature fluctuates through out the year, with increased temperatures during the summer months and decreased temperatures during the winter months.



Graph 8 shows unit #1 generator's guide and thrust bearing temperatures since October 1997. One can see the temperature dropped in July 1998 after the coolers were chemically cleaned with Trac 100. Since then one can also see how the temperatures have continually increased from year to year when you compare the consistent winter temperatures from year to year. This continuous increase in temperature from year to year is resulting from the gradual build up of particulates inside the cooler tubes and pipes.

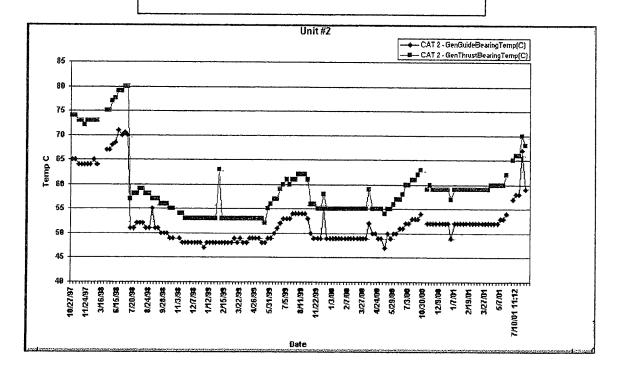
Generator Bearing Temperature Set Points:

Unit #1	Guide Bearing	Thrust Bearing
Alarm	72.5 °C	80 °C
Trip to Synchronous Condense Mode	75 °C	85 °C
Trip Unit Off Line	90 °C	95 °C

Table 23

Before the coolers were cleaned in the summer of 1998 the guide bearing temperature climbed to 67 °C, almost reaching the guide bearing alarm set point of 72.5 °C. The guide bearing temperatures are again on the rise since they're cleaning with Trac 100 in the summer of 1998. The recorded high temperatures this summer for the guide bearing were 65 °C.

Graph 9 - Unit #2 Gen Bearing Temperatures



Graph 9 shows unit #2 generator's guide and thrust bearing temperatures since October 1997. One can see the dramatic temperature dropped in July 1998 after the coolers were chemically cleaned with Trac 100. This graph also shows how the temperatures have been continually increasing from one year to the next. Comparing the winter temperature of 2001 with that of 1999 there has been an increase of at less 5 °C. This continuous increase in temperature from year to year is resulting from the gradual build up of particulates inside the cooler tubes which directly affects the heat transfer rate.

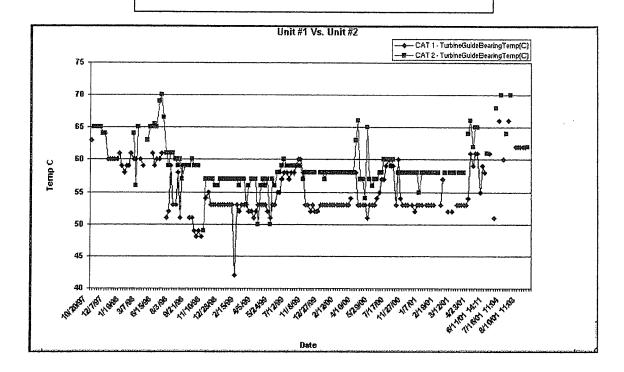
Generator Bearing Temperature Set Points:

Unit #2	Guide Bearing	Thrust Bearing
Alarm	71 °C	80 °C
Trip to Synchronous Condense Mode	76 °C	85 °C
Trip Unit Off Line	90 °C	95 °C

Table 24

The trust and guide bearing alarm set points were reached in the summer of 1998 before the coolers were cleaned with Trac 100.

Graph 10 - Turbine Bearing Temperature

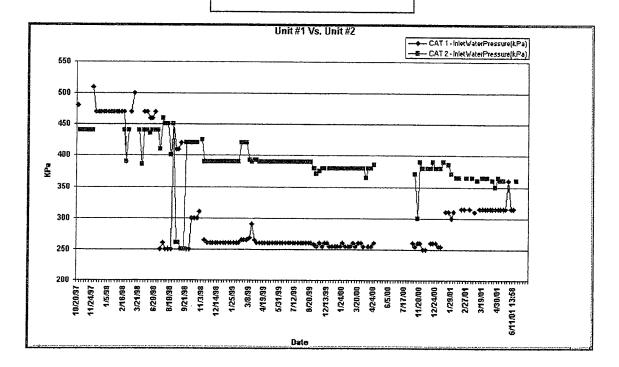


Graph 10 shows the Turbine guide bearing temperatures since October 1997. It can be seen from this graph the temperature drop in July 1998, which was due to chemically cleaning the cooler with Trac 100. The bearing is again starting to run hot due to the continuous build up of particulates over the last three years within the system.

Turbine Bearing Temperature Set Points for unit #1 and unit #2:

Alarm	75 °C
Trip to Synchronous Condense Mode	80 °C
Trip Unit Off Line	85 °C

Table 25



Graph 11 shows the water inlet pressure on the six-inch supply header that feeds each unit with cooling water. This pressure reading is taken down stream from the pressure reducing valve on each header. A Technician from New Valve adjusted the pressure reducing valve on unit #1 in July 1998, which caused the sudden drop in pressure. Reducing the pressure in the supply header directly affects the volume of cooling water being supplied.

To increase the water flow through unit #2 the pressure-reducing valve V-04-50 located in the inlet header was open from 70% to 100%. This caused an increase in pressure from 390 KPa to 410 KPa. The main supply pump is operating around 490 KPa. This pressure difference will be investigated during the fall 2001 outage under work order # 228335. It is thought that the valve may be malfunctioning, the by-pass valve V-04-52 was open fully, and the pressure remained at 410 KPa. It is now thought that the main supply header has considerable build up and the by-pass line is clogged. The pressure gauge was also changed, and the pressure still remained the same.

Test Samples

In August 2000 water and hard barnacle pipe deposits from the Cat Arm plant were sent to BetzDearborn for analysis. The water sample is directly from the penstock supply and the barnacle deposits are from the SAC cooling water piping. Table 26 shows the composition of the water sample.

Composition	Sample #1	Sample #2
PH	5.0	5.1
Specific Conductance @ 25C, umhos	91	77
Alkalinity "P" as CaCO ₃ , ppm	0	0
Alkalinity "M" as CaCO ₃ , ppm	< 2	< 2
Sulfur Total as SO ₄ , ppm	< 5	< 5
Chloride as CL, ppm	3.1	3.7
Hardness Total as CaCO ₃ , ppm	6.5	5.3
Calcium Hardness Total as CaCO ₃ , ppm	2.3	1.6
Magnesium Hardness Total as CaCO ₃ , ppm	4.2	3.6
Copper Total as Cu, ppm	< 0.05	< 0.05
Iron Total as Fe, ppm	0.79	0.87
Sodium as Na, ppm	2.2	2.1
Phosphate Total Inorganic as Po ₄ , ppm	< 0.2	< 0.2
Phosphate Ortho- as Po ₄ , ppm	< 0.2	< 0.2
Silica Total as SiO ₂ , ppm	1.5	1.5

Table 26

As one can see the pH level of 5.0 tells us that the water is acidic in nature. This type of water is very aggressive and will corrode piping and equipment.

Table 27 shows the composition of the SAC piping barnacle deposit.

Composition	Sample #1	Sample #2
Iron Fe2O3 + Fe3O4	72 %	66%
Loss on Ignition LOI	21%	18%
Manganese MnO ₂	6%	15%
Aluminum Al ₂ O ₃	1%	1%

Table 27

As one can see the sample deposits are mainly composed of metal oxides. These metal oxides are from the pipe wall, which is being corroded by the acidic water. Loss of ignition LOI refers to the organics within the sample.

The BetzDearborn analysis of the water and pipe samples can be found in Appendix B.

Cost Analysis

Maintenance Cost for Cleaning

In order to clean the service water coolers and piping in Cat Arm, a maintenance crew has to be assembled in Bay D'Espoir and drive to Cat Arm. Travel time to Cat Arm from Bay D'Espoir is normally eight hours.

Travel Arrangements (normal workweek)

Monday: Leave Bay D'Espoir in the morning and drive to the West coast. Work 4.0

hours upon arriving on site.

Tuesday to Thursday: Regular workweek 8.0 hours per day.

Friday: Work 4.0 hours and then drive back to Bay D'Espoir for the weekend.

Hours of actually work performed on site for one workweek is 32.0 hours.

Perdiem Expenses (\$9 Breakfast, \$11 Dinner, \$18 Supper, \$6 Incidentals (over night))

Monday: \$34 (no breakfast)

Tuesday to Thursday: \$43 per day Friday: \$20 (no supper or incidentals)

Total Perdiem charge per person per week: \$183

Having a work crew of more than 4 workers will require the services of a cook and perdiem will not be paid while the services of a cook is provided on site.

For the purpose of this study all workers will receive perdiem.

Minimum Work Crew and Wages

3 Workers at \$21.56 hr (2 workers on floor, 1 worker operating the crane)

1 Supervisor at \$23.72 hr (10% more than the worker)

Total over head costs = salary x 1.63

Travel to site will be by fleet vehicles, 2 required, one supervisor vehicle and one work crew truck. Tools and cleaning equipment will be transported to the site with these vehicles.

The supervisor is usually over seeing two or three jobs while on site. For this cost analysis 1/3 of the supervisors wage will be allocated to the job.

Required gas for travel is \$80 to site and \$80 return from site for one work truck.

Total Cost to Clean SAC per Unit

Time required to clean four SAC's for one work crew is four days (32.0 hrs), one cooler per day (8.0 hrs); this includes removal, cleaning, and reinstallation of cooler.

Labour: 3 (workers) x 40.0 hrs (32.0 cleaning, 8.0 driving) x \$21.56 = \$2,587.20 1 (supervisor) x 13.3 hrs (1/3 x 40.0 hrs) x \$23.72 = \$315.48

Total Over Head Costs: \$2,902.68 x 1.63 = \$4,731.37

Perdiem: 4 (work crew) x \$183 = \$732 (Monday \$34, Tuesday to Thursday \$129, Friday \$20)

Gas: $4 (2 \text{ vehicles}) \times \$80 = \$320$

Total cost: \$5,783.37

Total Cost to Clean SAC Piping per Unit

Time required to clean SAC piping inside of generator housing for one work crew is three days (24.0 hrs); this includes removal, cleaning, and reinstallation of piping.

Labour: 3 (workers) x 32.0 hrs (24.0 cleaning, 8.0 driving) x \$21.56 = \$2,069.76 1 (supervisor) x 10.7 hrs (1/3 x 32.0 hrs) x \$23.72 = \$253.80

Total Over Head Costs: $2,323.56 \times 1.63 = 3,787.40$

Perdiem: 4 (work crew) x \$140 = \$560 (Monday \$34, Tuesday to Wednesday \$86, Thursday \$20)

Gas: 4 (2 vehicles) x \$80 = \$320

Total cost: \$4,667.409

Total Cost to Clean Generator Coolers per Unit

Time required to clean two generator coolers for one work crew is four days (32.0hrs), two days (16.0 hrs) per cooler; this includes removal, cleaning, and reinstallation of cooler.

Labour: 3 (workers) x 40.0 hrs (32.0 cleaning, 8.0 driving) x \$21.56 = \$2,587.20 1 (supervisor) x 13.3 hrs (1/3 x 40.0 hrs) x \$23.72 = \$315.48

Total Over Head Costs: \$2,902.68 x 1.63 = \$4,731.37

Perdiem: 4 (work crew) x \$183 = \$732 (Monday \$34, Tuesday to Thursday \$129, Friday \$20)

Gas: $4 (2 \text{ vehicles}) \times \$80 = \$320$

Total cost: \$5,783.37

Total Cost to Clean Generator Cooler Piping per Unit

Time required to clean generator piping inside of generator housing for one work crew is three days (24 hrs); this includes removal, cleaning, and reinstallation of piping.

Labour: 3 (workers) x 32.0 hrs (24.0 cleaning, 8.0 driving) x \$21.56 = \$2,069.76 1 (supervisor) x 10.7 hrs (1/3 x 32.0 hrs) x \$23.72 = \$253.80

Total Over Head Costs: \$2,323.56 x 1.63 = \$3,787.40

Perdiem: 4 (work crew) x \$140 = \$560 (Monday \$34, Tuesday to Wednesday \$86, Thursday \$20)

Gas: $4 (2 \text{ vehicles}) \times \$80 = \$320$

Total cost: \$4,667.40

Maintenance Costs Over Piping Life (20 years) per Unit

SAC cleaning every 2 yrs = \$57, 833.70 SAC pipe cleaning every 10 yrs = \$9,334.80 Gen coolers cleaning every 5 yrs = \$23,133.48 Gen pipe cleaning every 10 yrs = \$9,334.80

ALTERNATIVE SOLUTIONS

General Information

The fouling problem with regard to the cooling water system is being caused by two problems. The first problem is corrosion of the piping system and the second problem is organic build up. The acidic water supply is causing the piping system to corrode and the organics are then attaching themselves to the corroded pipe. Over time the organics build up and are able to clog the pipe. The heat transferred into the cooling water from the heat exchangers cause the suspended organics in the water to participate out. This then causes the discharge piping to become clogged with organics and choke off the flow rate. A decreased flow rate allows for more organics to settle within the cooling water system. Eventually the entire cooling water system will become clogged with organics.

The following is a list of solutions that can be used to combat this problem.

- 1. Mechanical cleaning of the system.
- 2. Chemical cleaning of the system.
- 3. Replace the piping with corrosion resistant pipe.
- 4. Chemically treat the water.
- 5. Develop a flushing maintenance program.
- 6. Incorporate organic filters.
- 7. Convert the system to a closed loop operation.

A brief description of each proposed solution is discussed below.

Mechanical Cleaning

Mechanical cleaning of the cooling water system will require a maintenance cleaning program if this solution is going to be considered. Without a maintenance cleaning program the reliability of the service water system will be compromised and forced unit outages will happen.

Mechanically cleaning the service water system will require a cleaning maintenance crew and scheduled plant outages to perform the work. The piping and heat exchangers have to be removed from service and physically cleaned by hand. This hand cleaning decreases the life expectancy of both the piping and heat exchangers. The hand cleaning of piping and cooler tubes is done with rotating nylon brushes that physically scrape the pipe walls of organic build up. Also the possibility of mechanical damage is increased when man handling the piping and heat exchangers.

Chemical Cleaning

Chemical cleaning of the service water system requires a maintenance cleaning program to be established. Without a maintenance cleaning program the reliability of the service water system will be compromised and forced unit outages will happen.

Chemically cleaning the service water system will require a cleaning maintenance crew and scheduled plant outages to perform the work. The piping and heat exchangers don't have to be removed from the system. Instead isolation valves upstream and downstream are closed and mechanical branch connections are attached to the piping system in both upstream and downstream locations. The chemical mixture is then pumped through the system to dissolve any organic build up.

Chemical treatment is harsh on the piping and heat exchangers and decreases their life expectancy. The chemical leaves the metal in an unpassivated state and corrosion will occur very rapidly after returning the system to service.

Replace Piping

Currently the piping material is mild steel schedule 40. Two different piping materials have been considered for replacement of the mild steel pipe, they are 316 stainless steel pipe schedule 10 and polyvinyl chloride (PVC) pipe schedule 80.

The 316 stainless steel schedule 10 pipe is considered because of its corrosion resistance and mechanical properties. The stainless steel pipe will be placed in high traffic areas or in areas where the piping is likely to be hit to prevent damage.

The PVC schedule 80 pipe is considered because of its corrosion resistance, mechanical properties, and thermal properties. Schedule 80 will be more durable when compared with schedule 40. Due to PVC's excellent thermal properties there will be no need to insulate the pipe as compared to stainless steel. The PVC pipe will be placed in low traffic areas where the probability of the pipe being damaged is remote.

Chemical Treatment of the Water

The water can be chemically treated to reduce the acidity of the water by raising the ph level and also help keep all organic materials in a suspended state. The existing service water system is a once through operation and will require large amounts of chemical. BetzDearborn purposed a chemical treatment solution, which can be found in appendix C. It is estimated to cost \$5,000 to set up this system and \$45,000 per year for chemical usage.

Flushing Maintenance Program

Flushing each cooler individually to remove any organic build up will help keep the service water system clear. Flushing is performed when all water flow is directed through one particular cooler for a predetermined amount of time. Any lose organic material will be forced out of the cooler and washed away.

If a flushing program was implemented it would reduce the amount of lose organic build up within the service water system. The program would consist of flushing the coolers every four weeks starting in the spring and continuing over the summer. A flushing procedure for Cat Arm can be found in Appendix D.

Organic Filters

Organic filters can be incorporated at the beginning of the service water system to remove the organics from the water. Sand filters are an effective method of removing organics from water. Typical flow rates for sizing a sand filter are 3-6 gpm for every square foot of surface area. The smallest sand filter for Cat Arm would be around 14 ft in diameter to allow for 900 gpm. Space would then become a problem with this solution.

Closed System Operation

By adding another heat exchanger to the existing service water system one can create a closed system. There are various heat exchangers that can be implemented into the system such as water-to-water, air-to-water, or chemical-to-water.

Water-to-water would be the most practical in this situation due to the amount of heat that is being transferred through the exchanger. An air-to-water heat exchanger would have a very large surface area in order to remove the quantity of heat within the system, making this solution not practical. Using a chemical within the closed circuit system is not necessary considering the temperatures that we are dealing with.

This additional heat exchanger will require pumps, piping and valves in order to be incorporated into the service water system. In addition the style and location of this new heat exchanger will be incorporated into the design of the new system so that maintenance will be easier. Also this system will have 100% capacity back up so that cleaning of the heat exchanger will not require any unit outages.

The use of a cooling pond to supply water to the service water system can be considered a closed loop system because you are reusing the existing water that is in the cooling pond. The water in the cooling pond can be chemically treated to ensure that it remains neutral and does not become acidic. Again space would be a restriction with this type of solution.

VIABLE SOLUTIONS

In order to compare the viable solutions the Net Present Worth (NPW) method will be used to determine which solution is most feasibly from a financial point of view. The NPW method will only take into account the investment dollars needed to bring the solution to life. Other benefits to each solution is not taken into account using the NPW method because of the many variables involved in placing a dollar sign on there worth.

In the conclusions and recommendations section each solution will be discussed including all of the advantages and disadvantages associated with that solution.

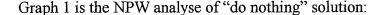
Continue to Maintain Current Operation

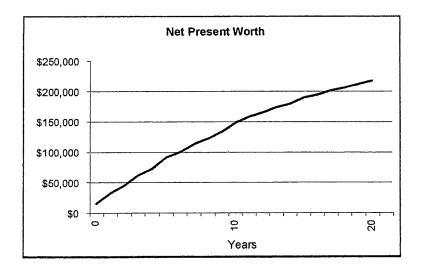
The "do nothing" approach is to continue operating the plant as we have in the past. This means mechanically cleaning the SAC's every second year, generator bearing coolers every five years, SAC piping every ten years, and generator bearing cooler piping every ten years. This solution will require high maintenance and unit outages so that the work can be performed.

The NPW cost associated with this solution is for only one unit in Cat Arm and in order to compare this solution to the others the NPW cost should be doubled.

NPW Analysis

Below is the NPW analysis of the "do nothing" solution. There is no capital expenditures related to this solution only yearly operating costs.





Graph 1

Table 28 shows the costs associated with this solution:

Capital Cost	
Total	0

Operating Cost	·
Pump consumption (49 weeks)	\$15,353
Clean SAC (2 yr)	\$5,783
Clean SAC Piping (10 yr)	\$4,667
Clean Gen Brg Coolers (5 yr)	\$5,783
Clean Gen Brg Cooler Piping (10	\$4,667

Table 28

The NPW is calculated over the life span of the piping, which is 20 years. The inflation rate used is 2%, the power rate used for the pump is \$0.05 kWh, and the rate of return for Hydro is 8.5%.

The total NPW of this solution is \$217,320 per unit.

The spreadsheet for the NPW graph showing each year's increase can be found in Appendix E.

Replace Piping Inside of Generator Housing

Stainless Steel is recommended as the ideal piping material to be used inside of the generator housing due to its corrosion resistance and mechanical properties. The generator cooler piping is carbon steel and should be replaced with stainless steel. The turbine cooler piping is already stainless steel. The surface air cooler piping is being replaced with stainless steel in the Fall 2001.

Generator Bearing Cooler Water Piping per Unit

The generator cooler water piping is currently carbon steel with victaulic couplings for all the connections. It is recommended to replace the carbon steel with stainless steel sch 10 inside the generator housing. The stainless steel system will reuse the existing carbon steel victaulic couplings with all new gaskets. Galvanic corrosion between the existing couplings and stainless steel pipe is not of any concern due to such a small contact surface area between the coupling and pipe. The following table is a list of parts needed to replace the piping with stainless steel. The price quote is from EMCO Distribution Ltd.

Parts Table:

Item #	Part Description	Quantity	Price	Total
1	2" Pipe s.s sch 10	105	\$7.51	\$788.55
2	2" Elbow s.s vic 90 degrees	8	\$70.15	\$561.20
3	2" Elbow s.s vic 45 degrees	8	\$70.15	\$561.20
4	2" Coupling c.s vic style 77 E gasket	10	\$11.50	\$115.00
5	2" E Gasket style 77	46	\$5.01	\$230.46
6	1/2" x 2 1/2" Bolts c/w nuts	40	\$2.00	\$80.00
7	2" Tee s.s vic	2	\$154.92	\$309.84
8	2" Vic-Flange adapter style 741	2	\$36.30	\$72.60

The total cost for parts is \$2,679.90 per unit.

Cost Analysis to Replace Generator Bearing Cooler Water Piping per Unit

The labour time required for a crew to replace the piping was calculated using RS Means Mechanical Cost Data 2000. An additional 25% labour time was added to the RS Means calculation for pipe location and restrictions. An additional 15% labour time was added to the RS Means calculation for removal of old piping system. One additional worker will be placed on this job, shortening the labour time by 25%. RS Means calculation can be found in Appendix F. The costs break down associated with travel, perdiem, and minimum work crew can be found under the Cost Analysis section on page 29.

Total labour required for work crew of three: 20.9 hrs Added labour due to pipe location and space restrictions: $20.9 \times 25\% = 5.2 \text{ hrs}$ Labour time for work crew to remove old piping: $26.1 \times 15\% = 3.9 \text{ hrs}$ Total labour time required to complete job: 30.0 hrs

In order to complete this job within the one week scheduled outage all work has to be done in 32.0 hours, leaving 8.0 hours for travel. The supervisor is usually over seeing two or three jobs while on site; therefore only 1/3 of the supervisors wage will be allocated to this particular job.

Labour: 3 (workers) x 38.0 hrs (30.0 installation + 8.0 driving) x \$21.56 = \$2,457.841 (supervisor) x 12.7 hrs (1/3 x 38.0 hrs) x \$23.72 (\$21.56 x 10%) = \$301.24

Total Over Head Costs: $2,759.08 \times 1.63 = 4,497.30$

Perdiem: 4 (work crew) x \$183 = \$732 (Monday \$34, Tuesday to Thursday \$129, Friday \$20)

Gas: 4 trips (2 vehicles) x \$80 = \$320

Total Cost per Unit: \$5,549.30

Replace Piping Outside of Generator Housing

Polyvinyl chloride (PVC) is recommended as the ideal piping material to be used outside of the generator housing due to its corrosion resistance, mechanical properties, thermal properties, and cost. The inlet header and discharge piping is carbon steel and should be replaced with PVC.

Inlet Header Piping per Unit

The inlet header piping for each unit branches off from the main supply header and uses a pipe rack to ascend from the floor to the ceiling where it then runs along the ceiling into the generator housing. Damage caused by accidental impact should not be of any concern due to this piping arrangement. The inlet header piping for each unit will be replaced starting from the discharge side of the pressure-reducing valve for each unit and continue to the entrance of the generator housing where it will meet the start of the stainless steel pipe. The following table is the list of parts needed to replace the inlet piping per unit with PVC. The price quote is from EMCO Distribution Ltd.

Item #	Part Description	Quantity	Price	Total
1	4" Pipe PVC Sch 80	20	\$4.17	\$83.40
2	4" Elbows 90 PVC Socket Sch 80	2	\$9.47	\$18.94
3	4" Flange PVC Socket Sch 80	1	\$13.09	\$13.09
4	6"x4" Reducer PVC Socket Sch 80	1	\$48.49	\$48.49
5	6"x6"x3" Tee PVC Socket Sch 80	2	\$36.30	\$72.60
6	2" Pipe PVC Sch 80	20	\$1.32	\$26.40
7	2" Elbows 90 PVC Socket Sch 80	3	\$2.54	\$7.62
8	2" Butterfly Valve PVC Flanged	1	\$184.85	\$184.85
9	2" Flange PVC Socket Sch 80	3	\$6.07	\$18.21
10	3"x2" Reducer PVC Socket Sch 80	2	\$10.00	\$20.00
11	1 1/4" Pipe PVC Sch 80	20	\$0.85	\$17.00
12	1 1/4" Elbows 90 PVC Socket Sch 80	1	\$1.82	\$1.82
13	1 1/4" Elbows 45 PVC Socket Sch 80	1	\$3.65	\$3.65
14	1 1/4" Butterfly Valve PVC Flanged	1	\$31.35	\$31.35
15	1 1/4" Flange PVC Socket Sch 80	3	\$4.80	\$14.40
16	6" Pipe PVC Sch 80	40	\$7.80	\$312.00
17	6" Elbows 90 PVC Socket Sch 80	6	\$29.96	\$179.76
18	6" Flange PVC Socket Sch 80	3	\$48.10	\$144.30
19	2"x1 1/4" Reducer PVC Socket Sch 80	1	\$3.64	\$3.64
20	6" Elbows 45 PVC Socket Sch 80	1	\$34.84	\$34.84

The total cost for parts is \$1, 236.36 for unit #1.

The total cost for parts is \$1,080.36 for unit #2. (Unit #2 needs 20 feet of 6 inch Pipe)

Cost Analysis to Replace Inlet Header Piping per Unit

The labour time required for a crew to replace the piping was calculated using RS Means Mechanical Cost Data 2000. An additional 25% labour time was added to the RS Means calculation for pipe location and restrictions. Also an additional 15% labour time was added to the RS Means calculation for removal of old piping system. RS Means calculations can be found in Appendix F. The costs break down associated with travel, perdiem, and minimum work crew can be found under the Cost Analysis section on page 29.

Total labour time for work crew of two: 35.1 hrs Added labour due to pipe location and space restrictions: $35.1 \times 25\% = 8.8$ hrs Labour time for work crew to remove old piping: $43.9 \times 15\% = 6.6$ hrs Total labour time for work crew to complete job: 50.5 hrs

In order to complete this job within a two-week scheduled outage all work has to be done in 64.0 hours, leaving 16.0 hours for travel. The supervisor is usually over seeing two — three jobs while on site; therefore only 1/3 of the supervisors wage will be allocated to this particular job.

Labour: 2 (workers) x 66.5 hrs (50.5 installation + 16.0 driving) x \$21.56 = \$2,867.481 (supervisor) x 22.2 hrs (1/3 x 66.5 hrs) x $$23.72 ($21.56 \times 10\%) = 526.58

Total Over Head Costs: $$3,394.06 \times 1.63 = $5,532.32$

Perdiem: 3 (work crew) x \$183 = \$549 (Monday \$34, Tuesday to Thursday \$129, Friday \$20) 3 (work crew) x \$140 = \$420 (Monday \$34, Tuesday to Wednesday \$86, Thursday \$20)

Gas: 4 trips (2 vehicles) x 2 weeks x \$80 = \$640

Total Cost per Unit: \$7,141.32

Discharge Header Piping per Unit

The discharge piping for each unit comes out of the ceiling and descends down the outside of the scroll case wall to the floor. Damage caused by accidental impact should not be of any concern due to the location of the piping on the concrete wall. The discharge piping for each unit will be replaced from where the stainless steel exits the generator housing and will continue until it meets the piping embedded in the floor. The following table is the list of parts needed to replace the piping with PVC. The price quote is from EMCO Distribution Ltd.

Item#	Part Description	Quantity	Price	Total
1	1 1/4" Pipe PVC Sch 80	20	\$0.85	\$17.00
2	2" Pipe PVC Sch 80	20	\$1.32	\$26.40
3	2.5" Pipe PVC Sch 80	40	\$2.12	\$84.80
4	3" Pipe PVC Sch 80	20	\$2.86	\$57.20
5	4" Pipe PVC Sch 80	40	\$4.17	\$166.80
6	6" Pipe PVC Sch 80	10	\$7.80	\$78.00
7	1 1/4" Elbows 90 PVC Socket Sch 80	4	\$1.82	\$7.28
8	2" Elbows 90 PVC Socket Sch 80	1	\$2.54	\$2.54
9	2.5" Elbows 90 PVC Socket Sch 80	4	\$5.96	\$23.84
10	4" Elbows 90 PVC Socket Sch 80	6	\$9.47	\$56.82
11	2.5" Elbows 45 PVC Socket Sch 80	1	\$12.62	\$12.62
12	4" Elbows 45 PVC Socket Sch 80	1	\$27.66	\$27.66
13	4"x4"x4" Tee PVC Socket Sch 80	2	\$14.27	\$28.54
14	2.5"x2.5"x2.5" Tee PVC Socket Sch 80	3	\$9.86	\$29.58
15	2.5"x 1 1/4" Reducer PVC Socket Sch 80	1	\$6.30	\$6.30
16	2.5"x2" Reducer PVC Socket Sch 80	3	\$6.30	\$18.90
17	4"x3" Reducer PVC Socket Sch 80	2	\$25.56	\$51.12
18	6"x4" Reducer PVC Socket Sch 80	1	\$52.14	\$52.14
19	1 1/4" Flange PVC Socket Sch 80	3	\$4.80	\$14.40
20	2" Flange PVC Socket Sch 80	5	\$6.07	\$30.35
21	2.5" Flange PVC Socket Sch 80	6	\$10.06	\$60.36
22 .	3" Flange PVC Socket Sch 80	2	\$11.12	\$22.24
23	4" Flange PVC Socket Sch 80	. 7	\$14.07	\$98.49
24	1 1/4" Pressure Tap Orifice Flanges s.s Socket Sch 80	1	\$387.69	\$387.69
	2" Pressure Tap Orifice Flanges s.s Socket Sch 80	1	\$479.75	\$479.75
26	4" Pressure Tap Orifice Flanges s.s Socket Sch 80	1	\$689.74	\$689.74
27	1 1/4" Butterfly Valve PVC Flanged	1	\$31.35	\$31.35
28	2" Butterfly Valve PVC Flanged	1	\$184.85	\$184.85
29	2.5" Butterfly Valve PVC Flanged	1	\$216.19	\$216.19
30	3" Butterfly Valve PVC Flanged	1	\$204.33	\$204.33
31	4" Butterfly Valve PVC Flanged	1	\$239.91	\$239.91

The total cost for parts is \$3,406.20 per unit.

Total cost with reusing existing pressure tap orifice flanges is \$1,849.02 per unit.

Cost Analysis to Replace Discharge Header Piping per Unit

The labour time required for a crew to replace the piping was calculated using RS Means Mechanical Cost Data 2000. An additional 25% labour time was added to the RS Means calculation for pipe location and restrictions. Also an additional 15% labour time was added to the RS Means calculation for removal of old piping system. RS Means calculations can be found in Appendix F. The costs break down associated with travel, perdiem, and minimum work crew can be found under the Cost Analysis section on page 29.

Total labour time for work crew of two: 41.4 hrsAdded labour due to pipe location and space restrictions: $41.4 \times 25\% = 10.4 \text{ hrs}$ Labour time for work crew to remove old piping: $51.8 \times 15\% = 7.8 \text{ hrs}$ Total labour time for work crew to complete job: 59.6 hrs

In order to complete this job within a two-week scheduled outage all work has to be done in 64.0 hours, leaving 16.0 hours for travel. The supervisor is usually over seeing two or three jobs while on site; therefore only 1/3 of the supervisors wage will be allocated to this particular job.

Labour: 2 (workers) x 75.6 hrs (59.6 installation + 16.0 driving) x \$21.56 = \$3,259.871 (supervisor) x 25.2 hrs (1/3 x 75.6 hrs) x \$23.72 (\$21.56 x 10%) = \$597.74

Total Over Head Costs: $$3,857.61 \times 1.63 = $6,287.90$

Perdiem: 3 (work crew) x \$183 = \$549 (Monday \$34, Tuesday to Thursday \$129, Friday \$20) 3 (work crew) x \$140 = \$420 (Monday \$34, Tuesday to Wednesday \$86, Thursday \$20)

Gas: 4 trips (2 vehicles) x 2 weeks x \$80 = \$640

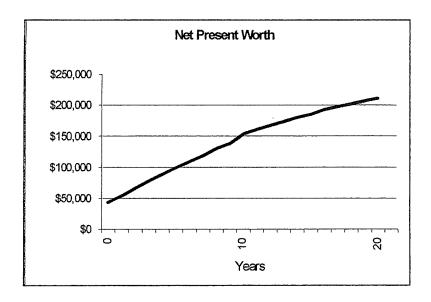
Total Cost per Unit: \$7,896.90

NPW Analysis

Below is the NPW analysis of the replace piping solution. There are capital expenditures with this solution along with operating expenditures. The capital is for replacing the existing SAC, generator bearing cooler piping inside the generator housing with stainless steel and replace the inlet and discharge header piping outside of the generator housing with PVC. The SAC piping inside the generator housing has been replaced already with stainless steel this year and will not be factored into the NPW calculations.

The NPW cost associated with this solution is for only one unit in Cat Arm and in order to compare this solution to the others the NPW cost should be doubled.

Graph 2 is the NPW analyse of replacing the piping solution:



Graph 2

Table 29 shows the costs associated with this solution:

Capital Cost	
Gen Brg Piping (Parts & Installation)	\$8,229
Inlet Piping (Parts & Installation)	\$8,378
Discharge Piping (Parts & Installation)	\$11,303
Total	\$27,910

Operating Cost	
Pump consumption (49 weeks)	\$15,353
Clean SAC (8 yr)	\$5,783
Clean SAC Piping (10 yr)	\$4,667
Clean Gen Brg Coolers (10 yr)	\$5,783
Clean Gen Brg Cooler Piping (10 yr)	\$4,667

Table 29

The NPW is calculated over the life span of the piping, which is 20 years. The inflation rate used is 2%, the power rate used for the pump is \$0.05 kWh, and the rate of return for Hydro is 8.5%.

The total NPW of this solution is \$210,126 per unit.

The spreadsheet for the NPW graph showing each year's increase can be found in Appendix E.

Closed System Operation

Heat Exchanger Selection

The style of heat exchanger that needed to be selected would have to meet the following criteria:

- 1. Compact design
- 2. Easy to maintain and clean
- 3. Will not clog
- 4. Capacity of 900 Usgpm

It was determined that a plate and frame heat exchanger would meet all of these requirements. Due to it's construction the exchanger can be expanded to meet future cooling requirements by adding more plates and this design also allows for easy access for cleaning.

Tom Furlong of Maynard Reece was contacted for a price estimate on this type of heat exchanger. A quoted price of \$17,500 per unit was established for this cost feasibility study.

Pump Selection

In order to select a pump for this system the pressure drop across the entire cooling water system including the new heat exchanger would have to be known. Using Design Flow Solutions one can enter the entire cooling water system into the program and determine the pressure drop at the desired flow rate.

It was determined that the pressure drop for Cat Arm at 900 Usgpm was 22 psia. A print out of the calculation can be found in Appendix G.

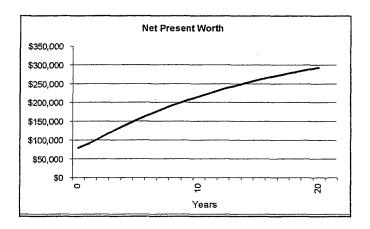
The pump selected for this application is a Goulds centrifugal pump 3196 (4 x 6 - 10H, 9" impeller). This pump is capable of 900 Usgpm @ 60 ft head using water as the medium. The pumps specification sheet can be found in Appendix H.

NPW Analysis

The closed loop solution has capital and operating expenditures associated with it. The capital expenditure is for purchasing the heat exchanger, recirculation pump, and associated piping and hardware for the installation. This solution will require 100% capacity back up so two heat exchangers and recirculation pumps will have to be purchased.

The closed loop solution will treat both units in Cat Arm so the NPW cost does not have to be doubled for this solution.

Graph 3 is the NPW analyse for the closed loop solution:



Graph 3

Table 30 shows the costs associated with this solution:

Capital Cost	
Pump	\$14,404
Heat Exchanger	\$35,000
Installation Piping & Hardware	\$8,000
Total	\$57,404

Operating Cost	
Pump consumption (49 weeks)	\$15,353
Recir Pump Consumption (49 weeks)	\$6,133

Table 30

The NPW is calculated over the life span of the piping, which is 20 years. The inflation rate used is 2%, the power rate used for the pump is \$0.05 kWh, and the rate of return for Hydro is 8.5%.

The total NPW of this solution is \$293,131 for both units.

The spreadsheet for the NPW graph showing each year's increase can be found in Appendix E.

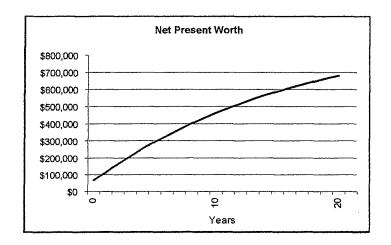
Chemical Injection

The chemical injection solution is based on injecting a chemical known as FLOGARD POT6101 into the cooling water system. This chemical has both cathodic and anodic inhibitors that react with the water to prevent corrosion of the piping and organic build up within the piping. The concentrations are very low 4 ppm and the impact on the environment would be very low considering the chemical is being discharged into the tailrace with the rest of the discharged water.

NPW Analysis

This solution has both capital and operating expenditures. The operating expenditures are very high due to the continuous replacement of the FLOGARD POT6101 chemical.

Graph 4 is the NPW analyse of the chemical injection solution:



Graph 4

BetzDearborn's proposal for chemical injection can be found in Appendix C.

Table 31 shows the costs associated with this solution:

Capital Cost	
Injection System	\$5,000
Test Coupon Rack	\$515
Total	\$5,515

Operating Cost		
Pump consumption (49 weeks)	\$15,353	
Chemical (49 weeks)	\$45,000	

Table 31

The NPW is calculated over the life span of the piping, which is 20 years. The inflation rate used is 2%, the power rate used for the pump is \$0.05 kWh, and the rate of return for Hydro is 8.5%.

The total NPW of this solution is \$679,865 for both units.

The spreadsheet for the NPW graph showing each year's increase can be found in Appendix E.

CONCULSIONS AND RECOMMENDATIONS

From the material presented there were four different solutions that could be taken to resolve the problem. To recap the four alternative solutions were to continue to operate as we have "do nothing approach", replace the piping with corrosion resistant material, inject chemical into the service water for treatment, or install a closed loop system with treated water to cool the units. Each solution has it's benefits and draw backs.

The NPW analysis calculated the following dollar figures for each solution;

Do Nothing	\$217,320 x 2 units = \$434,640
Replace the Piping with s.s & PVC	\$210,126 x 2 units = \$420,252
Closed Loop System	\$293,131
Chemical Injection	\$679,865

Table 30

The "continue to operate as we have" will mean scheduled outages for cooler and pipe cleaning. There is an uncertainty with this solution when it comes to forced outages due to cooling problems during the summer months. If a maintenance program for cleaning and maintaining the cooling water system is not implemented forced outages due to cooling problems during the summer months in the height of the maintenance season will occur. In order to prevent this a fouling monitoring program for the cooling water system has to be put in place.

In addition the cooling water system that is currently in place in Cat Arm has a redundant control valve. There is a pressure-reducing valve located in the inlet header and there are temperature control valves located in the discharge header. The service water pumps maximum pressure is still to low to damage any of the components in the service water system. It seems that the pressure control valve in the inlet header is back up pressure-reducing valve for the secondary water supply that comes off the penstock, yet the penstock lines have there own pressure-reducing valves. This warrants further investigation.

Also the temperature control valves located in the discharge lines regulate flow through the coolers based on the temperature of the water exiting the coolers and not on the temperature of the bearing oil, which they are cooling. This also warrants further investigation.

The other alternative of replacing the piping with corrosion resistant pipe solution has an initial capital investment with a low operating cost associated with it. The Cat Arm plant has been in operation since 1985 and most of the cooling water pipe's expected life is coming to an end. The labour cost of replacing this pipe is going to be the same regardless of what type of pipe you use to replace it. Already the SAC piping inside of the generator housing has been replaced with stainless steel sch 10 pipe.

One of the benefits of having the corrosion resistant pipe like stainless steel and PVC is lower maintenance. Unit outages for cleaning service water piping will be less frequent, hence will free up more manpower for other tasks during the maintenance season.

Another benefit to corrosion resistant piping is the reduced likely hood of the pipe becoming clogged with debris. Since the pipe is resistant to corrosion from the service water it is not likely that enough organic material will be able to adhere to the pipe wall to impend flow to the point of stagnation. It is believed that only a small layer of organics will adhere to the inner pipe wall and once that layer is in place the rest of the organics will be washed through the system. Cleaning of the coolers and piping will still have to be done to optimize the efficiency of the system but the frequency of cleanings will be drastically reduced from the current operation.

Another benefit to the replace piping with corrosion resistant pipe solution is that no new equipment or design changes have to be made to the existing system, just replace the existing pipe.

As can be seen from the NPW analysis replacing the piping with corrosion resistant pipe has a NPW of \$420,252 and the other solution of continuing to operate like we have in the past has a NPW of \$434,640. In order to continue to operate as we have the existing piping has to be replaced and the labour alone is \$42,000. This labour figure does not include the SAC piping that was replaced in the Fall 2001 outage.

The closed loop system has a NPW of \$293,131which makes this solution better than the other solution presented from a financial point of view. The problem with this solution is that it is add on to the existing cooling water system. Seeing that the service water piping is almost at its life expectancy the cost of replacing that piping has to also be considered.

With the closed loop solution the piping inside of the generator housing can be mild steel sch 40 pipe and the piping outside of the generator housing can be PVC to help reduce costs. This solution will use treated water for recirculating through the unit and use the existing service water to cool the heat exchangers.

The closed loop solution will have more components with the extra two recirculating pumps and heat exchangers. This increases the chances of more problems within the system.

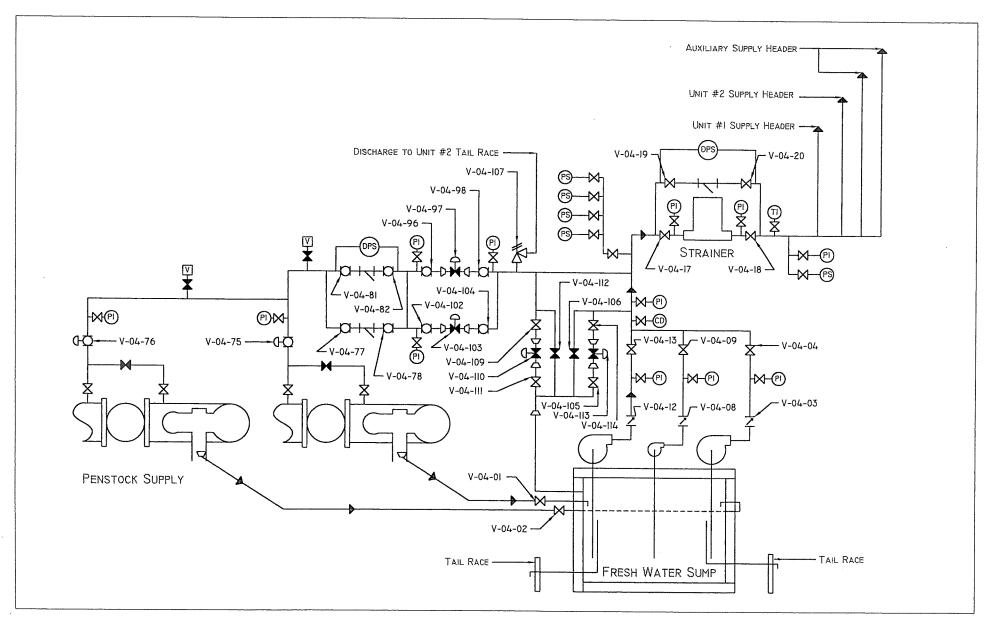
The maintenance of the unit's coolers and piping will be non-existent but the outside heat exchanger will have to be cleaned. The frequency of this clean will have to be determined from operating the system. These outside heat exchangers should be positioned for easy cleaning.

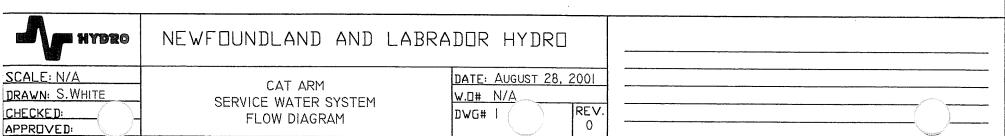
The chemical injection solution has a NPW of \$679,865, which makes this solution not feasible compared to the other alternative solutions. Also any solution that doesn't impact the environment is always a better alternative.

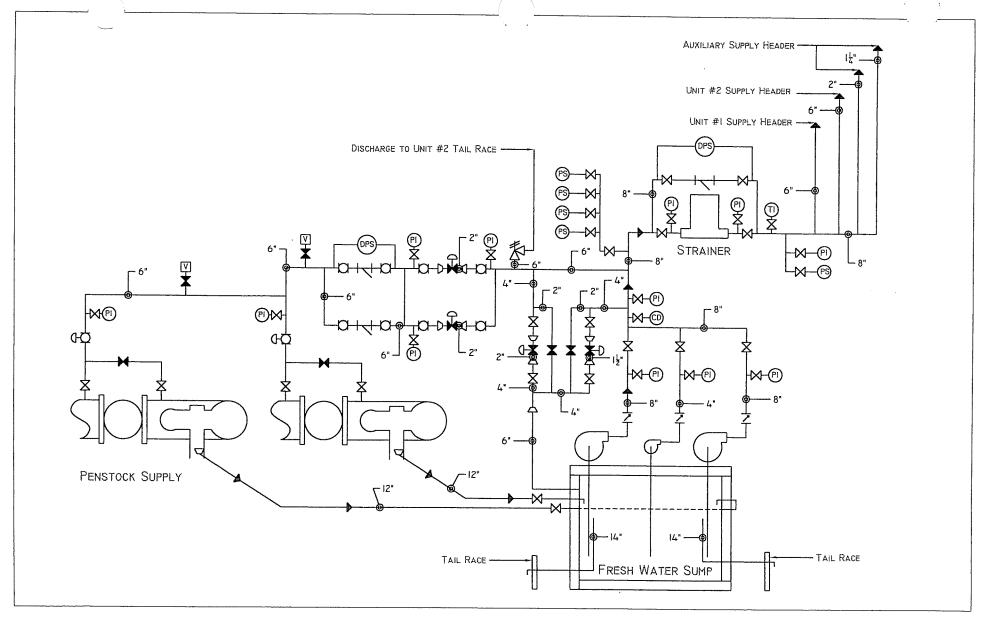
It is recommended that we go with the solution of "replacing the piping with corrosion resistant pipe" for Cat Arm. The pipe's life expectancy within the service water system is coming to an end and will need to be replaced in the near future. With this alternative we still have the ability of replacing sections of the existing system year by year until it is all changed over, reducing the over all capital expenditure for that year. Also this solution will result in lower maintenance costs for the system. Another benefit is that no new design work has to be done in order for this solution to be implemented.

It is also recommended that the current design of the cooling water system be reevaluated to determine if it is indeed operating in the most efficient way. It seems that there is a complexity build into the design that doesn't need to be there, i.e. too many control valves.

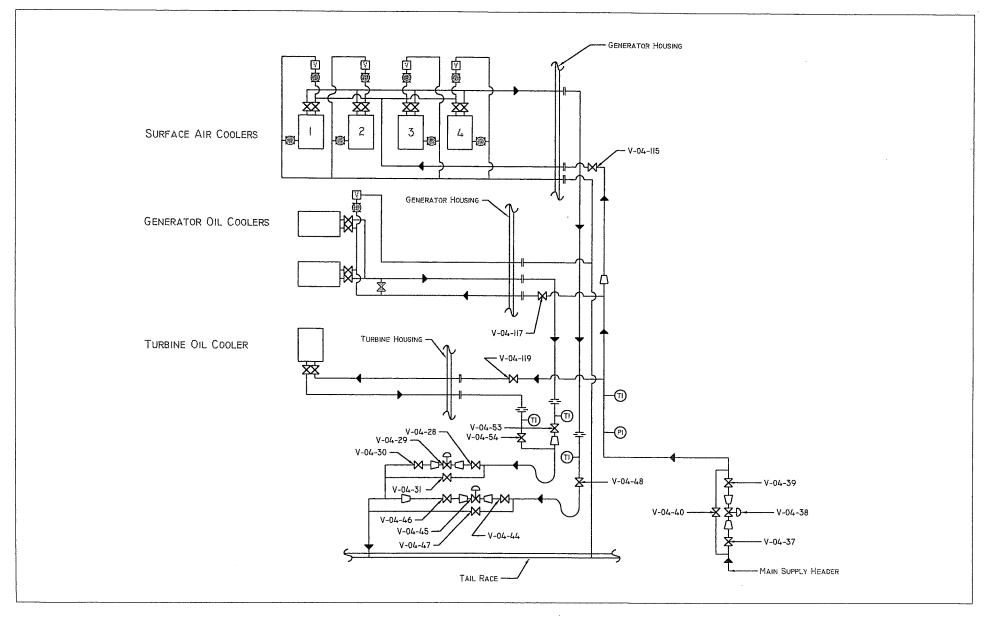
APPENDIX A



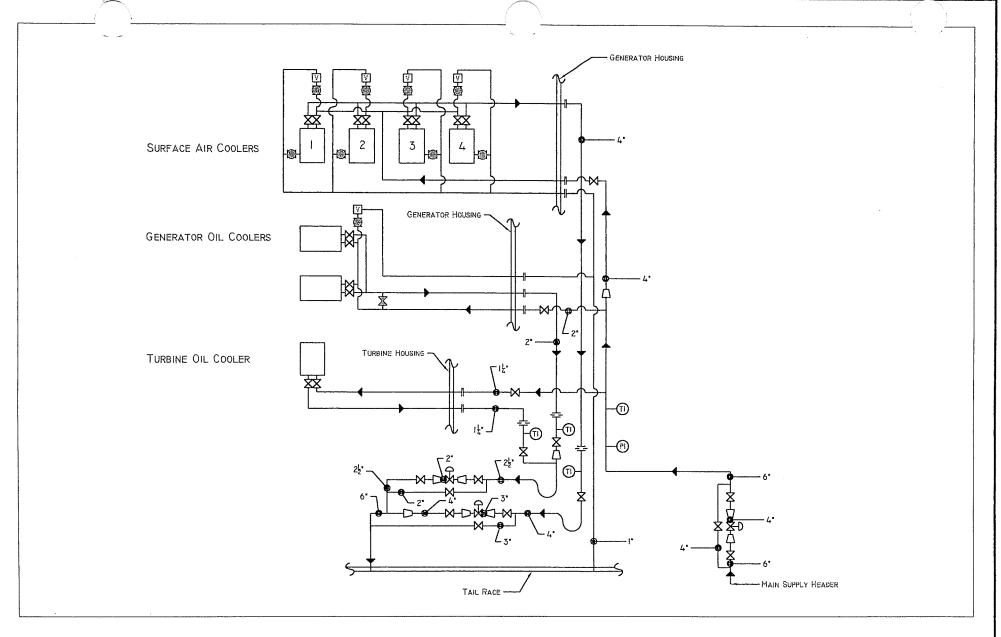




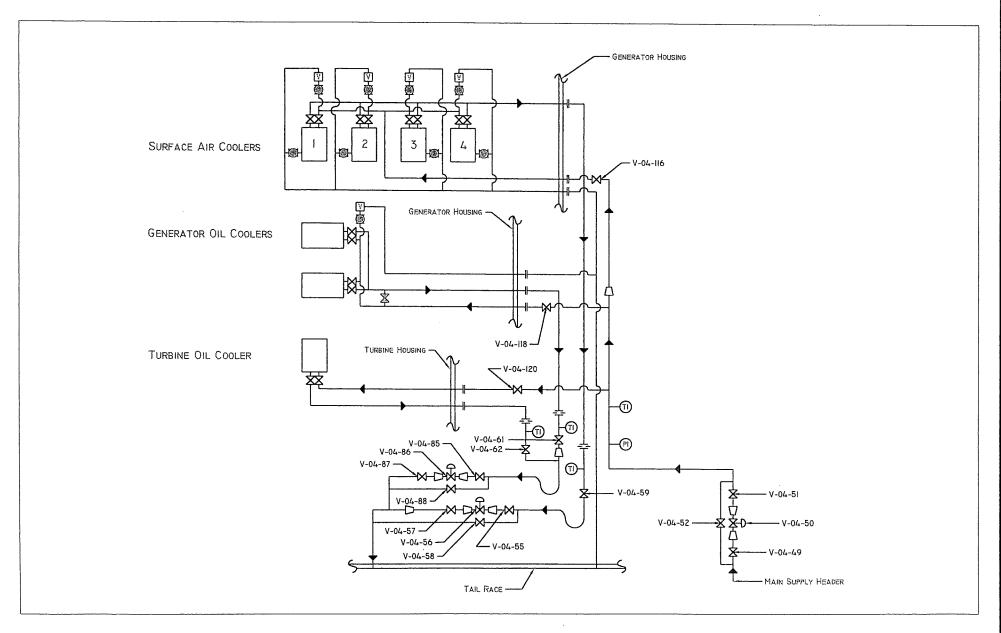
HYBRO	NEWFOUNDLAND AND LABRADOR HYDRO		
SCALE: N/A DRAWN: S.WHITE CHECKED: APPROVED:	CAT ARM SERVICE WATER SYSTEM FLOW DIAGRAM	DATE: AUGUST 28, 2001 W.D# N/A DWG# REV. 0	



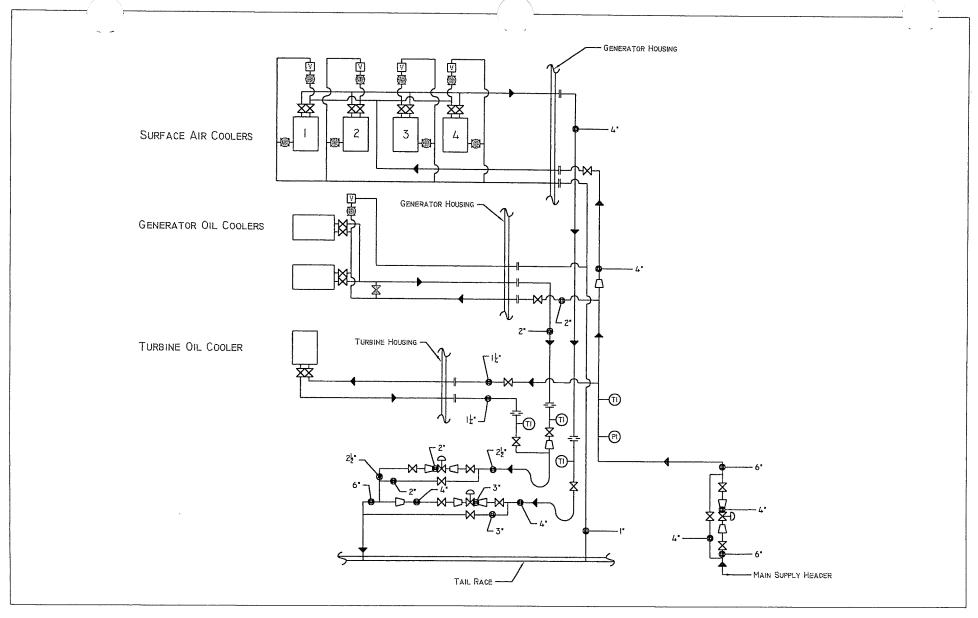
A HYDRO	NEWFOUNDLAND AND LABRADOR HYDRO		
SCALE: N/A DRAWN: S.WHITE CHECKED: APPROVED:	CAT ARM SERVICE WATER SYSTEM UNIT #1 FLOW DIAGRAM	DATE: AUGUST 27, 2001 W.0# N/A DWG# REV. 0	



HYDRO	NEWFOUNDLAND AND LABRADOR HYDRO		
SCALE: N/A DRAWN: S.WHITE CHECKED: APPROVED:	CAT ARM SERVICE WATER SYSTEM UNIT #I FLOW DIAGRAM	DATE: AUGUST 27, 2001 W.D# N/A DWG# REV. 0	



HYDRO	NEWFOUNDLAND AND LABRADOR HYDRO		
SCALE: N/A DRAWN: S.WHITE CHECKED: APPROVED:	CAT ARM SERVICE WATER SYSTEM UNIT #2 FLOW DIAGRAM	DATE: AUGUST 27, 2001 W.0# N/A DWG# REV. 0	



HYBRO	NEWFOUNDLAND AND LAB	BRADOR HYDRO
CALE: N/A PRAWN: S.WHITE HECKED: PPROVED:	CAT ARM SERVICE WATER SYSTEM UNIT #2 FLOW DIAGRAM	DATE: AUGUST 27, 2001 W.0# N/A DWG# REV. 0

APPENDIX B



WATER ANALYSIS REPORT

BC562412 NEWFOUNDLAND & LABRADOR HYDRO HOLYROOD GENERATING STATION HOLYROOD, NF A0A2R0 Sampled: 04-AUG-2000 Reported: 14-AUG-2000 Field Rep: Finn,Ed BB59M

	JM 01	JM 02
	K0809046	K0809047
pH «	5.0	5.1
Specific Conductance, at 25°C, µmhos	91	77
Alkalinity, "P" as CaCO ₃ , ppm	0	0
Alkalinity, "M" as CaCO ₃ , ppm	< 2	< 2
Sulfur, Total, as SO ₄ , ppm	< 5	< 5
Chloride, as Cl, ppm	3.1.	3.7
Hardness, Total, as CaCO ₃ , ppm	6.5	5.3
Calcium Hardness, Total, as CaCO ₃ , ppm	2.3	1.6
Magnesium Hardness, Total, as CaCO3, ppm	4.2	3.6
Copper, Total, as Cu, ppm	< 0.05	< 0.05
Iron, Total, as Fe, ppm	0.79	0.87
Sodium, as Na, ppm	2.2	2.1
Phosphate, Total Inorganic, as PO4, ppm	< 0.2	< 0.2
Phosphate, Ortho-, as PO4, ppm	< 0.2	< 0.2
Silica, Total, as SiO_2 , ppm	1.5	1.5



INORGANIC ANALYSIS REPORT

BC562412 NEWFOUNDLAND & LABRADOR HYDRO HOLYROOD GENERATING STATION Holyrood, NF A0A2R0 Laboratory ID: 61729.1

Sampled: 21-JUL-2000 Reported: 10-AUG-2000 Field Rep: Finn, Ed

BB59M

Sample Description:
 SAC #3 JM03

PRIMARY COMPOSITION (%)

Iron, $Fe_2O_3 + Fe_3O_4$ Loss on Ignition LOI 21 Manganese, MnO_2 Aluminum, Al_2O_3

X-ray fluorescence detects elements between fluorine and uranium in atomic number. Any of these elements not reported are below detection limits.

Stan Kasper, Laboratory Supervisor

Appendix 1 - Water Chemistry in Cat Arm Watershed

Location of Sample

Parameter	South Inlet	Seepage	<u>Outlet</u>
Alkalinity mg/l Hardness mg/l pH Conductance u mhos/cm Acidity mg/l Chloride mg/l Sulphate Total Kjeldahl N mg/l % Soluble Kjeldahl N % Particulate Kjeldahl N Nitrate mg/l	1.0 5.42 16.76 3.9 3.0 0.231 40 60 0.01	 4.28 34.78 15 0.394 57 43 0.01	0.6 4.2 5.03 19.37 0.394 63 37 0.012
Chemical Oxygen Demand (as carbon) mg/l % Soluble COD % Particulate COD Phosphorous mg/l % Soluble P % Particulate P Silicate mg/l Total Calcium mg/l % Soluble Calcium % Particulates Calcium Total Magnesium mg/l % Soluble Magnesium % Particulate Magnesium % Particulate Magnesium Total Manganese mg/l % Soluble Manganese % Particulate Manganese Total Iron mg/l % Soluble Iron % Particulate Iron Total Zinc mg/l Total Molybdenum Total Cobalt mg/l	35.5 53 47 0.056 38 62 0.073 0.535 100 0.261 61 39 0.017 59 41 0.386 30 70 0.01 0.001 0.001	92.5 77 23 0.073 75 25 0.436 1.270 92 8 0.682 97 3 0.033 85 15 1.018 88 12 0.01 0.003 0.01	41.8 77 23 0.040 63 37 0.143 0.745 94 6 0.408 67 33 0.017 58 42 0.498 48 52 0.01 0.001 0.01
Total Sodium mg/l Total Potassium mg/l Floride mg/l Copper mg/l Zinc mg/l Cadium mg/l	1.303 0.230 	2.352 0.230 	1.725 0.200 0.1 0.004 0.01 0.01

APPENDIX C

Corrosion Inhibitor Program FLOGARD POT6101

Newfoundland Hydro St. John's, Newfoundland

October 10, 2001

Edward Finn
District Representative

BetzDearborn Canada Inc. P.O. Box 1048 Carbonear, Newfoundland A1Y 1C5 Tel: 709-596-3100

Fax: 709-596-1332

October 18, 2001

Newfoundland Hydro P.O. Box 12400 St. Johns, NF A1B 4K7

Attention:

John Mallam

SUBJECT:

Cooling Water Inhibitor Proposal

John,

Please find below our proposal to treat the once-thru cooling water systems in your Hydroelectric Station with our corrosion inhibitor – **Flogard POT6101**.

In short, we propose that you install a chemical injection and monitoring system to dose the system with 4 ppm of Flogard POT6101.

The annual cost of the chemical treatment, based on continuous operation, would be \$30,000.

We suggest, you monitor the effectiveness of the program by using corrosion coupons that simulate the corrosion in the system and are analyzed in our lab.

THEORY:

The recent set of water samples, taken by yourselves, were tested by our analytical lab in the USA. A short table comparing the important parameters in these tests is below. These have been communicated to you previously, but we show them here for completeness.

As well, we have calculated the Langelier index, which is calculated by a nomagraph and is used in the water treatment industry as an overall indication of the scaling or corrosion tendency of any particular water.

Your waters all had a Langelier's index below –5.0, so these waters would be described as "Very Corrosive". Therefore, the problems you have been experiencing with rust and corrosion are predictable and understandable. Fortunately, they are also preventable with proper chemical treatment.

TABLE 1

	HINDS LAKE	CAT ARM	UPPER SALMON	BAIE D'ESPOIR
Date	08/21/2001	08/04/2000	08/2001	08/2001
рН	5.9	5.1	5.1	6.2
Conductivity (mmhos)	25	91	24	13.7
'M' alkalinity (ppm)	0.7	< 2	< 2	2.1
Total Hardness (ppm)	6.5	6.5	3.4	3.8
Copper (ppm)	0.05	0.05	0.06	< 0.05
Iron (ppm)	4.3	0.79	0.17	0.08
TOC (ppm)	2.4		5.1	4.7
Langelier Index	- 5.1	- 5	- 5.3	- 5.5

The deposits that we analysed were also reported to you by e-mail. These deposits proved to be high in iron and manganese. The iron is from the rusted piping, while the manganese is chemically associated with the organic matter in the surface water supply. This manganese is noteworthy because it is found in deposits where the surface water is high in organics like these. Manganese does foul piping by depositing on the pipe wall rather than corrode. Fortunately, it is a problem that can be treated chemcially.

In its simplest terms, corrosion is a reaction like the reactions that occur in a conventional lead - acid battery.

The Cathodic reaction is:

$$2H^+ + 2e^- \rightarrow H_2$$

This reaction occurs in a low pH – acidic environment because of the relative abundance of H⁺.

The Anodic reaction is:

Fe
$$\rightarrow$$
 Fe²⁺ + 2e⁻

This reaction results in the loss of metal from the piping.

If you can stop these reactions from occurring, by stopping the flow of electrons, then the corrosion is stopped .

Chemical corrosion inhibitors basically fall into two broad classes: Anodic and Cathodic, depending on how they act. The product we propose, Flogard POT6101, contains both a Cathodic and an Anodic inhibitor. The phosphate in the product acts as a weak anodic inhibitor, by forming a loosely adhered film of iron phosphate - FePO₄. The Cathodic inhibitor is zinc - Zn. As well, the zinc will sequester the manganese, which is currently causing fouling problems, so the problems with the manganese deposition will be significantly reduced.

PRODUCT:

Please see the Product Bulletin attached for the Inhibitor, which describes the inhibitor in detail. The product is available in both drums and 1136 kg semi - bulk tanks. I suggest, you obtain the product in these semi-bulk tanks. We have also attached product facts and its MSDS for your review.

PRICING:

The dosage is 4 ppm, based on the flow of the water. At an estimated flow rate of 600 imperial gallons per minute for 24-hrs per day, 365 days per year, the consumption of the Flogard POT6101 is 7970 kgs per year.

The price of the Flogard POT6101 in these semi-bulk tanks is \$3.85/ kg FCB Pointe Claire, QC. Freight and taxes extra. Therefore, the annual cost of the chemical would be \$30,685. If the facility is run less than 100% of the time, then the consumption will be less - directly proportional to operating hours.

REFERENCES:

BetzDearborn currently treats many similar applications to yours in Atlantic Canada. References include:

Contacts:

Mr. Bob Cass Manager of Water and Wastewater City of Port Hawkesbury Phone: 902-435-1494 Mr. Herve Richard Chief Engineer Noranda Inc. Brunswick Mines Phone: 506-546-6671

Mr. Pat Bellemare
Senior Operator
City of Dartmouth
Phone: 902-435-8300

WORK PLAN / SERVICE:

You should have on-site help from your chemical supplier to implement and monitor this chemical program, particularly since the references above needed to have the chemical introduced at a low concentration, which was gradually increased over several months.

As part of this proposal, we are offering as part of our service, 2-3 days of on-site service during start-up, followed by monthly visits for the first six months of the program and then twice yearly visits thereafter. This service is important. If the program is to succeed, operators need to be familiarized with testing procedures, corrosion coupon installation / changeout, the associated piping racks, chemical dosing pumps and chemical injection procedures and drawdowns. Site visits will be followed up by a written service report by BetzDearborn.

CHEMICAL FEED EQUIPMENT:

We have identified a chemical injection system, with a remote start / stop that would be suitable for this application (see the diagram attached). Prominant Fluid Controls can supply a dual metering pump skid, which can be automized to operate according to our needs. Options include:

- Duty and standby injection pumps.
- Flow switch to provide alarm-if-there is loss of chemical injection.
- Automatic switch over to stand-by pump in the event of duty pump failure.

The attached literature describes the Prominent options and provides a discussion matrix to select the chemical injection system to meet your application needs. We would be pleased to assist in selecting this system with Prominent. Budgetary cost for such a system would be \$5000.

CHEMICAL TESTING:

We suggest, you obtain a simple chemical test so that the operators can check the chemical concentration of PO_4 injected into the water. These chemical tests are straight forward and easy to use. Hach sells a simple PO_4 test (catalogue No. 2248-00), they are available from Atlantic Purification systems at 902-469-2806 and cost \$141.33 for a kit with 100 tests.

We will provide any instructions necessary for the operators to run this test. By using this test, we will unsure that the correct concentration of inhibitor is injected into the water.

CORROSION COUPONS:

As you are probably aware, corrosion coupons offer a method to quantitatively measure any reduction in the rate of corrosion over time. Coupons consist of a small strip of metal (either copper or mild steel) that measures approximately 50 x 10 x 5 mm and is inserted directly into the cooling water and left there for some time - typically 100 days. The coupons are then replaced and sent to the lab, where surface corrosion is noted. The weights before and after the in-service period are used to calculate a rate of corrosion in mil/year or g/ft² removed per year. Thus, the effectiveness of any corrosion reduction program can be evaluated quantitatively.

To ensure the results are reliable, the coupons must be installed properly and exposed to the correct flow rate. We recommend installation of a 1" diameter, iron corrision rack, with flow control valve, Part No. 2029978. The cost of this unit is \$515.

Do not hesitate to contact me at 709-596-3100, if you would like to discuss our proposal.

Yours truly,

BetzDearborn

Edward Finn

District Representative

Edward Finn

Cc: Shane White Phil Millard Yves Lefebvre

Enc.



Product Facts

FLOGARD™ POT6101 Potable Water Treatment

- NSF Approved for potable water
- Single-product liquid treatment
- Highly effective inhibitor

DESCRIPTION AND USE

FLOGARD™ POT6101 is a liquid blend of phosphate and zinc designed to inhibit corrosion of mild steel in mill supply water systems and once-through cooling systems. Corrosion control is accomplished by two mechanisms. At typical use levels, the major protection is due to the formation of a zinc-phosphate barrier film at the cathodic site of the corrosion cell. Phosphate also provides some additional corrosion protection by promoting the formation of a protective film at the anodic sites.

TREATMENT AND FEEDING REQUIREMENTS

The optimum dosage of FLOGARD POT6101 is a function of the corrosivity of the water to be treated and other conditions particular to a given installation. For best performance, this product should be fed continuously. While the typical feedrate is 4 - 20 ppm, this product is to be used in accordance with control procedures BetzDearborn establishes for a specific application and local potable water guidelines.

FLOGARD POT6101 may be fed directly from the shipping container or diluted to any convenient strength.

Tanks, pumps, piping and valves may be made of 316 stainless steel or most common plastics. Avoid the use of mild steel and copper alloys.

GENERAL PROPERTIES

Physical properties of FLOGARD POT6101 are shown on the Material Safety Data Sheet, a copy of which is available upon request.

PACKAGING INFORMATION

FLOGARD POT6101 is a liquid blend available in a variety of containers and delivery methods. Contact your BetzDearborn representative for details.

STORAGE

Protect from freezing. If this product is frozen during shipment or storage, slight mixing may be required to ensure homogeneity.

SAFETY PRECAUTIONS

A Material Safety Data Sheet containing detailed information about this product is available upon request.

BetzDearborn
Shaping the Future of Water & Process Treatment

www.betzdearborn.com



ISSUE DATE: 16-JAN-2001

MATERIAL SAFETY DATA SHEET

BetzDearborn Canada, Inc.*
3451 Erindale Station Road
Mississauga, ON L5C 2S9

Business telephone: (905) 279-2222

EMERGENCY TELEPHONE (HEALTH/ACCIDENT) (800) 963-5222 (Canada)

HMIS RATINGS

(See Section 16 for additional information)

HEALTH: 3 FLAMMABILITY: 0

REACTIVITY: 0

*Hercules Canada, Inc. and BetzDearborn Canada, Inc. carrying on business as Hercules Canada

1 PRODUCT IDENTIFICATION

PRODUCT NAME:

FLOGARD POT6101

PRODUCT APPLICATION AREA:

CORROSION INHIBITOR.

2 COMPOSITION / INFORMATION ON INGREDIENTS

Information for specific product ingredients as required by the WHMIS Regulations is listed. Refer to additional sections of this MSDS for our assessment of the potential hazards of this formulation.

HAZARDOUS INGREDIENTS:

Cas# Chemical Name Range(w/w%)

7664-38-2 PHOSPHORIC ACID 15-40

Corrosive

ORAL LD50-RAT: 1,530 MG/KG DERMAL LD50-RABBIT: 2,740 MG/KG

INHL. LC50: NO DATA.

7733-02-0 ZINC SULFATE 15-40

Severe irritant; potential reproductive toxin

ORAL LD50-RAT: 2,949 MG/KG

DERMAL LD50: NO DATA. INHL. LC50: NO DATA.

No component is considered to be a carcinogen by the U.S. National Toxicology Program (NTP), the International Agency for Research on Cancer (IARC) or under WHMIS.

3 HAZARDS IDENTIFICATION

EMERGENCY OVERVIEW

Severe irritant to the skin. Corrosive to the eyes. Mists/aerosols cause irritation to the upper respiratory tract.

Odor: None; Appearance: Colorless, Liquid

Fire fighters should wear positive pressure self-contained breathing apparatus(full face-piece type). Proper fire-extinguishing media: dry chemical, carbon dioxide, foam or water

POTENTIAL HEALTH EFFECTS

ACUTE SKIN EFFECTS:

Primary route of exposure; Severe irritant to the skin.

ACUTE EYE EFFECTS:

Corrosive to the eyes.

ACUTE RESPIRATORY EFFECTS:

Primary route of exposure; Mists/aerosols cause irritation to the upper respiratory tract.

INGESTION EFFECTS:

May cause severe gastrointestinal irritation.

TARGET ORGANS:

Prolonged or repeated exposures may cause tissue necrosis. Product or product component may cause reproductive toxicity at maternal toxic levels (based on animal testing).

MEDICAL CONDITIONS AGGRAVATED:

Not known.

SYMPTOMS OF EXPOSURE:

Inhalation of vapors/mists/aerosols may cause eye, nose, throat and lung irritation. Skin contact may cause severe irritation or burns.

4 FIRST AID MEASURES

SKIN CONTACT:

Wash thoroughly with soap and water. Remove contaminated clothing. Thoroughly wash clothing before reuse. Get medical attention if irritation develops or persists.

EYE CONTACT:

URGENT! Immediately flush eyes with plenty of low-pressure water for at least 20 minutes while removing contact lenses. Hold eyelids apart. Get immediate medical attention.

INHALATION:

Remove to fresh air. If breathing is difficult, give oxygen. If breathing has stopped, give artificial respiration. Get immediate

medical attention.

INGESTION:

Do not feed anything by mouth to an unconscious or convulsive victim. Do not induce vomiting. Immediately contact physician. Dilute contents of stomach using 3-4 glasses milk or water.

NOTES TO PHYSICIANS:

No special instructions

5 FIRE FIGHTING MEASURES

FIRE FIGHTING INSTRUCTIONS:

Fire fighters should wear positive pressure self-contained breathing apparatus (full face-piece type).

EXTINGUISHING MEDIA:

dry chemical, carbon dioxide, foam or water

HAZARDOUS DECOMPOSITION PRODUCTS:

Thermal decomposition (destructive fires) yields elemental oxides.

FLASH POINT:

> 200F > 93C P-M(CC)

6 ACCIDENTAL RELEASE MEASURES

PROTECTION AND SPILL CONTAINMENT:

Ventilate area. Use specified protective equipment. Contain and absorb on absorbent material. Place in waste disposal container. Flush area with water. Wet area may be slippery. Spread sand/grit.

DISPOSAL INSTRUCTIONS:

The waste characteristics of the absorbed material, or any contaminated soil, should be determined in accordance with provincial regulations. Water contaminated with this product may be sent to a sanitary sewer treatment facility, in accordance with any local agreement or discharged under provincial regulations. Incinerate or land dispose in an approved landfill.

7 HANDLING & STORAGE

HANDLING:

Acidic. Corrosive (Metal). Do not mix with alkaline material.

STORAGE:

Keep containers closed when not in use. Use approved containers only. Store in cool, well-vented area. Contact with metals may release flammable hydrogen gas.

8 EXPOSURE CONTROLS / PERSONAL PROTECTION

EXPOSURE LIMITS

Consult local authorities for acceptable provincial values.

CHEMICAL NAME

PHOSPHORIC ACID

PEL (OSHA): 1 MG/M3 TLV (ACGIH): 1 MG/M3

ZINC SULFATE

PEL (OSHA): NOT DETERMINED TLV (ACGIH): NOT DETERMINED

ENGINEERING CONTROLS:

Adequate ventilation to maintain air contaminants below exposure limits.

RESPIRATORY PROTECTION:

If air-purifying respirator use is appropriate, use a respirator with dust/mist filters.

SKIN PROTECTION:

rubber gloves-- Wash off after each use. Replace as necessary.

EYE PROTECTION:

splash proof chemical goggles

9 PHYSICAL & CHEMICAL PROPERTIES

Specific Grav. (70F, 21C) 1.398	Vapor Pressure (mmHG)	~ 18.0
Freeze Point (F) -13	Vapor Density (air=1)	< 1.00
Freeze Point (C) -25		
Viscosity(cps 70F,21C) 10	<pre>% Solubility (water)</pre>	100.0

Odor		None
Appearance		Colorless
Physical State		Liquid
Flash Point	P-M(CC)	> 200F > 93C
pH-As Is (approx.)		1.4
Evaporation Rate (Ether=1)	< 1.00

NA = not applicable ND = not determined

10 STABILITY & REACTIVITY

STABILITY:

Stable under normal storage conditions.

HAZARDOUS POLYMERIZATION:

Will not occur.

INCOMPATIBILITIES:

May react with strong oxidizers.

DECOMPOSITION PRODUCTS:

Thermal decomposition (destructive fires) yields elemental oxides.

BETZDEARBORN INTERNAL PUMPOUT/CLEANOUT CATEGORIES:
"B"

11 TOXICOLOGICAL INFORMATION

Oral LD50 RAT: >2,000 mg/kg

NOTE - Estimated value

Dermal LD50 RABBIT: >2,000 mg/kg

NOTE - Estimated value

12 ECOLOGICAL INFORMATION

AQUATIC TOXICOLOGY

Rainbow Trout 96 Hour Static Acute Bioassay

LC50: 21.3 mg/L

No Effect Level: 15.5 mg/L

Daphnia magna 48 Hour Static Acute Bioassay proposition

LC50: 3.8 mg/L

No Effect Level: 3.2 mg/L

Fathead Minnow 96 Hour Acute Toxicity

Product toxicity determined from bioassays conducted on individual components.

LC50: 16 mg/L

No Effect Level: 6.3 mg/L

BIODEGRADATION

No Data Available.

13 DISPOSAL CONSIDERATIONS

Incinerate or bury in approved landfill. Please be advised that there may be additional local or provincial requirements relating to the disposal of waste. Consult provincial and local regulations regarding the proper disposal of this material.

14 TRANSPORT INFORMATION

Transportation of Dangerous Goods:

Proper Shipping Name: Corrosive Liquids, n.o.s.

(Phosphoric Acid)

PIN: UN1760; Classification: 8(9.2); Packing Group: III

15 REGULATORY INFORMATION

This product has been classified in accordance with the hazard criteria of the CPR and the MSDS contains all the information required by the CPR. CEPA:

All components of this product comply with substance notification requirements under CEPA.

WHMIS CLASSIFICATION:

D2A D2B

FOOD AND DRUG ADMINISTRATION:

The ingredients in this product are Generally Recognized As Safe by FDA for direct addition to human food.

16 OTHER INFORMATION

NFPA/HMIS		CODE TRANSLATION
Health	3	Serious Hazard
Fire	0	Minimal Hazard
Reactivity	0	Minimal Hazard
Special	CORR	DOT corrosive
(1) Protective Equipment	В	Goggles,Gloves
		•

⁽¹⁾ refer to section 8 of MSDS for additional protective equipment recommendations.

CHANGE LOG

	EFFECTIVE		
	DATE	REVISIONS TO SECTION:	SUPERCEDES
MSDS status:	22-MAY-1998		** NEW **
	09-DEC-1998	15	22-MAY-1998
	23-MAR-2000	15	09-DEC-1998
	07-APR-2000	4	23-MAR-2000
	14-JUL-2000	15	07-APR-2000
	16-JAN-2001	14	14-JUL-2000

Prepared by the Regulatory Affairs Group, BetzDearborn Canada, Inc. Telephone: 1(905)279-2222 Date of preparation: 16-JAN-2001



Corrosion Test Coupon Racks

BetzDearborn Corrosion Test Coupon Racks provide a convenient means of monitoring the progress of corrosion in systems such as boilers, condensate lines, open recirculating cooling water, closed circulating hot or chilled water systems, etc. The corrosion test rack creates a side stream off the main system in which corrosion test coupons can be exposed to system water under controlled and reproducible conditions.

The corrosion coupons can be periodically removed and either visually examined or returned to the laboratory for determination of weight loss, corrosion rate. and pitting severity.

BLACK IRON CORROSION RACK

The Black Iron Corrosion Rack is recommended for corrosion monitoring in high temperature and/or highpressure installations such as steam condensate, high temperature water, hydronic heating, recirculating process systems, etc. The Black Iron Rack is constructed of 1" threaded black iron pipe. It is supplied with four 1" MNPT steel mounting plugs, and one 10 gpm Dole™ flow control valve. Caution: Maximum pressure & temperature are limited by the Dole flow control valve.

Maximum Pressure: 200 psig (13.8 bar) Maximum Temperature: 160° F (71° C)

PVC CORROSION RACK

The PVC Corrosion Rack is recommended for corrosion monitoring in low temperature systems such as open recirculating cooling water systems, chilled

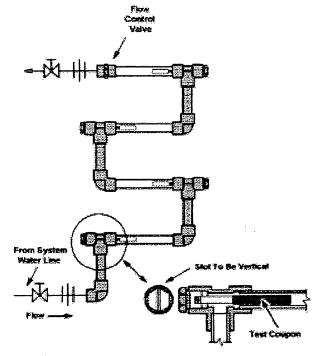


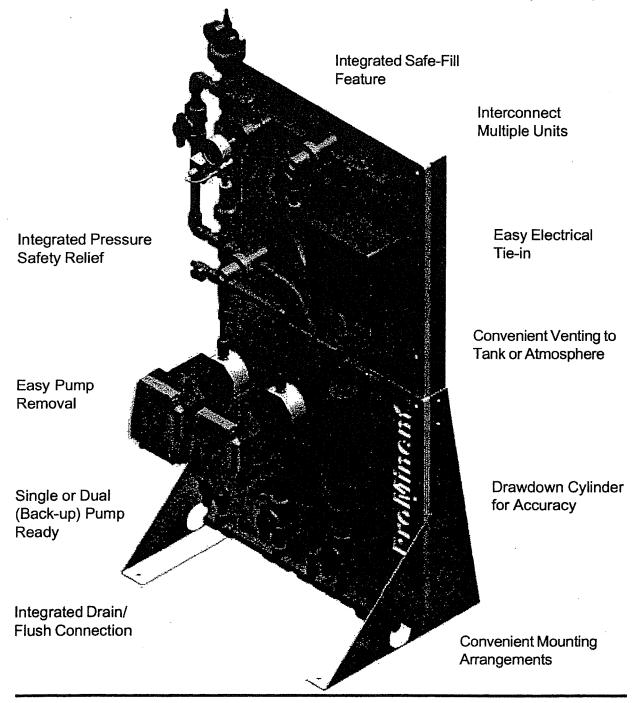
Figure 1

water, process water systems, etc. The PVC Rack is constructed of 1" threaded Sched. 80 PVC pipe. It is supplied with four 1" PVC mounting plugs and an 8 gpm Dole™ flow control valve. Two designs are available. One is constructed of all gray, opaque PVC. The other features transparent pipe sections for viewing the test coupons in place. See Figures 1 & 2. To discourage algae growth in the transparent sections, opaque snap-on pipe covering is supplied with this corrosion rack.

FLOW RATE	VE	LOCITY
	1" PVC Rack	1" Black Iron Rack
5 gpm	2.2 ft/sec (0.67 m/sec)	1.9 ft/sec (0.58 m/sec)
8 gpm	3.6 ft/sec (1.1 m/sec)	3.0 ft/sec (0.91 m/sec)
10 gpm	4.5 ft/sec (1.4 m/sec)	3.7 ft/sec (1.3 m/sec)
12 gpm	5.4 ft/sec (1.6 m/sec)	4.4 ft/sec (1.4 m/sec)

MODULAR DOSING SYSTEM... **Function by Design**

Offering industry a new standard in convenience, safety, and reliability. ProMinent's new modular design concept allows custom-tailored arrangements to suit your immediate needs. Matched with our exceptional line of chemical metering pumps - the functionality, flexibility, and performance you demand is yours today - all this at an industry-valued price.



ProMinent Fluid Controls Ltd. 490 Southgate Drive, Guelph, Ontario, N1G 4P5 ProMinent Fluid Controls, Inc. 136 Industry Drive, Pittsburgh, PA, 15275-1014

phone: 519-836-5692 fax: 519-836-5226 phone: 412-787-2484

fax: 412-787-0704

MODULAR SELECTION... As Easy as 1-2-3

STEP ONE: Select Pump

Using Prominent's comprehensive catalog determine the pump capacity and pressure you require. Up to 2 pumps may be incorporated into a single package - dual pumps offer redundent function and convenience for continous dosing. You may choose any of ProMinent's line of compact Solenoid-driven metering pumps - Concept, Beta, Gamma, Gala in most sizes and materials.

STEP TWO: Select Modules

Two modules are currently available. The Suction Module includes provision for up to 2 pumps - 1 primary, the other a backup. A calibration column for setting the pump for optimum performance, and all manual control valves required to isolate and service the system easily. The Discharge Module comes standard with integrated safety relief valve, our "Safe-Fill" feature, dual function Priming/Bleed valve and all necessary isolation valves. Just add any or all of the options below for added functionality and performance...

STEP THREE Select Options and Accessories

Select from a handful of safety and performance enhancements like...

- Pressure Gauge/Seal to accurately tune your system for the best results.
- Pulsation Dampener to improve flow characteristics and repeatability.
- Back Pressure Valve for better pump performance under variable conditions.
- Flow Monitor for flow confirmation.

above each letter location.

- Convenient junction box for all system wiring.
- Mounting arrangement wall-mount is standard, or you may choose floor stands or tote mount hanging brackets.

DEF-GHI-A B C J KL-М MOD В C Material Of Construction I/O Connection Size / Type Elastomer EPDM Schedule 80 PVC 1/2" FNPT FPM (Viton) G K D Flow Monitor Option Suction Module Discharge Module Wall-mount Module with Back Panel Not Applicable Not Applicable includes Pump Shelf (1), Calibration Wall-mount Module with Back Panel Type 1 or 2 Flow Monitor (1), and and "Safe-Fill" feature includes PRV Pipe & Fittings Column (1), Ball Valves (3), and (1), Ball Valves (3), and Pipe & Type 3 Flow Monitor (1) with Bypass Pipe & Fittings includes Ball Valve (1) and Pipe & E Calibration Column Pressure Gauge & Seal Kit 100 mL **Back Panel Mount Option** Not Applicable 0 500 mL Kit includes Pressure Gauge with Not Applicable Multiply Pump Strokes per Minute integral Seal (1), and Pipe & Fittings Corrosion-resistant, Plastic Floor by Pump mL per Second for 60 sec. Mount drawdown Corrosion-resistant, Stainless Steel Pulsation Dampener Kit Tote Mount Not Applicable Backup Pump Mount Kit Kit includes Pulsation Dampener (1), and Pipe & Fittings Not Applicable M Junction Box Option Kit includes Pump Shelf (1), Ball Valve (1), and Pipe & Fittings Not Applicable Back Pressure Valve Kit Option includes Prewired JB (1) for Not Applicable Single Pump Circle each number that applies Kit includes BPV (1), and Pipe & Option includes Prewired JB (1) for **Fittings** Dual Pump to your configuration and enter

Viton® is a registered trademark of Dupont Dow Elastomers

Maximum Pressure: 200 psi at 70° F (13.8 bar at 21° C)

120 psi at 120° F (6.9 bar at 49° C)

70 psi at 140° F (4.8 bar at 60° C)

FLOW VS VELOCITY CHART

Velocities in **BOLD** indicate standard flow controller supplied with that rack. For other available Dole flow control valves, see Equipment Fact Sheet EF15-07.

OPTIONS

A Corrater™ probe may be installed in the corrosion rack to provide instantaneous corrosion readings to supplement the data provided by the weight loss corrosion coupons.

CORROSION TEST RACK INSTALLATION

- The Corrosion Test Rack may be assembled for vertical mounting as shown in Figure 1, or a horizontal position, Figure 2. Items shown in single line schematic are not furnished.
- Attach the corrosion rack to a wall or column.
 DO NOT suspend it from the supply and return piping alone.
- To avoid air binding, pipe the corrosion rack so that water will flow upward through it, and in such a way that it will remain full of water at all times and not backdrain when the main recirculating system shuts own.
- 4. Install gate or ball-type isolation valves of both sides of the rack.
- DO NOT use this bypass loop for any other purpose such as chemical injection, or mounting of conductivity or pH sensors.

- 6. For measurement of corrosion at points of highest temperature in the circulating system, the water supply to the corrosion rack should be from the exit of the heat exchanger(s). Average corrosion rate measurements may be obtained by supplying the corrosion rack with water from the main cooling tower riser, etc.
- Return water may be piped to the recirculating pump suction header, cooling tower basin, or other suitable point with sufficiently low pressure to insure flow through the rack.
- Flow velocities should not be variable. Avoid extremely high or low velocity conditions. A Dole™ or other suitable flow control valve is recommended to insure constant velocity.
- For PVC Test Racks with transparent viewing sections, install the slotted polyfoam pipe insulation over the transparent sections to discourage algae growth.

CORROSION TEST COUPON INSTALLATION

- Keep the metal test coupon in the special treated envelope BEFORE AND AFTER exposure.
- DO NOT leave fingerprints on the coupon. They will cause false corrosion readings.
- Attach the coupon to the mounting stud using the special nut and bolt provided.

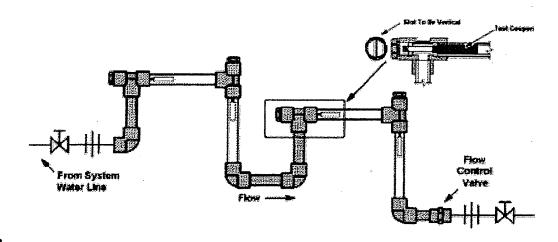


Figure 2

- 4. Corrosion coupons should always be installed so the water flow first over the plastic mounting rod and then over the coupon. Water flowing directly onto the coupon may cause erosion-corrosion and lead to false weight loss measurements.
- Use ONLY Teflon™ thread sealing tape on mounting plug threads. DO NOT use pipe dope.
- 6. The witness slot on the coupon mounting plug should be parallel with the flat surface of the corrosion test coupon. Install the mounting plug in the tee and align the witness slot (and coupon) in the VERTICAL position as shown in Figure 1.
- Note the date of installation on back of the white Tyvek™ Coupon Return Envelope (ENG 322) and retain both the Coupon Return Envelope and the treated brown envelope.
- 8. When removing, each test coupon should be carefully dismounted from the holder and immediately dried with a blast of hot air or blotted with a paper towel or clean rag. DO NOT CLEAN. Reinsert the coupon in the treated brown envelope in which it was received.
- Complete the back of the white Coupon Return Envelope, insert the treated brown envelopes with coupons inside, and return the envelope with the coupons to the Woodlands laboratory.

Part Numbers

2013971 Corrosion Rack, PVC, 1" NPT, w/ 4 coupon holders & 8 gpm flow control valve.

2042205 Corrosion Rack, PVC, 1" NPT w/ 4 coupon holders, 8 gpm valve and 4 TRANSPARENT viewing sections.

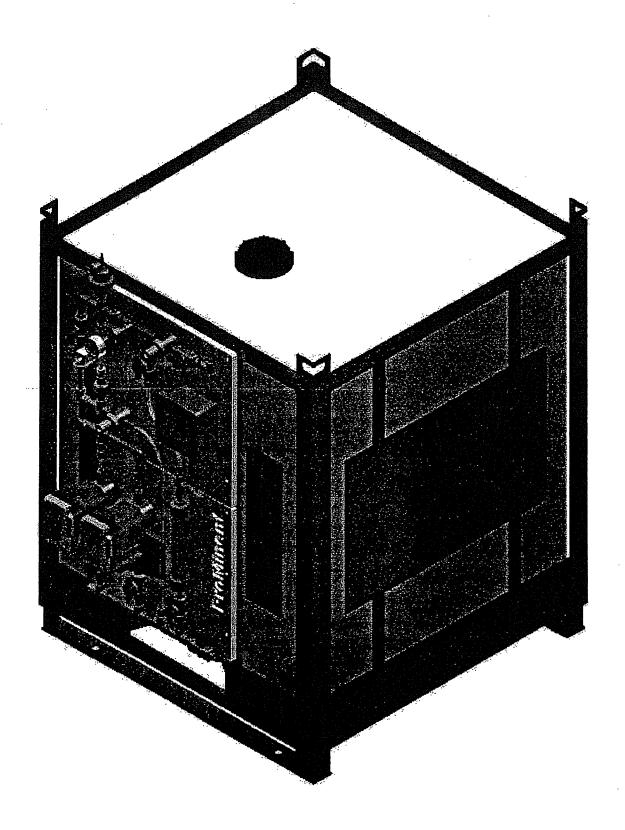
2029978 Corrosion Rack, Black Iron, 1" NPT, w/ 4 coupon holders & 10 gpm flow control valve.

2032806-Gorrosion-Rack, 304 SS, 1"-NPT, w/ 4 coupon holders.

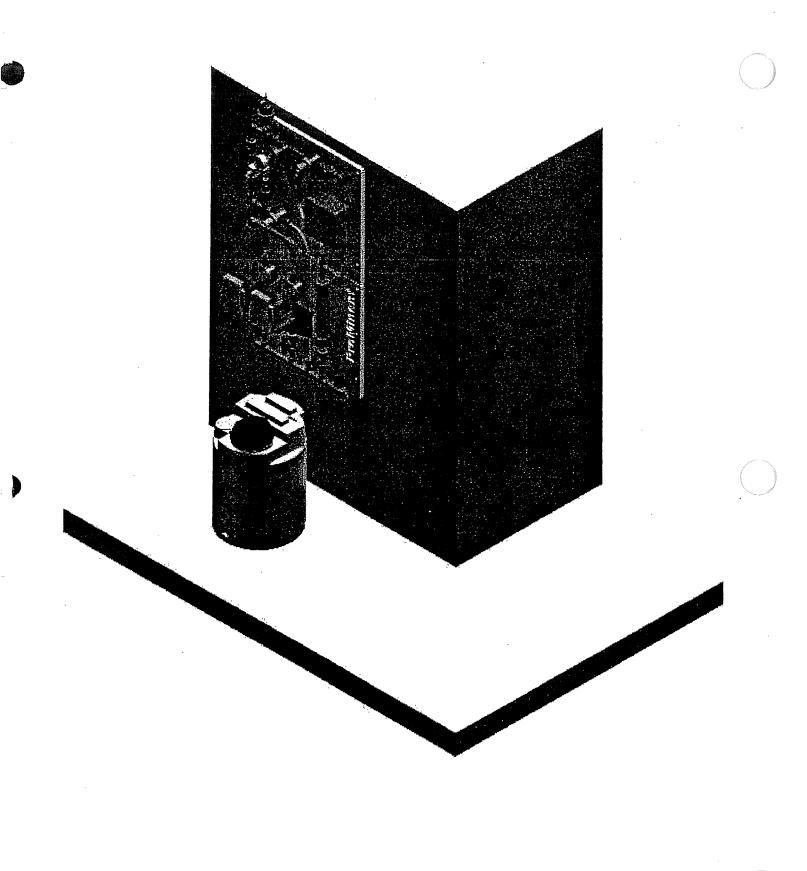
2015850 Replacement Coupon Holder, 1" PVC w/ 6" stem.

2041977 Replacement Coupon Holder, 1" Black Iron w/ 6" Teflon™ Stem and Teflon nut & Screw

Corrosion test coupons and mounting screws are not supplied with the corrosion rack and must be ordered separately from the BetzDearborn Woodlands, TX laboratory.



(



APPENDIX D

CAT ARM

Flushing Service Water Heat Exchangers Online

General

Flush each unit individually at a 50 MW load. Use the data chart on the following page to record the necessary readings (marked with an asterisk) before, during, and after flushing the service water heat exchangers. During flushing the stator temperatures will be monitored at all times to prevent over heating. If stator temperatures rise to alarm conditions during flushing reroute service water through SAC to cool the unit.

Procedure

All heat exchangers will be flushed on each unit, starting with the turbine guide cooler and generator guide/thrust bearing coolers being flushed together, and then the Surface Air Coolers (SAC) being flushed individually. Record all necessary readings before flushing. Fully open the Pressure Reducing Valve (Unit #1 V-04-38, Unit #2 V-04-50) on the inlet header to the unit to begin the flushing procedure.

1) Flushing turbine and generator bearing coolers

Place the temperature control valve in the full open position (Unit #1 V-04-29, Unit #2 V-04-86) and also open the isolation valve for the by-pass discharge line (Unit #1 V-04-31, Unit #2 V-04-88). Make sure turbine isolation discharge valve (Unit #1 V-04-54, Unit #2 V-04-62) and generator isolation discharge valve (Unit #1 V-04-53, Unit #2 V-04-61) are in the full open position. Manually throttle SAC inlet header isolation valve to 30% normal flow (7.8 l/s) (Unit #1 V-04-115, Unit #2 V-04-116), this valves normal operating position is full open. Flush turbine and generator bearing coolers for 10 minutes and record readings half way through these coolers during flushing as per the data chart. After flushing return SAC inlet header isolation valve to full open, then close the isolation valve for the by-pass discharge line, then return service water temperature control valve to normal operating position, and finally record readings through these coolers as per the data chart.

2) Flushing Surface Air Coolers

Place the temperature control valve in the full open position (Unit #1 V-04-45, Unit #2 V-04-56) and also open the isolation valve for the by-pass discharge line (Unit #1 V-04-47, Unit #2 V-04-58). Flush SAC by isolating three coolers and allowing all service water to flow through the remaining cooler. Flush the SAC in the following order starting with cooler #2, #3, #1, and #4. Record readings through these coolers during flushing as per the data chart. Flush each cooler for 10 minutes. After flushing all SAC open all cooler isolation valves, then close the isolation valve for the by-pass discharge line, then return service water temperature control valve to normal operating position, and finally record readings through the coolers as per the data chart.

Flushing F

ure data

Cat Arm Readings	Before	During Flushing	After Flushing	Durin	g Flushing S	urface Air C	oolers	After Flushing
Unit #1	Flushing	Gen & Turb	Gen & Turb	#1	#2	#3	#4	SAC
				BENGANA BENGALAK	agains which will a		PRINCIPLE DESCRIPTION	B TO CONTROL OF THE PARTY OF THE
Inlet water pressure	*	*	*	*	*	*	*	*
SAC Air inlet temp	*					*		*
SAC Air outlet temp	*					*		*
Stator A temp	*	*	*	*	*	*	*	*
Stator B temp	*	*	*	*	*	*	*	*
Stator C temp	*	*	*	*	*	*	*	*
Water inlet temp	*	*	*	*	*	*	*	*
SAC water outlet temp	*	*	*	*	*	*	*	*
Gen brg water outlet temp	*	*	*					
Turb brg water outlet temp	*	*	*					
Gen brg oil temp	*	*	*					
Turb brg oil temp	*	*	*					
SAC flow rate	*	*	*	*	*	*	*	*
Gen brg flow rate	*	*	*	*	*	*	*	*
Turb brg flow rate	*	*	*	*	*	*	*	*

Flushing Procedure data

Cat Arm Readings	Before	During Flushing	After Flushing	Durin	g Flushing S	urface Air C	oolers	After Flushing
Unit #2	Flushing	Gen & Turb	Gen & Turb	#1	#2	#3	#4	SAC
Inlet water pressure	*	*	*	*		*		*
SAC Air inlet temp	*					*		*
SAC Air outlet temp	*					*		*
Stator A temp	*	*	*	*	*	*	*	*
Stator B temp	*	*	*	*	*	*	*	*
Stator C temp	*	*	*	*	*	*	*	*
Water inlet temp	*	*	*	*	*	*	*	*
SAC water outlet temp	*	*	*	*	*	*	*	*
Gen brg water outlet temp	*	*	*					
Turb brg water outlet temp	*	*	*					
Gen brg oil temp	*	*	*					
Turb brg oil temp	*	*	*					
SAC flow rate	*	*	*	*	*	*	*	*
Gen brg flow rate	*	*	*	*	*	*	*	*
Turb brg flow rate	* .	*	*	*	*	*	*	*

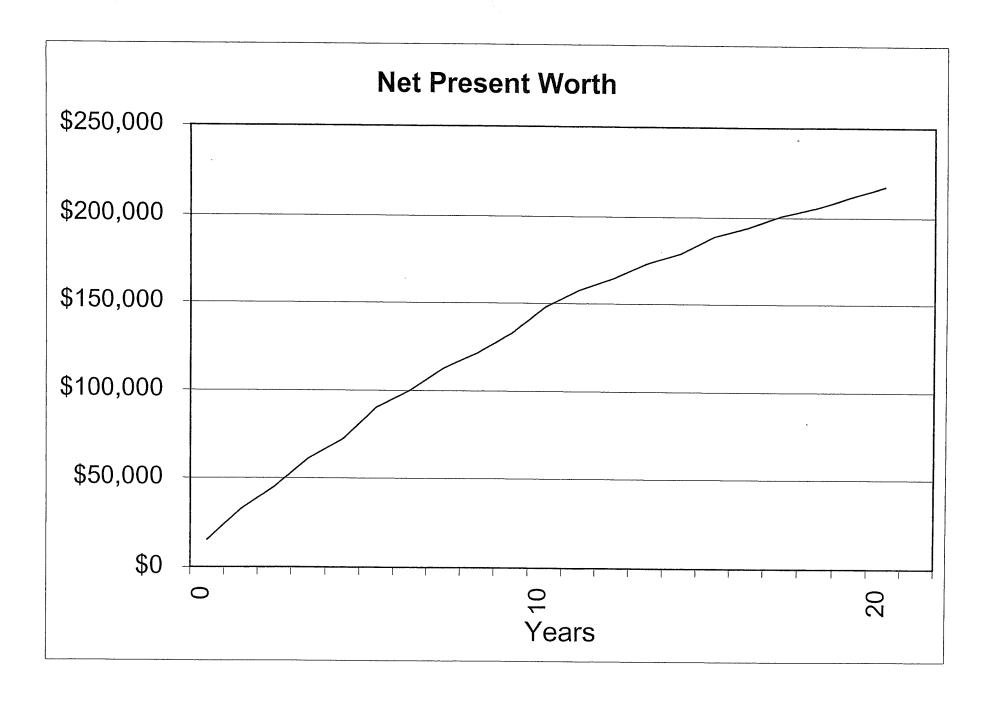
APPENDIX E

DO NOTHING (Per Unit)

Capital Cost	
Total	C

Operating Cost	
Pump consumption (49 weeks)	15,353
Clean SAC (2 yr)	5,783
Clean SAC Piping (10 yr)	4,667
Clean Gen Brg Coolers (5 yr)	5,783
Clean Gen Brg Cooler Piping (10 yr)	4,667

	Year	Cash Flow	NPW
0	2002	\$15,353	\$15,353
1	2003	\$21,559	\$32,463
2	2004	\$15,973	\$44,969
3	2005	\$22,430	\$61,154
4	2006	\$16,619	\$72,206
5	2007	\$29,721	\$90,423
6	2008	\$17,290	\$100,191
7	2009	\$24,279	\$112,832
8	2010	\$17,988	\$121,464
9	2011	\$25,259	\$132,636
10	2012	\$37,143	\$147,777
11	2013	\$26,280	\$157,650
12	2014	\$19,471	\$164,392
13	2015	\$27,342	\$173,118
14	2016	\$20,258	\$179,077
15	2017	\$36,229	\$188,899
16	2018	\$21,076	\$194,165
17	2019	\$29,596	\$200,980
18	2020	\$21,928	\$205,634
19	2021	\$30,791	\$211,657
20	2022	\$31,407	\$217,320

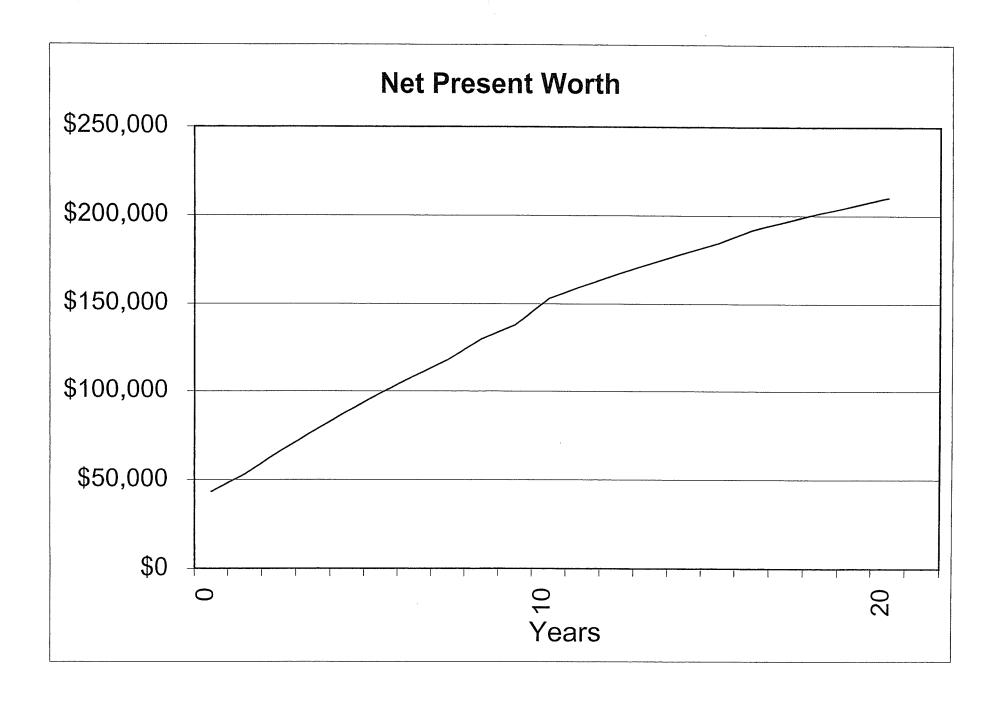


REPLACE PIPING (per Unit)

Capital Cost	
Gen Brg Piping (Parts & Installation)	8,229
Inlet Piping (Parts & Installation)	8,378
Discharge Piping (Parts & Installation)	11,303
Total	27,910

Operating Cost	
Pump consumption (49 weeks)	15,353
Clean SAC (8 yr)	5,783
Clean SAC Piping (10 yr)	4,667
Clean Gen Brg Coolers (10 yr)	5,783
Clean Gen Brg Cooler Piping (10 yr)	4,667

	Year	Cash Flow	NPW
0	2002	\$43,263	\$43,263
1	2003	\$15,660	\$53,176
2	2004	\$15,973	\$65,682
3	2005	\$16,293	\$77,438
4	2006	\$16,619	\$88,490
5	2007	\$16,951	\$98,880
6	2008	\$17,290	\$108,648
7	2009	\$17,636	\$117,830
8	2010	\$24,764	\$129,714
9	2011	\$18,348	\$137,829
10	2012	\$37,143	\$152,970
11	2013	\$19,090	\$160,142
12	2014	\$19,471	\$166,884
13	2015	\$19,861	\$173,223
14	2016	\$20,258	\$179,181
15	2017	\$20,663	\$184,783
16	2018	\$29,015	\$192,033
17	2019	\$21,498	\$196,983
18	2020	\$21,928	\$201,637
19	2021	\$22,366	\$206,013
20	2022	\$22,814	\$210,126

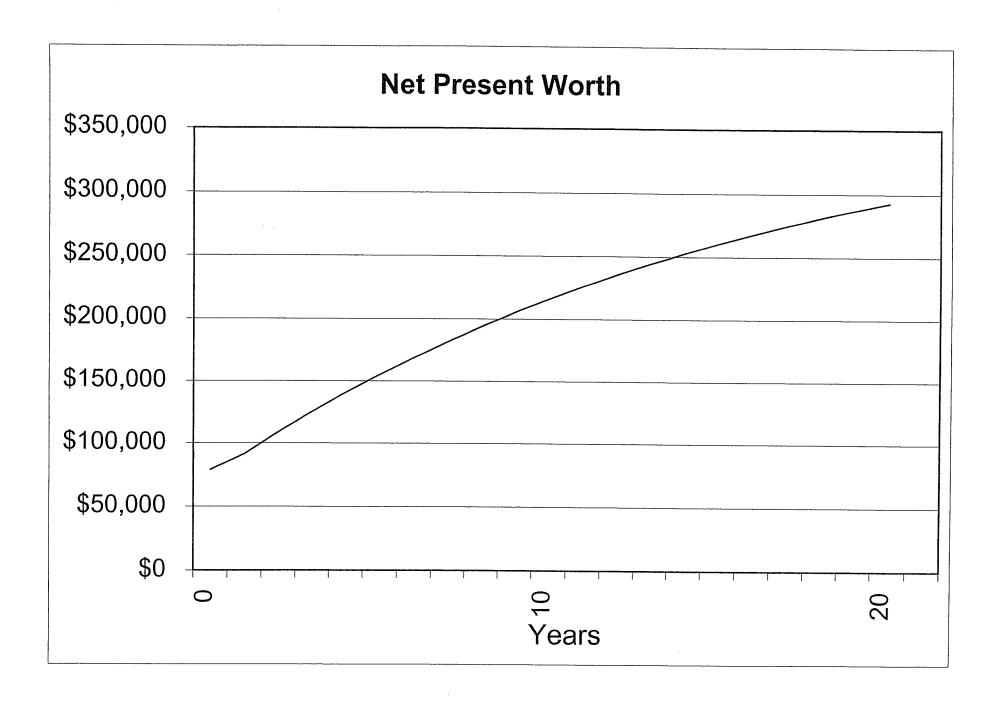


CLOSED LOOP SYSTEM (Two Units)

Capital Cost	
Pump	\$14,404
Heat Exchanger	\$35,000
Installation Piping & Hardware	\$8,000
Total	\$57,404

Operating Cost	
Pump consumption (49 weeks)	\$15,353
Recir Pump Consumption (49 weeks)	\$6,133
,	

	Year	Cash Flow	NPW
0	2002	\$78,890	\$78,890
1	2003	\$21,916	\$91,326
2	2004	\$22,354	\$108,827
3	2005	\$22,801	\$125,279
4	2006	\$23,257	\$140,746
5	2007	\$23,722	\$155,287
6	2008	\$24,197	\$168,956
7	2009	\$24,680	\$181,806
8	2010	\$25,174	\$193,887
9	2011	\$25,678	\$205,244
10	2012	\$26,191	\$215,920
11	2013	\$26,715	\$225,957
12	2014	\$27,249	\$235,393
13	2015	\$27,794	\$244,263
14	2016	\$28,350	\$252,602
15	2017	\$28,917	\$260,441
16	2018	\$29,495	\$267,811
17	2019	\$30,085	\$274,739
18	2020	\$30,687	\$281,252
19	2021	\$31,301	\$287,375
20	2022	\$31,927	\$293,131

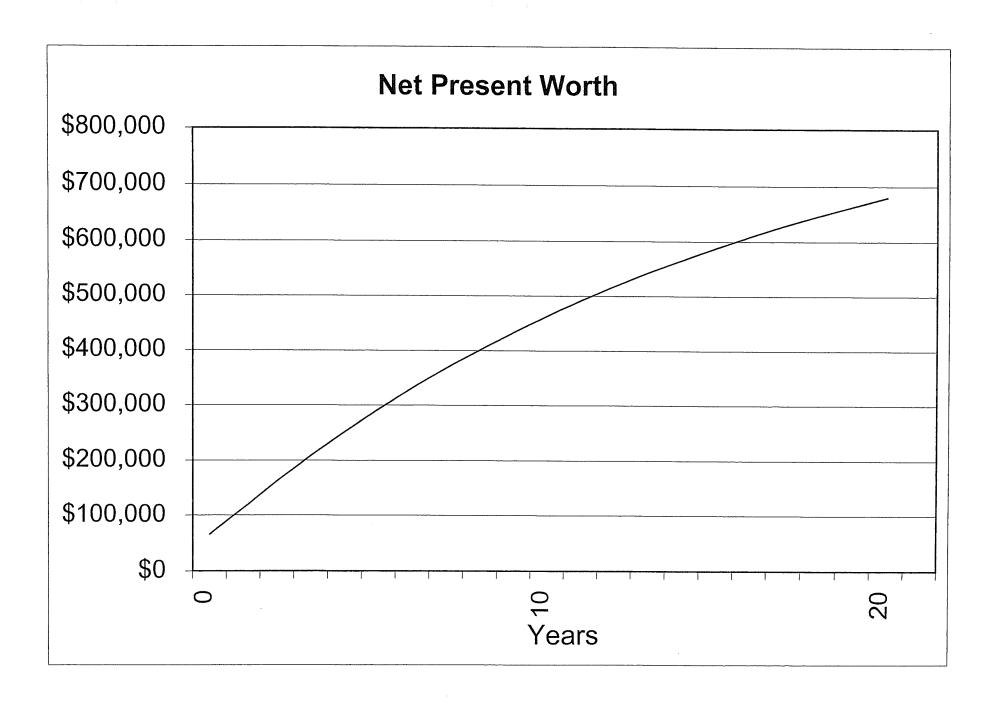


CHEMICAL INJECTION (Two Units)

Capital Cost	
Injection System	5,000
Test Coupon Rack	515
Total	5,515

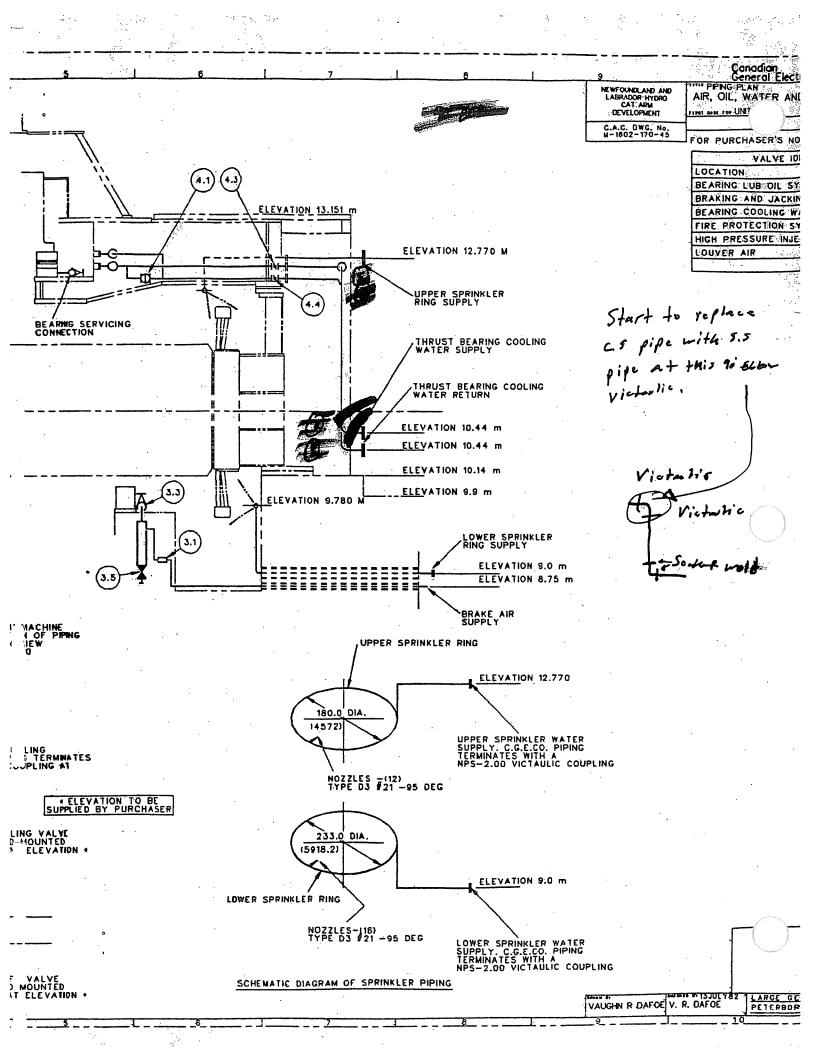
Operating Cost	
Pump consumption (49 weeks)	15,353
Chemical (49 weeks)	45,000

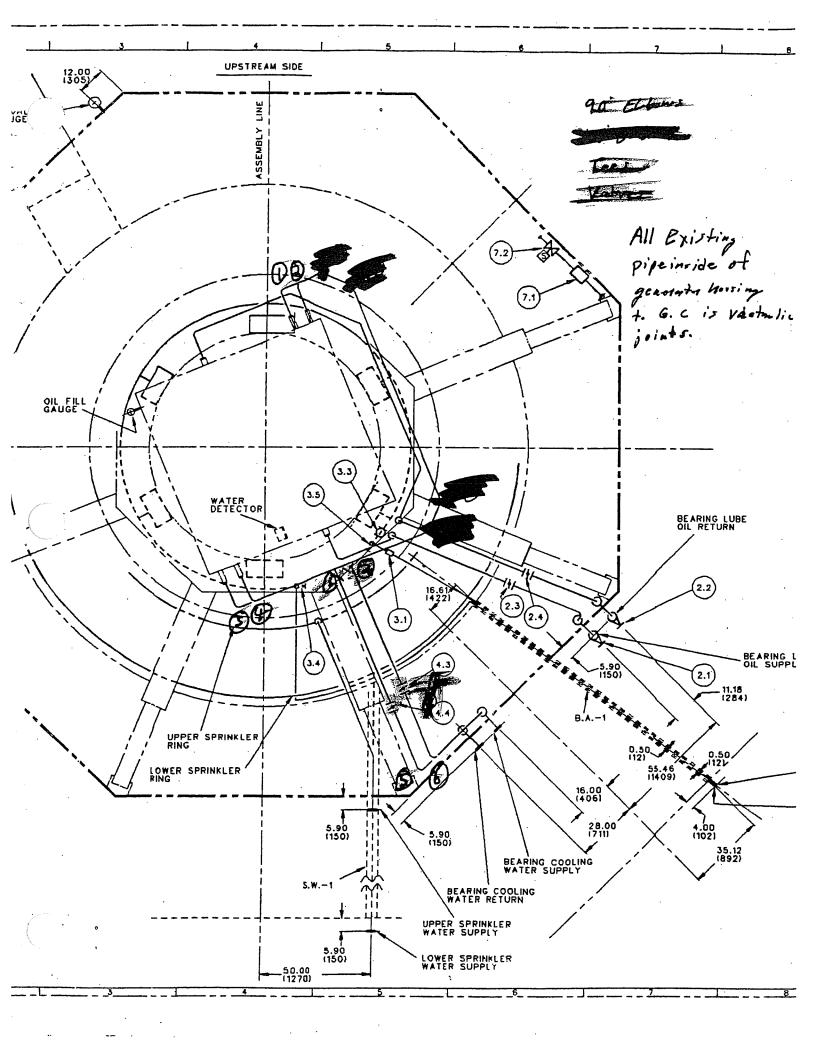
	Year	Cash Flow	NPW
0	2002	\$65,868	\$65,868
1	2003	\$61,560	\$113,000
2	2004	\$62,791	\$162,160
3	2005	\$64,047	\$208,375
4	2006	\$65,328	\$251,821
5	2007	\$66,635	\$292,664
6	2008	\$67,967	\$331,061
7	2009	\$69,327	\$367,157
8	2010	\$70,713	\$401,091
9	2011	\$72,127	\$432,992
10	2012	\$73,570	\$462,982
11	2013	\$75,041	\$491,175
12	2014	\$76,542	\$517,679
13	2015	\$78,073	\$542,595
14	2016	\$79,635	\$566,019
15	2017	\$81,227	\$588,039
16	2018	\$82,852	\$608,741
17	2019	\$84,509	\$628,202
18	2020	\$86,199	\$646,497
19	2021	\$87,923	\$663,696
20	2022	\$89,681	\$679,865

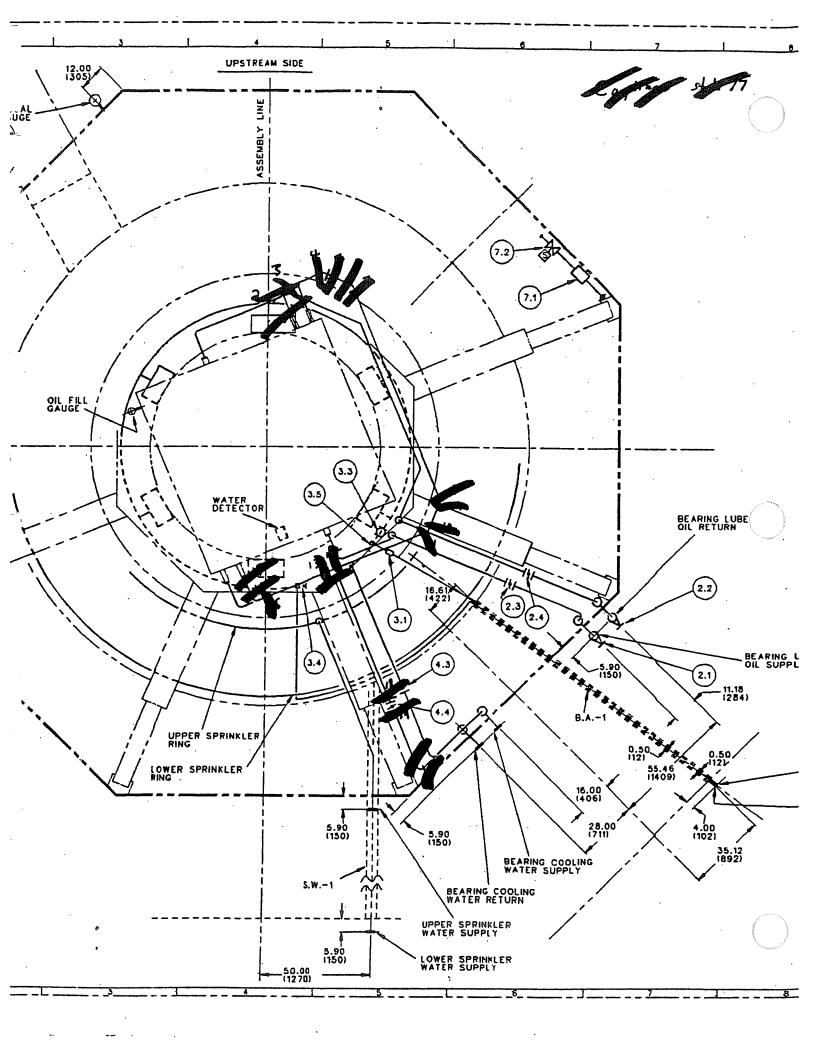


APPENDIX F

bour Costs, Cat				manusus magastus pagus a Segangay ng NGMBayana Segangang manusus magastuggang ng
n. Bry. Piping	(2")			
	and the second state of th			
Estimate		والمستعدد	Acti	isl
Poscription	Crew	day	Quantity.	day
Sch 10, black, 2"	IPLUM	43'	105'	2.44
90'445' Elbons, 2"	LPLVM	25	16	0.64
Tee, 2"	IPLVM	17	2	0.12
Coupling, 2"	IPLUM	50	46	0.92
Roll Groving, 2"	12	116	46	0.40
,				_
ine required f = 2.44 + 0.64 + +dd additional 1 = 4.12 x 0.75	0.12 + 0,92 work reduces	= 4.12 day	γs	Plum & l Apprentice
= 2.44 + 0.64 + +dd additional 1 = 4.12 × 0.75 +al Time requir	0.12 + 0,92 work reducer = 3.09 o	= 4.12 da, time by lays	257.	Plum & l'Apprentice
= 2.44 + 0.64 + +dd additional 1 = 4.12 × 0.75	0.12 + 0,92 work reducer = 3.09 o	= 4.12 da, time by lays	257.	Plum & l Apprentice
= 2.44 + 0.64 + +dd additional 1 = 4.12 × 0.75 +al Time requir	0.12 + 0,92 work reducer = 3.09 o	= 4.12 da, time by lays	257.	Plum & l'Apprentice
= 2.44 + 0.64 + Edd additional 1 = 4.12 × 0.75 In Time requir	0.12 + 0,92 work reducer = 3.09 o	= 4.12 da, time by lays	257.	Plva & l'Apprentice
2.44 + 0.64 + Idd additional 1 = 4.12 × 0.75 In Time requir	0.12 + 0,92 work reducer = 3.09 o	= 4.12 da, time by lays	257.	Plum & l'Apprentice
= 2.44 + 0.64 + Edd additional 1 = 4.12 × 0.75 In Time requir	0.12 + 0,92 work reducer = 3.09 o	= 4.12 da, time by lays	257.	Plum & l'Apprentice
= 2.44 + 0.64 + Edd additional 1 = 4.12 × 0.75 In Time requir	0.12 + 0,92 work reducer = 3.09 o	= 4.12 da, time by lays	257.	Plva & l'Apprentice
= 2.44 + 0.64 + Edd additional 1 = 4.12 × 0.75 In Time requir	0.12 + 0,92 work reducer = 3.09 o	= 4.12 da, time by lays	257.	Plva & l'Apprentice
= 2.44 + 0.64 + Edd additional 1 = 4.12 × 0.75 In Time requir	0.12 + 0,92 work reducer = 3.09 o	= 4.12 da, time by lays	257.	Plva & l'Apprentice







2,	15	100 Building Services Pipin	9								
	161	07 Metal Pipe & Fittings	, at #	DAIL	Y LABOR			2000 BA	RE COSTS		TOTAL
	101	U/ Metal Pipe & Fiftings	# CRE		UT HOURS		MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P
660	9342	4" to 8" pipe, 6" stem	1 Plu	m 14	.571	Ea.	38.50	19		57.50	71.7%
· 1	9343	8" pipe and larger, 6" stem		13	.615	"	38.50	20.50		59	73.50
ı	9400	Mechanical joint ends for plain end pipe		_	1	77.					Ä
- 1	9410	Malleable iron, black									
- 1	9420	90° Elbows, 1-1/4"	Q1	29	.552	Ea.	9.30	16.50		25.80	35.50
ı	9430	1-1/2"		27	.593	!	10.20	17.75		27.95	38
1	9440	2"	<i>{ </i>	24	.667		12.05	19.95		32	43.50
ı	9490	Tee, reducing outlet	୬ '		1	'					- 4
	9510	1-1/4" x 1/2"	01	18	.889	Ea.	7.45	26.50		33.95	48.50
	9520	1-1/4" x 3/4"	Ĭ	18	.889	Ī	7.45	26.50		33.95	48.50
	9530	1-1/4" x 1"		18	.889	H +	7.45	26.50		33.95	48.50
	9540	1-1/2" x 1/2"	77	17	.941		7.90	28		35.90	51
	9550	1-1/2" x 3/4"		17	.941		7.90	28		35.90	51
	9560 .	1-1/2" x 1"		17	.941		7.90	28		35.90	51
	9570	2" x 1/2"		15	1.067	H +	9.65	32		41.65	59
	9580	2" x 3/4"	11	15	1.067		9.65	32		41.65	59
	9590	2" x 1"	 - 	15	1.067	1 1	9.65	32		41.65	59
	9640	Tee, reducing run and outlet	_ Y			'		J.		11.50	340
	9660	1-1/4" x 1" x 1/2"	0.1	18	.889	Ea.	7.95	26.50		34.45	49.50
	9670	1-1/4" x 1" x 3/4"		18	.889	Ī	7.95	26.50		34.45	49.50
	9680	1-1/4" x 1" x 1"		18	.889	-	7.95	26.50		34.45	49.50
- 1	9690	1-1/2" x 1-1/4" x 1/2"		17	.941		8.45	28		36.45	52.
L	9700	1-1/2" x 1-1/4" x 3/4"	<u> </u>	17	.941		8.45	28		36.45	52
	9710	1-1/2" x 1-1/4" x 1"		17	.941		8,45	28		36.45	52
	9720	2" x 1-1/2" x 1/2"	(/) 	15	1.067		10.25	32		42.25	60
	9730	2" x 1-1/2" x 3/4"		15	1.067		10.25	32		42.25	60
ŀ	9740	2" x 1-1/2" x 1"		15	1.067		10.25	32		42.25	60
7.4	9790	Tee, outlet	. '		,	. '					
<u> </u>	9810	3" x 1-1/4"	Q-I	29	.552	∖Ea.	18.05	16.50		34.55	45
I	9820	3" x 1-1/2"		28	.571		18.05	17.10		35.15	46
ı	9830	3" x 2"	1	26	.615		20	18.40		38.40	50
- 1	9840	4" x 1-1/4") ·	28	.571		22.50	17.10		39.60	50.50
I	9850	4" x 1·1/2"		26	.615		23.50	18.40		41.90	54
ŀ	9860	4" x 2"	↓	24	.667	. 🔻	23.50	19.95		43.45	56
ı	9940	For galvanized fittings for plain end pipe, add			1	:	20%				
	2 3	Š.A.	·		7 4	:					
690	0010 PI	PE, GROOVED-JOINT STEEL FITTINGS & VALVES									. 238
	0020	Pipe includes coupling & clevis type hanger 10' O.C.									
	0500	Schedule 10, black	÷								ja ja
	0550	2" diameter	1 Plu		.186	L.F.	3.02	. 6.20		9.22	12.65
	0560	2-1/2" diameter	Q1	61	.262		3.65	7.85		11.50	15.90
	0570	3" diameter	: 1	. 55	.291		4.18	8.70		12.88	17.75
	0580	3-1/2" diameter		53	.302		5.35	9.05		14.40	19,55
	0590	4" diameter		49	.327		5.65	9.75		15.40	21
	0600	5" diameter	₩	40	400		8.95	11.95		20.90	28
	0610	6" diameter	Q-2	46	.522		9.60	16.20		1 25.80	35
	0620	8" diameter		41	.585	*	18.45	18.15		36.60	48
	0700	To delete couplings & hangers, subtract	1 E.,								
	0710	2" diam. to 5" diam.	1		1		25%	20%			
	0720	6" diam. to 8" diam.			:	<u> </u>	27%	15%			17451
	1000	Schedule 40, black	.]						. "		
	1040	3/4" diameter	1 Plur		.113	L.F.	2.04	3.75		5.79	7.90
	1050	1" diameter	<u>, I</u> T	63	.127		2.17	4.22	r.	6.39	8.80
	1060	1-1/4" diameter		58	.138	<u>.</u>	2.64	4.59		7.23	9.85
	1070	1-1/2" diameter	$\top \top$	51	.157		2.97	5.20		8.17	11.15
1	1080	2" diameter	;	40	.200	Ŀ¥	3.46	6.65		10.11	13.85
											37.5

City Control	Building Services Pi		0.01		•					
			DAILY	LABOR-			2000 BAR	E COSTS		TOTAL
15107	Metal Pipe & Fittings	CREW	OUTPUT		UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL O&P
1090	2-1/2" diarneter	0-1	57	.281	L.F.	4.68	8.40		13.08	17.85 6
1100	3" diameter		50	.320		5.70	9.60		15.30	21
1110	4" diameter		45	.356		8.05	10.65		18.70	25
1120	5" diameter	1 1	37	.432		12.40	12.95		25.35	33
1130	6" diameter	0-2	42	.571	$\vdash \vdash$	15.90	17.75		33.65	44.50
1	8" diameter	\\ \frac{\psi_2}{1}	37	.649		23.50	20		1 1	1
1150				.774		l l	1		43.50	56.50
1	10" diameter		31	1 1		36	24		60	76
1160	12" diameter		27	.889		47.50	27.50		75 ·	93.50
1170	14" diameter		20	1.200		56	37		93	118
1180	16" diameter		17	1.412		79.50	44		123.50	154
1190	18" diameter		14	1.714		142	53		195	237
1200	20" diameter		12	2		108	62		170	213
1210	24" diameter	♦	10	2.400	₩	128	74.50		202.50	254
1/40	To delete coupling & hanger, subtract									
1/50	3/4" diam. to 2" diam.					35%	27%			
1760	2-1/2" diam. to 5" diam.					18%	. 18%	!		
1770	6" diam. to 12" diam.					14%	13%			
1800	Galvanized		l							
1840	3/4" diameter	1 Plum	71	.113	L.F.	2.27	3.75		6.02	8.15
1850	1" diameter	1 1	63	.127		2,34	4.22		6.56	9
1860	1-1/4" diameter		58	.138		2.85	4.59		7,44	10.10
1870	1-1/2" diameter	1	51	.157		3.23	5.20		8.43	11.45
1880	2" diameter	——————————————————————————————————————	40	.200		3.81	6.65		10.46	14.25
1890	2-1/2" diameter	0-1	57	.281	١ .	5.25	8.40		13.65	18.45
1900	3" diameter		50	.320	$\vdash \vdash$	6.40	9.60		16	21.50
1910	4" diameter		45	.356		9.10	10.65		19.75	26
1920	5" diameter		37	.432		15.25	12.95	.—	28.20	36.50
1930	6" diameter	0-2	42	.571		19.80	17.75		37.55	49
1940	8" diameter		37	.649		29.50	20		49.50	63
1950	10" diameter		31	.774		44	24		68	85
1960	12" diameter		27	.889		58	27.50		85.50	106
l l	To delete coupling & hanger, subtract	▼	\ '\	.003	•	J6	27.30		05.50	100
2540) 2550	3/4" diam. to 2" diam.					36%	27%			
3:	•					l I	18%			1
7560	2-1/2" diam. to 5" diam.		<u> </u>			19%	13%			
2570	6" diam. to 12" diam.					14%	1370			1
	edule 80, black	1.5		102		0.21	4.00		C 40	0.75
2610	3/4" diameter	1 Plum	65	.123	L.F.	2.31	4.09		6.40	8.75
2650	1" diameter		61	.131		2.50	4.36		6.86	9.35
2660	1-1/4" diameter		55	.145		3.12	4.84		7.96	10.75
2670	1-1/2" diameter		49	.163	<u> </u>	3.57	5.45		9.02	12.15
2680	2" diameter	+	38	.211		4.35	7		11.35	15.40
2690	2-1/2" diameter	Q-1	54	.296		5.95	8.85		14.80	. 19.90
2700	3" diameter	1 1	48	.333		7.45	10		17.45	23.50
2710	4" diameter		44	.364		10.75	10.90		21.65	28.50
2720	5" diameter	+	35	.457		12.55	13.70		26.25	34.50
2730	6" diameter	Q-2	40	.600		20.50	18.60		39.10	50.50
2740	8" diameter		35	.686		47.50	21.50		· 69	84.50
2750	10" diameter		29	.828		75.50	25.50		101	122
2760	12" diameter		24	1	\	83.50	31		114.50	139
3240	To delete coupling & hanger, subtract	ľ			'					1
3250	3/4" diam. to 2" diam.		 	 		30%	25%			
3260	2-1/2" diam. to 5" diam.	ļ				14%	17%		[·
3270	6" diam, to 12" diam.		-			12%	12%		 	
	Galvanized					12,0	1277			
3310	3/4" diameter	1 Plum	65	.123	L.F.	2.01	4.09		6.10	8.40
L L	•	1 1	61	.131]	2.01	4.36		6.42	8.85
350	1" diameter		01	.131	¥	2.00	4.30		Į 0.4Z	0.00

	00 Building Services Pip		DAILA	LABOR-	<u>0</u> 28320		2000 BAJ	PE COSTS		TOTAL
1510	7 Metal Pipe & Fittings	CREW		HOURS	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P
3360	1-1/4" diameter	1 Plum	55	.145	L.F.	2.51	4.84	EQUA:	7.35	10.0
170	1-1/2" diameter		46	.174		2.83	5.80		8.63	11.8
J380	2" diameter		38	.211		3.26	7		10.26	14.2
3390	2-1/2" diameter	Q-1	54	.296		4.25	8.85		13.10	18.0
3400	3" diameter	——————————————————————————————————————	48	.333	$\vdash \vdash$	5.25	10		15.25	21
3410	4" diameter	1 1	44	.364		7.55	10.90		18.45	25
3420	5" diameter		35	.457		15.45	13.70		29.15	37.
3430	6" diameter	0-2	40	.600		26.50	18.60		45.10	57.
3440	8" diameter		35	.686		46	21.50		67.50	82.
3450	10" diameter		29	.828		73	25.50		98.50	120
3460	12" diameter		24	1	1	81	31		112	136
3920	To delete coupling & hanger, subtract		24		•	0,	21		112	130
3930	3/4" diam, to 2" diam.				<u> </u>	30%	25%			
	•	ı				1				
3940	2-1/2" diam. to 5" diam. 6" diam. to 12" diam.		ļ. ——			15%	17%			
3950		1				11%	12%			
	Fittings: cplg. & labor required at joints not incl. in fitting									·
3994	price. Add 1 per joint for installed price.									
	Elbow, 90° or 45°, painted			160		1010			17.40	
4030	3/4" diameter	1 Plum	50	.160	Ea.	12.10	5.30		17.40	21
4040	1" diameter		50	.160		12.10	5.30		17.40	. 21
4050	1-1/4" diameter	1 1	40	.200		12.10	6.65		18.75	23
4060	1-1/2" diameter		33	.242		12.10	8.05		20.15	25
4070	2" diameter	₩	25	.320		12.10	10.65	·	22.75	29
4080	2-1/2" diameter	Q-1	40	.400		. 12.10	11.95		24.05	31
4090	3" diameter		33	.485		21.50	14.50		36	45
4100	4" diameter		25	.640		23.50	19.15		42.65	55
10	5" diameter	₩	20	.800		56.50	24		80.50	98
_0	6" diameter	Q-2	25	.960		66.50	30		96.50	118
4130	8" diameter	1 1	21	1.143		139	35.50		174.50	207
4140	10" diameter		18	1.333		254	41.50		295.50	340
4150	12" diameter		15	1.600		405	49.50		454.50	520
4170	14" diameter		12	2		725	62		787	895
4180	16" diameter	+ ·	11	2.182		945	67.50		1,012.50	1,150
4190	18" diameter	Q-3	15	2.133		1,200	67.50		1,267.50	1,425
4200	20" diameter		13	2.462		1,575	78		1,653	1,875
4210	24" diameter	_	11	2.909		2,300	92.50		2,392.50	2,675
4250	For galvanized elbows, add				*	26%				
4690	Tee, painted									
4700	3/4" diameter	1 Plum	38	.211	Ea.	18.65	7		25.65	31
1740	1" diameter		33	.242		18.65	8.05		26.70	32
4750	1-1/4" diameter		27	.296		18.65	9.85		28.50	35
4760	1-1/2" diameter		22	.364		18.65	12.10		30.75	39
1770	2" diameter	1	17	.471		18.65	15.65		34.30	44
4780.	2-1/2" diameter	Q1	27	.593		18.65	17.75		36.40	47
1790	3" diameter		22	.727		26	22		48	62
1800	4" diameter	1 .	17	.941		40	28		68	86
1810	5" diameter	1	13	1.231		93.50	37		130.50	159
1820	6" diameter	02	17	1.412		108	44		152	186
1830	8" diameter		14	1.714	-	238	53		291	345
1840.	10" diameter	!]	12	2		495	62		557	640
850	12" diameter		10	2.400	-	690	74.50		764.50	875
851	14" diameter		9	2.667		730	83		813	930
~~ <u>-</u>	16" diameter		8	3		825	93		918	1,050
וו	10 Manielet		٠			1			1	
	19" diameter		11	ו מחמיכו	, ,	1 1025	Q2 KA :	1	1 117501	1 1//2
.d 854	18" diameter 20" diameter	03	11	2.909 3.200		1,025 1,475	92.50 101		1,117.50 1,576	1,275 1,775

	. I pending servic		الكريس	DARLY	LADOR			2000 041	L COSTS			Ŧ
15107	Metal Pipe & Fittings		CDEM		LABOR- HOURS		BAST	LABOR	E COSTS	I rores	TOTAL	١
1900	For galvanized tees, add	· · · · · · · · · · · · · · · · · · ·	CREW	1001101	HOUKS	Ea.	MAT. 24%	LABUK	EQUIP.	TOTAL	INCL 0&P	+
· 1	plings, rigid style, painted		1.			L.G.	24/0					ľ
1908	1" diameter		I Plum	100	.080	Ea.	8.80	2.66		11.46	13.65	\mathbf{I}
1909	1-1/4" diameter			100	.080	Ĭ.	8.80	2.66		11.46	13.65	- 11
1910	1-1/2" diameter	-	╂┼	67	.119		8.80	3.97		12.77	15.65	
1912	2" diameter			50	.160		9	5.30		14.30	17.95	
1914	2-1/2" diameter	- /////////	♦	80	,200	- -	. 10.40	6		16.40	20.50	_8
1916	3" diameter		l i	67	.239		12.15	7.15		19.30	20.50	
1918	4" diameter		╂┼┼	50	.320	 	17.20	9.60		26.80	33.50	
1920	5" diameter		ΙL	40	.400		22.50	11.95		34.45	42.50	
1922	6" diameter		Q-2	50	.480	$\vdash \vdash$	30	14.90		44.90	55.50	- 1
1924	8" diameter	* - [۲۰۷	42	.571		47	17.75		1		
1926	10" diameter	<i>a</i> •	╂┼┼	35	.686	$\vdash \vdash$	84	21.50		64.75 105.50	78.50 125	4
928	12" diameter			32	.750		94.50	23.50		1 1		١
930	14" diameter		- -	24	1	 	123	31		118 154	139 182	4
931	16" diameter	,		20	1.200		161	37		I i		١
932	18" diameter		 	18	1.333		186	41.50		198 227.50	234 267	4
933	20" diameter			16	1.500		221	46.50		1 1	267 315	
934	24" diameter		Q-9	13	1.231	├-	325	36		267.50		4
1	Flexible, standard, painted		ψy	13	1.231	₩	323	30		361	415	١
950	3/4" diameter		1 Plum	100	.080	E-	6.30	2.66		0.00	10.05	4
960	1" diameter		i rum	100	.080	Ea.]			8.96	10.95	- 1
70.	1-1/4" diameter				.100		6.30	2,66		8.96	10.95	
80	1-1/4" diameter			80 67	.100		8.40	3.33		11.73	14.30	- 1
90	2" diameter			50	.119		9.20 9.70	3.97 5.30		13.17	16.10	- 1
00	2-1/2" diameter		∀ 0-1	80	.200		11.60			15	18.70	1
010	3" diameter		4,	67	.239		12.80	6 7.15		17.60	22 25	4
20	3-1/2" diameter		l I	57	.239		18.70	7.13 8.40		19.95	25 33	
)30	4" diameter		 -	50	.320		18.70	9.60		27.10 28.30	35	4
40	5" diameter			40	.400		28.50	11.95		40.45		
150	6" diameter		▼ Q-2	50	.480		34	14.90		48.90	49.50 60	_
70	8" diameter		١	42	.460		55.50	17.75		73.25	•	
90	10" diameter		$\vdash \vdash$	35	.686		92	21.50		113.50	88 133	4
10	12" diameter		.	32	.750		105	23.50		128.50	150	
20	14" diameter		⊢-	24	1		103	31		158	187	4
30	. 16" diameter			20	1.200		167	37		204	240	
40	18" diameter		\vdash	18	1.333		195	41.50		236.50	278	4
50	20" diameter			16	1.500		305	46.50		351.50	410	1
60	24" diameter		$\vdash \perp$	13	1.846	-1-	335	57.50		392.50	455	-
76	Lightweight style, painted		•	10	1.010	•	333	57.50		332.30	455	
78	1-1/2" diameter	· ·	1 Plum	67	.119	Ea.	8	3.97		11.97	14.80	4
80	2" diameter		7	50	.160	Ī	8.20	5.30		13.50	17.05	- 1
82	2-1/2" diameter		Q·1	80	.200		9.50	6		15.50	19.50	
84	3" diameter	4	Ĭ	67	.239		11.05	7.15		18.20	23	ı
86	3-1/2" diameter			57	.281	+-	15.65	8.40		24.05	30.	+
88	4" diameter			50	.320		15.65	9.60		25.25	31.50	۱ ر
90	5" diameter			40	.400		22.50	11.95		34.45	43	1
92	6" diameter		Q-2	50	.480		27	14.90		41.90	52.50	١
94	8" diameter		+	42	.571		42.50	17.75		60.25	74	-
96	10" diameter	٠		35	.686		115	21.50		136.50	158	1
98	12" diameter		•	32	.750	-	128	23.50		151.50	176	4
00	For galvanized couplings, add	·	₩	JL	., 50		33%	23.30		131.30	1/0	
	educing, painted					_₩	33/0					4
20 1ee, r	educing, painted 2" x 1-1/2" diameter		Q-1	- 38	.421	Ea.	40.50	12.60		53.10	63.50	,
	2-1/2" x 2" diameter	<u>.</u>	- 1 1	28	.421	Cd.	40.50	17.10		53.10	70.50	- 9
26 ^				- 1	.571		35.50	l l		56.50	70.50	- 5
27	3" x 2-1/2" diameter		▼	23	,050	Ÿ	33.30	21		50,50	70,00	/ P

	O Building Services Piping									
15107	Metal Pipe & Fittings	·	DAILY	1				RE COSTS	3 3 948	TOTAL
5228	4" x 3" diameter	CREW	_	_	+	MAT.	LABOR	EQUIP.	TOTAL	INCL O
5229		Q-1	18	.889	Ea.	48	26.50		74.50	9
5230	5" x 4" diameter	<u> *</u>	15	1.067		103	32		135	16
	6" x 4" diameter	Q-2	18	1.333		114	41.50		155.50	18
5231	8" x 6" diameter	$\bot \bot$	15	1.600		238	49.50		287.50	33
5232	10" x 8" diameter	1	13	1.846		310	57.50		367.50	43
5233	12" x 10" diameter		11	2.182		475	67.50		- 542.50	62
5234	14" x 12" diameter		10	2.400		530	74.50		604.50	70
5235	16" x 12" diameter	₩	9	2.667		660	83		743	85
5236	18" x 12" diameter	Q3	12	2.667		790	84.50		874.50	1,00
5237	18" x 16" diameter	Ŀ	11	2.909		. 1,000	92.50		1,092.50	1,25
5238	20" x 16" diameter		10	3.200		1,300	101		1,401	1,57
5239	24" x 20" diameter	₩	9	3.556	↓	2,050	113		2,163	2,45
į.	educer, concentric, painted			:						*************
5241	2-1/2" x 2" diameter	Q-1	43	.372	Ea.	14.10	11.15		25.25	3
5242	3" x 2-1/2" diameter		35	.457		17.05	13.70		30.75	3
5243	4" x 3" diameter		29	.552		20.50	16.50		37	4
5244	5" x 4" diameter	1	22	.727		29	22		51	6
5245	6" x 4" diameter	Q2	26	.923		33.50	28.50		62	8
5246	8" x 6" diameter		23	1.043		87.50	32.50		120	14
5247	10" x 8" diameter		20	1.200		178	37		215	25
5248	12" x 10" diameter	1	16	1.500	\	320	46.50	······································	366.50	42
5255	Eccentric, painted	ļ '			'					, :
5256	2-1/2" x 2" diameter	Q-1	42	.381	Ea.	30	11.40		41.40	5
5257	3" x 2-1/2" diameter		34	.471		34	14.10		48.10	5
5258	4" x 3" diameter	f	28	.571		42	17.10		59.10	7
5259	5" x 4" diameter	↓	21	762		57	23		80	9.
5260	6" x 4" diameter	Q-2	25	.960		66.50	30		96.50	11
5261	8" x 6" diameter		22	1.091	.	135	34		169	19
5262	10" x:8" diameter		19	1.263		370	39		409	47
5263	: 12" x 10" diameter	↓	- 15	1.600		510	49.50		559.50	63
5270 Co	upling, reducing, painted					-				
5272	2" x 1-1/2" diameter	1 Plum	. 52	.154	Ea.	14.20	5.10		19.30	2:
5274	2-1/2" x 2" diameter	Q-1	82	.195		18.55	5.85	· · · · · · · · · · · · · · · · · · ·	24.40	2
276	3" x 2" diameter		69	.232		21	6.95		27.95	3
278	4" x 2" diameter		52	.308		34	9.20		43.20	5
5280	5" x 4" diameter	↓	42	.381		38.50	11.40		49.90	5
282	6" x 4" diameter	Q2	52	.462		58	14.30		72.30	8
284	8" x 6" diameter .	,	44	.545		87	16.95		103.95	12
290 Out	let coupling, painted	-		. :	· ·).
294	1-1/2" x 1" pipe size	1 Plum	65	123	Ea.	17.70	4.09		21.79	2
296	2" x 1" pipe size	,	48	.167		18.20	5.55		23.75	28
298	2-1/2" x 1" pipe size	Q-1	· 78	.205		28	6.15		34.15	40
300	2-1/2" x 1" pipe size	1 Płum	70	.114		32	3.80		35.80	4:
302	3" x 1" pipe size	Q-1	65	.246		27	7.35		34.35	4:
304	4" x 3/4" pipe size	Hid	48	.333	$\dashv \dashv$	40	10	1 1 1	50	59
306	4" x 1-1/2" pipe size		46	.348		57	10.40		67.40	7.
308	6" x 1-1/2" pipe size	02	44	.545	1	81	16.95		97.95	11
	ge, w/groove gasket, black steel (see 15107-660-0620, bolt sets)	`-			▼				57,55	9
	ANSI class 125 and 150, painted									
780	· ·	1 Plum	23	.348	Ea.	41.50	11.55		53.05	6:
790	2-1/2" pipe size	Q-1	37	.432		50	12.95		62.95	74
300	3" pipe size	\ \.	31	.432		54	15.45		69.45	8:
320			23	.696		72.50	21	<u> </u>	93.50	. 11.
330	4 pipe size 5" pipe size		19	.842			25			
340	6" pipe size	0.2			\dashv	84			109	131
1		Q2	- 1	1.043		92	Į.	. '	124.50	150
350	8" pipe size	- ▼	17.	1.412	V	104	44	1	148	181

			DAILA	LABOR-			2000 BAF	E COSTS		Táza	
1.5	107 Metal Pipe & Fittings	CREW	OUTPUT			MAT.	LABOR	EQUIP.	TOTAL	TOTAL INČL 0&P	
0 5860	10" pipe size	Q-2	14	1.714	Ea.	164	53	240	217	262	690
.5870	12" pipe size		12	2		215	62		277	330	
5880	14" pipe size		10	2.400		495	74.50		569.50	660	/
5890	16" pipe size		9	2.667		575	83	,	658	755	ſ
5900	18" pipe size	H	6	4	-	705	124		829	965	
5910	20" pipe size		5	4.800		850	149		999	1,150	
5920	24" pipe size	╽╁	4.50	5.333	╁	1,075	165		1,240	1,450	
5940	ANSI class 350, painted	*			\		100		2,2.0	1,.00	
5946	2" pipe size	1 Plum	23	.348	Ea.	50.50	11.55		62.05	73	
5948	2-1/2" pipe size	Q-1	37	.432	Ĭ	58.50	12.95		71.45	84	
5950	3" pipe size	├	31	.516	$\vdash \vdash$	80	15.45		95.45	112	
5952	4" pipe size		23	.696		107	21		128	. 150	
5954	5" pipe size	╂	19	.842		121	25		146	172	ł
5956	6" pipe size	Q-2	23	1.043		141	32.50		173.50	205	
5958	8" pipe size	. 1	17	1.412	-	162	44		206	246	1
5960	10" pipe size	1 1	14	1.714		259	53		. 312	365	
5962	12" pipe size	1 Plum	12	.667	\pm	276	22		298	340	ĺ
6100	Coupling, for PVC plastic pipe	1 1 10111	1 12	.007	▼	2/0	22		230	340	
6110	2" diameter	1 Plum	50	.160	Ea.	10.80	5.30		16.10	19.95	ł
6112	2-1/2" diameter	Q-1	80	.200	La.	15.20	6		21.20	26	
6114	3" diameter	1	67	.239	\vdash	18.45	7.15		25.60	31.50	ł
6116	4" diameter		50	.320		24	9.60		33.60	41	
6118	6" diameter	0-2	50	.480		40	14.90		54.90	66.50	ł
6120	8" diameter	ا	42	.571		65.50	17.75		83.25	99	١.
6122	10" diameter	-+	35	.686	 	108	21.50	· · · · · ·	129.50	150	
6124	12" diameter		32	.750		136	23.50		159.50	185	•
7400	Suction diffuser		JŁ	.730		130	23.30		133.30	103	:
7400	Grooved end inlet x flanged outlet										
7410	3" x 3"	Q-1	50	.320	Ea.	425	9.60		434.60	485	
7412	4" × 4"	Ĭ	38	.421	La.	620	12.60		632.60	705	,
7414	5" x 5"	$\vdash \vdash$	30	.533	<u> </u>	675	15.95		690.95	765	
7414	6" x 6"	♦ Q2	38	.632		850	19.60		869.60	965	
7418	8" x 8"	1 42	27	.889	$\vdash\vdash$	1,575	27.50		1,602.50	1,800	
7420	10" x 10"		20	1.200		2,150	37		2,187	2,425	
7422	12" x 12"		16	1.500		3,550	46.50		3,596.50	3,975	1
7424	14" x 14"		15	1.600		4,475	49.50		4,524.50	5,000	
7426	16" x 14"		14	1.714		4,600	53		4,653	5,150	
7500	Strainer, tee type, painted	٧	• •		•	,,,,,,			1,000	0,100	
7506	2" pipe size	I Plum	38	.211	Ea.	265	7		272	300	
7508	2-1/2" pipe size	Q-1	62	.258	Ī	278	7.70		285.70	315	·
7510	3" pipe size	\ <u>`</u>	50	.320	┝╼┾╼	315	9.60		324.60	360	1
7512	4" pipe size		38	.421		355	12.60		367.60	410	
7514	5" pipe size	1	30	.533	├-├	515	15.95		530.95	590	
7514	6" pipe size	Q-2	38	.632		555	19.60		574.60	640	ŀ
7518	8" pipe size	<u> </u>	27	.889		855	27.50		882.50	980	l
7520	10" pipe size		20	1.200		1,250	37		1,287	1,425	l
7522	12" pipe size		16	1.500		1,625	46.50		1,671.50	1,850	1
7524	14" pipe size		15	1.600		5,750	49.50		5,799.50	6,400	1
7524 7526	14' pipe size	$\vdash \perp \vdash$	14	1.714	$\vdash \perp$	7,150	53		7,203	7,925	
7570	• •	▼	17	1./14	₩	,,130	JJ		7,200	11000	
	Expansion joint, max. 3" travel	1 Plum	38	.211	Ea.	218	7		225	250	1
7572	2" diameter		50	.320	La.	255	9.60	,	264.60	296	l
7574	3" diameter	01	38	.320	$\vdash \vdash$	320	12.60		332.60	370	
7576	4" diameter		- 1	.632		1 !			574.60	645	
7578	6" diameter	Q2	38	.032	▼	555	19.60		3/4.00	. 040	Townson.
7800	Ball valve w/handle, carbon steel trim	, n	E0	160	r-	CAEO	5.30		69.80	79	
7810	1-1/2" pipe size	1 Plum	50	.160	Ea.	64.50	3.3 U		บอ.ชบ	/3	Viguage S

37	15	100 Building Services Piping										
10000			l	DAILA	LABOR			2000 BA	RE COSTS			鼺
	151	107 Metal Pipe & Fittings	CREW	,	HOURS		MAT.	LABOR	EQUIP.	TOTAL	TOTAL	1
690	7812	2" pipe size	1 Plum	_	.211	Ea.	89	7 7	EQUIP.	96	INCL 0&P 109	690
	7814	2-1/2" pipe size	Q1	62	.258	Ī	184	7.70		191.70	214	100
	/816	3" pipe size	 ``	50	.320	++	290	9.60		299.60	-335	-
	7818	4" pipe size		38	.421		445	12.60		457.60	510	
	7820	6" pipe size	Q-2	30	.800	╁╁	1,300	25		1,325		-
	7830	With gear operator	٧-	30	.000	▼	1,500	23		1,323	1,500	
	7834	2-1/2" pipe size	Q-1	62	.258	Ea.	325	7.70		320.70	200	4
	7836	3" pipe size	4,	50	.320	La.	430	9.60		332.70	365	
	7838	4" pipe size	-	38	.421	\vdash				439.60	485	1
	7840	6" pipe size	02	30	l .		575	12.60		587.60	655	1
	7870	Check valve	Q2	30	.800	*	1,475	25		1,500	1,675	1
	7874	2-1/2" pipe size	١,,		250	_ ا		7.70				
	7876		Q-1	62	.258	Ea.	116	7.70		123.70	140	1
		3" pipe size		50	.320		137	9.60		146.60	166	
	7878	4" pipe size		38	.421	 	145	12.60		157.60	178	1
	7880	5" pipe size	\ \	30	.533		241	15.95		256,95	289	1
	7882	6" pipe size	Q2	38	.632		286	19.60		305.60	345	
	7884	8" pipe size		27	.889		390	27.50		417.50	470	
	7886	10" pipe size	lacksquare	20	1.200		1,125	37		1,162	1,300	
	7888	12" pipe size	\ \	16	1.500	\ \	1,350	46.50		1,396.50	1,550	
	7900	Plug valve, balancing, w/lever operator	<u>L</u>	<u> </u>								
- 1	7906	3" pipe size	Q-1	50	.320	Ea.	238	9.60		247.60	277	
L	7908	4" pipe size		38	.421		262	12.60		274.60	305	
	7909	6" pipe size	Q-2	30	.800	l ♦	470	25		495	555	
	7916	With gear operator										
	7920	3" pipe size	Q-1	50	.320	Ea.	430	9.60		439.60	490	l
	7922	4" pipe size		38	.421		455	12.60		467.60	520	1
	724	6" pipe size	Q-2	38	.632		660	19.60		679.60	760	l
٤.,	26	8" pipe size		27	.889		885	27.50		912.50	1,025	İ
	7928	10" pipe size		20	1.200		1,400	37		1,437	1,575	l
E.	7930	12" pipe size	V	16	1.500		2,025	46.50		2,071.50	2,300	1
	8000	Butterfly valve, 2 position handle, with standard trim	j									l
	8010	1-1/2" pipe size	1 Plum	50	.160	Ea.	103	5.30		108.30	121	
	8020	2" pipe size	"	38	.211		103	7		110	124	l
	8030	3" pipe size	Q-1	50	.320		147	9.60		156.60	177	1
	8050	4" pipe size	#	38	.421		162	12.60		174.60	197	l
	8070	6" pipe size	Q-2	38	.632		355	19.60		374.60	420	
	8080	8" pipe size		27	.889		540	27.50		567.50	635	1
1	8090	10" pipe size	V	20	1.200	+	775	37		812	910	
	8200	With stainless steel trim										1
	8240	1-1/2" pipe size	1 Plum	50	.160	Ea.	130	5.30		135.30	151	
	3250	2" pipe size	n	38	.211		130	7		137	154	
	8270	3" pipe size	Q-1	50	.320		175	9.60	.]	184.60	207	1
	3280	4" pipe size	"	38	.421		190	12.60	. 1	202.60	228	
	3300	6" pipe size	Q2	38	.632		355	19.60		374.60	420	1
8	3310	8" pipe size		27	.889		605	27.50		632.50	705	
	3320	10" pipe size	.	20	1.200		960	37		997	1,100	
8	3322	12" pipe size		16	1.500		1,225	46.50		1,271.50	1,425	
8	3324	14" pipe size		15	1.600		1,600	49.50		1,649.50	1,850	1
8	3326	16" pipe size	+	14	1.714	11	2,200	53		2,253	2,500	[
18	328	18" pipe size	Q3	12	2.667		2,700	84.50		2,784.50	3,100	
	3330	20" pipe size	\dashv	11	2.909	11	3,675	92.50		3,767.50	4,1.75	
	332	24" pipe size	↓	1	3.200	↓	4,675	101		4,776	5,275	l
, .	3	Note: sizes 12" up w/manual gear operator					7-1-5				,	
(از	Cut one groove, labor	1		- 1			İ		I		1
19	010	3/4" pipe size	Q-1	152	.105	Ea.		3.15		3.15	4.77	
	020	1" pipe size		140	.114	1		3.42		3.42	5.15	
ئا						_¥	1	,-1				

1	Building Services Pip		-	DAJLY	LABOR-	A SECTION AND ADDRESS OF THE PARTY OF THE PA		2000 RA	RE COSTS	<u>i i ia ete Sajirili salelli</u>	TOTAL
15107	Metal Pipe & Fittings	•	CREW	1	T HOURS		MAT.	LABOR	EQUIP.	TOTAL	TOTAL INCL 0&P
030	1-1/4" pipe size	:	0-1	124	.129	Ea.	(1031)	3.86	LQUIT.	3.86	5.85
9040	1-1/2" pipe size		Ì	114	.140			4.20		4.20	6,35
050	2" pipe size		\vdash	104	.154	1		4.60		4.60	6.95
060	2-1/2" pipe size			96	.167			4.99		4.99	7.55
9070	3" pipe size		\vdash	88	.182		 	5.45		5.45	8.25
080	3-1/2" pipe size			83	.193			5.75		5.75	8.75
0090	4" pipe size		\vdash	78	.205	╁┼╴		6.15	<u> </u>	6.15	9.30
0100	5" pipe size			72	.222			6.65		6.65	10.05
110	6" pipe size		-	70	.229	\vdash		6.85	-	6.85	10.35
120	8" pipe size	•		54	.296			8.85		8.85	13.40
130	10" pipe size		-	38	.421			12.60		12.60	19.05
140	12" pipe size			30	.533			15.95		15.95	24
150	14" pipe size			20	.800			24		24	36
160	16" pipe size			19	.842			25		25	38
170	18" pipe size		\dashv	18	.889	┢┼		26.50		26.50	40.50
180	20" pipe size			17	.941			28		28	42.50
190	24" pipe size		1	15	1.067			32	 	32	48.50
1	one groove		*			•		"-		J.	40.50
220	3/4" pipe size		Q-1	266	.060	Ea,		1.80		1.80	2.72
230	1" pipe size	1	Ì	228	.070			2.10		2.10	3.18
240	1-1/4" pipe size		_	200	.080	\vdash		2.39		2.39	3.62
250	1-1/2" pipe size	j	- [178	.090			2.69	}	2.69	4.07
260	2" pipe size		_	116	.138			4.13		4.13	6.25
270	2-1/2" pipe size	1		110	.145			4.35		4.35	6.60
280	3" pipe size		_	100	.160			4.79		4.79	7.25
290	3-1/2" pipe size	ı	ı	94	.170			5.10		5.10	7.70
300	4" pipe size			86	.186			5.55		5.55	8.40
310	5" pipe size		1	84	.190			5.70	1	5.70	8,60
320	6" pipe size		$\neg \vdash$	80	.200			6	·	6	9.05
330	8" pipe size	l	· •	66	.242			7.25		7,25	11
340	10" pipe size			58	.276			8.25		8.25	12.50
350	12" pipe size		_	46	.348			10.40		10.40	15.75
360	14" pipe size			30	.533			15.95		15.95	. 24
370	16" pipe size			28	.571			17.10		17.10	26
380	18" pipe size			27	.593			17.75		17.75	27
390	20" pipe size			25	.640			19.15		19.15	29
100	24" pipe size	. 1	\forall	23	.696	\ ₩		21		21	31.50
	AINLESS STEEL	l									
	d, with clevis type hangers 10' O.C.										
ſ	chedule 5, type 304		015	100	105		2.01	4.21	20	0.00	100-
540	1/2" diameter		Q-15	128	.125	L.F.	3.91	3.74	.38	8.03	10.35
560 560	3/4" diameter 1" diameter			116 103	.138 .155		4.46 5.35	4.13	.42	9.01	11.60
570	1-1/4" diameter			93	.155		6.05	4.65 5.15	.47 .52	10.47	13.40
80	1-1/4" diameter 1-1/2" diameter			93 85	.172		6.95	5.65		11.72	15.10
90 sh	2" diameter		+-	69	.232		8.30	6.95	.57 .71	13.17 15.96	16.80 20.50
90	2" diameter 2-1/2" diameter	[53	.232		8.30 11.40	9.05			
10	2-1/2" diameter 3" diameter			55 48	.302		13.70	10	.92 1.02	21.37 24.72	27 31.50
l l		ļ		40 44	.353						
30	4" diameter			36	.354	\dashv	17.45 35	10.90	1.11	29.46	37 60
1	5" diameter]	▼	36 42	. 444 .571			13.30	1.36	49.66 50.01	
40 50	6" diameter		Q16	34	.706	\dashv	32 49	17.75 22	1.16	50.91 72.43	64 88.50
1	8" diameter			26	.923						!
60 70 	10" diameter		-		1.143		69	28.50	1.87	99.37	122 156
/U]	12" diameter To delete hangers, subtract	- 1	▼	21	1.143	₩	90.50	35.50	2.32	128.32	120

Ave Control

Labour losts, lat Arm

Inlet Piping per un	it are the	Sume (unit # 2	has anly 20' of 6"0, 0 pige)
Estimate			actual
Ctew	perday	Quantity	days
6 0.0 PVC 5480 Q1	38'	40'	1.05
4" O. DPUC 2480 Q1	48'	201	0.44 > 1.85
2" 0.0 PVC x40. Q1	551	20'	0,36
14" O. P PVC Schoo Plum	39'	20'	0.51
6" 90 Ebbon Epoxy Q1	8	6+1	0.75 0.875
4" 90 Ector Epoxy Q1	13	2	0.15
2" go Elbon Epoxy Q1	2 T	3	0.13
90 ELGO. Elony Ql.	23	1+1	2.05 0.09
" Tee Epoxy Q1	5	2	0.4
" Flange E foxy Q1	16	3	0.1815
-" Flange Epoxy Q1	26	l	0.04 > 0.34;
" Flange Epoxy Q1	46	3	0.06
" Flange Eyoxy Q1	46	3	0.06
X4" Reducer bushing Q1	17	1	0.05 7,004
X2" Roduces bushing Q1	22	}	0.04
" Valve Illum	21		0.048
Valve I Plum			0,06

abour Costi, Cat Arm	
inlet Piping per unit	
Time required for 1960m.	
= 0.048 + 0.06 + 0.51 = 0.618 days	AND THE STREET OF THE STREET O
Add an additional worker reduces time by 25%.	
= 0.618 x 0.75 = 0.46 days	
Time required for 10 crew,	
1.85 + 1.245 + 0.3475 + 0.09 + 0.4 = 3.93 days	
Total time for lacrem.	
= 3.93 + 0.46 = 4.39 days (35.12 hrs)	()
·	

Work costs, lat am

•	Pinchange	Piping	for	Both Units	NYC	the	Same
		//	/				

Estimate		and a second and a second and a second and a second and a second a second a second a second a second a second	A	This
	Crew	Perday	Quant	ity days
6" 0.0 PVC 50480	Ql	38'	10'	0.26
4" 0. D PVC 5ch 80	Q,	461	40'	0.87
2.5" O.V PUC Schio	Q 1 ·	52'	40'	0.77 2.26
2" 0. D PVC 52480	Q 1	55'	201	0.36)
14" 0.0 PUC 5-430	1 Plus	391	201	0.51
4" 90'493 ELGOS Epoxy	G,	13	7	0.54
3" 90 248 ESS-S Ejong		19	, 5	0.26 21.01
i dts' Elbon, Epoxy		23	1	0.04
" go' drs' Elder Elex		23	4	0.17)
r" Tee Epory	Q,	8	2	0.25 0.48
Tec Eyoxy	2	13		0.23
7 7	1	26	7	0.27
Plane Byon Q	1	32	2	0.06
" Plunge Epoxy Q1		39	6	0.15
"Flance Ejoxy Q1		+6	5	0.11
Playe Exemy Q1	5	46	3	0.015)
14" Reducer bushy Q.		!7	1	0,06
X3" foduer bys; Q1		9	3	0.10 7 0.31
Reducer bushing Q1	2) 5	3	0.12
X14" Roducer buss R1	3	0	(0.03

_				·
-charge Piping	per unit		10cren = 1	PLVM + Appronfice
Estimate	Section of the sectio	and an experience of the second second second second second second second second second second second second se	Actua	l
Description	cten	dax	Quantity	day
Valve, 4"	10	20		0.05
Valve, 3"	10		1	0.04 0.13
Valve, 22"	l a			0.04
Valve, 2"	1 PLVM	17:	1	0.06 > 0.11
Valve, 14"	1 PL vm	21	1	0.05
Time required	for 1960m	•		
0.51 + 0.11				
Add an addition	worker re	duce time by	y 25 <i>J</i> .	
= 0.62 x 0	.75 = 0.4	6 day		
= 0.62 x 0	.75 = 0.4	6 day		
ime required		•		
	for 10 cr	en,		
ime required. 2,26 + 1.01 +	for 10 cr -0.48 + 0.6!	en. 55 + 0.31 =	: 4.72 days	
ime required. 2,26 + 1.01 +	for 10 cr -0.48 + 0.6!	en. 55 + 0.31 =	: 4.72 days	
ime required. 2,26 + 1.01 +	for 10 cr -0.48 + 0.6!	en. 55 + 0.31 =	: 4.72 days	
ime required. 2,26 + 1.01 +	for 10 cr -0.48 + 0.6!	en. 55 + 0.31 =	: 4.72 days	
ime required 2,26 + 1.01 +	for 10 cr -0.48 + 0.6!	en. 55 + 0.31 =	: 4.72 days	
ime required. 2,26 + 1.01 +	for 10 cr -0.48 + 0.6!	en. 55 + 0.31 =	: 4.72 days	
ime required 2,26 + 1.01 +	for 10 cr -0.48 + 0.6!	en. 55 + 0.31 =	: 4.72 days	
ime required. 2,26 + 1.01 +	for 10 cr -0.48 + 0.6!	en. 55 + 0.31 =	: 4.72 days	
ime required. 2,26 + 1.01 +	for 10 cr -0.48 + 0.6!	en. 55 + 0.31 =	: 4.72 days	

07	Metal Pipe & Fittings	12.	Topic of		LABOR-			2000 BAI			TOTAL
7]	Melai ripe & riiings	i Angle		OUTPUT		UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P
7	2"	;	Q-1	9	1.778	Ea.	. 133	53		186	227
<u> </u>	For couplings and unions use 3000 lb., type	316									
: 30	000 lb., type 304										٠.
	Coupling				;						. 44.
∵.	1/8"		1 Plum	19	.421	Ea.	2.41	14		16.41	23.50
ť	1/4" ·	;		19	.421		2.53	14		16.53	24
· · ·	3/8"			19	.421		3.04	14		17.04	24.50
	1/2"	5 4		19	.421		4.84	14		18.84	26.50
	3/4"			18	.444		7.30	14.80	·	22.10	30.50
)	1"		↓	15	.533		12.40	17.75		30.15	40:50
:	1-1/4"		Q-1	26	.615		28	18.40		46.40	58.50
į	1-1/2"	:		24	.667		32	19.95		51.95	65.50
•	2"		 	21	.762	V	46	23		69	85.50
	. Union.		'			'					
	1/8"	: .,	1 Plum	12	.667	· Ea,	25.50	22		47.50	61.50
;	1/4"			. 12	.667		25.50	22		47.50	61.50
- ; ,	3/8"			12	.667	111	27.50	22	, .	49.50	63.50
) 4.				11	.727		27.50	24	-,	51.50	66.50
 :	3/4"	:		10	.800		33.50	26.50		60	77
	1"	; •	↓	9	.889		56	29.50		85.50	106
	1-1/4"		Q·1	16	1		78.50	30		108.50	132
	1-1/2"		} }	15	1.067		88	32		120	146
	2"		V	13	1.231	V	123	37		160	192
30	000 lb., type 316		,			.					
	Coupling		-1								
1	1/8"		1 Plum	19	.421	Ea.	2.95	14		16.95	24.50
, /	1/4"			19	.421		3.25	14		17.25	24.50
-	3/8"			19	.421		3.46	14		17.46	25 ∜.
· ·	1/2"	:		19	.421	$\dashv \dashv$	5.60	14		19.60	27
i,	3/4"			18	.444		8.25	14.80		23.05	31.50
- ;	1"		V	15	.533		13.95	17.75		31.70	42:50
	1-1/4"	.	Q1	26	.615		32	18.40		50.40	63:50
	1-1/2"			24	.667		36.50	19.95		56.45	70
<u>;</u>	2"		↓	21	.762	V	53	23		76	93
	Union				Ţ,		•		:	· ;	·
į	1/8"		1 Plum	12	.667	Ea.	26	22		.:48	62:50
	1/4"	i		12 -	.667	\Box	26	22	_ 	48	62.50
	3/8"			12	.667		32	22	-	54	69 :
· · ·	1/2"	. }		11	.727	$\neg \uparrow \uparrow$	32	24		56	72 ·
: .	3/4"		;	- 10	.800		36.50	26.50	•	· . 63	80
	1"			9	889	\Box	63	29.50		92.50	114 %
*	1-1/4"		Q-1	16	i		94	30		124	149
r .	1-1/2"	1		15	1.067	-1-1	118	32		. 150	178
•	2"	1	↓	13	1.231	↓]	154	37		191	225
		1 1		:							
18 __	Plastic Pipe & Fittings			· ;							
PE, PLAS	STIC	1 25.5)						* * ;
	ass reinforced, couplings 10' O.C., hangers 3 pe	er 10'		,	* .						
	neral service			;					~ 		
	2" diameter	:	Q-1	59	.271	L.F.	9.65	8.10	1	17.75	23
	3" diameter	·		52	.308	71	13	9.20		22.20	28.50
(4" diameter			48	.333		15.85	10		25.85	32.50
	6" diameter			39	.410	+	23	12.30		35.30	43.50
·	8" diameter		Q2	49	.490		36.50	15.20		51.70	63,⊹
- ;-	10" diameter		-i- -l	41	.585	++	53.50	18.15		71.65	86.50
	10 diameter		-	36	.667	1 1	65.50	20.50		86	104

15100	Plastic Pipe & Fittings		$K_{i}^{(i)}$	DAILY	LABOR-			2000 BAI	RE COSTS	TOTAL
	Plasne Pipe & Firings				HOURS	UNIT	MAT.	LABOR	EQUIP. TOTAL	INCL 0&F
0200	High strength				11 11					130
0240	2" diameter	: 	Q-1	58	.276	L.F.	10.75	8.25	999 g 1 kasa ay 19	7
0260	3" diameter			51	.314		14.65	9.40	24:05	36.
0280	4" diameter	4	l	47	.340		17.65	10.20	27.85	35
0300	6" diameter			38	.421		26	12.60	38.60	47.
0320	8" diameter	* 1	Q2	48	.500		41	15.50	56.50	68.
0340	10" diameter			. 40	.600		60	18.60	78.60	
0360	12" diameter		₩	36	.667	4	73.50	20.50	94	113
0550	To delete coupling & hangers, subtract		<u> </u>		4	<u> </u>			· · · · · · · · · · · · · · · · · · ·	
0560	2" diam, to 6" diam.	7					33%	56%		1.,
0570	8" diam. to 12" diam.	•		 	7		31%	52%		1 12
	VC, high impact/pressure, cplgs. 10' O.C., hangers 3 per 10'	:	, ;		\ `;		3270	52. 7		
1020	Schedule 80		 		+ -					
1040	1/4" diameter		1 Plum	58	.138	L.F.	2.17	4.59	6.76	9
1060	3/8" diameter		1110/11	55	.145		2.26	4.84	7.10	
1070	1/2" diameter			50	.160		2.20	5.30	7.30	
1080	: 3/4" diameter	. :	├┼	47	.170	 	2.20	5.65	7.30	<u> </u>
1090	1" diameter			47	.170		2.20	5.65 6.20	7.85	i i
100	1-1/4" diameter	:		39	1 1		2.80	6.80	9.60	1
110	1-1/4 diameter 1-1/2" diameter			34	.205 .235		1	7.80	1 1	1
1120	2" diameter		01	55			3.01	8.70	10.81	15 16
1130			Q-1	52	.291 .308		1		11.89	1 .
1140	2-1/2" diameter			1	.320		3.30	9.20	12.50	17
1	3" diameter			50	.320		4.56	9.60	14.16	1
150	4" diameter		<u> </u>	46			6.05	10.40	16.45	- 22
1160	5" diameter	1		42	.381		10.35	11.40	21.75	
1170	6" diameter		₩	38	.421		9.30	12.60	21.90	4
1180	8" diameter	.s	Q-2	47	.511		14.95	15.85	30.80	1
1190	10" diameter			42	.571	4	23.50	17.75	41.25	
1200	12" diameter		*	38	.632	₩	30	19.60	49.60	62
1730	To delete coupling & hangers, subtract						600/	000/	<u> </u>	. '
1740	1/4" diam. to 1/2" diam.						62% 58%	80%		
1750	3/4" diam. to 1-1/4" diam.	<u> </u>		ļ	· · · ·		40%	73% 57%		
1760 1770	1-1/2" diam. to 6" diam.						1			
	8" diam. to 12" diam.		, .	·	· .		34%	50%		<u> </u>
	C, couplings 10' O.C., hangers 3 per 10'									ł
1820	Schedule 40		1.0	-	140	, -	1.00	4.02		
1860	1/2" diameter		1 Plum I	54	.148	LF.	1.90	4.93 5.20	6.83	
1870	3/4" diameter		<u> </u>	51	.157		2.06	5.80	7.26	10
1880	1" diameter			46	.174		2.57		8.37	
890	1-1/4" diameter			42	.190		2.61	6.35	8.96	
1900	1-1/2" diameter		*	36 ,	.222		2.81	7.40	10.21	14
1910	2" diameter		Q-1 :	59	.271		2.83	8.10	10.93	
	2-1/2" diameter	i	'	56	.286		3.52	8.55	12.07	16
930	3" diameter			53	.302	<u> </u>	4.05	9.05	13.10	
1940	4" diameter		1	48	.333		5.50	10	15.50	
950	5" diameter			43	.372		7.50	11.15	18.65	
960	6" diameter		(♦	39	.410		8.30	12.30	20.60	
970	8" diameter		Q-2	48	.500		13.15	15.50	28.65	
300	10" diameter			43	.558		27.50	17.30	44.80	
990	12" diameter	<u> </u>		42	.571		35	17.75	52.75	
000	14" diameter			31	.774		108	24	132	156
2010	, 16" diameter	<u>:</u>		23	1.043	A	136	32.50	168.50	198
340	To delete coupling & hangers, subtract			-1	٠.			-		1
360	1/2" diam. to 1-1/4" diam.					eiwa ee	65%	74%		1:3
370	1-1/2" diam. to 6" diam.				•		44%	57%	14.1	1
380	8" diam. to 12" diam.	. 1			i.		41%	53%	e je krije e	1.

08	Plastic Pipe & Fittings								RE COSTS		JOTAL
		1 45 19	CREW	ОИТРИТ	HOURS	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P
. 1	14" diam. to 16" diam.	•		1	1 3		48%	45%	1.42		37
:	Schedule 80			<u> </u>	: 1			ĺ		19.50	
į	1/4" diameter		1 Plum	ł	.138	L.F.	1:91	4.59	1	6.50	9.
	3/8" diameter	· .		55	.145		1.91	4.84	٠.	6.75	9.4
•	1/2" diameter	:		50	.160		2.08	5.30	30. 40	7.38	10.3
	3/4" diameter		1 -	47 -	.170		2.31	5.65		7.96	41.3
,	1" diameter		1	43	.186		2.84	6.20	†	9.04	.12:
	1-1/4" diameter			39	.205		3.02	6.80		9.82	13:6
:	1-1/2" diameter	1	1 🗼	34	.235		3,27	7.80		11.07	15.4
	2" diameter	. :	0-1	55	.291		3.57	8,70		12.27	17.
	2-1/2" diameter		 	52	.308	\vdash	3.86	9,20		13.06	18.3
4	3" diameter			50	.320		5.30	9.60		l I	
- :	4" diameter		╂-	46	.348		7.15	10.40		14.90	20.5
	5" diameter			ı			1	(' '	17.55	23.5
- :	6" diameter	<u> </u>	1	42	.381	\Box	9.75	11:40		21.15	28
:		•	♥ ¹	38	.421		11.35	12.60		23.95	31.
<u>:.</u>	a didition	<u> </u>	0-2	47	.511	\Box	18.10	15.85	<u> </u>	33.95	44
•	10" diameter	•		42	.571		28	17.75		·· 45.75	57.5
ţ		<u>:</u>		38	.632	₩	36	19.60		55.60	69
•	· · To delete coupling & hangers, subtract										•:
	1/4" diam. to 1/2" diam.			<u> </u>			66%	80%			Phy.
	3/4" diam. to 1-1/4" diam.				7		61%	73%	N 12	1.00	•17:
;	1-1/2" diam. to 6" diam.						41%	57%			
:	8" diam. to 12" diam.	:			i,		-31%	50%			3.5
: 5	Schedule 120			·	,			,			*:
	1/2" diameter		1 Plum	- 50	.160	L.F.	2.63	5.30		7.93	10.9
1	3/4" diameter		4	47	.170		3.03	5.65		8.68	11.9
	1" diameter	1		43	.186		3.89	6.20		10.09	13.6
٠.	1-1/4" diameter			39	.205		4.50	6.80		11.30	15.2
	1-1/2" diameter	٠. ١		33	242		5.05	8.05		13.10	17.5
:	2" diameter	į,	Q1	54	.296		6.10	8.85	,	14.95	20:
	2-1/2" diameter			52	.308	\dashv	8.30	9.20	, ,	17.50	23
1	3" diameter	• .		49	.327		10.45	9.75		20.20	26.5
 -	4" diameter	<u>-</u>	H	45	.356		15.70	10.65	1,	26.35	33.5
	6" diameter	: !		37	1						
	To delete coupling & hangers, subtract		I ₹		.432	₩.	27.50	12.95		40.45	50
ž.	A 4800 1 10 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	ĺ	,	i. ,			500/	740/		· · ·	
- ''			 				52%	74%			+1. *1.
<u> </u>					9		30%	57%	1. 175.4	•	
DVO	6" diam.		·	·	-		17%	50%			
	pressure, couplings 10' O.C., hangers 3 per 10'				į.	Ì	ļ		* 5 * 1		
	DR 26, 160 psi					<u> </u>			74. 74	*	<u>.</u>
1	1-1/4 didilictei		1 Plum	42	.190	L.F.	2.44	6.35	1,77	8.79	12.3
Ąú	· · · · · · · · · · · · · · · · · · ·	4 1		36	.222	$\perp \perp \perp$	2.62	7.40		10.02	14.1
	1.4 2" diameter		Q-1	59	.271	IT	2.80	8.10		. 10.90	15.4
	L1/L didiffictor	<u>.</u>		56	.286		3.15	8.55	y .	11.70	16:4
:	3" diameter			53	.302		3.65	9.05		12.70	17.6
j 4:	4" diameter	\$ 7		48	.333		5.10	10	٠. ا	15.10	20.5
:	6" diameter	1. 1. 1.		39	.410	++	8.05	12.30		20.35	27.5
	8" diameter		Q2	48	.500	1	13.15	15.50	s 5	28.65	38
:-	To delete coupling & hangers, subtract	- 1	1			-					
	1-1/4" diam.			.	\$	1	63%	68%			
, <u> </u>	1-1/2" diam. to 4" diam.		\vdash		3		48%	57% -		·	***
		77.16		1	3	1	1	1			
<u> </u>	6" diam. to 8" diam.		1.0		-111		60%	54%		- 221	
─ : SI	DR 21, 200 psi, 1/2" diameter	. 1	1 Plum	54	.148	L.F.	2.01	4.93		6.94	9.6
	3/4" diameter	4	$\sqcup \sqcup$	51	.157	$\perp \perp$	2.18	5.20		7.38	10:3
	1 didifictor	: 1	1	46:	.174		2.63	5.80		8.43	11.6
į ar	iii 1-1/4" diameter		1 L 1	42	.190	\perp \mid	2.75	6.35	.:-	9.10	12.6

15	108 Plastic Pipe & Fittings	1	MA V		LABOR-				RE COSTS		1004
, .,.		1. j. š.j.n			T HOURS	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL (M
3770	1-1/2" diameter		1 Plum		.222	L.F.	2.96	7:40	ीत हर १०%	1	, ju
3780	2" diameter	į	Q1	59	.271		3.17	8.10		€ 05011.27	I
3790	2-1/2" diameter	î,		56	.286		4.15	8.55	* * * * 1.	12.70	1
3800	3" diameter	- (53	.302		4.58	9.05	1,37 % 5	13.63	
3810	4" diameter			48	.333		6.25	10 -		16.25	U
3830	6" diameter		₩	-39	.410		10.05	12.30	5-11-4	22.35	
3840	8" diameter		Q2	48	.500	4	16.70	15.50	54.	32.20	
4000	To delete coupling & hangers, subtract	<u>;</u> ;				'					
4010	1/2" diam. to 3/4" diam.	3 .					71%	77%	n ngga		
4020	1" diam. to 1-1/4" diam.						63%	70%	·		
4030	1-1/2" diam. to 6" diam.	1.5	-	╁			44%	57%			
4040	8" diam.	- :	;		1819/		46%	54%			
4100	DWV type, schedule 40, couplings 10' O.C., hangers 3 per 10'		 		1		7070	3470	ļ	10.	
4120	ABS								47	4	
4140	1-1/4" diameter	- :	1 Plum	42	.190	L.F.	2.58	C 25	£164.	0.02	
4150	1-1/2" diameter		I I IUIIII	36	.222	L.I.	2.56	6.35		8.93	
4160	2" diameter		01				-11	7.40	·	9.96	- 10
4170	3" diameter	Ý.	Q1	59	.271		2.66	8.10	1 0	10.76	11
4170		- ;	1 1 4	53	.302		3.28	9.05	: :	12.33	
	4" diameter	;		48	.333		4.44;	10,		14.44	
4190	6" diameter		*	39	.410	₩	7.10	12.30	1, 31	19.40	N.
4360	To delete coupling & hangers, subtract				1 1						
4370	1-1/4" diam.						64%	68%		, str	9
4380	1-1/2" diam. to 6" diam.	- i			15		54%	57%	:7		33
1400	PVC ·	9 3			1.0						
1410	1-1/4" diameter	1 .	1 Plum	42	:190	L.F.	2.66	6.35	:	9.01	
1420	1-1/2" diameter	:		36	.222		2.73	7.40	a 1.	10.13	111
460	2" diameter		Q1	59	.271		2.91	8.10		11.01	117
1470	3" diameter			53	.302		3.79	9.05		12.84	1
1480	4" diameter	: :	J.	48	.333	7	5.10	10	٠ ,	15.10	
1490	6" diameter		↓	39	410		7.40	12.30	.1:	19.70	1).
500:	8" diameter	i.	Q2	48	.500		16.35	15.50		31.85	7/1
750	To delete coupling & hangers, subtract	:				•		İ	,		
760	1-1/4" diam. to 1-1/2" diam.						71%	64%			
770	2" diam. to 8" diam.	\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \		12			60%	57%	•		
800	PVC, clear pipe, cplgs. 10' O.C., hangers 3 per 10', Sched. 40	· ·		<u> </u>	:						
840	1/4" diameter	1,	1 Plum	59	.136	L.F.	2.32	4.51		6.83	ı
850	3/8" diameter			56	.143		2.51	4.75		7.26	1
860	1/2" diameter			-54	.148		2.87	4.93		7.80	10
870	3/4" diameter	-		51	.157		3.36	5.20	?	8.56	
880	1" diameter			46	.174		4.51	5.80		10.31	115 115 115 115 115 115 115 115 115 115
890	1-1/4" diameter			42	.174	\dashv	5.25				1
900	1-1/2" diameter			36	222		1	6.35		11.60	
910	2" diameter		01			44	5.95	7.40	** ** `	13.35	111
- 1		3 1	Q-1	59 !	271		7.25	8.10	Ì	15.35	á)
920	2-1/2" diameter			56	.286		10.20	8.55		18.75	И
930	3" diameter	()		53	.302		12.75	9.05		21.80	21
940	3-1/2" diameter		11	50	.320		15.65	9.60		25.25	J.
950	4" diameter		*	48 .	.333	V	16.40	10		26.40	ü
250	To delete coupling & hangers, subtract			1,0	12 3 12 2				·	·	
260	1/4" diam. to 3/8" diam.		.]		1		60%	81%		1 10 11 11 11 13 13 13	
270	1/2" diam. to 3/4" diam.	1					41%	77%	· ·	0	
280	1" diam. to 1-1/2" diam.	. 5				1	26%	67%			
290	2" diam. to 4" diam.		- 1	Ì		ļ	16%	58%			
360	CPVC, couplings 10' O.C., hangers 3 per 10'										
1		1	- 1					1	2. 15. 14.2		
380	Scriedule 40	' : 提									
80	Schedule 40 1/2" diameter	\dashv	1 Plum	54	.148	L.F.	2.63	4.93	2 (92) 42 (72)	7.56	105

) Building Services Pip		35.52.6E						- 000		
108	Plastic Pipe & Fittings	AraK.	M X		LABOR-	:	:		E COSTS	Ter 1984	TOTAL
-		980 353		OUTPUT		UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P
	1" diameter		1 Plum	46	.174	L.F.	3.98	5.80	•	9.78	13.15
	1-1/4" diameter	:-		42	.190		4.57	6.35	· .	10.92	14.65
	1-1/2" diameter	. :	₩	: 36	.222		5.20	7.40	\$ "" · · ·	12.60	16.90
	2" diameter	1	0-1	59	.271		6.05	8.10		14.15	19:
	2-1/2" diameter	:		56	.286		8.85	8.55		17.40	22.50
•	3" diameter	:		53	.302		10.55	9.05		19.60	25.50
; ,	4" diameter			48	.333		14.50	10		24.50	31 · ·
ŀ	6" diameter		↓	43	.372		26	· 11.15		37.15	45.50
el;	To delete coupling & hangers, subtract	:		. "	in the second						1.7
. :	1/2" diam. to 3/4" diam.	٠					37%	77%			
)	1" diam. to 1-1/4" diam.				- 3		27%	70%	31.		
ot i	1-1/2" diam. to 3" diam.				ŝ.		21%	57%			
	4" diam. to 6" diam.				4:		16%	57%			
	: : Schedule 80								,		
	1/2" diarneter		1 Plum	50	.160	L.F.	2.74	5.30	::	8.04	11.05
I,	3/4" diameter	,	1	47	.170		3.22	5.65		8.87	12.10
	1" diameter			43	.186		4.24	6.20		10.44	14 %
y [†]	1-1/4" diameter	*		39	.205	.	4.96	6.80		11.76	15.79
nd;	1-1/2" diameter	- 1		. 34	.235		5.70	7.80		13.50	18.1
. ;	2" diameter		Q-1	55	- 291		6.85	8.70		15.55	20.50
,,	2-1/2" diameter	<u></u>		52	.308		9.90	9.20		19:10	25
12	3" diameter	:		50	.320		12.10	9.60		21.70	: 28∋
J	4" diameter			: 46	.348		17	10.40		27.40	34.50
	6" diameter			38	.421		31.50	12.60		44.10	53:5
	8" diameter	·	Q2	47	.511	+	68.50	15.85	·····	84.35	. 99:5
	To delete couplings & hangers, subtract	;	j. 1	<u> </u>	- 5	•					
	1/2" diam. to 3/4" diam.				:		44%	77%			
バ	1" diam. to 1-1/4" diam.		:	<u> </u> : .			32%	71%			s 1
)	1-1/2" diam. to 4" diam.						25%	58%			• :
/ I p	: 6" diam. to 8" diam. :	:				ľ	20%.	53%			· **:
· ·	CTS, 1/2" diameter		1 Plum	54	.148	L.F.	2.08	4.93		7.01	· 9:7
). 	3/4" diameter			51	.157		2.80	5.20		8	e di
<u>'</u>	1" diameter		 	46	.174		3.58	5.80		9.38	12:7
	1 1/4"	, 1	 	42	.190	-	4.22	6.35		10.57	14.2
16:	1 1/2" diameter			₃ 36	.222		5.05	7.40		12.45	16.7
	2" diameter	: .	Q:1	: 59	.271		7.10	8.10		15.20	201.
· · · · · · · · · · · · · · · · · · ·	To delete coupling & hangers, subtract		\	£	 	: V					
1.	1/2" diam.	: ; ;	ŀ		10 A A C T .		51%	79%			1 4
) :	3/4" diam.	- 	·		1, 1, 1		40%	76%			(58)
T.	1" thru 2" diam.	3 -].			72%	68%			
Poh	yethylene, flexible, no couplings or hangers		l		5	· -				 	
, ,	te: For labor costs add 25% to the couplings and fittings l	ahor total		2	1	:					į.
	SDR 15, 100 psi	2001 (041)									
Pr	1	4,000	; :		4 /	L.F.	.17			.17	.1
	, 374 diameter	- : :		-	1 2	- 	.22			.22	.2
	* Ciditiotoi			ľ			.40			.40	ı.
<u></u>	1-1/4" diameter	<u> </u>		-	+	-	.50			50	1
₹	1-1/2" diameter	81 1			* .		.80			.80	
	2" diameter	· · · · ·	<u> </u>		7.5		.00				
<u> </u>	SIDR 9, 160 psi	3)	V 7 K + 1,5]: .		: L.F.	.23	•		.23	1
<u>}</u> ;	1/2" diameter			-		L.F.	.23			.23	
~	3/4" diameter	:		ľ.	3		1			.36	
<u>1</u>) 1" diameter	<u> </u>	<u> </u>	ļ	1	$\vdash \vdash$.36			.60	
	1-1/4" diameter		l.	ľ			.60			.84	1.
1	1-1/2" diameter		ļ	<u> </u>	4	<u> </u>	.84			1.38	
	2" diameter	:		j		♦	1.38			i	•
ıł .	SDR 9, 200 psi	:		l	Li	41				15 25 %	,

• • • •	3.11	Plastic Pipe & Fitting	e un cara Na A	क्या है।	CREW	DAILY OUTPU	LABOR- T HOURS		MAT.	LABOR	RE COSTS EQUIP.	TOTAL	TOTAL Incl 0&P
8150	1 '	3/4" diameter	•	7		1	1 200	L.F.	.20		4.64		-5%2 2
8160	-	1" diameter		! .	1				.33			A33	
8170 8420	1 :	1-1/4" diameter SDR 7, 250 psi			;		2 6	₩	.49		Aver 1	.49	
8440		3/4" diameter	· · · · · · · · · · · · · · · · · · ·		ļ	1	1 . 5	 	00		1 *	٠.	
8450		1" diameter		. Î.,			1,40	L.F.	.29 .46			.29	32
8460		1-1/4" diameter			1 1	1	1 5	$\vdash \vdash$.79		, c. 3 - 21	.46	्र.51 ०७
8800	PVC	, type PSP, drain & sewer, belled end ga	sket int., no hngi					Y	./5				.87
8840	├ ── <i>÷</i>	3" diameter		· · ·	F ;	1	. ;	L.F.	.32		7 (1549)	.32	: 35
8850		4" diameter		: 1 3-	l	'			.40			.40	:44
8860	:	6" diameter		į		1.	1	 	.89		. ,	.89	:98
9000		Perforated		1 1			3	 		1.73%			æ
9040	1	4" diameter		:			. 4	L.F.	.42			.42	.46
	2			:			18.7					Specifical Control	
		ASTIC, FITTINGS	· .	:		1	1 1.				14,	, .	470
0030	Epo	ky resin, fiberglass reinforced, general se Elbow, 90°, 2″	rvice	·		02	٠. ا		45.50				
0100	, 4	3" 2 · 5" 19			Q1	23 16	.696	Ea.	45.50	21	٠,٠٠	66.50	81:50
0110		4"			-	13	1.231		64.50 104	30 37	. Na Turks	94.50 141	116 170
0120	į, v	6"	:	. ?		8	1.251		156	60		216	263
0130	:	8"			02	: 9	2.667		260	83		343	4103
0140	2	10"	•	:	:	7	3.429		360	106		466	555
0150	1	12"		: ;		5	4.800		500	149	1,15.4	649	775
0160	į.	45° Elbow, same as 90°		2.7				'					
0170		Elbow, 90°, flanged		j. 1 .			🎘				ngi-, a	Wu T	(10)
0172	:	2"		1	Q-1	23	.696	Ea.	91	. ; 21	₹15. ±1	··.·· 1·12	132
0173	}	3"	,	2		16	1		105	:30	,1,0	135	<u>1</u> 62€
0174		4" 6"			!	13	1.231		138	- 37		" 175	
)177		8″	٠	•	*	-8	2.		249	60	27.5	309	\
)178		10"		· (Q2	9 7. **	2.667 3.429		450 615	83		533	615
179	:	12"		4 4		5	4.800		835	106 149		721 984	835
186	· .		· · · · · · · · · · · · · · · · · · ·				7,000		033	143		904	1,150
188		2"		1 4	. Q1	23	.696	Ea.	91.50	. 21.		112.50	133
189		3″		, , , , , , , , , , , , , , , , , , , 		16	- 1		105	30		135	162
190		. 4"		, ,		13	1.231		137	37		174	207
192	:	6" .			*	8	2		251	.60		311	365
193		8″		:	Q-2	9	2.667		450	83		533	620
194		10"				7	3.429		615	106	,	721	835
195	,	12"		- 1 -	↓	5	4.800	$\perp \downarrow \perp \downarrow$	835	149		984	1,150
290 300		Tee, 2" 2.5" \ 7		·	Q1	17	.941		61	28.		89 1	110%
310	 ,	4"		· · · · ·		10	1.600: 2	- •	71.50 85	. 48· 60		119.50 145	151
320	:	6"		· :		5	3.200		228	96		324	184 🦄 395
330		8"			Q-2	6	4	++	263	124		387 .	475
340		10"				5	4.800		420	149		569	685
350		12"		- ;	+	4	6	+	510	186	1 7 .	696	840
352		Tee, flanged		;:	_ '	- [;	•					
354	-	2"		:	Q1	17	.941	Ea.	124	28		152	179
355	:	3"				10	1.600		166	48		214	256 : 18
356	٠	4"		1	-	8	. 2		185	60		245	294
358		6"		<u>;</u> _	<u>000</u>	5	3.200	44	365	96		461	545
359	<i>]}</i>	-	i. Sa	- 1	Q-2	6	4		625	124	** .	749	875
360 361	- \ \	10"				5	4.800		905	149		1,054	1,7
365		Wye, flanged		* \$	▼	4	6	₩	1,150	186		1,336	1,550
100		itye, nangeo			ì,								24.73
		4											

		1	14 3 7 7 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	DAILY	LABOR	C 4/2/2/2019/5/46		2000 RA	RE COSTS		TOTAL
1108	Plastic Pipe & Fittings	ده. انهار ونفره	CREW	OUTPU			MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P
Ĭ	2"		0-1	17	.941	Ea.	320	28	LQUII.	348	395
3)	: 3 ⁿ		Ĭ	10	1.600	Į.	355	48		: 403	465 <u>:</u>
1	4"		\vdash	8	2	\vdash	440	60		500	400: 575:
Ţ	6"	. :		5	3.200	.	530	96		626	725
2	. 8"		Q-2	6	4	$\vdash \vdash$	690	124		814	945
Į.	10"		٧2.	5	4.800		1,175	149		I	
	12"	<u>i_</u>		4	6	 	1,175	186		1,324	1,500
'n	Couplings		. 🔻	4	9	*	1,420	180		1,611	1,825
0	2"		Q-l	28	.571	<u> </u>	10.90	1710			
1	3"		(A)	20	l	Ea. I		17.10		28	38
<u></u>		<u> </u>		17	.800		18.85	24		42.85	56.50
0	6″			1	1		20			48	64.50
-	8"		▼ 0.2	12	1.333		38	40		78	103 %
	10"		Ų-Z	1	1		58	49.50		107.50	139
0	12"		$\vdash \vdash$	11	2.182		87.50	67.50		155	198
1	•	(*	10	2.400	*	117	74.50		191.50	242
1	High corrosion resistant couplings, add			· ·		ļ	30%				118
	Reducer, concentric, flanged	÷	١,,	20	-50		,,,,	10		 	
6 6	2" x 1-1/2"		Q-1	30	.533	Ea.	132	15.95		147.95	169
P)	3" x 2"	ز		24	.667		150	19.95		169.95	195
	4" x 3"		<u> </u>	19	.842	$\sqcup \sqcup$	158	25		183	212
SI :	6" x 4"		*	15	1.067		206	32		238	276
2	8" x 6"		0.2	. 16	1.500		289	46.50		335.50	390:
<u> </u>	10" x 8"			13	1.846		385	57.50		: 442.50	510
	12" x 10"		. 🔻	11	2.182	*	555	67.50		622.50	710
	Adapter, bell x male or female	·									Aug.
	2"		01	. 28	.571	Ea.	19.65	17.10		36,75	47.50
	3"	i '	.	: 20	800		. 25	24		. 49	63.50
V.	4"		\perp	17	.941	- -	34.50	28		62.50	80.50
2	6"	5	*	12	1.333		68.50	40		108.50	136
1	8"		Q.2	15	1.600		95.50	49.50		145	180
	10"			11	2.182	♦	168	67.50		235.50	287
	Flange										YE
	2.3" 39	,	Q1	46	.348	Ea.	17.40	10.40		27.80	35
	3"		\perp	32	.500		21	14.95		35.95	46
	4"	· ·		26	.615		29.50	18.40		47:90	60.50
	6"		*	16	1		50	30		. 80	101;
ŀ	8"	1	Q2	. 18	1.333		82	41.50		123.50	153
	10"	j 1		14	1.714		114	53		167	207
	12"	: l	. ♦	10	2.400	♦	161	74.50		235.50	290 ***
	PVC schedule 80		. *		#. }						
1	90° elbow, 1/2"	; }	1 Plum	. 18	.444	Ea.	.89	14.80		15.69	23:50
	3/4"			17	.471		1.14	15.65		16.79	25 🔆
	A SAMPLE OF THE	<i>i</i> 1		15	.533		1.83	17.75		19.58	29
<u> </u>	, -	2.18	,	14	.571		2.44	19		21.44	31:13
1	1-1/2"	1	+	13	.615		2.62	20.50		23.12	34
	2"	100	Q-1	22	.727		3.16	22		25.16	36.50
E. :	3"	à .			1.143		8.30	34		42.30	61
	4"			12	1.333		12.65	40		52.65	74.50
	6"	<u>;</u> , , ;	V	7	2.286	77	42.50	68.50		111	15131
	8" - 3"		Q.2	8	å		117	93		210	270 101
Towns.	45° elbow, 1/2"		1 Plum	18	.444	7	1.68	14.80		16.48	24.50
	3/4"			17	.471		2.54	15.65		18.19	26.50
	1"	: 1		15	.533	-	3.84	17.75		21.59	31
	1-1/4"			14	.571		4.87	19		23.87	34:
<u>Fa</u>	1-1/2"		+	13	.615	++	5.75	20.50		26.25	37:50
Ps.											W. 1.50

15108	B Plastic Pipe & Fittings	6			LABOR-			2000 BAI	RE COSTS	186, 85.	TOTAL
		1. 图 1. 以外海线	CREW	OUTPU	HOURS	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 0&
2320	3″	,	Q-1	14	1.143	Ea.	19.05	34		53.05	73
2330	, . 4"			12	1.333		34.50	40		74.50	. 98
2340	6"		V	7	2.286		43	68.50		111.50	152
2350	. 8"		Q-2	8	3		83	93		176	232
2400	: Tee, 1/2"		1 Plum	12	.667		2.50	22		24.50	36
2420	3/4″			11	.727		2.62	24		26.62	39
2430	. 1"			10	.800	\vdash	3.27	26.50		29.77	43
2440	1-1/4"			9	.889		9	29.50		38.50	54
2450	1-1/2"			8	1 1	$\vdash\vdash$	9	33.50		42.50	60
2460	2"		♥ Q-1	14	1.143		11.25	34		45.25	64
2470	3"	*	V-1	9	1.778	\vdash	15.30	53			
2480	. 3			ĺ	2		1			68.30	97
2490	6"		 - -	8		Н-	17.70	60		77.70	110
ł		•	♥	5	3.200		60.50	96		156.50	212
2500	8"	<u> </u>	Q-2	6	4		85.50	124		209.50	282
2510	Flange, socket, 150 lb., 1/2"		1 Plum	34	.235		4.84	7.80		12.64	17
2514	3/4"			32	.250		5.20	8:30		13.50	18
2518	1"	,		28	.286		5.80	9.50	٠,	15.30	20
2522	1-1/2"		▼	24	.333		6.10	11.10		17.20	23
2526	. 2"		Q·1	42	.381		8.10	11.40		19.50	. 26
530	: 4"		!	30	.533		17.45	15.95		33.40	. 43
534	. 6"		V	22	.727		27.50	22		49.50	63
2538	. 8″	•	Q-2	26	.923		50	28.50		78.50	. 98
550	Coupling, 1/2"		1 Plum	18	.444		1.61	14.80		16.41	24
570	3/4"			17	.471		2.17	15.65		17.82	26
580	: 1"			15	.533		2.23	17.75		19.98	29
590	1-1/4"			14	.571		3.39	19		22.39	32
600	1-1/2"		 	13	.615		3.66	20.50		24.16	35
610	2"		01	22	.727		3.92	22		25.92	37
620	3″			19	.842		11.10	25		36.10	50
630	4"			16	1		13.90	30		43.90	61
640	· · · 6"		 	12	1.333		30	40		70	93
650	8"		♦ Q-2	14	1.714		54	53		107	140
660	10"		1	13	1.846		84	57.50		141.50	179
670			.	12	2		1 1			:	
1	12"			12			112	.62		174	217
1	PVC (white), schedule 40, socket joints	: `		00	354	_					57
760	90° elbow, 1/2″		1 Plum	22	.364	Ea.	.23	12.10		12.33	18
770	3/4"			21	.381		.25	12.65		12.90	19
780	. 1"		$oxed{oxed}$	18	.444		.45	14.80		15.25	23
790	1-1/4"	•		17	.471		.80	15.65		16.45	24
800	1-1/2".		\	16	.500		.85	16.65		en s 17:50	26
810	2"	: ::	Q1	28	.571		1.34	17.10		∘18.44	27
820	2-1/2"	· :		22	.727		4.06	22		26.06	37
330.	3"	,		17	.941		4.86	28		32.86	48
	4"	· · · · · · · · · · · · · · · · · · ·		14	1.143		8.70	34		42.70	61
	5″			12	1.333		22.50	40		62.50	85
350	6"		₩ -	8	2		27.50	60		87.50	121
850 860			Q-2	10	2.400		77	74.50		151.50	198
350 360	8"		\ \-		.364	-	.37	12.10		12.47	18
850 860 870			1 Plum.	22	.004						
850 860 870 980	8" 45° elbow, 1/2"						.57	12.65		13.22	19
850 860 870 980	8" 45° elbow, 1/2" 3/4"			21	.381		.57 .68	12.65 14.80			
850 860 870 980 990	8" 45° elbow, 1/2" 3/4" 1"			21 18	.381 .444		.68	14.80		15.48	23
850 860 870 980 990 990	8" 45° elbow, 1/2" 3/4" 1" 1-1/4"			21 18 17	.381 .444 .471		.68 .96	14.80 15.65		- 15.48 16.61	23 24
850 860 870 980 990 900 910	8" 45° elbow, 1/2" 3/4" 1" 1-1/4" 1-1/2"		1 Plum. ₩	21 18 17 16	.381 .444 .471 .500		.68 .96 1.20	14.80 15.65 16.65		15.48 16.61 17.85	23 24 26
840 850 860 870 980 990 900	8" 45° elbow, 1/2" 3/4" 1" 1-1/4" 1-1/2" 2"	:		21 18 17 16 28	.381 .444 .471 .500		.68 .96 1.20 1.57	14.80 15.65 16.65 17.10		15.48 16.61 17.85 18.67	23 24 26 27
850 860 870 980 990 900 900	8" 45° elbow, 1/2" 3/4" 1" 1-1/4" 1-1/2"		1 Plum. ₩	21 18 17 16	.381 .444 .471 .500		.68 .96 1.20	14.80 15.65 16.65		15.48 16.61 17.85	19 23 24 26 27 37 49

N. 4. V.	1		Code Yes			DAILA	LABOR		an essa escripturates tracto	ንስሳሳ ወላ	RE COSTS		
108		Plastic Pipe	& Fittings						MAT.	LABOR	EQUIP.	TOTAL	TOTAL
7	7	5"			Q1	12	1.333		22.50	40	EQUIP.	101AL 62:50	INCL 0&P
		6"			T T	8	2	La.	28	60			
		8"		·	0.2	10	2.400	╂╌├─	93	74.50		88	122 ;
Į.		Tee, 1/2"		ş	1 Plur	{	.571		1.	ł		167.50	215
1		3/4"		:	. 1101	13	.615		.28	19		19.28	29
		1"		4		12	.667		Į.	20.50		20.82	31.50
	:	1-1/4"		<u> </u>	+		. t	1-1-	.59	22		22.59	34 .
	1	1-1/4"		•		11	.727		.94	24		24.94	37.50
<u> </u>	. ,	2"		:	▼	10	.800	 	1.13	26.50		27.63	41 %
4.	•	2-1/2"		:	Q·1	17	.941		1.65	28		29.65	44:50
	-	3"		<u>.</u>		14	1.143	+-	5.45	34		39.45	58.5.
		4"		1		11		1	7.15	43.50		. 50.65	74
<u> </u>	·	5″			+		1.778	—	12.90	53		65.90	94.50
	٠.	6"				8	2 200		31	60		91	125
1		8"		<u>, </u>	V Q-2	5	3.200		43.50	96		139.50	193
	٠	Coupling, 1/2"		:	1 Plum	1	361		53	124		177	246
		3/4"			1 1100	21	.364		.18	12.10		12.28	18.50
_		3/4 1″		:		1			.24	12.65		12.89	19.40
ļ		1-1/4"		:		. 18 :	444		.41	14.80		15.21	23
١,	:	1-1/4"		•		17 16	.471		.57	15.65		16.22	24
	· 3				V Q1	28	.500 .571	lacksquare	.61 .95	16.65		17.26	25.50
•	:	2-1/2"			T Vi	20	.800		1	17.10		18.05	27
<u> </u>	<u>.</u>	3"		<u> </u>	+	19	.842	-	2.08 3.27	24		26.08	38:50
!		3. 4"	•			19	,042		4.72	25 30	*	28.27	41.50
		5"			++	14	1.143	\vdash	8.65	30	- /	34.72	50.50
A Commence of the Commence of	×.,	. 6"		:		12	1.333		14.90	40		42.65	61.50
1	7	8"			Q-2	14	1.714		28	53		54.90 81	77
1	مار معد	J	edule 40, socket weld	:	Y.	17	1./14	▼	20	33		01	1115
	 	3/4"	odalo 10, obonet nela		1 Plum	20	.400	Ea.	.70	13.30		14	21.
		1"		;		18	.444	1 1	1.19	14.80		15.99	24:3
		1-1/2"			1 😾	16	.500	\vdash	1.25	16.65		17.90	26.50
		2"		i i	· Q-1	31	.516		1.59	15.45		17.90	25.50
		· 4"				22	.727	\vdash	7.05	22		29.05	41:07
		- 6″	•			14	1.143		17.45	34		51.45	71
		8"		3.7	Q-2		1.333		61	41.50		102.50	130
		Reducing insert, soci	ket weld x female/male thread					•	٠.	12.00		102.50	
	<u>.</u>	1/2"			1 Plum	24	.333	Ea.	1.41	11.10		12.51	18.30
	; 	3/4"		ą.	: 1	23:4	.348		.87	11.55		12.42	18.45
-	;					. 20	400		1.22	13.30		14.52	21.50
		1-1/2"	: •	4 1		. 16	.500		2.20	16.65		18.85	27.50
		2"		- · ·	Q1	26	.615	++	1.17	18.40		19.57	29.50
	<u>.</u>	·. 4"	•	· · · · · · · · · · · · · · · · · · ·			1.143	1	4.61	34		38.61	57.13
		Male adapter, socket	weld x male thread			- :	4.1						; · ·
		1/2"		- 3	1 Plum		.333	Ea.	.27	11.10		11.37	17.05
		3/4"		1.		23	.348	11	.30	11.55		11.85	17.85
	; ;	1"		:		20	.400		.53	13.30	.,	13.83	20.50
	: ;	1-1/2"		· ; ; .		16 _{.24.}	.500	++	.87	16.65		17.52	26.50
	((),	0			.Q1	26	.615		1.14	18.40		19.54	29:50
		4" .		7	7 1		1.143		6.30	34		40.30	59 ±
			et weld x female thread	· · · · · · · · · · · · · · · · · · ·	.	1.17	1.175	▼	0.50	34		40.50	93 .a
		1/2"	· · · · · ·		1: Plum:	24	.333	Eà.	33	11.10		· 11.43	17.10
_	· N	3/4" .		. !	1 1011115	23	.333	<u> </u>	.42	11.55	}	11.43	17.10
-{)-	1"			. - 	20	.400		.42	13.30		13.79	20.50
1		1-1/2"				ŧ	.500		.87	16.65	. [٠.,
	.,.	2"		;	Q:1		.615	++	1.17	18.40		17.52	26⊚≽ 29.50
		. 4") i	4.7	· ·	1.143		6.60	34		40.60	29.50 59.50
		•	the state of the s	10 B]	14	1.145	- 1	0.00 (.34	- 1.	4U.DU	:09:50

15109	Plastic Pipe & Fittings		rii vi		LABOR-		······································	2000 BAR		no gan i	TOTAL
14 14 14 14 14 14 14 14 14 14 14 14 14 1	- 발표 기계 기계 기계 기계 기계 기계 기계 기계 기계 기계 기계 기계 기계		CREW	OUTPUT		UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 08
3800	PVC, schedule 80, socket joints		14						1		\$\langle \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \
810	Reducing insert		. 5)	00	240	-		11.55		10.00	ا ا
812	3/4"		1 Plum:	23	.348	Ea.	.67	11.55		12.22	
813	. #1. 1"			20 · ·	.400		1.91	13.30		15.21	2
3815	1-1/2"		*	16	.500		4.09	16.65		20.74	2
3816	2"		Q1 :	28	.571		5.35	17.10		22.45	3
817	4"			16	1.		22	.30		52	7
3818	6"	•	*	12	1.333		31	40		71	9
3819	8"	1.0	Q-2	14 .	1.714	▼	22.50	53		75.50	10
3830	Reducing insert, socket weld x female/male thread				4. 1						J.
3832:	1/2"	à	1 Plum	24	.333	Ea.	1.78.	11.10		12.88	j
3833	3/4"		. :	23	.348		1.11	11.55		12.66	· 1
3834	: 1"	,.		20	.400		1.92	13.30		15.22	2
3836	1-1/2"		₩	16 -	.500		3.22	16.65		19.87	.2
3837	. 2"		0.1	28	.571		4.66	17.10		21.76	3
3838	4"		*	16	1	. ↓	41	30		52m 71	9
844	Adapter, male socket x male thread		<u>.</u> ,		3 1					11	7
846	1/2"	2. 1	1 Plum	24	.333	Ea.	1.01	11.10		12.11	1
847	3/4"	(23	.348		1.11	11.55		12.66	
848	1"	,		- 20 -	.400		1.92	13.30		15.22	
850	1-1/2"	- : 1		16	.500		3.22	16.65		19.87	1 4
851	2"	i d	. Q1 :	28	.571		4.66	17.10	İ	21.76	
852	: 4"		3.0	16	1		10.45	30		40.45	
860	Adapter, female socket x female thread			1		▼					
862	1/2"		1 Plum	24	.333	Ea.	.81	11.10		11.91	
863	3/4"	, i n	1 1011	23	.348	l iii	2.88	11.55		14.43	
	7/4	3 1 1	 	20	.400	\vdash	4.25	13.30		17.55	
864	- ·			16	.500		8.45	16.65	garja reger	25.10	1 ;
3866	1-1/2"	- 1	0-1	28	.571		14.75	17.10		31.85	
3867	-		Α,	16	1		45	30		75	
3868	4"			10	-		+5			.,,	-
3872	Union, socket joints		1 Plum	19	.421	Ea.	4.25	14	•	18.25	1.
387.4	1/2" 3/4"		1 1 10111	18	.444	La.	5.40	14.80	· ·	20.20	
3875			▎	15	.533		6.15	17.75	}	23.90	1
8876	11/0	1 1		. 13	.533	1-	13.85	20.50		34.35	4
3878	1-1/2"	: :	▼	27	.593	1	18.80	1		36.55	:
3879	2" .		Q1	. 21	 	*	10.00	17.73		30.00	
3888	Сар	3	1 Di	26	200	, '	202	7.40		9.43	
3890	1/2"	<u>, , , , , , , , , , , , , , , , , , , </u>	1 Plum	I	.222	Ea.	2.03	7.40		9.93	:
3891	3/4"			34	.235		2.13	8.85		12.65	4
3892	. 1"	· ·	<u> </u>	30	.267	 -	3.80	10.25		14.83	
3894	1-1/2"		*	. 26	.308		4.58	1		19.95	•
3895	·· 2"		01	44	.364	1 1	9.05	10.90			
3896	4"		.	32	.500		36.50	14.95	14.3	102.95	1
897	6"	: '	*	24	667	 -	83	19.95	<u> </u>		
3898	. 8"		Q-2	. 28	.857	+	107	26.50		133.50	
	DWV, ABS, non pressure, socket joints	3 1			- 4	<u> </u>	ļ	1 - 2 - 2 -		1.55	
1540	1/4 Bend, 1-1/4"	7 %	1 Plum	1	.471	Ea.	.99	15.65	1	16.64	
1560	1-1/2"	<u> </u>		. 16	.500	<u> </u>	.53	16.65	-1	17.18	
1570	2"	-	Q-1	28	.571		.87	17.10	1	17.9	
1580	3"			1.7	.941		2.05	28	·	30.0	
1590	4"	:		14	1.143		3.57	34		37.5	
1600	6"	1.44	₩	8	2	₩	22.50	60	1	82.50) 1
1650	1/8 Bend, same as 1/4 Bend	: :		1	1	Τ				Ta -	1
1800	Tee, sanitary	÷ .	ŀ	1							L
1820	1-1/4"		1 Plum	11	.727	Ea.	1.25	24	1	25.2	5
1830	1-1/2"	Z 3	I	10	.800	1 1	.77	i .	}	1 27.2	7

,	OR Plastic Pir	e & Fittings			推議:	DAILY	ł				RE COSTS	y 1 ig	TOTAL
	VA Plastic Pip	e or cuttings	Tig. (AV)) y zi	CREW	OUTPU	HOURS	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P
01	. 2"				Q·1	17	.941	Ea,	1.10	28		29.10:	43.50
Ŋ	3"				;	11-	1.455		2.79	43.50		.46.29	. 69 1
	4 ⁿ			,		9	1.778		6.90	53		59.90	88.
- î	Tee, sanitary, re	educing, 2" x 1-1/2"				17	.941	} }	1.63	28		29.63	44.50
寸	3" x 2"		;			11	1.455	 	2.36	43.50		45.86	68.50
1	4" x 3"					10	1.600		7.70	48		55.70	81
1	Combination Y a	and 1/8 hend		-	<u> </u>	+	1 ;		 				
1	1-1/2"	2,0 2,0 00			1 Plum	1 10	.800	Ea.	2.34	26.50		28.84	42.50
+	2"			-	Q-1	17	.941		2.84	28		30.84	45.50
].	3"		•	1	Į.	11	1.455		5.	43.50		48.50	71.50
+	: Δ"				┝╌┼╌	9	1.778		9.85	53		62.85	91.50
	i '		•	:		11	1		1 1			: .	
1	3" x 1-1/2"			_			1.455		5.85	43.50	ļ	49.35	72.50
	4" x 3"			.	. ▼	10	1,600		8.80	48		56,80	82 -
1	Wye, 1-1/4"		·	_	1 Plum	L	.727		1.44	24		25.44	38 -
	1-1/2"				" .	. 10	.800		1.47	26,50		27.97	41.50
1	2"				Q-1	17	.941		1.51	28		29.51	44 :
1	3"					11	1.455		3.47	43.50		46.97	70::
1	4"			,		9	1.778		8.20	53		61.20	89.50
T	6"	1	*	1		5	3.200		31	96		127	180 : .:
1	3" x 1-1/2"					11	1.455		3.43	43.50		46.93	70 -
1	4" x 3"			į.		10	1.600		5.70	48		53.70	79
	, 6" x 4"			:	₩	6	2.667		25.50	80		105.50	150 🕮
T	Double Wye, 1-1	./2"			1 Plum	8	1		3.12	33.50		36.62	54 :
	2"				· Q-I	12	1.333		4.01	40		44.01	65
,	3"					8	2		10.35	60		70.35	102
	· 4"			10	:	6	2.667		21	80		101	144
1	2" x 1-1/2"		·····	1		11	1.455		4.01	43.50		47.51	70;50
	3" x 2"			1 :1		8	2		7.70	60		67.70	99 181
1	4" x 3"					7	2.286		16.65	68.50		85.15	122
	6" x 4"	V.				5	3.200		34.50	96		130.50	183 🔩
1	Reducer bushing	z. 2" x 1-1/2"		:]		30	.533		.51	15.95		16.46	24.50
	3" x 1-1/2"	(3"42"	22)			24	.667		1.85	19.95		21.80	32
+	4" x 2"	<u></u>		-		20	.800	$\vdash\vdash$	4.27	24		28.27	40.50
	6" x 4"					17	.941		11.40	28		39,40	55%
+	Couplings, 1-1/2	, n(-	1 Plum	(.500	\vdash	.56	16.65		17.21	25.50
	2"	,			Q-1	28	.571		.33	17.10		17.43	26.50
1	3"		· · · · · · · · · · · · · · · · · · ·	-	4.	22	.727	┞╌┼╌	1.15	22		23.15	34:50
	. 4 [#]					17	.941		1.77	28		29.77	44.50
	6"					12	1.333	$\vdash \vdash$	11.85	40	 	51.85	73.50
1						30	.533		1 1	40 15.95		16.29	24.50
1	2" x 1-1/2"				-	1	I	├	.34			21.10	31.50
	3 A 1 1/2					24	.667		1.15	19.95		(
L	4" x 3"				1 0	19	.842	$\vdash \vdash$	4.53	25	<u> </u>	29.53	43.5
1	Closet flange, 4'	, ,			1 Plum	1	.250		4.69	8.30	,	12.99	17.70
L	4" x 3"				. *	34	.235	<u> </u>	4.02	7.80		11.82	16.25
l	DW, PVC, schedule 40,				•								1.4%
	1/4 bend, 1-1/4				1 Plum	1	.47.1	Ea.	.93	15.65		16.58	24.50
事物	1-1/2"			, 1g	🧗	16	.500		.41	16.65		17.06.	25:50
Ů,	. 2" .				Q-1	28	.571		.63	17.10		17.73	26,50
	3"			7		17	.941		1.57	. 28 👉		29.57	44:
	4"				.	14	1.143		2.82	34		36.82	55,5
Ę	6"				+	8	2		17.15	60		77.15	109
	8"	•			Q-2	10	2.400		34.50	74.50	,	109	151
1 Total 1 Tota	10"		<u> </u>	-1	. "	7.	3.429	\vdash	37.50	106		143.50	202
ž.	1/4 bend, long s	sween, 1-1/2"	:		1 Plum	16	.500		1.28	16.65		17.93	26:50
115	2 1/4 Delia, lotte	1100P1 1 1/ L				28	.571	┝╼┼╼	1.05	17.10		18.15	27
	2"			, ; 🖫	· Q-1	1 7×	5/1			17 111		1 1X: 1 K	221 1 83

Managara includes and earliest ancestalling and expensive and the second appropriate

.941

1.21

28

29.21

0-1

17

5333

2"

nie zen	00 Building Services Pi		202	DAILA	LABOR			אם התחכ	RE COSTS		TOTAL
5108	Plastic Pipe & Fittings	Park (C)		OUTPU	,		MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P
7	3"		0.1		1.455	Ea.	2.79	43.50		46.29	69 A
35	4"		Į.	9	1.778	La.	ı	53	ĺ		
**	6"		\vdash	5		-	5.10	L	ļ	58.10	86
		: .	▼		3.200		33 🗟	96		129	182
	8"		-Q-2	5	4.800		37.50	149		186.50	267
38	10"			. 4	6		58.50	186		244.50	345
39 .	. 12"		*	3	8		86.50	248		334.50	470 : -
ľ	2" x 1-1/2"		Q ₁	17	.941		2.13	28		30.13	45
-	3" x 1-1/2"		$oxed{oxed}$	12	1.333		2.82	40		42.82	63.50
43	4" x 3"	1		. 10 -	1.600		4.79	48		52.79	78
	6" x 4"		* \	6	2.667		18.80	80 ·		98.80	142
	8" x 6"		· Q-2	8	3		45	93		138	191
47	Double wye, 1-1/2"		1 Plum	8	Ì		2.57	33.50		36.07	53.50
10:	2"	:	Q·1	12	1.333		3.30	40		43.30	64 😘
ļ	3"		-	: 8	2		8.50	60		68.50	100 √
الإين	4"	,		6	2.667		17.25	80		97.25	140 💠
54	2" x 1-1/2"		<u> </u>	11	1.455		3.02	43.50	!	46.52	69:50
	3" x 2"		\Box	8	2		6.35	60		66.35	97.50
. 1	4" x 3"			7	2.286		13.70	68.50		82.20	1.19
57	6" x 4"		•	5	3.200	1	28.50	96		124.50	17.7
ii. k	Coupling, 1-1/4"		1 Plum	17	.471	1 1	.78	15.65		16.43	24.50
-	1-1/2"		R	16	.500		.26	16.65	·	16.91	25.50
8	2"		Q-1	. 28	.571		.27	17.10		17.37	26.50
101 (8)	3"			. 22	.727		.78	22		22.78	34.
	4"		.	17	.941		1.28	28		29.28	44 . 6
	6"			12	1.333		6.85	40		46.85	68:47
2	8"		Q2	14	1.714		15.45	53		68.45	97.50
14	2" x 1-1/2"	. 3.	Q-1	30	.533	- 	.68	15.95		16.63	25
	3" x 1-1/2"	, ·	١٧٠	25	.640		2.15	19.15		21.30	31.50
NR 5	4" x 3"	\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\		18	.889		3.73	26.50		30.23	44.50
8	Di Lorento (See On 1.174)) } (s		31	.516		.46	15.45		15.91	24%3
	2" x 1-1/2"			30	.533	- -	.46	15.95		15.91	24:50
	3" x 1-1/2"	; ;	. .	25	.640		2.01	19.15	İ	21.16	24:50 31%
3	3 x 1-1/2	; /	+	. 24	:.667	-	.93	19.15		20.88	31 %
<u>9</u>				22			3.51	22		25.51	37 %
			-	20		-]	1.94	24	<u> </u>		
e-i-	, 4 4 3		.		.800		1 1			25.94	38
6	6" x 4" 8" x 6"		<u> </u>	14	1.143		10.05	34		44.05	63 🐇
	•	7 1	Q2	18	1.333		20	41.50		61.50	84.50
	Closet flange 4"		Q1	32	.500		4.73	14.95		19.68	27.50
0	4" x 3"			34	.471	*	3.55	14.10	. '	17.65	25.50
	Solvent cement for PVC, industrial grade, per quart				- 1 2 1	Qt.	10.80			10.80	11.90
. C	PVC, Schedule 80, threaded joints					_					
21.	90° Elbow, 1/4″	1	1 Plum	- 20	.400	Ea.	5.35	13.30		18.65	26 🔆
0	1/2"	į.		18	.444		2.09	14.80		16.89	25 ⊡
	1 3/4" - 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1			17	.471		2.67	15.65		18.32	26,50
	. 1"	4 (.	15	.533		4.24	17.75		21.99	31.50
	1-1/4"			14	.571		9,20	19:50		.28.20	38:50
No.	1-1/2"	₹ } ≪ .	+	13	.615	133	10.25	20.50		7. 7. 30.75	42:50
_	2" :	7. 66m A.	Q1	22	.727		12.40 ⁻	22/41/		34:40	46.50
	2-1/2"	1 1		18	.889		28.50	26.50	7	55	72 🗄
	§ 3. 3. 3"	ં પ્રો	. :	14	1.143		32	34		66	87.50
	4"	3.11		12	1.333		58	40		98	125s
1	6"		. ↓ .	: 7°	2.286	ें 🗸 े	" ii17 ,	68.50		: 185.50	232:09
	45° Elbow same as 90° Elbow			· 	,			-			177%
	Tee, 1/4"		1 Plum	14	.571	Ea.	6.55	19 🕾		25.55	35.50
5	1/2"	7 1	7	12	.667	1	6.55	22		28.55	40.50
ã.	3/4"			11	.727		6.65	24		30.65	44

151	108 Plastic Pipe & Fittings		A ()		LABOR-			2000 BAI		in the first term of the first	TOTA
150				ОИТРИТ		UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCLO
5890	1.1/4"		1 Plum	i	.800	Ea.	8.15	26.50		34.65	
5900				9 .	889	Щ.,	12.90	29.50		42.40	ैं।
910	1-1/2"	W.	. 🖈	8	1	.	· 14.80	33.50		48.30	
5920	2"		Q1	14	1.143		16.45	. 34		50.45	
5930	2-1/2"	:		12	1.333		42	40		82	10
5940	g 1 (m) 3"			9.	1.778		42	53		95	Ŋ
5950	4"	7 3		8	2		56	60		116	
5960	6"	÷ .	*	5	3.200		145	96		241	3
5000	Coupling, 1/4"		1 Plum	20	.400		5.70	13.30		19	
5020	1/2"			18	.444		2.21	14.80		17.01	
5030	3/4"	/		17	.471		3.09	15.65		18.74	
6040	* · · 1**			15 -	.533	•	4.16	17.75	, g	21.91	
5050	1-1/4"			14	.571		6.25	19	<u>-</u>	25.25	
5060.	1-1/2"	:	1	13	.615		7.85	20.50		28:35	
070	2"		Q-1	22	.727		9.15	22		31.15	
5080	2-1/2"		1	20	.800		20.50	24		44.50	
090	; 3"			19	.842	 -	20.50	. 25	21	44.50	- 3
100	4"	: V.		16	.042		22			i.	* 1 1
110	6"	· · · · ·		12	1.333		68	30 40		59	80
- 1	•		.₩				1 1		*:	108	1
120	OTC 100 pai at 100°F but and cald water		Q-2	14	1.714	<u> </u>	126	53		179	2.
200	CTS, 100 psi at 180°F, hot and cold water	1.1	: ··	00		۱ ـ				10.07	
230	90° Elbow, 1/2"		1 Plum	20 (.400	Ea.	.07	13.30	· · · · · · · · · · · · · · · ·	13.37	36
250	3/4"		{	19	.421		:.16	14		14.16	
251	1"			16	.500		.52	16.65		17.17	N.
252	1-1/4"	ί.		15 ,	.533		.89	17.75		18.64	Ň
253	1-1/2"	5 1	\rightarrow	14	.571		1.43	19	٠.	20.43	
254	·· 2"		Q·1	23	.696		3.08	21		24.08	
260	45° Elbow, 1/2"		1 Plum	. 20	.400		.12	13.30		13.42	
280	3/4"			19	.421		.18	14		14.18	G
281	: · · · ·]		16	.500		.48	16.65		17.13	. /8
282	1-1/4"	1		15	.533		.94	17.75		18.69	: 9
283	1-1/2"		\downarrow	14	.571		1.49	19		20.49	
284	2"	7 .	Q-1	23	.696	.1	3.14	21		24.14	1
290	Tee, 1/2"	_ { }	1 Plum	13	.615		.10	20.50	;	20:60	
310	3/4"	3.11		12	.667		.23	- 22		22.23	1,4
311	1"			11	.727		1.18	24		25.18	***
312	1-1/4"		-	10	.800		1.80	26.50	3	28.30	
313	1-1/2"		1	10	.800		2.34	26.50		28.84	
314	2"		Q·1	17	.941	-	3.80	28		31.80	7
320	Coupling, 1/2"	: 1	1 Plum	22	.364		.09	12.10		12.19	
340	3/4"			21	.381		.10	12.65		12.75	- 4
341	1"			18	.444		.45	14.80		15.25	an algorithms
342	1-1/4"	 		17	.471		.56	15.65		16.21	3
ł	1-1/4"			16	.500	1	1 1				10 m
343			▼		- 7 1		.79	16.65		17.44	
344	-	1	Q-1	- 28	.571	▼	1.58	17.10		18.68	
360	Solvent cement for CPVC, commercial grade, per quart					Qt.	7.30			7.30	
990	Polybutyl/polyethyl pipe, for copper fittings see 15107-460-7000) : I) }	ļ			
000	Compression type, PVC, 160 psi cold water	1								1	1/2
010	Coupling, 3/4" CTS	` · ·	1 Plum	21	.381	Ea.	1.90	12.65		14.55	:
020	1" CTS			18	.444		2.34	14.80		17.14	2.
030	1-1/4" CTS		71	17	.471		3.27	15.65		18.92	15
040	1-1/2" CTS	B		16	.500		4.50	16.65		21.15	4
050	2" CTS		- -	15	.533	_	6.30	17.75		24.05	
060	Female adapter, 3/4" FPT x 3/4" CTS			23	.348		3.01	11.55		14.56	.5
070	3/4" FPT x 1" CTS	- 1	+-	21	.381	+	4.50	12.65		17.15	7
080	1" FPT x 1" CTS		11	20	400		4.53	13.30		17.83	1

¥	0 Building Serv	ACCES PROMIS					¥.,						
3	Plastic Pipe & Fitting	1 c).X.)	G. Y	DAILY	LABOR	F			2000.BA	RE COSTS	1	TOTAL
1	The state of the s	,s		CREW	OUTPU	HOURS	UN	Π	mat.	LABOR	EQUIP.	TOTAL	INCL 0&P
	1-1/4" FPT x 1-1/4" CTS			I. Plum	. 18:	.444	Ea	. [5.95	14.80	·	20.75	29 %
	1-1/2" FPT x 1-1/2" CTS		-		16	.500			6.95	16.65	1	23.60	32.50
	2" FPT x 2" CTS		ΫŢ		13	.615			10.30	20.50		30.80	42.50
	Male adapter, 3/4" MPT x 3/4" CT	TS:	1		23	.348		ļ	2.71	11.55	.:	14.26	20.50
	3/4" MPT x 1" CTS				2,1	.381		1	3.34	12.65		15.99	23
	1" MPT x 1" CTS		.		20	.400		.	3.42	13.30		16.72	24.
_	1-1/4" MPT x 1-1/4" CTS		,		18	444		7	5.25	14.80	 	20.05	28.50
	1-1/2" MPT x 1-1/2" CTS		m .		16	.500		-	6.05	16.65		22.70	31.50
	2" MPT x 2" CTS		<i>"</i> †	\top	13	.615		十	9.70	20.50	 	30.20	41.50
	Spigot adapter, 3/4" IPS x 3/4" C	TS .	ŀ		. 23	.348		-	2.71	11.55		14.26	20.50
	3/4" IPS x 1" CTS.			17	21	.381		_	2.71	12.65	 	15.36	22:-
	1" IPS x 1" CTS	MED	۱ ا		20	.400			2.94	13.30		16.24	23
	1-1/4" IPS x 1-1/4" CTS		<i>/</i> †	11	18	444		\top	5.25	14.80	<u> </u>	20.05	28:50
	. 1-1/2" IPS x 1-1/2" CTS				16	.500			6.05	16.65	1 '	22.70	31:50
	2" IPS x 2" CTS	· · · · · · · · · · · · · · · · · · ·			13	.615		\dashv	9.70	20.50	1	30.20	41,50
	Price includes insert stiffeners			1			• '				İ	30.20	14.7
	250 psi is same price as 160 psi		_			 	<u> </u>	+			 		: /4:
	Insert type, nylon, 160 & 250 psi, cold	water	- }	1			ł	-			Ì		47
	Clamp ring stainless steel, 3/4" IPS		5 1	Plum	115	.070	Ea.	_	.62	2,31	 	2.93	4,18
	1" IPS	Toon .			107	.075	Ī		.63	2,49		3.12	4.45
	1-1/4" IPS		1	++	101	.079	-	+	.63	2,63	<u> </u>	3.26	4.67
	1-1/2" IPS			1 1	95	084			.64	2.80	Ì	3.44	4:94
	2" IPS		7 †	++	85	.094	\vdash	+	.64	3.13	 	3.77	5.45
	Coupling, 3/4" IPS		ال	11	22	.364			.56	12.10	l	12.66	18.90
	1-1/4" IPS		-	++	18	.444	╁	+	1.34	14.80	 	16.14	24
of the same	1-1/2" IPS				17	.471			1.74	15.65		17.39	25:50
	2" IPS		+	++	16	.500	H	+	2.09	16.65		18.74	27:50
-	Elbow, 90°, 3/4" IPS		1	11	22	.364			.82	12.10		12.92	19.20
	1" IPS		m 🕇	++	19	.421	1	+	.90	14		14.90	22
	1-1/4" IPS			1 1	18	.444	3.1		1.01	14.80		15:81	23.50
	1-1/2" IPS	:	+	++	17	.471		+	1.19	15.65	· · · · · · · ·	16.84	25.50
	2".IPS	:	- 1		16	.500		-	1.67	16.65	·	18.32	27:
	Male adapter, 3/4" IPS x 3/4" MPT	· · · · · · · · · · · · · · · · · · ·	+	++	25	.320	+	+-	.57	10.65		11.22	16.75
	1" IPS x 1" MPT		.		21	.381		1	.74	12.65	e sedera,	13.39	19.95
	1-1/4" IPS x 1-1/4" MPT		1+	++	20	.400	+	+	1.23	13.30		14.53	21.50
	1-1/2" IPS x 1-1/2" MPT		,		18	.444			1.63	14.80	4 ,	16.43	24:50
	2" IPS x 2" MPT			╁╌┼	15	.533	-+	┽	2.09	17.75		19.84	29.50
	Tee, 3/4"/IPS		- 1		14	.571			1.07	17.75		20.07	29:50
	1" IPS	- Д · і	+	╁╼┾	13	.615		╁	1.75	20.50		22.25	33.8
	1-1/4" IPS				12	.667			3.14	22	1.3	-25.14	37: 1
	1-1/2" IPS	WUV\	'	++	11	.727	-	+	3.95	24		27.95	41
	2" IPS	5	1.	\perp \perp	10	.800	1		5.35	26.50	·	31.85	46···
	, Insert type, PVC, 100 psi @ 180°F, hot &	& cold water		Y		-000		+		20.30		31,03	340 · · ·
1	Coupler, male, 3/8" CTS x 3/8" MP		111	olum :	29	.276	Ea.		.96	9.15		. 10.11	14,95
	3/8" CTS x 1/2" MPT			1 -	28	.286		+	.96	9.10		10.11	15,40
٠	1/2" CTS x 1/2" MPT				27	.296			.30	9.85	1	10.46	15.25
7 -	1/2" CTS x 3/4" MPT		+	+-+	26	.308	-	+	.86	10,25			16.45
. :	3/4" CTS x 1/2" MPT		1		25	.320		-	1		e eye by l	11.11	
;	3/4" CTS x 3/4" MPT		+				-	+	.86	10.65.	, Seria	11.51	17.05
					25	.320	.		4.11	10.65:	5.95	14.76	20,50
	Coupling, 3/8" CTS x 1/2" CTS		.	-	25	.320		4	2.15	10.65		12.80	18.45
(3	1/2" CTS		} }	-	23	.348			2.50	11.55		14.05	20.50
	1/2" CTS x stub	mmmf Immini	1	<u> </u>	23	.348	\perp	1	1.96	11.55	i sa wayi	13.51	19.65
7	3/4" CTS		-		22	.364	. .		3.96	12.10	1 11	16.06	- 22.50
, ,	Elbow 90°, 3/8" CTS		1_		25	.320	\perp	1	.65	10.65	od, dow	: 11.30	16.80
	1/2" CTS				23	.348			.65	11.55		12.20	18.20
) }	3/4" CTS	1	1		22	.364	\downarrow		.82	12.10	in New 2	12.92	19.20

hander of an hard committee the sail and the sample

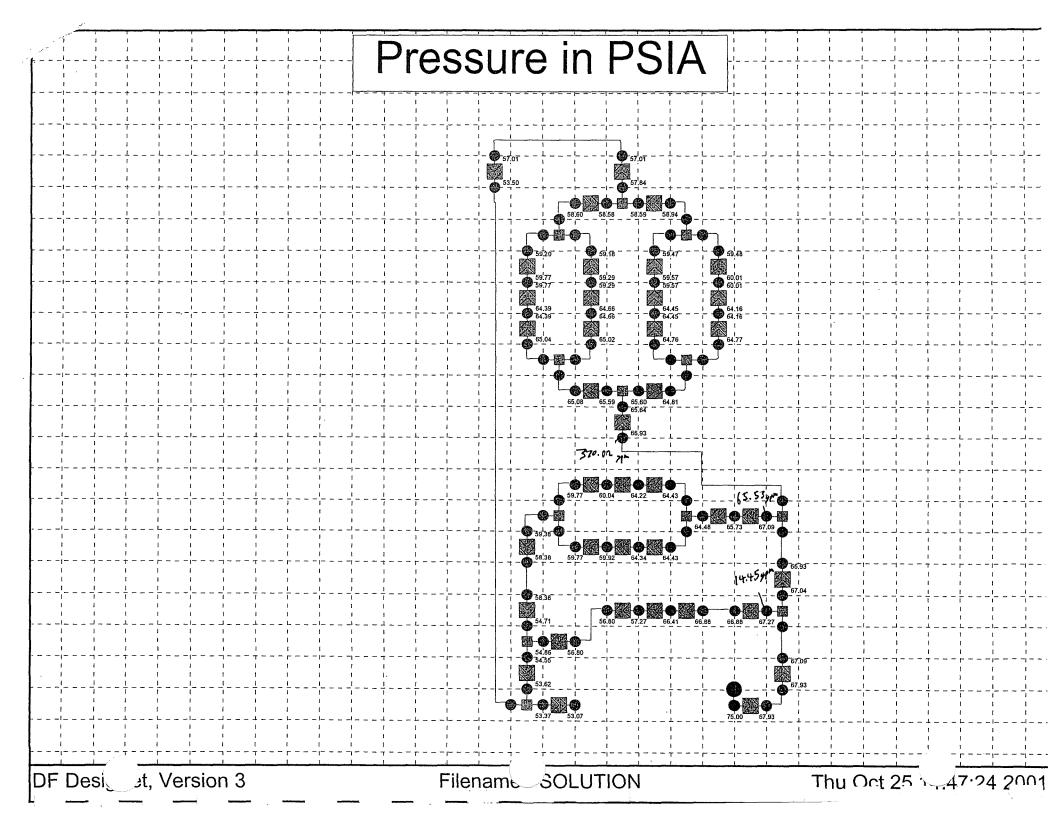
15	108	Plastic Pipe & Fittings	No.	1 pr. 1	DAILY	LABOR-			2000 BA	RE COSTS		TOTA
***	108	Plastic Pipe & Fiftings		CRE	N OUTPUT			MAT.	LABOR	EQUIP.	TOTAL	INCL
8800	:	Rings, crimp, copper, 3/8" CTS	2 .	1 Plu	m: 120.	.067	Ea,	.11	2.22		2.33	4
8810	8	1/2" CTS	\$ 2 ***		117	.068		.12	2.27		2.39	
8820		3/4" CTS			115	.070		.15	2.31		2.46	
8850.		Reducer tee, 3/8" x 3/8" x 1/2" CTS			17	.471		1.46	15.65		17.11	
8860		1/2" x 3/8" x 1/2" CTS			15	.533		1.25	17.75		. 19	
8870	4	3/4" x 1/2" x 1/2" CTS			14	.571		1.31	19		20.31	
8890		3/4" x 3/4" x 1/2" CTS		\vdash	- 14	.571		1.24	.19		20.24	*
8900		3/4" x 1/2" x 3/8" CTS	minimal poopor	1	14	.571	-	1.09	-19		20.09	
8930	-	Tee, 3/8" CTS		\Box	17	.471		1.05	15.65		16.70	
8940		1/2" CTS	· ·		15	.533		1.19	17.75		18.94	
8950	:	3/4" CTS	八月	1	14	.571		1.29	19		20.29	
8960	•	Copper rings included in fitting price		'	. .	\ \\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	*	1.			20.23	
9000	F	lare type, assembled, acetal, hot & cold wat	er honorin –		+-			 				- 0
9010		Coupling, 1/4" & 3/8" CTS		1 Plur	n 24	.333	Ea.	2.14	11.10		13.24	
9020		1/2" CTS			22	.364		2.45	12.10		14.55	
9030		3/4" CTS			21	.381		3.61	12.65	-	1	18 39
9040		1" CTS		\vdash	18	.301	┟┼	4.61	14.80	L	16.26 19.41	,
9050	;	Elbow 90°, 1/4" CTS			26	.308		2.38	10.25		19.41	
9060		3/8" CTS	[]	-	24	.333	┞┼	2.55	11.10	277	L	45 19
9070	:	1/2" CTS			22	.364	r_n	3.01	12.10	15.50	13.65	A. A. A. A. A. A. A. A. A. A. A. A. A. A
9080	<u> </u>	3/4" CTS			21	.381		4.61	12.10		15.11	į
9090	<i>:</i>	1" CTS			18	.444		5.80			17.26	1000
9110		Tee ,1/4": & 3/8" CTS	\triangle : .4	-	15	.533		2.62	14.80		20.60	36.5
9120		1/2" CTS			14				17.75		20.37	
9130		3/4" CTS				.571		3.44	19		22,44	
1	ŧ	1" CTS			13	.615		5.25	20.50		25.75	
9140 9550	<u> </u>	For plastic hangers see 15060-300-8000			12	.667	*	7	22		29	
9560	;	For copper/brass fittings see 15107-460-	7000			,						1,000
1	DIDE UIC	H DENSITY POLYETHYLENE PLASTIC (HE		···-		` .						
0020		cl. hangers, trenching, backfill, hoisting or dig	· ·									
0030		ard length is 40', add a weld for each joint.	sging equipment,	- : -		· :				<u> </u>		
0050	Stáiltí	Straight	, ,		.	1				,	,	
0054		1" diameter DR 11		• :•			1.5	700				3
0058		1-1/2" diameter DR 11				: 1	L.F.	.28				1
00562		2" diameter DR 11			11			.62			.62	
0066		3" diameter DR 11	1		1 1			.79			.79	12. 12. 13.
		3" diameter DR 17			 		-1	1.72		,	1.72	200
0070	** *	4" diameter DR 11	1			. 1		1.15	1	:	1.15	Ž.
0074		4" diameter DR 17	·		 		-	2.84			2.84	Ž
0078			•]			j		1.91)		1.91	
0082	· ·	6" diameter DR 11			 			6.15			6.15	Š.
0086	•	6" diameter DR 17	ł					4.13	}	1	4.13.	W.
0090		8" diameter DR 11			 		 	10.40			10.40	249 219
0094		8" diameter DR 26						4.69	•		4.69	
0098		10" diameter DR 11				<u>.</u>		16.20			16.20	4
0102		10" diameter DR 26	·]				-	7.25			7.25	
106		12" diameter DR 11	<u> </u>					23			23	Š
0110		12" diameter DR 26				-		10.25	Ì		10.25	- 185 - 185
114		16" diameter DR 11	ż					34	14.5		34	(9) (8)
118	4	16" diameter DR 26	ł		1	*		15.20	.1		15.20	
l i		18" diameter DR 11				(43			43	3
122		18" diarneter DR 26	:			1		19.20		. "	19.20	- 8
122		20" diameter DR 11	4			4.		53			53	7
122 126 130					,		1	22.50			23.50	- T
122 126 130 134		20" diameter DR 26			.			23.50	Į	1	23.30	33
0122 0126 0130 0134 0138		20" diameter DR 26						64			23.50 64	<i>?</i> !
0122 0126 0130 0134	:	20" diameter DR 26					-				8	

100 Building Services Pip							0000	N. 00		4041	
10 Valves		OPTH	,	LABOR-	113/57	1147	2000 BAF		lat Balan 1	TOTAL	
] + Çe	7	ОИТРИТ		UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P	
1-1/2" size		1 Stpi	11	.727	Ea.	274	. 24.50	*	. 298.50	335	
2" size		<u> </u>	8	1		330	33.50		363.50	415 .	
2-1/2" size		Q-5	5 .	3.200		360	96.50		456.50	540	
3" size			4.50	3.556	\ \	380	107		. 487 .	580	
Flanged											
3" size		Q-5	4.20.	3.810	Ea.	415	115		530	630	
4" size	,	"	3	5.333		835	161		996	1,175	
5" size		· Q6	3.80	6.316		990	197		1,187	1,400	
6" size			. 3	8		1,200	250		1,450	1,700	
8" size			2.50	9.600		1,775	300		2,075	2,400	
10" size			2.20	10.909	\vdash	2,525	340		2,865	3,300	
12" size	;		2.10	11.429		7,075	355		7,430	8,350	
14" size			2	12	\vdash	10,100	375	· · · · · ·	10,475	11,700	
14 326		*	-	12.	*	10,100	3/3	• ;	10,475		
HIVE DIACTIC				3.1						·:'.	
ALVES, PLASTIC	R15100										
Angle, PVC, threaded	730	1 50	25	300							
1/4" size		1 Plum	26	.308	Ea.	47.50	10.25		57.75	67:50	
1/2" size			26	.308		47.50	10.25		57.75	67.50	
3/4" size			25	.320		55.50	10.65		66.15	77	
1" size		*	23	.348	₩	66.50	11.55		78.05	90.50	
Ball, PVC, socket or threaded, single union		ŀ		. 6						V.1	
1/4" size	:	1 Plum	26	.308	Ea.	22	10.25		32.25	39.50	
3/8" size	:		· 26	.308		22	10.25		. 32.25	39.50	
1/2" size	l.		26	.308		22	10.25		. 32.25	39.50	
3/4" size			25	.320	\Box	26.50	10.65		37.15	45	
1" size	,		23	348		31	11.55	•	42.55	51.50	
1-1/4" size			21	.381		41.50	12.65		54.15	65	
1-1/2" size			20	.400		52	13.30		65.30	77: ±	
2" size			. 17	.471	$\dashv \dashv$	74.50	15.65		90.15	105	
2-1/2" size		∀ 01	26	.615		185	18.40		203.40	232 8:	
3" size		1	24	.667	-+-	185	19.95		204.95	234:33	
4" size			20	.800		320	24		344	-385 A	
For PVC, flanged, add				.000	-++	100%	15%				
1/17 / A		1 Plum	26	.308		1	10.25		35,25	.1829 13 11	
Double union 1/2" size		- - - - -	25	.30ę	$-\!\!+\!\!-\!$	25 28		*:	1	43.	
3/4" size	: I					I	10.65		38,65	46.50	
1" size		<u> </u>	23	.348	\dashv	35	11.55		46.55	56:	
1-1/4" size	·		21	.381		58	12.65		70.65	83	
1-1/2" size			20	.400		58	13.30		71.30	84:5	
2" size		♥	. 17	.471	▼	79.50	15.65		95.15	. 111	
CPVC, socket or threaded, single union		:					·			1.	
1/2" size		1 Plum	26	.308	Ea.	36.50	10.25	* .**	46.75	55.50	
3/4" size	1.		25	.320		43.50	10.65		54.15	63.50	
The particular life size			- 23	.348		51	11.55		62.55	73.50	
1-1/4" size			21	.381	_	88	12.65		100.65	116	
1-1/2" size		.	20	.400		88	13.30		101.30	117	
2" size		. ↓ .	17	.471		118	15.65		133.65	154	
3" size		Q-1	24	.667		248	19.95		267.95	305	
For CPVC, flanged, add	3			14		65%	. 15%			•	
For true union, socket or threaded, add			:		+	50%	5%		<u> </u>		
Polypropylene, threaded	· , ' [[3	▼ [
For true union, socket or threaded, add Polypropylene, threaded 1/4" size	-H	1 Plum	26	.308	Ea.	30	10.25		40.25	48.50	
	· []	1 1 10111	26	.308	La.		10.25	·, ··		48.50	
3/8" size	} 					30		·····	40.25		
1/2" size		<u>," </u>	26	.308		30	10.25	, į	40.25	48.50	
3/4" size		_ =	25	.320	$\dashv \downarrow$	37.50	10.65		48.15	57:	
1" size		~	23	.348		44.50	11.55		56.05	66:50	
1-1/4" size	. ↓	. 🕹 🖫	21	.381	₩	64.50	12.65	:	5 3 - 77.15.	90	

- >**		1,00		DAHA	LABOR-	1.17		2000 BAR	E COSTS	i galiya i	TOTAL
151	10 Valves				HOURS	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P
2170	1-1/2" size	R15100	1 Plum	20	.400	Ea.	74	13.30		87.30	102
2180	2" size	-090	1	1.7	.471	· .	101	15.65		116.65	13
2190	3" size		Q-1	24	.667		266	19.95	334	285.95	325
2200	4" size	. 4	"	20	.800	₩	445	24		469	525
2550	PVC, three way, socket or threaded				. :				•	il mastrii.	11,600
2600	1/2" size		1 Plum	26	.308	Ea.	56.50	10.25	r	66.75	77.50
2640	3/4" size			25	.320		64	10.65		74.65	86.50
2650	1" size			- 23	348		69.50	11.55		81.05	94
2660	1-1/2" size			20	.400		140	13.30		153.30	174《湯
2670.		٠.	↓	17	.471		188	15.65	-3	203.65	231
2680	3" size		Q:1	24	.667		455	19.95	1.0	474.95	530
2740	For flanged, add		1 1/2	} ;	1.		60%	15%	,	25 575	
3150	Ball check, PVC, socket or threaded			<u> </u>	16%	_					\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\
3200	1/4" size		1 Plum	-26	.308	Ea.	25	10.25		35.25	43
3220	3/8" size		1	26	.308		25	10.25		35.25	43.0
3240	1/2" size	.		26	.308		25	10.25	1.	35.25	43
3250	3/4" size	: : :	1	25:	.320		28	10.65		38.65	46.50
3260	1" size		1:	23	.348		35	11.55		46.55	56
3270	1-1/4" size		1	21	.381	\vdash	58	12.65		70.65	83
3280	1-1/2" size	.		20	.400		58	13.30		71.30	84
3290	2" size		1 🛨	17	.471	\vdash	. 79	15.65		35 300, 94 :65	1.00
3310	3" size		Q-1	24	.667		183	19.95		202.95	231
3320	4" size		,	20	.800		259	. 24	- :	283	320
3360	For PVC, flanged, add	·				↓	50%	15%	·		
3750	CPVC, socket or threaded		<u> </u>		\$ 8 E						
3800	1/2" size	<u>.</u>	1 Plum	26	.308	Ea.	36.50	10.25		46.75	55.50
3840	3/4" size			25	.320	H	43.50	10.65		54.15	6,°
3850	1" size	*		23	.348		51	11.55		62.55	. 7
3860	1-1/2" size			20	.400	\vdash	88	13.30		101.30	117
3870	2" size	,		17	.471		118	15.65	. '	133.65	154
3880	3" size		Q1	24	.667	 	249	19.95		268.95	305
3920	4" size		,	20	.800		335	24		359	400
3930	For CPVC, flanged, add		 				40%	15%		111 111	- UN 193
	Polypropylene, threaded					.▼	100	10%		100 NOS 20	
4340	1/2" size	· · · · ·	1 Plum	26	.308	Ea.	25	10.25		35.25	43
4400	3/4" size			25	.320	Ĩ	29	10.65		39.65	48
4440	1" size			. 23	.348		37.50	11.55	,	49.05	58.50
4450	1-1/2" size		4	20	.400		72.50	13.30		85.80	100
4460	2" size	 :-	╂╁	17	.471		91	15.65		106.65	124
4500	For polypropylene flanged, add	.	*	1	.4/1	<u> </u>	200%	15%		100.05	72
4850	Foot valve, PVC, socket or threaded		 				20070	15/0		1 1 1	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
4900	1/2" size		1 Plum	34	.235	Ea.	36.50	7.80		44.30	52 0
4900	3/4" size		1 1 10111	32	.250		41.50	8.30		49.80	58
•	1" size		ľ I .	28	.286		54	9.50	,	63.50	
4940	1 Size 1-1/4" size		+-	27	.296		104	9.85		113.85	./
4950	1-1/4" Size 1-1/2" size			26	.308		104	10.25		114.25	1.19
4960	2" size		1	24	.333	 -	120	11.10		3 131.10	
4970		· .		20	.333		287	13.30	, s	300.30	
4980	3" size		-	18	.444	 	505	14.80		519.80	.,
4990	4" size		1	ΤQ	,444		! !			1	300
5000	For flanged, add		 			*	25%	10%	, 41,	k 1,440	
5050	CPVC, socket or threaded	· [16.1	_ ا		7.00	٠.,	70.00	00
5060	1/2" size		1 Plum	34	.235	Ea.	64.50	7.80		72.30	h
5070	3/4" size			32	.250		78	8.30		86.30	8 1
5080	1" size			28	.286		92	9.50		101.50	
5090	1-1/4" size	.		27	.296	,	129	9.85		138.85	4 3
5100	1-1/2" size	. 1	Τ ↓	26	.308	₩	150	10.25		160.25	181

eller,	100 Building Services Piping				DAILY LABOR- 2000 BARE COSTS						
) Valves		CDEIN	1	Labor- Hours	UNIT	MAT.	LABOR		TOTAL	TOTAL
	2" size		1 Plum	_	.333	Ea.	193	11.10	EQUIP.	TOTAL 204.10	INCL 0&P 230
		R15100 -090	l I Idini	20	.400	La.		i i		1 1	420
	3" size		-	L			365	13.30		378.30	
	4" size		*	18	.444		790	14.80		804.80	890
	For flanged, add			ļ			25%	10%		ļ	
	Needle valve, PVC, threaded		1 0	200	200	_	70	10.05			
	1/4" size		1 Plum	26	.308	Ea.	32	10.25		42.25	50.5
	3/8" size			26	.308		37	10.25		47.25	56
	1/2" size		<u> </u>	26	.308		37	10.25		47.25	56
	For polypropylene, add		1			*	10%				
_	Y check, PVC, socket or threaded		<u> </u>	L						L	· · · · · · · · · · · · · · · · · · ·
	1/2" size		1 Plum	26	.308	Ea.	52.50	10.25		62.75	73
	3/4" size			25	.320		56.50	10.65		67.15	78
	l" size	,		23	.348		62	11.55		73.55	85.5
	1-1/4" size			21	.381		97	12.65		109.65	126
	1-1/2" size			20	.400		105	13.30		118.30	136
_	2" size			17	.471		131	15.65		146.65	169
	2-1/2" size		+	15	.533		277	17.75		294.75	330
	3" size		Q-1	24	.667		260	19.95		279.95	315
	4" size		"	20	.800		455	24		479	535
	For PVC flanged, add					↓	45%	15%		1	
	Y sediment strainer, PVC, socket or threaded										
	1/2" size		1 Plum	26	.308	Ea.	29.50	10.25		39.75	48
-	3/4" size			24	.333		32	11.10	~	43.10	52.5
	1" size			23	.348		39	11.55		50.55	60.5
•	1-1/4" size			21	.381		64.50	12.65		77.15	90
	1-1/2" size			20	.400		67.50	13.30		80.80	94,5
	2" size			17	.471		78.50	15.65		94.15	110
	2-1/2" size			15	.533		192	17.75		209.75	238
	3" size		Q-1	24	.667		192	19.95		211.95	241
	4" sìze		,	20	.800		320	24		344	385
	For PVC, flanged, add	·	1			*	55%	15%			
٧	ALVES, SEMI-STEEL	R15100	 								
	Lubricated plug valve, threaded, 200 psi	-090	1							1	
•	1/2" pipe size		1 Plum	18	.444	Ea.	61.50	14.80		76.30	90
	3/4" pipe size			16	.500		61.50	16.65		78.15	92.5
•	1" pipe size			14	.571		79	19		98	116
	1-1/4" pipe size			12	.667		95	22		117	139
	1-1/2" pipe size			11	.727		102	24		126	149
	2" pipe size	1		8	1		120	33.50		153.50	183
	2-1/2" pipe size		Q1	5	3.200		186	96		282	. 350
	3" pipe size		,	4.50	3.556		228	106		334	410
	Flanged, 200 psi		1			-					
	2" pipe size		1 Plum	8	1	Ea.	145	33.50		178.50	211
	2-1/2" pipe size		Q-1	5	3.200		218	96	·	314	385
	3" pipe size		Ì	4.50	3.556		264	106		370	· 450
	4" pipe size		╂╌┼╌	3	5.333		335	160		495	610
	5" pipe size			2.50	6.400		500	192		692	840
	6" pipe size		Q2	3	8	\vdash	655	248		903	1,100
	8" pipe size		1	2.50	9.600		1,125	298		1,423	1,700
	10" pipe size		1	2.20	10.909	\vdash	1,725	340	<u> </u>	2,065	2,400
	• •	1		1.70	14.118		2,975	440		3,415	3,925
۱	12" pipe size		1-	1./0	14.110	-	4,313	'1'' 'U		7,71	2,343
4	AI VES, STEEL	R15100 -090									i
	.rsl Check valve, swing type, 150 lb., flanged		 		 					ļ	

APPENDIX G

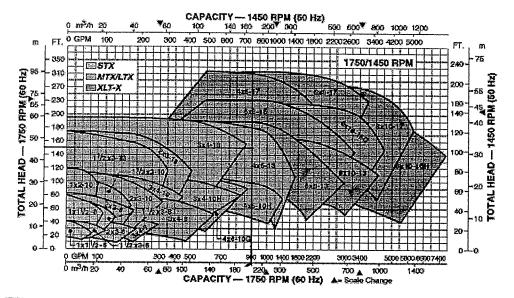


4	۲	۲	ᆫ	N	U	/	r	1

-14



Previous Page



50 Hz	60 Hz
1480 RPM	1780 RPM
1X1.5-6-Alloy	1X1.5-6-Alloy
1x1.5-6-Iron	1X1.5-6-Iron
1.5X3-6	1.5X3-6
2x3-6-Allov	2x3-6-Alloy
2x3-6-Iron	2x3-6-Iron
1x1.5-8-Alloy	1x1.5-8-Alloy
1x1.5-8-Iron	1X1.5-8-Iron
1.5X3-8-Alloy	1.5X3-8-Alloy
1.5X3-8-Iron	1.5X3-8-Iron
2X3-8-Alloy	2X3-8-Alloy
2X3-8-Iron	2X3-8-Iron
$\frac{3x4-7}{3x4-3}$	3x4-7
3X4-8	3X4-8
3X4-8G	3X4-8G
1X2-10-Alloy 1X2-10-Iron	1X2-10-Alloy
1X2-10-1001 1 5 V2 10 Alland	1X2-10-Iron
1.5X3-10-Alloy	1.5X3-10-Alloy 1.5X3-10-Iron
1.5X3-10-Iron 2X3-10	1.00.0-10-11011
3x4-10	2X3-10 3X4-10
3X4-10H	3X4-10 3X4-10H
4X6-10	4X6-10
4X6-10H-Alloy	4x6-10H-Alloy
4x6-10H-Iron	4x6-10H-Iron
4X6-10G	4X6-10G
1.5x3-13-Alloy	1.5x3-13-Alloy
1.5x3-13-Iron	1.5x3-13-Iron
2X3-13	2X3-13
3x4-13	3x4-13
4X6-13	4X6-13
6X8-13	6X8-13
8x10-13	8x10-13
6X8-15	6X8-15
8X10-15	8X10-15G
8X10-15G	8x10-16H

