MYDRO

Newfoundland & Labrador Hydro

Hydro Plant Corrosion / Fouling Study 2002

Hinds Lake Generating Station SERVICE WATER SYSTEM

Newfoundland & Labrador Hydro



Hinds Lake Generating Station

SERVICE WATER SYSTEM

Piping
Strainer
Supply Pump
Control Valves
Heat Exchangers

Prepared for:

Newfoundland & Labrador Hydro

Hydro Generation

Submitted to:

John Mallam, P.Eng

Mechanical Supervising Engineer

Submitted by:

Shane White, B.Eng

Mechanical Engineer

Date:

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SUMMARY

It was determined that a hydro plant cooling water study was needed to determine the most effective solution to the cooling water fouling that is plaguing our hydro plants. The methodology for this study was planned out to include the following: prioritize plants and systems for review, review drawings, inspect coolers for extent of fouling, calculate actual flow rates, and determine the best solution for each hydro plant.

It was determined that Upper Salmon, Cat Arm, and Hinds Lake had the most problems with regards to cooling water.

In order to first determine which plant had the worse problems an in-depth analysis of each plants cooling water system had to be undertaken. Next a complete review of the plants work history had to be done. This was accomplished by reviewing all work orders related to the plants cooling water system in the J.D.Edwards. From this it can be determined which plant had the worse problems.

What was needed next was a review of how the plant's cooling water system has been operating. This was accomplished by using the Trend Monitoring Program that I designed. From the trend graphs one could see just how efficiently the plant has been operating and how the work on the cooling water system affects it. This gives us a time frame for cleaning components of the system so that we could set up a maintenance program for the cooling water system.

A cost analysis was done to determine the amount of money being spent on the current cooling water system in each plant. Also a cost analysis for replacing the piping was done using RSMeans Mechanical Cost Data for each plant.

Several solutions were presented to combat the fouling problem and they are; chemical cleaning of the system, replace the piping with corrosion resistant pipe, add a corrosion inhibitor to the water, use organic filters, or convert to a closed cooling water system.

From these solutions four were chosen for further investigation and they are; replace piping with corrosion resistant pipe, add a corrosion inhibitor to the water, convert the system to a closed system, and continue to operate as we have. Each solution was researched and a Net Present Worth calculation was done to determine the most economical solution. It was determine that replacing the piping with corrosion resistant pipe is the best solution, considering that the pipe has to be replaced in the next few years the other solutions did not seem economical.

The NPW of this solution for Hinds Lake is \$218,064 over the pipe life of 20 years. The NPW of continuing to operate as we have is \$152,494 but this does not include replacing the existing piping, which labour alone is \$52,000. The closed loop solution has a NPW of \$213,427 but the existing piping has to be replaced for this solution to be affective. The closed loop solution can always be added on after the piping is replaced.

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Recirculation Pump Analysis

The generator surface air coolers are supplied by a common six inch header piped directly from discharge of the turbine/generator cooling water pump to the generator housing. The six inch discharge header has tap-ins for the generator bearing oil coolers, turbine bearing oil coolers and the turbine shaft seal. After the six inch discharge header penetrates the generator housing it branches in two four inch headers. One header serves coolers #1 & #4 while the second header serves coolers #2 & #3.

Surface air coolers are supplied with normally open isolation gate valves on both supply and return; air vent line complete with in-line water flow indicator and normally open gate valve; also drain line with normally closed gate valve.

Generator surface air cooler return lines are also divided into two four inch headers. One four inch header serves coolers #3 & #4 while the other four inch header serves coolers #1 & #2. Each return line has a Barton flow orifice and globe valve installed on the downstream generator face. Each Barton flow meter is piped to a flow panel located on column D outside the generator housing. The two four inch discharge headers join together into a six inch header and run through a trench along the upstream wall of the pump room where a six inch isolation valve and check valve are also located. From there the six inch discharge line is embedded into the pump room floor and travels directly to the tailrace surge chamber.

Generator upper guide bearing oil cooler is supplied by a two inch pipe, which taps into the six inch main supply header that feeds the surface air coolers. A normally open isolation valve is installed on the down streamside of the generator face directly above the catwalk.

The six generator lower guide bearing and thrust bearing coolers are supplied by a three inch pipe which also taps into the six inch main supply header that feeds the surface air coolers. Upon entering the generator housing the three inch pipe reduces to a two and half inch header, which feeds all six coolers. The supply and discharge pipes that branch from the two and half inch header and feed directly into the coolers are only two inches. There is a total of six coolers all equipped with normally open isolation valves on both the supply and discharge lines. Main isolation valve #W35V1 normally open is located on the downstream generator face.

The generator upper guide bearing oil cooler return line has a Barton flow orifice and a globe valve installed on the downstream generator face. The Barton flow orifice is piped to a flow meter panel located on column D outside the generator housing. The generator upper guide bearing oil cooler return line connects into a common four inch header with return lines from generator lower guide and turbine bearing cooler return. These returns travel through a trench in the floor and travel along the up stream wall of the pump room where a four inch check valve #W40RV2 and a normally open four inch isolation valve #W40RV3 are installed. From there the return header runs embedded in the pump room floor and travels directly to the tailrace surge chamber.

Generator lower guide bearing and thrust bearing cooler return has a Barton flow orifice and a globe valve installed on the downstream generator face. The Barton flow orifice is piped to a flow meter panel located on column D outside the generator housing. The generator lower guide bearing and thrust bearing cooler return lines connects into a common header described above.

Flow meter panel settings:

Flow Rates	Set Points
Surface Air Cooler Flow	1250 L/min per discharge header
Upper Generator Cooler Flow	60 L/min
Lower Generator Cooler Flow	640 L/min

Table 1

Turbine guide bearing coolers are supplied by a two inch pipe which also taps into the main six supply header that feeds the surface air coolers. There are a total of four coolers equipped with normally open isolation valves on both the supply and return lines. Main isolation valve normally open #W40V1 is located on the downstream generator face.

Turbine flow rate setting:

Flow Rate	Set Point
Turbine Cooler Flow	50 L/min

Table 2

The turbine guide bearing cooler return connects into a common header with the generator upper and lower guide bearing and returns to the tailrace as described above.

Turbine shaft seal supply taps into the six inch main supply header that feeds the surface air coolers. Shaft seal water passes through two strainers complete with isolation valves, which enable these strainers to act as backup to one another. Strainers and valves are located on the down streamside generator face. Strainers have to be checked and cleaned manually on a regular basis with the frequency established by experience.

Turbine shaft seal supply has a flow meter installed for visual inspection of the amount of flow (L/min) being supplied to the shaft seal, a pressure gauge for visual inspection of amount of pressure and a pressure switch which activates an alarm for low-set pressure in the supply line.

Turbine shaft seal flow rate setting:

	Flow Rate	Set Point
-	Turbine Shaft Seal Flow Rate	50 L/min

Table 3

Turbine shaft seal water escaping above the head cover is drained via embedded pipes to the penstock head gallery where they terminate approximately six inches above a drain. Once in the drain it travels via embedded drainage pipe to the drainage sump.

If complete isolation of the unit is required all main shut off valves, which are normally in the open position when the station is running, should be placed in the closed position. These valves are as follows:

- Generator surface air cooler supply valve #W39V11
- Generator upper guide bearing supply valve #W35V2
- Generator lower guide bearing supply valve #W35V1
- Turbine bearing supply valve #W46V1
- Shaft Seal supply valve #W41V15

Also close the return valves located in the pump room. These valves are as follows:

- Cooling water return valve #W39RV4
- Generator upper and lower guide bearing return valve and turbine bearing valve #W40RV3

The Flow diagrams for Hinds Lake can be found in Appendix A.

HISTORY OF SERVICE WATER SYSTEM

General Information

All work orders that are in the J.D.Edwards system since fall 1994 pertaining to the service water pumps, strainers, and heat exchangers have been reviewed to piece together an overview of the major work done on the service water system. All of the major work done on this system is listed below in the following table. It can be seen from table 4 that the SAC's have only been cleaned once since 1993. It can also be seen that the SAC piping has been cleaned once since 1993. The rotary strainer is cleaned approximately every three years. The generator coolers have been cleaned only once since 1993, but from the amount of build up found within these coolers this cleaning frequency should have been more then what it was.

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Table 4

Review of Trend Monitoring Readings

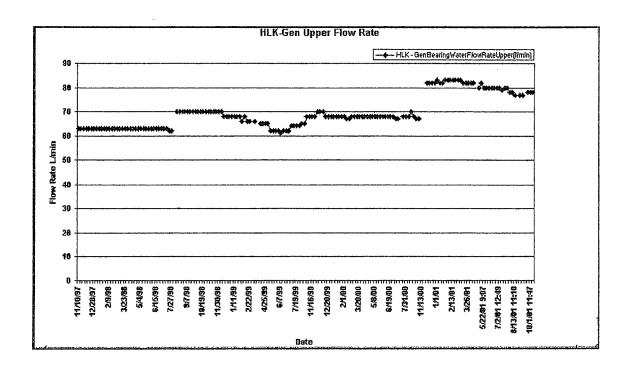
Trend Monitoring readings are taken weekly by operations for all hydro generating stations except Snooks Arm and Venams Bight. With knowledge of the work history performed on the generating station coupled with the trend monitoring readings one can develop a picture of how the generating station has operated over the last few years.

The Trend monitoring readings are now being stored into a database using Microsoft Access. A hard copy of the weekly readings is being kept on site for backup. The Microsoft Access Trend Monitoring program now allows quick graphing of operating parameters to help us determine the efficiency of the unit. The program is user friendly and allows operations to view the units operating parameters over an extended period of time.

Table 2 shows the missing trend monitoring readings for Hinds Lake.

	Missing Dates	Period
DATES	1999/08/20 to 1999/11/08	Fall 1999
	2000/07/31 to 2000/11/30	Late Summer 2000

Table 5



Graph 7 - Upper Generator Cooler Flow Rate

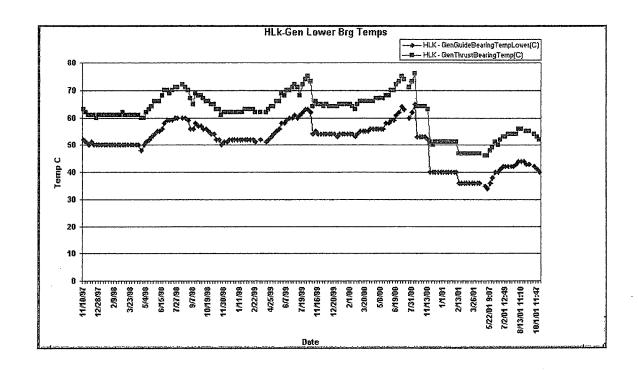
Graph 7 shows the upper generator cooler flow rate since November 1997. The recommended flow rate is 60 L/min. A low flow rate is 55 L/min and a high flow rate is 90 L/min.

Actual Velocity Calculations:

Flow Rate per tube $Q_t = 0.25$ L/sec Area per tube $A_t = 1.23$ in²

Velocity per tube
$$V_t = \frac{Qt}{At} = 1.03$$
 ft/sec

The upper guide bearing coolers flow rate is above the manufactures recommended normal flow of 60 L/min. The flow rate is not above the manufactures recommended high flow rate of 90 L/min but this extra cooling water that is being given to this cooler can be used else where in the system since all cooling water comes from the same common six inch header.



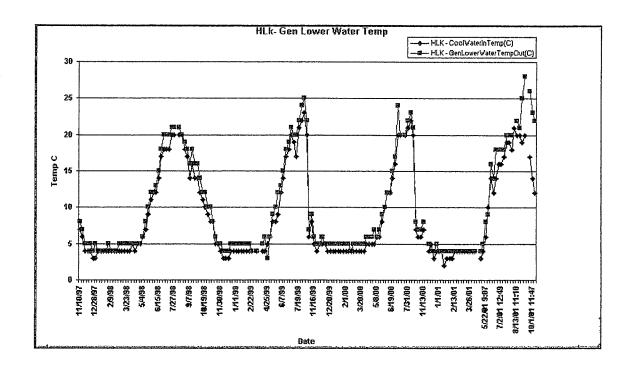
Graph 6 - Lower Generator Bearing Temperatures

Graph 6 shows the generators lower guide and thrust bearing temperatures since November 1997. One can see the temperature drop after the three coolers were cleaned in November 2000 and again in January 2001 after two more coolers were cleaned.

Lower Generator Bearing Temperature Set Points:

	Guide Bearing	Thrust Bearing
Alarm	70 °C	
Trip Unit	80 °C	

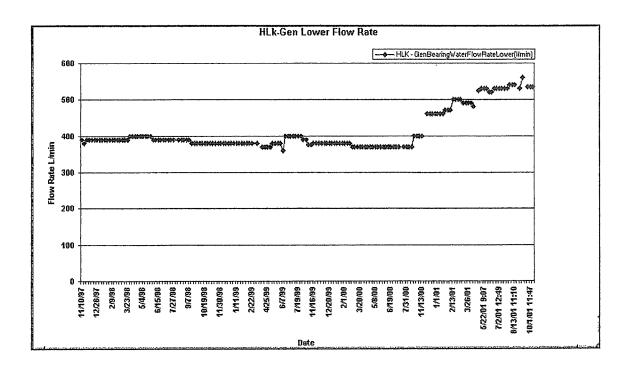
The guide bearing temperatures of 65 °C in the summer 2000 was close to the alarm set point of 70 °C. Since the coolers cleaning the temperatures have drop back towards normal.



Graph 5 - Lower Generator Cooler Water Temperatures

Graph 5 shows the water temperature differential for the generator coolers since November 1997. This graph clearly shows how the water temperatures fluctuate through out the year, with increased temperatures during the summer months and decreased temperatures during the winter months.

1 1



Graph 4 - Lower Generator Cooler Flow Rates

Graph 4 shows the flow rates for the generator lower coolers since November 1997. The recommended flow rate is 640 L/min, with 510 L/min considered low and 960 L/min considered high. One can see the 60 L/min increased flow rate in November of 2000 when three of the six coolers where cleaned. The increase in February 2000 was when two of the remaining three coolers were cleaned and the increase in April 2000 was when the last of the six coolers was cleaned.

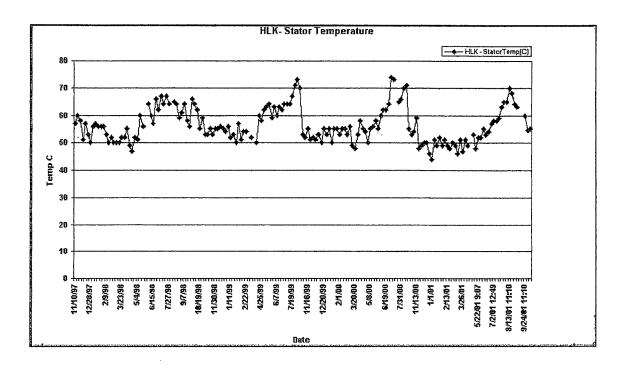
Actual Velocity Calculations:

Flow Rate per tube $Q_t = 0.070 \text{ L/sec}$ Area per tube $A_t = 0.264 \text{ in}^2$

Velocity per tube
$$V_t = \frac{Qt}{At} = 1.35$$
 ft/sec

The low flow rate of 400 L/min up until the summer 2000 was below the manufactures recommended low flow rate of 510 L/min and far below the normal recommended flow rate of 640 L/min. The flow rate as of this summer was improved to 535 L/min and this can be improved if the supply and discharge piping is cleaned.

The supply and discharge piping for the lower generator coolers was cleaned during the Fall 2001 outage. Have no data as of yet.



Graph 3 - Stator Temperatures

Graph 3 shows the stator temperatures since November 1997. This graph clearly shows how the stator temperatures fluctuate through out the year, with increased temperatures during the summer months and decreased temperatures during the winter months.

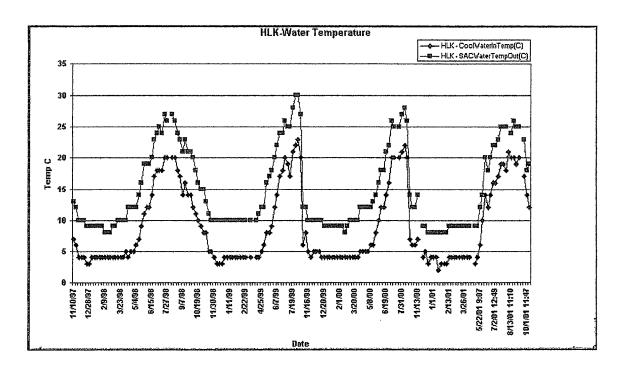
The stator iron alarm has been changed from 75 °C to 79 °C.

Stator Temperature Set Points:

Core Alarm	79 °C
Iron Alarm	79 °C

Table 6

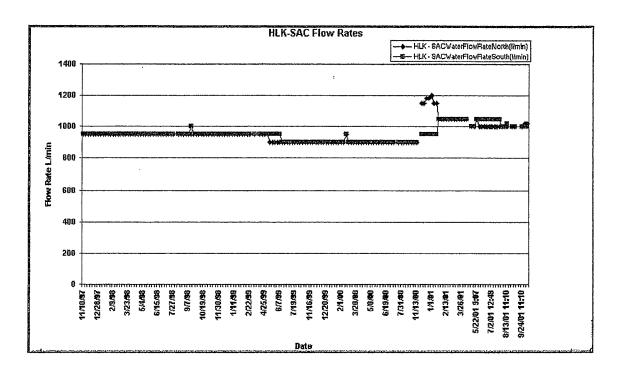
During the summer of 1999 and 2000 the stator temperatures almost reached the iron and core alarm set point of 79 °C. The iron alarm was changed because of this.



Graph 2 - SAC Water Temperatures

Graph 2 shows the water temperature differential for the SAC's since November 1997. This clearly shows how the water temperatures fluctuate through out the year, with increased temperatures during the summer months and decreased temperatures during the winter months. Even though the temperature fluctuates the differential temperature between inlet and discharge remains constant around an average of 6 °C.

1 1



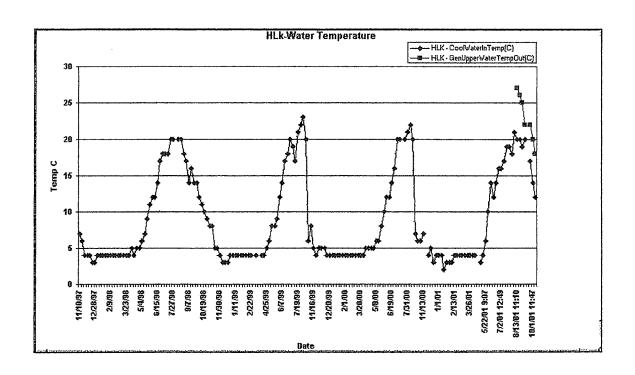
Graph 1 - SAC Flow Rates

Graph 1 shows the SAC's flow rates since November 1997. The recommended flow rates are 1250 L/min per bank, with 1000 L/min considered low and 1800 L/min considered high. One can see the 250 L/min increase in flow rate of the north bank around November 2000 after coolers #1 and #4 were cleaned. The 50 L/min increase in flow rate of the south bank around November 2000 was caused by cooler #3 being flushed in place. The second increase in flow rate of the south bank was the cleaning of cooler #2 in January 2001. Cooler #3 was removed and cleaned in April 2001.

Actual Velocity Calculations:

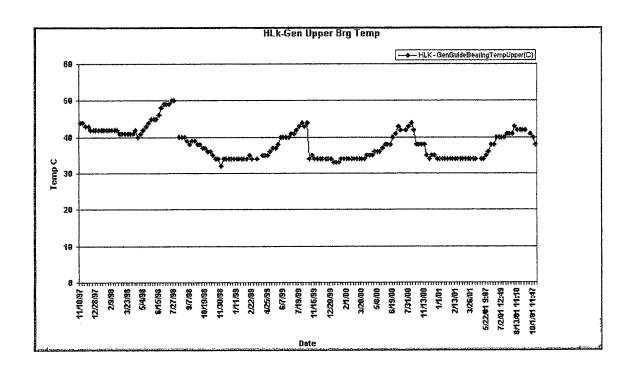
Flow Rate per tube $Q_t = 0.146$ L/sec Area (elliptical cross section) per tube $A_t = 231$ mm²

Velocity per tube
$$V_t = \frac{Qt}{At} = 2.08 \text{ ft/sec}$$



Graph 8 - Upper Generator Cooler Water Temperatures

Graph 8 shows the upper generator cooler water temperature since August 2001. This temperature was not being recorded before and it was recommended that we record this temperature for trending.



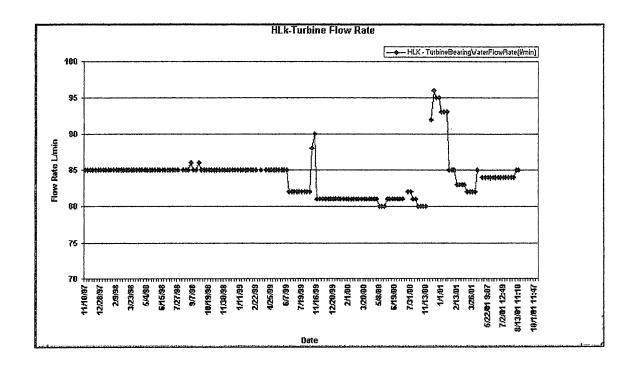
Graph 9 - Upper Generator Guide Bearing Temperature

Graph 9 shows the upper guide bearing temperature since November 1997.

Upper Guide Bearing Temperature Set Points:

	Guide Bearing Temperature
Alarm	70 °C
Trip Unit	80 °C

The upper guide bearing temperature is low due to the extra cooling water that has been supplied to the cooler. The upper guide bearing oil may be operating in a cooler than recommended range. The bearing oil maybe operating in a less than optimum heat range due to this.



Graph 10 - Turbine Cooler Flow Rate

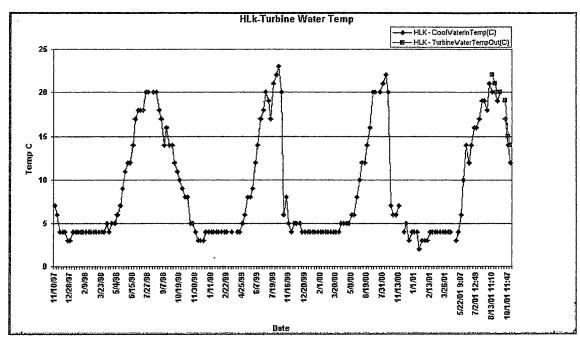
Graph 10 shows the turbine cooler water flow rate since November 1997. The recommended flow rate is 50 L/min.

Actual Velocity Calculations:

Flow Rate Q = 1.42 L/secArea of tube $A = 0.44 \text{ in}^2$

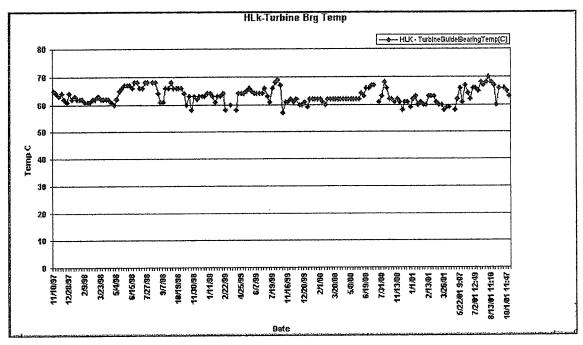
Velocity
$$V = \frac{Q}{A} = 16.4$$
 ft/sec

The turbine cooler flow rate of 85L/min is above the manufactures recommended normal flow rate of 50 L/min. Again this extra cooling water can be used else where within the system seeing all cooling water is supplied form the same common six-inch header.



Graph 11 - Turbine Cooler Water Temperature

Graph 11 shows the turbine cooler water temperature since August 2001. This temperature was not being recorded before and it was recommended that we record this temperature for trending reasons.



Graph 12 - Turbine Bearing Temperature

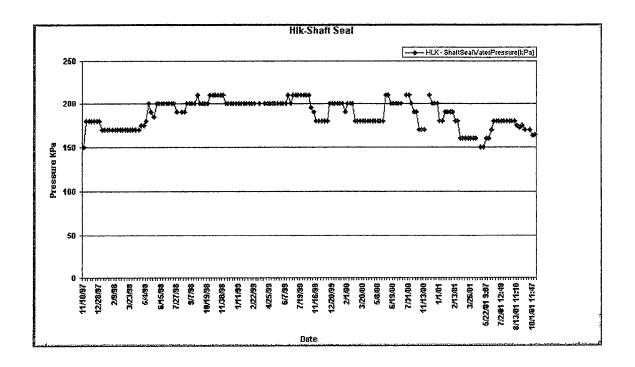
Graph 12 shows the turbine guide bearing temperature since November 1997.

Turbine Bearing Temperature Set Points:

	Turbine Bearing Temperature		
Alarm	75 °C		
Trip Unit	85 °C		

The turbine bearing during the summer months has had high temperatures of 70 °C bring the bearing near the temperature set alarm point of 75 °C. Form this one would think that since the turbine bearing coolers are receiving extra cooling water the temperatures would be lower than what they are. It was recommended that the turbine bearing coolers be check for fouling during the Fall 2001 outage.

The turbine bearing coolers were cleaned during the Fall 2001 outage.



Graph 13 - Shaft Seal Pressure

Graph 13 shows the shaft seal pressure since November 1997. A new shaft seal was installed during the Fall 2000 outage. Due to leakage problems the seal was reseated in late Fall 2000.

Test Samples

In August 2001 water samples from the Hinds Lake plant were sent to BetzDearborn for analysis. The water sample is directly from the penstock supply. Table 3 shows the composition of the water sample.

Composition	Sample #1
PH	6.9
Specific Conductance @ 25C, umhos	25
Alkalinity "P" as CaCO ₃ , ppm	0
Alkalinity "M" as CaCO ₃ , ppm	7.1
Sulfur Total as SO ₄ , ppm	< 5
Chloride as CL, ppm	3.4
Hardness Total as CaCO ₃ , ppm	6.5
Calcium Hardness Total as CaCO ₃ , ppm	4.6
Magnesium Hardness Total as CaCO ₃ , ppm	1.9
Copper Total as Cu, ppm	0.05
Iron Total as Fe, ppm	4.3
Sodium as Na, ppm	2.0
Phosphate Total Inorganic as Po ₄ , ppm	< 0.2
Carbon Total Organic as C, ppm	2.4
Silica Total as SiO ₂ , ppm	1.2

Table 3

In the Fall 2000 two pipe deposits were taken from the SAC piping. Sample #1 was from the four inch supply header and sample #2 was from the 3 inch inlet branch into one of the coolers. Table 4 shows the composition of the SAC piping deposits.

Composition	Sample #1	Sample #2
Iron Fe2O3 + Fe3O4	74 %	19%
Loss on Ignition (LOI)	10%	24%
Manganese MnO ₂	12%	47%
Aluminum Al ₂ O ₃	1%	4%
Calcium CaO	1%	2%
Silicon SiO ₂	1%	1%
Copper CuO	1%	2%
Zinc ZnO		1%

Table 4

From the test samples one can see that the water is almost neutral with little organics. The pipe samples tell us that there is indeed corrosion with a 74% iron content and that there is organic build up with 24% LOI and 47% manganese. The low organics found in the water sample could be the result of when the water sample was taken. It is recommended that another test sample be taken during the spring run off when the organics would be the highest.

The BetzDearborn analysis of the water and piping deposits can be found in Appendix B.

Cost Analysis

Maintenance Cost for Cleaning

In order to clean the service water coolers and piping in Hinds Lake maintenance crew has to be assembled in Bay D'Espoir and drive to Hinds Lake. Travel time to Hinds Lake from Bay D'Espoir is normally six hours.

Travel Arrangements (normal workweek)

Monday: Leave Bay D'Espoir in the morning and drive to the West Coast. Work 4.0

hours upon arriving on site.

Tuesday to Thursday: Regular workweek 8.0 hours per day.

Friday: Work 4.0 hours and then drive back to Bay D'Espoir for the weekend.

Hours of actually work performed on site for one workweek is 32.0 hours.

Perdiem Expenses (\$9 Breakfast, \$11 Dinner, \$18 Supper, \$6 Incidentals (overnight))

Monday: \$34 (no breakfast)

Tuesday to Thursday: \$43 per day Friday: \$20 (no supper or incidentals)

Total Perdiem charge per person per week: \$183

Having a work crew of more than 4 workers will require the services of a cook and perdiem will not be paid while the services of a cook is provided on site.

For the purpose of this study all workers will receive perdiem.

Minimum Work Crew and Wages

- 3 Workers at \$21.56 hr (2 workers on floor, 1 worker operating the crane)
- 1 Supervisor at \$23.72 hr (10% more than the worker)

Total over head costs = salary x 1.63

Travel to site will be by fleet vehicles, 2 required, one supervisor vehicle and one work crew truck. Tools and cleaning equipment will be transported to the site with these vehicles.

The supervisor is usually over seeing two or three jobs while on site. For this cost analysis 1/3 of the supervisors wage will be allocated to the job.

Required gas for travel is \$70 to site and \$70 return from site for one work truck.

Total Cost to Clean SAC

Time required to clean four SAC's for one work crew is four days (32.0 hrs), one cooler per day (8.0 hrs); this includes removal, cleaning, and reinstallation of cooler.

Labour: 3 (workers) x 40.0 hrs (32.0 cleaning, 8.0 driving) x \$21.56 = \$2,587.20 1 (supervisor) x 13.3 hrs (1/3 x 40.0 hrs) x \$23.72 = \$315.48

Total Over Head Costs: \$2,902.68 x 1.63 = \$4,731.37

Perdiem: 4 (work crew) x \$183 = \$732 (Monday \$34, Tuesday to Thursday \$129, Friday \$20)

Gas: 4 (2 vehicles) x \$70 = \$280

Total cost: \$5743.37

Total Cost to Clean SAC Piping

Time required to clean SAC piping inside of generator housing for one work crew is three days (24.0 hrs); this includes removal, cleaning, and reinstallation of piping.

Labour: 3 (workers) x 32.0 hrs (24.0 cleaning, 8.0 driving) x \$21.56 = \$2,069.76 1 (supervisor) x 10.7 hrs (1/3 x 32.0 hrs) x \$23.72 = \$253.80

Total Over Head Costs: $2,323.56 \times 1.63 = 3,787.40$

Perdiem: 4 (work crew) x \$140 = \$560 (Monday \$34, Tuesday to Wednesday \$86, Thursday \$20)

Gas: $4 (2 \text{ vehicles}) \times $70 = 280

Total cost: \$4,627.40

Total Cost to Clean Lower Generator Coolers

Time required to clean six lower generator coolers for one work crew is five days (36.0 hrs), one cooler every 6.0 hours; this includes removal of head cover, cleaning, and reinstallation of head cover.

Labour: 3 (workers) x 40.0 hrs (36.0 cleaning, 4.0 driving) x \$21.56 = \$2,587.20 3 (workers) x 4.0 hrs (4.0 driving) x \$43.12 = \$517.44 (Double Pay, Finish Job) 1 (supervisor) x 13.3 hrs (1/3 x 40.0 hrs) x \$23.72 = \$315.48

Total Over Head Costs: $\$3,420.12 \times 1.63 = \$5,574.80$

Perdiem: 4 (work crew) x \$226 = \$904 (Monday \$34, Tuesday to Friday \$172, Saturday \$20)

Gas: $4 (2 \text{ vehicles}) \times $70 = 280

Total cost: \$6,758.80

Total Cost to Clean Lower Generator Cooler Piping

The lower generator cooler supply and discharge header piping cannot be removed for cleaning due to the confined space in which it is laid. Only the branch piping from the headers to the coolers can be removed for cleaning. Time required to clean branch piping for one crew is 2 days (16.0 hrs); this includes removal of piping, cleaning, and reinstallation of piping.

Labour: 3 (workers) x 24.0 hrs (16.0 cleaning, 8.0 driving) x \$21.56 = \$1,552.32 1 (supervisor) x 8.0 hrs (1/3 x 24.0 hrs) x \$23.72 = \$189.76

Total Over Head Costs: $1,742.08 \times 1.63 = 2,839.59$

Perdiem: 4 (work crew) x \$97 = \$388

(Monday \$34, Tuesday \$43, Wednesday \$20)

Gas: 4 (2 vehicles) x \$70 = \$280

Total cost: \$3,507.59

Total Cost to Clean Upper Generator Cooler

Due to the configuration and location of this cooler mechanical cleaning methods are not practicable. Chemical cleaning could be considered for this cooler. There is no record in J.D.Edwards of this cooler being cleaned.

Total Cost to Clean Upper Generator Cooler Piping

Time required too clean upper generator piping for one crew is 2 days (16 hrs); this includes removal of piping, cleaning, and reinstallation of piping.

Labour: 3 (workers) x 24.0 hrs (16.0 cleaning, 8.0 driving) x \$21.56 = \$1,552.32 1 (supervisor) x 8.0 hrs (1/3 x 24.0 hrs) x \$23.72 = \$189.76

Total Over Head Costs: \$1,742.08 x 1.63 = \$2,839.59

Perdiem: 4 (work crew) x \$97 = \$388 (Monday \$34, Tuesday \$43, Wednesday \$20)

Gas: $4 (2 \text{ vehicles}) \times $70 = 280

Total cost: \$3,507.59

ALTERNATIVE SOLUTIONS

General Information

The fouling problem with regard to the cooling water system is being caused by two problems. The first problem is corrosion of the piping system and the second problem is organic build up. The acidic water supply is causing the piping system to corrode and the organics are then attaching themselves to the corroded pipe. Over time the organics build up and are able to clog the pipe. The heat transferred into the cooling water from the heat exchangers cause the suspended organics in the water to participate out. This then causes the discharge piping to become clogged with organics and choke off the flow rate. A decreased flow rate allows for more organics to settle within the cooling water system. Eventually the entire cooling water system will become clogged with organics.

The following is a list of solutions that can be used to combat this problem.

- 1. Mechanical cleaning of the system.
- 2. Chemical cleaning of the system.
- 3. Replace the piping with corrosion resistant pipe.
- 4. Chemically treat the water.
- 5. Develop a flushing maintenance program.
- 6. Incorporate organic filters.
- 7. Convert the system to a closed loop operation.

A brief description of each proposed solution is discussed below.

Mechanical Cleaning

Mechanical cleaning of the cooling water system will require a maintenance cleaning program if this solution is going to be considered. Without a maintenance cleaning program the reliability of the service water system will be compromised and forced unit outages will happen.

Mechanically cleaning the service water system will require a cleaning maintenance crew and scheduled plant outages to perform the work. The piping and heat exchangers have to be removed from service and physically cleaned by hand. This hand cleaning decreases the life expectancy of both the piping and heat exchangers. The hand cleaning of piping and cooler tubes is done with rotating nylon brushes that physically scrape the pipe walls of organic build up. Also the possibility of mechanical damage is increased when man handling the piping and heat exchangers.

Chemical Cleaning

Chemical cleaning of the service water system requires a maintenance cleaning program to be established. Without a maintenance cleaning program the reliability of the service water system will be compromised and forced unit outages will happen.

Chemically cleaning the service water system will require a cleaning maintenance crew and scheduled plant outages to perform the work. The piping and heat exchangers do don't have to be removed from the system. Instead isolation valves upstream and downstream are closed and mechanical branch connections are attached to the piping system in both upstream and downstream locations. The chemical mixture is then pumped through the system to dissolve any organic build up.

Chemical treatment is harsh on the piping and heat exchangers and decreases their life expectancy. The chemical leaves the metal in an unpassivated state and corrosion will occur very rapidly after returning the system to service.

Replace Piping

Currently the piping material is mild steel schedule 40. Two different piping materials have been considered for replacement of the mild steel pipe, they are 316 stainless steel pipe schedule 10 and polyvinyl chloride (PVC) pipe schedule 80.

The 316 stainless steel schedule 10 pipe is considered because of its corrosion resistance and mechanical properties. The stainless steel pipe will be placed in high traffic areas or in areas where the piping is likely to be hit to prevent damage.

The PVC schedule 80 pipe is considered because of its corrosion resistance, mechanical properties, and thermal properties. Schedule 80 will be more durable when compared with schedule 40. Due to PVC's excellent thermal properties there will be no need to insulate the pipe as compared to stainless steel. The PVC pipe will be placed in low traffic areas where the probability of the pipe being damaged is remote.

Chemical Treatment of the Water

The water can be chemically treated to reduce the acidity of the water by raising the ph level and also help keep all organic materials in a suspended state. The existing service water system is a once through operation and will require large amounts of chemical. BetzDearborn purposed a chemical treatment solution, which can be found in Appendix C. It is estimated to cost \$5,000 to set up this system and \$30,000 per year for chemical usage.

Flushing Maintenance Program

Flushing each cooler individually to remove any organic build up will help keep the service water system clear. Flushing is performed when all water flow is directed through one particular cooler for a predetermined amount of time. Any lose organic material will be forced out of the cooler and washed away.

If a flushing program was implemented it would reduce the amount of lose organic build up within the service water system. The program would consist of flushing the coolers every four weeks starting in the spring and continuing over the summer. The effectiveness of this has not yet been determined.

Organic Filters

Organic filters can be incorporated at the beginning of the service water system to remove the organics from the water. Sand filters are an effective method of removing organics from water. Typical flow rates for sizing a sand filter are 3-6 gpm for every square foot of surface area. The smallest sand filter for Hinds Lake would be around 12 ft in diameter to allow for 630 gpm. Space would then become a problem with this solution.

Closed System Operation

By adding another heat exchanger to the existing service water system one can create a closed system. There are various heat exchangers that can be implemented into the system such as water-to-water, air-to-water, or chemical-to-water.

Water-to-water would be the most practical in this situation due to the amount of heat that is being transferred through the exchanger. An air-to-water heat exchanger would have a very large surface area in order to remove the quantity of heat within the system, making this solution not practical. Using a chemical within the closed circuit system is not necessary considering the temperatures that we are dealing with.

This additional heat exchanger will require pumps, piping and valves in order to be incorporated into the service water system. In addition the style and location of this new heat exchanger will be incorporated into the design of the new system so that maintenance will be easier. Also this system will have 100% capacity back up so that cleaning of the heat exchanger will not require any unit outages.

The use of a cooling pond to supply water to the service water system can be considered a closed loop system because you are reusing the existing water that is in the cooling pond. The water in the cooling pond can be chemically treated to ensure that it remains neutral and does not become acidic. Again space would be a restriction with this type of solution.

VIABLE SOLUTIONS

In order to compare the viable solutions the Net Present Worth (NPW) method will be used to determine which solution is most feasibly from a financial point of view. The NPW method will only take into account the investment dollars needed to bring the solution to life. Other benefits to each solution is not taken into account using the NPW method because of the many variables involved in placing a dollar sign on there worth.

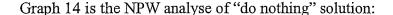
In the conclusions and recommendations section each solution will be discussed including all of the advantages and disadvantages associated with that solution.

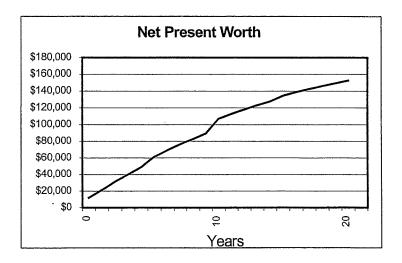
Continue to Maintain Current Operation

The "do nothing" approach is to continue operating the plant as we have in the past. This means mechanically cleaning the SAC's every ten years, generator bearing coolers every five years, SAC piping every ten years, and generator bearing cooler piping every ten years. This solution will require high maintenance and unit outages so that the work can be performed.

NPW Analysis

Below is the NPW analysis of the "do nothing" solution. There is no capital expenditures related to this solution only yearly operating costs as can be seen below.





Graph 14

Table 7 shows the costs associated with this solution:

Capital Cost	
Total	0

Operating Cost	
Pump consumption (49 weeks)	\$11,936
Clean SAC (10 yr)	\$5,743
Clean SAC Piping (10 yr)	\$4,627
Clean L Gen Brg Coolers (5 yr)	\$6,759
Clean L Gen Brg Cooler Piping (10 yr)	\$3,508
Clean U Gen Brg Cooler Piping (10 yr)	\$3,508

Table 7

The NPW is calculated over the life span of the piping, which is 20 years. The inflation rate used is 2%, the power rate used for the pump is \$0.05 kWh, and the rate of return for Hydro is 8.5%.

The total NPW of this solution is \$152,494 for both units.

The spreadsheet for the NPW graph showing the yearly increases can be found in Appendix D.

Replace Piping Inside of Generator Housing

Stainless Steel is recommended as the ideal piping material to be used inside of the generator housing due to its corrosion resistance and mechanical properties. The SAC piping, upper generator cooler piping, and lower generator cooler piping is carbon steel and should be replaced with stainless steel. The turbine cooler piping and shaft seal piping is already stainless steel inside of the generator housing.

SAC Water Piping

The SAC cooler water piping is currently carbon steel with flanges for all the connections. It is recommended to replace the carbon steel with stainless steel sch 10 inside the generator housing. The following table is a list of parts needed to replace the piping with stainless steel. The price quote is from EMCO Distribution Ltd.

Parts Table:

Item#	Part Description	Quantity	Price	Total
1	3" Pipe s.s sch 10	40	\$11.41	\$456.40
2	4" Pipe s.s sch 10	240	\$12.97	\$3,112.80
3	4"x3" Reducer s.s Vic	4	\$90.22	\$360.88
4	4"x4"x4" Tee s.s Vic	1	\$292.93	\$292.93
5	4"x4"x3" Tee s.s Vic	4	\$170.41	\$681.64
6	4" 90-Elbow s.s Vic	1	\$140.58	\$140.58
7	4" 45-Elbow s.s Vic	12	\$101.06	\$1,212.72
8	3" 90-Elbow s.s Vic	12	\$77.76	\$933.12
9	3" 45-Elbow s.s Vic	10	\$70.88	\$708.80
10	3" Butterfly valve c.s Vic-300	8	\$160.02	\$1,280.16
11	3" Flange adapter Vic-741	8	\$41.13	\$329.04
12	3" Coulping c.s Vic-77 with E-Gasket	64	\$16.86	\$1,079.04
13	4" Flange adapter Vic-741	3	\$47.51	\$142.53
14	4" Coulping c.s Vic-77 with E-Gasket	64	\$26.57	\$1,700.48

The total cost for parts is \$12,431.12

Cost Analysis to Replace SAC Water Piping

The labour time required for a crew to replace the piping was calculated using RS Means Mechanical Cost Data 2000. An additional 25% labour time was added to the RS Means calculation for pipe location and space restrictions. Also an additional 15% labour time was added to the RS Means calculation for removal of old piping system. Two additional workers will be placed on this job, shortening the labour time by 50%. RS Means calculations can be found in Appendix E. The costs break down associated with travel, perdiem, and minimum work crew can be found under the Cost Analysis section on page 25.

Total labour time required for work crew of four: 43.4 hrsAdded labour due to pipe location and space restrictions: $43.4 \times 25\% = 10.8 \text{ hrs}$ Labour time for work crew to remove old piping: $54.2 \times 15\% = 8.2 \text{ hrs}$ Total labour time required to complete job = 62.4 hrs

In order to complete this job within the two week scheduled outage all work has to be done within 64.0 hours, leaving 16.0 hours for travel. The supervisor is usually over seeing two or three jobs while on site; therefore only 1/3 of the supervisors wage will be allocated to this particular job. For this cost estimate the supervisor will stay in the nearest hotel.

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Labour: 4 (workers) x 78.4 hrs (62.4 installation + 16.0 driving) x $21.56 = $6,761.22 1 (supervisor) x 26.1 hrs (1/3 x 78.4 hrs) x $23.72 ($21.56 \times 10\%) = $619.10
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Total Over Head Costs: $\$7,380.32 \times 1.63 = \$12,029.92$

Perdiem: 5 (work crew) x 2 weeks x \$183 = \$1,830 (Monday \$34, Tuesday to Thursday \$129, Friday \$20)

Hotel (1 supervisor) = $8 \text{ (nights)} \times \$80 = \$640$

Gas: 4 Trips (2 vehicles) x 2 weeks x \$70 = \$560

Total Cost: \$15,059.92

Upper Generator Bearing Cooler Water Piping

The upper generator cooler water piping is currently carbon steel with flanges for all the connections. It is recommended to replace the carbon steel with stainless steel sch 10 inside the generator housing. The following table is a list of parts needed to replace the piping with stainless steel. The price quote is from EMCO Distribution Ltd.

Parts Table:

Item #		Quantity	Price	Total
1	2" Pipe s.s sch 10	60	\$7.51	\$450.60
2	2" Elbow s.s vic 90 degrees	16	\$70.15	\$1,122.40
3	2" Coupling c.s vic style 77 E gasket	28	\$11.50	\$322.00
4	2" Vic-Flange Adapters style 741 c.s	2	\$36.30	\$72.60

The total cost for parts is \$1,967.60

Cost Analysis to Replace Upper Generator Bearing Cooler Water Piping

The labour time required for a crew to replace the piping was calculated using RS Means Mechanical Cost Data 2000. An additional 25% labour time was added to the RS Means calculation for pipe location and restrictions. An additional 15% labour time was added to the RS Means calculation for removal of old piping system. RS Means calculations can be found in Appendix E. The costs break down associated with travel, perdiem, and minimum work crew can be found under the Cost Analysis section on page 25.

Labour time for work crew of two: 18.1 hrs

Added labour due to pipe location and space restrictions: $18.1 \times 25\% = 4.5 \text{ hrs}$

Labour time for work crew to remove old piping: $22.6 \times 15\% = 3.4 \text{ hrs}$

Total labour time required to complete job = 26.0 hrs

In order to complete this job within the one week scheduled outage all work has to be done within 32.0 hours, leaving 8.0 hours for travel. The supervisor is usually over seeing two or three jobs while on site; therefore only 1/3 of the supervisors wage will be allocated to this particular job.

It will take the work crew up until 2:00 o'clock Thursday afternoon before this job is complete. The work crew will remain on site for Thursday night and drive back to Bay D'Espoir Friday morning.

Labour: 2 (workers) x 34.0 hrs (26.0 installation + 8.0 driving) x \$21.56 = \$1,466.08 1 (supervisor) x 11.3 hrs (1/3 x 34.0 hrs) x \$23.72 (\$21.56 x \$10%) = \$268.04

Total Over Head Costs: $$1,734.12 \times 1.63 = $2,826.61$

Perdiem: 3 (work crew) x \$183 = \$549.00 (Monday \$34, Tuesday to Thursday \$129, Friday \$20)

Gas: 4 Trips (2 vehicles) x \$70 = \$280

Total Cost: \$3,655.61

Lower Generator Bearing Cooler Water Piping

The lower generator cooler water piping is currently curved carbon steel with flanges for all the connections. It is recommended to replace the carbon steel with stainless steel sch 10 inside the generator housing. All curved piping can be substituted with straight pipe using 30 degree and 22 ¼ degree elbows. An AutoCAD drawing can be found in Appendix F showing the new piping arrangement.

The following table is a list of parts needed to replace the piping with stainless steel. The price quote is from EMCO Distribution Ltd.

Parts Table:

Item#	Part Description	Quantity	Price	Total
1	2" Pipe s.s sch 10	40	\$7.51	\$300.40
2	2 1/2" Pipe s.s sch 10	80	\$10.53	\$842.40
3	3" Pipe s.s sch 10	20	\$11.41	\$228.20
4	2 1/2" 90 Long Radius Elbow s.s Vic	4	\$115.00	\$460.00
5	2 1/2" 30 Long Radius 6D Elbow s.s Vic	16	\$206.47	\$3,303.52
6	2 1/2" 22.5 Long Radius 6D Elbow s.s Vic	4	\$249.64	\$998.56
7	2 1/2" x 2" Reducer s.s Vic	4	\$112.45	\$449.80
8	2 1/2" x 2 1/2" x 2" Reducer Tee s.s Vic	8	\$241.00	\$1,928.00
9	2 1/2" x 2 1/2" x 2 1/2" Tee s.s Vic	2	\$234.29	\$468.58
10	3" x 2 1/2" Reducer s.s Vic	2	\$72.88	\$145.76
11	2" 90 Long Radius Elbow s.s Vic	24	\$70.15	\$1,683.60
12	2" Butterfly valve c.s Vic-300	12	\$163.99	\$1,967.88
13	2" Vic Flange Adapter Style 741	12	\$36.30	\$435.60
14	3" Vic Flange Adapter Style 741	2	\$41.13	\$82.26
15	2" Coulping c.s Vic-77 with E-Gasket	80	\$11.50	\$920.00
16	2 1/2" Coulping c.s Vic-77 with E-Gasket	70	\$14.93	\$1,045.10
17	3" Coulping c.s Vic-77 with E-Gasket	2	\$16.86	\$33.72

The total cost for parts is \$15,293.38

Cost Analysis to Replace Lower Generator Bearing Cooler Water Piping

The labour time required for a work crew to replace the piping was calculated using RS Means Mechanical Cost Data 2000. An additional 25% labour time was added to the RS Means calculation due to pipe location and space restrictions. An additional 15% labour time was added to the RS Means calculation for removal of old piping system. Two additional workers will be placed on this job, shortening the labour time by 50%. RS Means calculations can be found in Appendix E. The costs break down associated with travel, perdiem, and minimum work crew can be found under the Cost Analysis section on page 25.

Total labour time required for a work crew of four: 32.6 hrs Added labour due to pipe location and space restrictions, $32.6 \times 25\% = 8.2 \text{ hrs}$ Added labour required to remove old piping: $40.8 \times 15\% = 6.1 \text{ hrs}$ Total labour time required to complete job = 46.9 hrs

In order to complete this job within the two week scheduled outage all work has to be done within 64.0 hours, leaving 16.0 hours for travel. The supervisor is usually over seeing two or three jobs while on site; therefore only 1/3 of the supervisors wage will be allocated to this particular job. For this cost estimate the supervisor will stay in the nearest hotel.

Labour: 4 (workers) x 62.9 hrs (46.9 installation + 16.0 driving) x \$21.56 = \$5,424.50 1 (supervisor) x 21.0 hrs (1/3 x 62.9 hrs) x \$23.72 ($$21.56 \times 10\%$) = \$498.12

Total Over Head Costs: $$5,922.62 \times 1.63 = $9,653.87$

Perdiem: 5 (work crew) x \$183 = \$915 (Monday \$34, Tuesday to Thursday \$129, Friday \$20) 5 (work crew) x \$97 = \$485 (Monday \$34, Tuesday \$43, Wednesday \$20)

Hotel (1 supervisor) = $8 \text{ (nights)} \times \$80 = \$640$

Gas: 4 Trips (2 vehicles) x 2 weeks x \$70 = \$560

Total Cost: \$12,253.87

Replace Piping Outside of Generator Housing

Polyvinyl chloride (PVC) is recommended as the ideal piping material to be used outside of the generator housing due to its corrosion resistance, mechanical properties, thermal properties, and cost. The inlet header and discharge piping should be replaced with PVC.

Inlet Header Piping

The inlet header piping branches off from the main supply header and ascends from the pump floor up the wall to the ceiling where it then runs along the walls into the generator housing. Damage caused by accidental impact should not be of any concern due to this piping arrangement. The inlet header piping will be replaced starting from the discharge side of the cooling water pump and continue to the entrance of the generator housing. The following table is the list of parts needed to replace the inlet piping with PVC. The price quote is from EMCO Distribution Ltd.

Parts table:

Item #	Part Description	Quantity	Price	Total
1	6" Pipe PVC Sch 80	50	\$7.80	\$390.00
2	6" Elbows 90 PVC Socket Sch 80	7	\$26.96	\$188.72
3	6" Flange PVC Socket Sch 80	2	\$48.10	\$96.20
4	6"x5" Reducer PVC Socket Sch 80	1	\$58.20	\$58.20
5	6"x6"x6" Tee PVC Socket Sch 80	1	\$46.31	\$46.31
6	6"x6"x3" Reducing Tee PVC Socket S80	5	\$36.30	\$181.50
7	3"x1 1/2" Reducer Bushing Socket Sch 80	2	\$9.51	\$19.02
8	6" Elbows 45 PVC Socket Sch 80	1	\$34.84	\$34.84
9	6" Butterfly Valve PVC Flanged	2	\$362.01	\$724.02
10	6" Check Valve Wafer PVC Flanged	1	\$646.45	\$646.45
11	5" Flange PVC Socket Sch 80	1	\$25.43	\$25.43
12	3" Pipe PVC Sch 80	20	\$2.86	\$57.20
13	3" Elbows 90 PVC Socket Sch 80	3	\$6.38	\$19.14
14	3" Elbows 45 PVC Socket Sch 80	2	\$14.60	\$29.20
15	3" Butterfly Valve PVC Flanged	1	\$204.33	\$204.33
16	3" Flange PVC Socket Sch 80	4	\$10.57	\$42.28
17	2" Pipe PVC Sch 80	10	\$1.32	\$13.20
18	2" Elbows 90 PVC Socket Sch 80	3	\$2.54	\$7.62
19	2" Butterfly Valve PVC Flanged	1	\$184.85	\$184.85
20	2" Flange PVC Socket Sch 80	2	\$6.07	\$12.14
21	1 1/2" Pipe PVC Sch 80	30	\$1.00	\$30.00
22	1 1/2" Elbows 90 PVC Socket Sch 80	13	\$2.00	\$26.00
23	1 1/2" Elbows 45 PVC Socket Sch 80	1	\$4.42	\$4.42
24	1 1/2" Ball Valve PVC Flanged	5	\$98.53	\$492.65
25	1 1/2" Flange PVC Socket Sch 80	9	\$4.66	\$41.94
26	1.5"x1.5"x1.5" Tee PVC Socket Sch 80	3	\$6.89	\$20.67
27	1 1/2" Pressure Tap Orifice Flanges s.s (1set)	2	\$288.25	\$576.50

The total cost for parts is \$4,172.83

Cost Analysis to Replace Inlet Header Piping

The labour time required for a crew to replace the piping was calculated using RS Means Mechanical Cost Data 2000. An additional 25% labour time was added to the RS Means calculation for pipe location and space restrictions. Also an additional 15% labour time was added to the RS Means calculation for removal of old piping system. One additional worker will be placed on this job, shortening the labour time by 25%. RS Means calculations can be found in Appendix E. The costs break down associated with travel, perdiem, and minimum work crew can be found under the Cost Analysis section on page 25.

Total labour time required for work crew of three: 41.0 hrsAdded labour due to pipe location and space restrictions: $41.0 \times 25\% = 10.2 \text{ hrs}$ Labour time for work crew to remove old piping: $51.2 \times 15\% = 7.7 \text{ hrs}$ Total labour time required to complete job = 58.9 hrs

In order to complete this job within the two week scheduled outage all work has to be done within 64.0 hours, leaving 16.0 hours for travel. The supervisor is usually over seeing two or three jobs while on site; therefore only 1/3 of the supervisors wage will be allocated to this particular job.

Labour: 3 (workers) x 74.9 hrs (58.9 installation + 16.0 driving) x \$21.56 = \$4,844.531 (supervisor) x 25.0 hrs (1/3 x 74.9 hrs) x \$23.72 ($$21.56 \times 10\%$) = \$593.00

Total Over Head Costs: $$5,437.53 \times 1.63 = $8,863.17$

Perdiem: 4 (work crew) x 2 weeks x \$183 = \$1,464.00 (Monday \$34, Tuesday to Thursday \$129, Friday \$20)

Gas: 4 Trips (2 vehicles) x 2 weeks x \$70 = \$560

Total Cost: \$10,887.17

Discharge Header Piping

The discharge piping descends down the outside of the scroll case wall to the floor. Damage caused by accidental impact should not be of any concern due to the location of the piping on the concrete wall. The discharge piping will be replaced from where the stainless steel exits the generator housing and will continue until it meets the piping embedded in the floor. The following table is the list of parts needed to replace the piping with PVC. The price quote is from EMCO Distribution Ltd.

Parts Table:

Item #	Part Description	Quantity	Price	Total
1	6" Pipe PVC Sch 80	20	\$7.80	\$156.00
2	6" Elbows 90 PVC Socket Sch 80	4	\$26.96	\$107.84
3	6" Flange PVC Socket Sch 80	5	\$48.10	\$240.50
4	6"x4" Reducer Coupling PVC Socket Sch 80	1	\$52.14	\$52.14
5	6"x6"x4" ReducingTee PVC Socket Sch 80	1	\$50.72	\$50.72
6	6" Butterfly Valve PVC Flanged	1	\$362.01	\$362.01
7	6" Check Valve PVC Flanged	1	\$646.45	\$646.45
8	4" Pipe PVC Sch 80	40	\$4.17	\$166.80
9	4" Elbows 90 PVC Socket Sch 80	8	\$9.47	\$75.76
10	4" Check Valve PVC Flanged	1	\$549.28	\$549.28
11	4" Butterfly Valve PVC Flanged	3	\$204.33	\$612.99
12	4" Flange PVC Socket Sch 80	9	\$13.36	\$120.24
13	4"x4"x4" Tee PVC Socket Sch 80	1	\$14.27	\$14.27
14	4" Pressure Tap Orifice Flanges s.s (2set)	2	\$689.74	\$1,379.48
15	3" Pipe PVC Sch 80	10 .	\$2.86	\$28.60
16	3" Elbows 90 PVC Socket Sch 80	1	\$6.38	\$6.38
17	3" Butterfly Valve PVC Flanged	1	\$204.33	\$204.33
18	3" Flange PVC Socket Sch 80	2	\$11.12	\$22.24
19	4"x3" Reducer Coupling PVC Socket Sch 80	1	\$25.56	\$25.56
20	3" Pressure Tap Orifice Flanges s.s (1set)	1	\$501.54	\$501.54
21	2" Pipe PVC Sch 80	20	\$1.32	\$26.40
22	2" Elbows 90 PVC Socket Sch 80	1	\$2.54	\$2.54
23	2" Butterfly Valve PVC Flanged	1	\$184.85	\$184.85
24	2" Flange PVC Socket Sch 80	1	\$6.07	\$6.07
25	4"x2" Reducer Coupling PVC Socket Sch 80	2	\$28.99	\$57.98
26	2" Pressure Tap Orifice Flanges s.s (1set)	1	\$479.75	\$479.75
27	1 1/2" Pipe PVC Sch 80	10	\$1.00	\$10.00
28	1 1/2" Elbows 90 PVC Socket Sch 80	2	\$2.00	\$4.00
29	1 1/2" Ball Valve PVC Flanged	1	\$98.53	\$98.53
30	1 1/2" Flange PVC Socket Sch 80	2	\$4.66	\$9.32
31	2"x1 1/2" Reducer PVC Socket Sch 80	11	\$3.45	\$3.45

The total cost for parts is \$6,206.02

Total cost with reusing existing pressure tap orifice flanges is \$3,845.25

Cost Analysis to Replace Discharge Header Piping

The labour time required for a crew to replace the piping was calculated using RS Means Mechanical Cost Data 2000. An additional 25% labour time was added to the RS Means calculation for pipe location and space restrictions. Also an additional 15% labour time was added to the RS Means calculation for removal of old piping system. One additional worker will be placed on this job, shortening the labour time by 25%. RS Means calculations can be found in Appendix E. The costs break down associated with travel, perdiem, and minimum work crew can be found under the Cost Analysis section on page 25.

Total labour time required for work crew of three: 36.0 hrs Added labour due to pipe location and space restrictions: $36.0 \times 25\% = 9.0 \text{ hrs}$ Labour time for work crew to remove old piping: $45.0 \times 15\% = 6.8 \text{ hrs}$ Total labour time required to complete job = 51.8 hrs

In order to complete this job within the two week scheduled outage all work has to be done within 64.0 hours, leaving 16.0 hours for travel. The supervisor is usually over seeing two or three jobs while on site; therefore only 1/3 of the supervisors wage will be allocated to this particular job.

```
Labour: 3 (workers) x 67.8 hrs (51.8 installation + 16.0 driving) x $21.56 = $4,385.31 1 (supervisor) x 22.6 hrs (1/3 x 67.8 hrs) x $23.72 ($21.56 \times 10\%) = $536.07
```

Total Over Head Costs: \$4,921.38 x 1.63 = \$8,021.85

```
Perdiem: 4 (work crew) x $183 = $732

(Monday $34, Tuesday to Thursday $129, Friday $20)

4 (work crew) x $140 = $560

(Monday $34, Tuesday to Wednesday $86, Thursday $20)
```

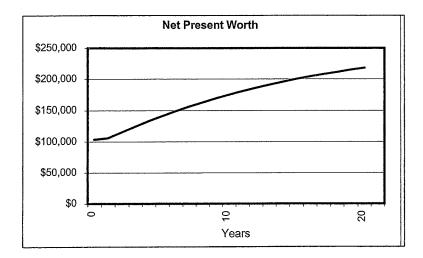
Gas: 4 Trips (2 vehicles) x 2 weeks x \$70 = \$560

Total Cost: \$9,873.85

NPW Analysis

Below is the NPW analysis of the replace piping solution. There are capital expenditures with this solution along with operating expenditures. The capital is for replacing the existing SAC, generator bearing cooler piping inside the generator housing with stainless steel and replace the inlet and discharge header piping outside of the generator housing with PVC.

Graph 15 is the NPW analyse of replacing the pipe solution:



Graph 15

Table 8 shows the costs associated with this solution:

Capital Cost	
SAC Piping (Parts & Installation)	\$27,491
Gen U Brg Piping (Parts & Installation)	\$5,623
Gen L Brg Piping (Parts & Installation)	\$27,547
Inlet Piping (Parts & Installation)	\$15,060
Discharge Piping (Parts & Installation)	\$16,079
Total	\$91,800

Operating Cost	
Pump consumption (49 weeks)	\$11,936

Table 8

The NPW is calculated over the life span of the piping, which is 20 years. The inflation rate used is 2%, the power rate used for the pump is \$0.05 kWh, and the rate of return for Hydro is 8.5%.

The total NPW of this solution is \$218,064.

The spreadsheet for the NPW graph showing the yearly increases can be found in Appendix D.

Closed System Operation

Heat Exchanger Selection

The style of heat exchanger that needed to be selected would have to meet the following criteria:

- 1. Compact design
- 2. Easy to maintain and clean
- 3. Will not clog
- 4. Capacity of 530 Usgpm

It was determined that a plate and frame heat exchanger would meet all of these requirements. Due to it's construction the exchanger can be expanded to meet future cooling requirements by adding more plates and this design also allows for easy access for cleaning.

Tom Furlong of Maynard Reece was contacted for a price estimate on this type of heat exchanger. A quoted price of \$17,500 per unit was established for this cost feasibility study.

Pump Selection

In order to select a pump for this system the pressure drop across the entire cooling water system including the new heat exchanger would have to be known. Using Design Flow Solutions one can enter the entire cooling water system into the program and determine the pressure drop at the desired flow rate.

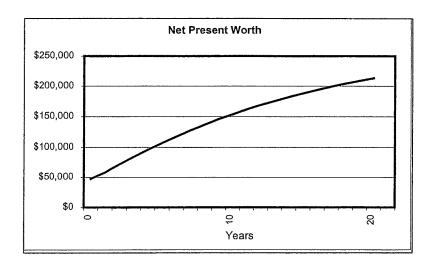
It was determined that the pressure drop for Hinds Lake at 530 Usgpm was 21 psia. A print out of the calculation can be found in Appendix G. Attached is a disk with the system worked through in the Design Flow Solutions program.

The pump selected for this application is a Goulds centrifugal pump 3196 (3 x 4 - 10H, 9" impeller). This pump is capable of 530 Usgpm @ 67 ft head using water as the medium. The pumps specification sheet can be found in Appendix H.

NPW Analysis

The closed loop solution has capital and operating expenditures associated with it. The capital expenditure is for purchasing the heat exchanger, recirculation pump, and associated piping and hardware for the installation. This solution will require 100% capacity back up so two heat exchangers and recirculation pumps will have to be purchased.

Graph 16 is the NPW analyse for the closed loop solution:



Graph 16

Table 9 shows the costs associated with this solution:

Capital Cost	
Pump	\$5,345
Heat Exchanger	\$17,500
Installation Piping & Hardware	\$8,000
Total	\$30,845

Operating Cost	
Pump consumption (49 weeks)	\$11,936
Recir Pump Consumption (49 weeks)	\$4,610

Table 9

The NPW is calculated over the life span of the piping, which is 20 years. The inflation rate used is 2%, the power rate used for the pump is \$0.05 kWh, and the rate of return for Hydro is 8.5%.

The total NPW of this solution is \$213,427.

The spreadsheet for the NPW graph showing the yearly increases can be found in Appendix D.

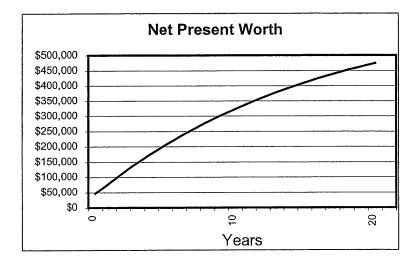
Chemical Injection

The chemical injection solution is based on injecting a chemical known as FLOGARD POT6101 into the cooling water system. This chemical has both cathodic and anodic inhibitors that react with the water to prevent corrosion of the piping and organic build up within the piping. The concentrations are very low 4 ppm and the impact on the environment would be very low considering the chemical is being discharged into the tailrace with the rest of the discharged water.

NPW Analysis

This solution has both capital and operating expenditures. The operating expenditures are very high due to the continuous replacement of the FLOGARD POT6101 chemical.

Graph 17 is the NPW analyse of the chemical injection solution:



Graph 17

Table 10 shows the costs associated with this solution:

Capital Cost	
Injection System	\$5,000
Test Coupon Rack	\$515
Total	\$5,515

Operating Cost	
Pump consumption (49 weeks)	\$11,936
Chemical (49 weeks)	\$30,000

Table 10

The NPW is calculated over the life span of the piping, which is 20 years. The inflation rate used is 2%, the power rate used for the pump is \$0.05 kWh, and the rate of return for Hydro is 8.5%.

The total NPW of this solution is \$473,956.

The spreadsheet for the NPW graph showing the yearly increases can be found in Appendix D.

CONCULSIONS AND RECOMMENDATIONS

From the material presented there were four different solutions that could be taken to resolve the problem. To recap the four alternative solutions were to continue to operate as we have "do nothing approach", replace the piping with corrosion resistant material, inject chemical into the service water for treatment, or install a closed loop system with treated water to cool the units. Each solution has it's benefits and draw backs.

The NPW analysis calculated the following dollar figures for each solution;

Do Nothing	\$152,494
Replace the Piping with s.s & PVC	\$218,064
Closed Loop System	\$213,427
Chemical Injection	\$473,956

Table 11

The "continue to operate as we have" will mean scheduled outages for cooler and pipe cleaning. There is an uncertainty with this solution when it comes to forced outages due to cooling problems during the summer months. If a maintenance program for cleaning and maintaining the cooling water system is not implemented forced outages due to cooling problems during the summer months, in the height of the maintenance season, will occur. In order to prevent this a fouling monitoring program for the cooling water system has to be put in place.

The service water system currently has all of its original piping that was installed when the plant was first came on-line in 1980. This life expectancy of this pipe is near its end. The cooling water pipe will have to be replaced in the near future. A quick calculation of the labour cost associated with replacing that piping is \$52,000 this figure does not include the pipe.

The other alternative of replacing the piping with corrosion resistant pipe has an initial capital investment with a low operating cost associated with it. The labour cost of replacing the pipe in the cooling water system is going to be the same regardless of what type of pipe you use to replace it.

One of the benefits of having the corrosion resistant pipe like stainless steel and PVC is lower maintenance. Unit outages for cleaning service water piping will be less frequent, hence will free up more manpower for other tasks during the maintenance season.

Another benefit to corrosion resistant piping is the reduced likely hood of the pipe becoming clogged with debris. Since the pipe is resistant to corrosion from the service water it is not likely that enough organic material will be able to adhere to the pipe wall to impend flow to the point of stagnation. It is believed that only a small layer of organics will adhere to the inner pipe wall and once that layer is in place the rest of the organics will be washed through the system. Cleaning of the coolers and piping will still have to be done to optimize the efficiency of the system but the frequency of cleanings will be drastically reduced from the current operation.

Another benefit to the replace piping with corrosion resistant pipe solution is that no new equipment or design changes have to be made to the existing system, just replace the existing pipe.

As can be seen from the NPW analysis replacing the piping with corrosion resistant pipe has a NPW of \$218,064 and the other solution of continuing to operate like we have in the past has a NPW of \$152,494. The NPW of the solution to continue to operate as we have has a lower NPW. This NPW figure doesn't include replacing the existing piping with the same mild steel sch 40 pipe. The cost of labour to replace this pipe not including the pipe is \$52,000. If this figure was included into the NPW analysis these two solution would be very close.

The closed loop system has a NPW of \$213,427 making this solution on par with the other alternative solution of replacing the piping with corrosion resistant pipe. The problem with this solution is that it is add on to the existing cooling water system. Seeing that the service water piping is almost at its life expectancy the cost of replacing that piping has to also be considered. A quick calculation of labour costs just to replace the piping not including the pipe is around \$52,000.

With the closed loop solution the piping inside of the generator housing can be mild steel sch 40 pipe and the piping outside of the generator housing can be PVC to help reduce costs. This solution will use treated water for recirculating through the unit and use the existing service water to cool the heat exchangers.

The closed loop solution will have more components with the extra two recirculating pumps and heat exchangers. This increases the chances of more problems within the system. Also Hinds lake power house does not have much room to accommodate such a system.

The maintenance of the unit's coolers and piping will be non-existent but the outside heat exchanger will have to be cleaned. The frequency of this clean will have to be determined from operating the system. These outside heat exchangers should be positioned for easy cleaning.

The chemical injection solution has a NPW of \$473,956 which makes this solution not feasible compared to the other alternative solutions. Also any solution that doesn't impact the environment is always a better alternative.

It is recommended that we go with the solution of "replacing the piping with corrosion resistant pipe" for Hinds Lake. The pipe's life expectancy within the service water system is coming to an end and will need to be replaced in the near future. With this alternative we still have the ability of replacing sections of the existing system year by year until it is all changed over, reducing the over all capital expenditure for that year. Also this solution will result in lower maintenance costs for the system. Another benefit is that no new design work has to be done in order for this solution to be implemented.

APPENDIX A

APPENDIX B



WATER ANALYSIS REPORT

4000018855

NEWFOUNDLAND & LABRADOR HYDRO
HOLYROOD GENERATING STATION
Holyrood, NF
Canada A0A 2-R0

Sampled: 21-AUG-2001 Reported: 04-SEP-2001 Field Rep: Finn, Edward 91000078

	JMO/HLK
	L0823125
рН	6.9
Specific Conductance, at 25°C, µmhos	25
Alkalinity, "P" as CaCO ₃ , ppm	0
Alkalinity, "M" as CaCO ₃ , ppm	7.1
Sulfur, Total, as SO ₄ , ppm	< 5
Chloride, as Cl, ppm	3.4
Hardness, Total, as CaCO3, ppm	6.5
Calcium Hardness, Total, as CaCO3, ppm	4.6
Magnesium Hardness, Total, as CaCO3, ppm	1.9
Copper, Total, as Cu, ppm	0.05
Iron, Total, as Fe, ppm	4.3
Sodium, as Na, ppm	2.0
Phosphate, Total Inorganic, as PO4, ppm	< 0.2
Phosphate, Ortho-, as PO4, ppm	I
Phosphate, Filtered Ortho-, as PO ₄ , ppm	< 0.2
Silica, Total, as SiO ₂ , ppm	1.2



WATER ANALYSIS REPORT

4000018855

NEWFOUNDLAND & LABRADOR HYDRO
HOLYROOD GENERATING STATION
Holyrood, NF
Canada A0A 2-R0

Sampled: 21-AUG-2001 Reported: 04-SEP-2001 Field Rep: Finn, Edward 91000078

	JMO/HLK
	L0823125
Carbon, Total Organic, as C, ppm	2.4
Color, Apparent, Color Units (APHA)	140



WATER ANALYSIS REPORT

4000018855 NEWFOUNDLAND & LABRADOR HYDRO HOLYROOD GENERATING STATION Holyrood, NF Canada AOA 2-RO

Sampled: 21-AUG-2001 Reported: 04-SEP-2001 Field Rep: Finn, Edward 91000078

Result Legend

 $\ensuremath{\text{I}}$ - A chemical or physical interference prevented the labs ability to perform this test.

APPENDIX C

Corrosion Inhibitor Program FLOGARD POT6101

Newfoundland Hydro St. John's, Newfoundland

October 10, 2001

Edward Finn
District Representative

BetzDearborn Canada Inc. P.O. Box 1048 Carbonear. Newfoundland A1Y 1C5

Tel: 709-596-3100 Fax: 709-596-1332

October 18, 2001

Newfoundland Hydro P.O. Box 12400 St. Johns, NF A1B 4K7

Attention:

John Mallam

SUBJECT:

Cooling Water Inhibitor Proposal

John,

Please find below our proposal to treat the once-thru cooling water systems in your Hydroelectric Station with our corrosion inhibitor – **Flogard POT6101**.

In short, we propose that you install a chemical injection and monitoring system to dose the system with 4 ppm of Flogard POT6101.

The annual cost of the chemical treatment, based on continuous operation, would be \$30,000.

We suggest, you monitor the effectiveness of the program by using corrosion coupons that simulate the corrosion in the system and are analyzed in our lab.

THEORY:

The recent set of water samples, taken by yourselves, were tested by our analytical lab in the USA. A short table comparing the important parameters in these tests is below. These have been communicated to you previously, but we show them here for completeness.

As well, we have calculated the Langelier index, which is calculated by a nomagraph and is used in the water treatment industry as an overall indication of the scaling or corrosion tendency of any particular water.

Your waters all had a Langelier's index below –5.0, so these waters would be described as "Very Corrosive". Therefore, the problems you have been experiencing with rust and corrosion are predictable and understandable. Fortunately, they are also preventable with proper chemical treatment.

TABLE 1

	HINDS LAKE	CATARM	UPPER SALMON	BAIE D'ESPOIR
Date	08/21/2001	08/04/2000	08/2001	08/2001
рН	5.9	5.1	5.1	6.2
Conductivity (mmhos)	25	91	24	13.7
'M' alkalinity (ppm)	0.7	< 2	< 2	2.1
Total Hardness (ppm)	6.5	6.5	3.4	3.8
Copper (ppm)	0.05	0.05	0.06	< 0.05
Iron (ppm)	4.3	0.79	0.17	0.08
TOC (ppm)	2.4		5.1	4.7
Langelier Index	- 5.1	- 5	- 5.3	- 5.5

The deposits that we analysed were also reported to you by e-mail. These deposits proved to be high in iron and manganese. The iron is from the rusted piping, while the manganese is chemically associated with the organic matter in the surface water supply. This manganese is noteworthy because it is found in deposits where the surface water is high in organics like these. Manganese does foul piping by depositing on the pipe wall rather than corrode. Fortunately, it is a problem that can be treated chemcially.

In its simplest terms, corrosion is a reaction like the reactions that occur in a conventional lead - acid battery.

The Cathodic reaction is:

$$2H^+ + 2e^- \rightarrow H_2$$

This reaction occurs in a low pH – acidic environment because of the relative abundance of H⁺.

The Anodic reaction is:

This reaction results in the loss of metal from the piping.

If you can stop these reactions from occurring, by stopping the flow of electrons, then the corrosion is stopped .

Chemical corrosion inhibitors basically fall into two broad classes: Anodic and Cathodic, depending on how they act. The product we propose, Flogard POT6101, contains both a Cathodic and an Anodic inhibitor. The phosphate in the product acts as a weak anodic inhibitor, by forming a loosely adhered film of iron phosphate - FePO₄. The Cathodic inhibitor is zinc - Zn. As well, the zinc will sequester the manganese, which is currently causing fouling problems, so the problems with the manganese deposition will be significantly reduced.

PRODUCT:

Please see the Product Bulletin attached for the Inhibitor, which describes the inhibitor in detail. The product is available in both drums and 1136 kg semi - bulk tanks. I suggest, you obtain the product in these semi-bulk tanks. We have also attached product facts and its MSDS for your review.

PRICING:

The dosage is 4 ppm, based on the flow of the water. At an estimated flow rate of 600 imperial gallons per minute-for 24 hrs per-day, 365 days per year, the consumption of the Flogard POT6101 is 7970 kgs per year.

The price of the Flogard POT6101 in these semi-bulk tanks is \$3.85/ kg FCB Pointe Claire, QC. Freight and taxes extra. Therefore, the annual cost of the chemical would be \$30,685. If the facility is run less than 100% of the time, then the consumption will be less - directly proportional to operating hours.

REFERENCES:

BetzDearborn currently treats many similar applications to yours in Atlantic Canada. References include:

Contacts:

Mr. Bob Cass Manager of Water and Wastewater City of Port Hawkesbury Phone: 902-435-1494 Mr. Herve Richard Chief Engineer Noranda Inc. Brunswick Mines Phone: 506-546-6671

Mr. Pat Bellemare
Senior Operator
City of Dartmouth
Phone: 902-435-8300

WORK PLAN / SERVICE:

You should have on-site help from your chemical supplier to implement and monitor this chemical program, particularly since the references above needed to have the chemical introduced at a low concentration, which was gradually increased over several months.

As part of this proposal, we are offering as part of our service, 2-3 days of on-site service during start-up, followed by monthly visits for the first six months of the program and then twice yearly visits thereafter. This service is important. If the program is to succeed, operators need to be familiarized with testing procedures, corrosion coupon installation / changeout, the associated piping racks, chemical dosing pumps and chemical injection procedures and drawdowns. Site visits will be followed up by a written service report by BetzDearborn.

CHEMICAL FEED EQUIPMENT:

We have identified a chemical injection system, with a remote start / stop that would be suitable for this application (see the diagram attached). Prominant Fluid Controls can supply a dual metering pump skid, which can be automized to operate according to our needs. Options-include:

- Duty and standby injection pumps.
- Flow switch to provide alarm if there is loss of chemical injection.
- Automatic switch over to stand-by pump in the event of duty pump failure.

The attached literature describes the Prominent options and provides a discussion matrix to select the chemical injection system to meet your application needs. We would be pleased to assist in selecting this system with Prominent. Budgetary cost for such a system would be \$5000.

CHEMICAL TESTING:

We suggest, you obtain a simple chemical test so that the operators can check the chemical concentration of PO₄ injected into the water. These chemical tests are straight forward and easy to use. Hach sells a simple PO₄ test (catalogue No. 2248-00), they are available from Atlantic Purification systems at 902-469-2806 and cost \$141.33 for a kit with 100 tests.

We will provide any instructions necessary for the operators to run this test. By using this test, we will unsure that the correct concentration of inhibitor is injected into the water.

CORROSION COUPONS:

As you are probably aware, corrosion coupons offer a method to quantitatively measure any reduction in the rate of corrosion over time. Coupons consist of a small strip of metal (either copper or mild steel) that measures approximately $50 \times 10 \times 5$ mm and is inserted directly into the cooling water and left there for some time - typically 100 days. The coupons are then replaced and sent to the lab, where surface corrosion is noted. The weights before and after the in-service period are used to calculate a rate of corrosion in mil/year or g/ft^2 removed per year. Thus, the effectiveness of any corrosion reduction program can be evaluated quantitatively.

To ensure the results are reliable, the coupons must be installed properly and exposed to the correct flow rate. We recommend installation of a 1" diameter, iron corrision rack, with flow control valve, Part No. 2029978. The cost of this unit is \$515.

Do not hesitate to contact me at 709-596-3100, if you would like to discuss our proposal.

Yours truly, BetzDearborn

Edward Finn

District Representative

Idward Tinn

Cc: Shane White Phil Millard Yves Lefebvre

Enc.



Product Facts

FLOGARD™ POT6101 Potable Water Treatment

- NSF Approved for potable water
- Single-product liquid treatment
- Highly effective inhibitor

DESCRIPTION AND USE

FLOGARD™ POT6101 is a liquid blend of phosphate and zinc designed to inhibit corrosion of mild steel in mill supply water systems and once-through cooling systems. Corrosion control is accomplished by two mechanisms. At typical use levels, the major protection is due to the formation of a zinc-phosphate barrier film at the cathodic site of the corrosion cell. Phosphate also provides some additional corrosion protection by promoting the formation of a protective film at the anodic sites.

TREATMENT AND FEEDING REQUIREMENTS

The optimum dosage of FLOGARD POT6101 is a function of the corrosivity of the water to be treated and other conditions particular to a given installation. For best performance, this product should be fed continuously. While the typical feedrate is 4 - 20 ppm, this product is to be used in accordance with control procedures BetzDearborn establishes for a specific application and local potable water guidelines.

FLOGARD POT6101 may be fed directly from the shipping container or diluted to any convenient strength.

Tanks, pumps, piping and valves may be made of 316 stainless steel or most common plastics. Avoid the use of mild steel and copper alloys.

GENERAL PROPERTIES

Physical properties of FLOGARD POT6101 are shown on the Material Safety Data Sheet, a copy of which is available upon request.

PACKAGING INFORMATION

FLOGARD POT6101 is a liquid blend available in a variety of containers and delivery methods. Contact your BetzDearborn representative for details.

STORAGE

Protect from freezing. If this product is frozen during shipment or storage, slight mixing may be required to ensure homogeneity.

SAFETY PRECAUTIONS

A Material Safety Data Sheet containing detailed information about this product is available upon request.



www.betzdearborn.com



ISSUE DATE: 16-JAN-2001

MATERIAL SAFETY DATA SHEET

BetzDearborn Canada, Inc.* 3451 Erindale Station Road Mississauga, ON L5C 2S9

Business telephone: (905) 279-2222

EMERGENCY TELEPHONE (HEALTH/ACCIDENT) (800) 963-5222 (Canada)

(See Section 16 for

additional information) HEALTH:

HMIS RATINGS

FLAMMABILITY:

REACTIVITY:

*Hercules Canada, Inc. and BetzDearborn Canada, Inc. carrying on business as Hercules Canada

PRODUCT IDENTIFICATION

PRODUCT NAME:

FLOGARD POT6101

PRODUCT APPLICATION AREA:

CORROSION INHIBITOR.

2 COMPOSITION / INFORMATION ON INGREDIENTS

Information for specific product ingredients as required by the WHMIS Regulations is listed. Refer to additional sections of this MSDS for our assessment of the potential hazards of this formulation.

HAZARDOUS INGREDIENTS:

Cas# Chemical Name Range (w/w%)

7664-38-2 PHOSPHORIC ACID 15 - 40

Corrosive

ORAL LD50-RAT: 1,530 MG/KG DERMAL LD50-RABBIT: 2,740 MG/KG

INHL. LC50: NO DATA.

7733-02-0 ZINC SULFATE 15 - 40

Severe irritant; potential reproductive toxin

ORAL LD50-RAT: 2,949 MG/KG

DERMAL LD50: NO DATA. INHL. LC50: NO DATA.

No component is considered to be a carcinogen by the U.S. National Toxicology Program (NTP), the International Agency for Research on Cancer (IARC) or under WHMIS.

3 HAZARDS IDENTIFICATION

EMERGENCY OVERVIEW

Severe irritant to the skin. Corrosive to the eyes. Mists/aerosols cause irritation to the upper respiratory tract.

Odor: None; Appearance: Colorless, Liquid

Fire fighters should wear positive pressure self-contained breathing apparatus(full face-piece type). Proper fire-extinguishing media: dry chemical, carbon dioxide, foam or water

POTENTIAL HEALTH EFFECTS

ACUTE SKIN EFFECTS:

Primary route of exposure; Severe irritant to-the skin.

ACUTE EYE EFFECTS:

Corrosive to the eyes.

ACUTE RESPIRATORY EFFECTS:

Primary route of exposure; Mists/aerosols cause irritation to the upper respiratory tract.

INGESTION EFFECTS:

May cause severe gastrointestinal irritation.

TARGET ORGANS:

Prolonged or repeated exposures may cause tissue necrosis. Product or product component may cause reproductive toxicity at maternal toxic levels (based on animal testing).

MEDICAL CONDITIONS AGGRAVATED:

----Not known.

SYMPTOMS OF EXPOSURE:

Inhalation of vapors/mists/aerosols may cause eye, nose, throat and lung irritation. Skin contact may cause severe irritation or burns.

4 FIRST AID MEASURES

SKIN CONTACT:

Wash thoroughly with soap and water. Remove contaminated clothing. Thoroughly wash clothing before reuse. Get medical attention if irritation develops or persists.

EYE CONTACT:

URGENT! Immediately flush eyes with plenty of low-pressure water for at least 20 minutes while removing contact lenses. Hold eyelids apart. Get immediate medical attention.

INHALATION:

Remove to fresh air. If breathing is difficult, give oxygen. If breathing has stopped, give artificial respiration. Get immediate

medical attention.

INGESTION:

Do not feed anything by mouth to an unconscious or convulsive victim. Do not induce vomiting. Immediately contact physician. Dilute contents of stomach using 3-4 glasses milk or water.

NOTES TO PHYSICIANS:

No special instructions

5 FIRE FIGHTING MEASURES

FIRE FIGHTING INSTRUCTIONS:

Fire fighters should wear positive pressure self-contained breathing apparatus (full face-piece type).

EXTINGUISHING MEDIA:

dry chemical, carbon dioxide, foam or water

HAZARDOUS DECOMPOSITION PRODUCTS:

Thermal decomposition (destructive fires) yields elemental oxides.

FLASH POINT:

> 200F > 93C P-M(CC)

6 ACCIDENTAL RELEASE MEASURES

PROTECTION AND SPILL CONTAINMENT:

Ventilate area. Use specified protective equipment. Contain and absorb on absorbent material. Place in waste disposal container. Flush area with water. Wet area may be slippery. Spread sand/grit.

DISPOSAL INSTRUCTIONS:

The waste characteristics of the absorbed material, or any contaminated soil, should be determined in accordance with provincial regulations. Water contaminated with this product may be sent to a sanitary sewer treatment facility, in accordance with any local agreement or discharged under provincial regulations.

Incinerate or land dispose in an approved landfill.

7 HANDLING & STORAGE

HANDLING:

Acidic. Corrosive (Metal). Do not mix with alkaline material.

STORAGE:

Keep containers closed when not in use. Use approved containers only. Store in cool, well-vented area. Contact with metals may release flammable hydrogen gas.

8 EXPOSURE CONTROLS / PERSONAL PROTECTION

EXPOSURE LIMITS

Consult local authorities for acceptable provincial values.

CHEMICAL NAME

PHOSPHORIC ACID

PEL (OSHA): 1 MG/M3 TLV (ACGIH): 1 MG/M3

ZINC SULFATE

PEL (OSHA): NOT DETERMINED TLV (ACGIH): NOT DETERMINED

ENGINEERING CONTROLS:

Adequate ventilation to maintain air contaminants below exposure limits.

RESPIRATORY PROTECTION:

If air-purifying respirator use is appropriate, use a respirator with dust/mist filters.

SKIN PROTECTION:

rubber gloves -- Wash off after each use. Replace as necessary.

EYE PROTECTION:

splash proof chemical goggles

9 PHYSICAL & CHEMICAL PROPERTIES

Specific Grav. (70F, 21C) 1.398	Vapor Pressure (mmHG)	~ 18.0
Freeze Point (F) -13	Vapor Density (air=1)	< 1.00
Freeze Point (C) -25		
Viscosity(cps 70F,21C) 10	<pre>% Solubility (water)</pre>	100.0

Odor		None
Appearance		Colorless
Physical State		Liquid
Flash Point	P-M(CC)	> 200F > 93C
pH As Is (approx.)	1.4
Evaporation Rate	(Ether=1)	< 1.00

NA = not applicable ND = not determined

10 STABILITY & REACTIVITY

STABILITY:

Stable under normal storage conditions.

HAZARDOUS POLYMERIZATION:

Will not occur.

INCOMPATIBILITIES:

May react with strong oxidizers.

DECOMPOSITION PRODUCTS:

Thermal decomposition (destructive fires) yields elemental oxides.

BETZDEARBORN INTERNAL PUMPOUT/CLEANOUT CATEGORIES: "B"

D

11 TOXICOLOGICAL INFORMATION

Oral LD50 RAT: >2,000 mg/kg
NOTE - Estimated value

Dermal LD50 RABBIT: >2,000 mg/kg
NOTE - Estimated value

12 ECOLOGICAL INFORMATION

AQUATIC TOXICOLOGY

Rainbow Trout 96 Hour Static Acute Bioassay

LC50: 21.3 mg/L

No Effect Level: 15.5 mg/L

Daphnia magna 48 Hour Static Acute Bioassay for the

LC50: 3.8 mg/L

No Effect Level: 3.2 mg/L

Fathead Minnow 96 Hour Acute Toxicity

Product toxicity determined from bioassays conducted on individual components.

LC50: 16 mg/L

No Effect Level: 6.3 mg/L

BIODEGRADATION

No Data Available.

13 DISPOSAL CONSIDERATIONS

Incinerate or bury in approved landfill. Please be advised that there may be additional local or provincial requirements relating to the disposal of waste. Consult provincial and local regulations regarding the proper disposal of this material.

14 TRANSPORT INFORMATION

Transportation of Dangerous Goods:

Proper Shipping Name: Corrosive Liquids, n.o.s.

(Phosphoric Acid)

PIN: UN1760; Classification: 8(9.2); Packing Group: III

15 REGULATORY INFORMATION

This product has been classified in accordance with the hazard criteria of the CPR and the MSDS contains all the information required by the CPR. CEPA:

All components of this product comply with substance notification requirements under CEPA.

WHMIS CLASSIFICATION:

D2A D2B

FOOD AND DRUG ADMINISTRATION:

The ingredients in this product are Generally Recognized As Safe by FDA for direct addition to human food.

16 OTHER INFORMATION

NFPA/HMIS CODE TRANSLATION

Health	3	Serious Hazard
Fire	0	Minimal Hazard
Reactivity	0	Minimal Hazard
Special	CORR	DOT corrosive
(1) Protective Equipment	В	Goggles,Gloves

⁽¹⁾ refer to section 8 of MSDS for additional protective equipment recommendations.

CHANGE LOG

	EFFECTIVE		
	DATE	REVISIONS TO SECTION:	SUPERCEDES
MSDS status:	22-MAY-1998		** NEW **
	09-DEC-1998	15	22-MAY-1998
	23-MAR-2000	15	09-DEC-1998
	07-APR-2000	4	23-MAR-2000
	14-JUL-2000	15	07-APR-2000
	16-JAN-2001	14	14-JUL-2000

Prepared by the Regulatory Affairs Group, BetzDearborn Canada, Inc. Telephone: 1(905)279-2222 Date of preparation: 16-JAN-2001



Corrosion Test Coupon Racks

BetzDearborn Corrosion Test Coupon Racks provide a convenient means of monitoring the progress of corrosion in systems such as boilers, condensate lines, open recirculating cooling water, closed circulating hot or chilled water systems, etc. The corrosion test rack creates a side stream off the main system in which corrosion test coupons can be exposed to system water under controlled and reproducible conditions.

The corrosion coupons can be periodically removed and either visually examined or returned to the laboratory for determination of weight loss, corrosion rate, and pitting severity.

BLACK IRON CORROSION RACK

The Black Iron Corrosion Rack is recommended for corrosion monitoring in high temperature and/or highpressure installations such as steam condensate, high temperature water, hydronic heating, recirculating process systems, etc. The Black Iron Rack is constructed of 1" threaded black iron pipe. It is supplied with four 1" MNPT steel mounting plugs, and one 10 gpm Dole™ flow control valve. Caution: Maximum pressure & temperature are limited by the Dole flow control valve.

Maximum Pressure: 200 psig (13.8 bar)

Maximum Temperature: 160° F (71° C)

PVC CORROSION RACK

The PVC Corrosion Rack is recommended for corrosion monitoring in low temperature systems such as open recirculating cooling water systems, chilled

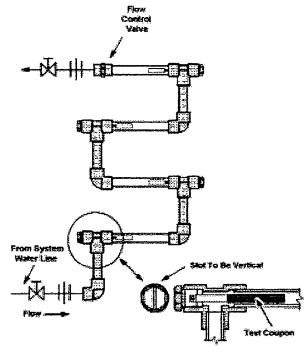


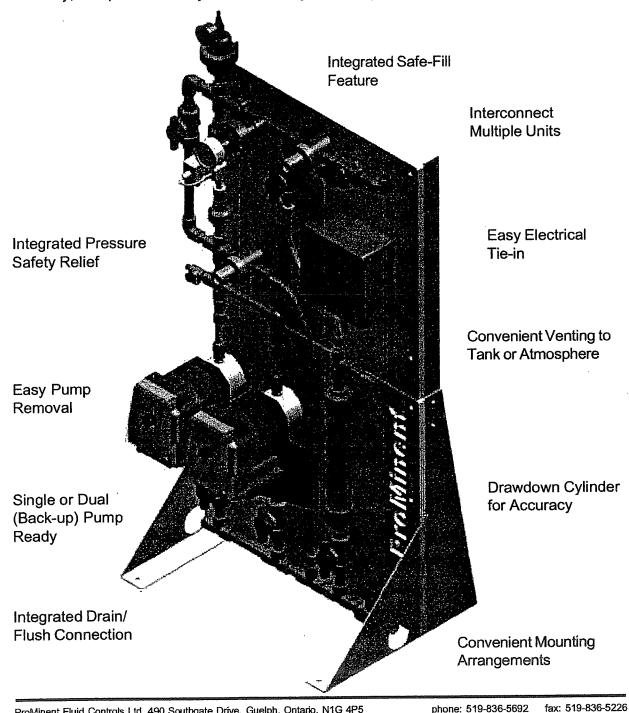
Figure 1

water, process water systems, etc. The PVC Rack is constructed of 1" threaded Sched. 80 PVC pipe. It is supplied with four 1" PVC mounting plugs and an 8 gpm Dole™ flow control valve. Two designs are available. One is constructed of all gray, opaque PVC. The other features transparent pipe sections for viewing the test coupons in place. See Figures 1 & 2. To discourage algae growth in the transparent sections, opaque snap-on pipe covering is supplied with this corrosion rack.

FLOW RATE	VE	LOCITY
	1" PVC Rack	1" Black Iron Rack
5 gpm	2.2 ft/sec (0.67 m/sec)	1.9 ft/sec (0.58 m/sec)
8 gpm	3.6 ft/sec (1.1 m/sec)	3.0 ft/sec (0.91 m/sec)
10 gpm	4.5 ft/sec (1.4 m/sec)	3.7 ft/sec (1.3 m/sec)
12 gpm	5.4 ft/sec (1.6 m/sec)	4.4 ft/sec (1.4 m/sec)

MODULAR DOSING SYSTEM... Function by Design

Offering industry a new standard in convenience, safety, and reliability. ProMinent's new modular design concept allows custom-tailored arrangements to suit your immediate needs. Matched with our exceptional line of chemical metering pumps - the functionality, flexibility, and performance you demand is yours today - all this at an industry-valued price.



phone: 519-836-5692 phone: 412-787-2484

fax: 412-787-0704

MODULAR SELECTION... As Easy as 1-2-3

STEP ONE: Select Pump

Using Prominent's comprehensive catalog determine the pump capacity and pressure you require. Up to 2 pumps may be incorporated into a single package - dual pumps offer redundent function and convenience for continuous dosing. You may choose any of ProMinent's line of compact Solenoid-driven metering pumps - Concept, Beta, Gamma, Gala in most sizes and materials.

STEP TWO: Select Modules

Two modules are currently available. The Suction Module includes provision for up to 2 pumps - 1 primary, the other a backup. A calibration column for setting the pump for optimum performance, and all manual control valves required to isolate and service the system easily. The Discharge Module comes standard with integrated safety relief valve, our "Safe-Fill" feature, dual function Priming/Bleed valve and all necessary isolation valves. Just add any or all of the options below for added functionality and performance...

STEP THREE Select Options and Accessories

Select from a handful of safety and performance enhancements like...

- Pressure Gauge/Seal to accurately tune your system for the best results.
- Pulsation Dampener to improve flow characteristics and repeatability.
- Back Pressure Valve for better pump performance under variable conditions.
- Flow Monitor for flow confirmation.

above each letter location.

- Convenient junction box for all system wiring.
- Mounting arrangement wall-mount is standard, or you may choose floor stands or tote mount hanging brackets.

ABC-DEF-GHI-J KL-M MOD В C **Material Of Construction** Elastomer I/O Connection Size / Type 1/2" FNPT Schedule 80 PVC **EPDM** FPM (Viton) D G Suction Module Discharge Module Flow Monitor Option Wall-mount Module with Back Panel Not Applicable Not Applicable includes Pump Shelf (1), Calibration Wall-mount Module with Back Panel Type 1 or 2 Flow Monitor (1), and and "Safe-Fill" feature includes PRV Column (1), Ball Valves (3), and Pipe & Fittings Pipe & Fittings (1), Ball Valves (3), and Pipe & Type 3 Flow Monitor (1) with Bypass includes Ball Valve (1) and Pipe & E Calibration Column Pressure Gauge & Seal Kit 100 mL Not Applicable **Back Panel Mount Option** 500 mL Kit includes Pressure Gauge with Not Applicable Multiply Pump Strokes per Minute integral Seal (1), and Pipe & Fittings Corrosion-resistant, Plastic Floor by Pump mL per Second for 60 sec. Mount drawdown Corrosion-resistant, Stainless Steel Pulsation Dampener Kit Tote Mount Not Applicable Backup Pump Mount Kit Kit includes Pulsation Dampener (1), and Pipe & Fittings Not Applicable M Junction Box Option Kit includes Pump Shelf (1), Ball Valve (1), and Pipe & Fittings Not Applicable Back Pressure Valve Kit Option includes Prewired JB (1) for Not Applicable Single Pump Circle each number that applies Kit includes BPV (1), and Pipe & Option includes Prewired JB (1) for Dual Pump to your configuration and enter

Viton® is a registered trademark of Dupont Dow Elastomers

Maximum Pressure: 200 psi at 70° F (13.8 bar at 21° C) 120 psi at 120° F (6.9 bar at 49° C)

70 psi at 140° F (4.8 bar at 60° C)

FLOW VS VELOCITY CHART

Velocities in **BOLD** indicate standard flow controller supplied with that rack. For other available Dole flow control valves, see Equipment Fact Sheet EF15-07.

OPTIONS

A Corrater™ probe may be installed in the corrosion rack to provide instantaneous corrosion readings to supplement the data provided by the weight loss corrosion coupons.

CORROSION TEST RACK INSTALLATION

- The Corrosion Test Rack may be assembled for vertical mounting as shown in Figure 1, or a horizontal position, Figure 2. Items shown in single line schematic are not furnished.
- Attach the corrosion rack to a wall or column.
 DO NOT suspend it from the supply and return piping alone.
- To avoid air binding, pipe the corrosion rack so that water will flow upward through it, and in such a way that it will remain full of water at all times and not backdrain when the main recirculating system shuts own.
- 4. Install gate or ball-type isolation valves of both sides of the rack.
- DO NOT use this bypass loop for any other purpose such as chemical injection, or mounting of conductivity or pH sensors.

- 6. For measurement of corrosion at points of highest temperature in the circulating system, the water supply to the corrosion rack should be from the exit of the heat exchanger(s). Average corrosion rate measurements may be obtained by supplying the corrosion rack with water from the main cooling tower riser, etc.
- Return water may be piped to the recirculating pump suction header, cooling tower basin, or other suitable point with sufficiently low pressure to insure flow through the rack.
- Flow velocities should not be variable. Avoid extremely high or low velocity conditions. A Dole™ or other suitable flow control valve is recommended to insure constant velocity.
- For PVC Test Racks with transparent viewing sections, install the slotted polyfoam pipe insulation over the transparent sections to discourage algae growth.

CORROSION TEST COUPON INSTALLATION

- Keep the metal test coupon in the special treated envelope BEFORE AND AFTER exposure.
- DO NOT leave fingerprints on the coupon. They will cause false corrosion readings.
- 3. Attach the coupon to the mounting stud using the special nut and bolt provided.

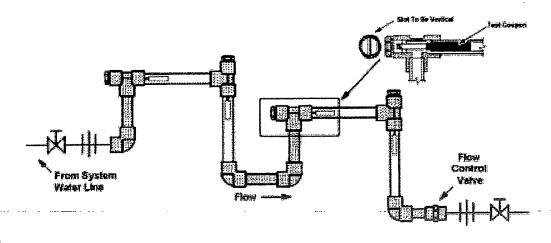


Figure 2

- 4. Corrosion coupons should always be installed so the water flow first over the plastic mounting rod and then over the coupon. Water flowing directly onto the coupon may cause erosion-corrosion and lead to false weight loss measurements.
- Use ONLY Teflon™ thread sealing tape on mounting plug threads. DO NOT use pipe dope.
- The witness slot on the coupon mounting plug should be parallel with the flat surface of the corrosion test coupon. Install the mounting plug in the tee and align the witness slot (and coupon) in the VERTICAL position as shown in Figure 1.
- Note the date of installation on back of the white Tyvek™ Coupon Return Envelope (ENG 322) and retain both the Coupon Return Envelope and the treated brown envelope.
- When removing, each test coupon should be carefully dismounted from the holder and immediately dried with a blast of hot air or blotted with a paper towel or clean rag. DO NOT CLEAN. Reinsert the coupon in the treated brown envelope in which it was received.
- Complete the back of the white Coupon Return
 Envelope, insert the treated brown envelopes
 with coupons inside, and return the envelope with
 the coupons to the Woodlands laboratory.

Part Numbers

2013971 Corrosion Rack, PVC, 1" NPT, w/ 4 coupon holders & 8 gpm flow control valve.

2042205 Corrosion Rack, PVC, 1" NPT w/ 4 coupon holders, 8 gpm valve and 4 TRANSPARENT viewing sections.

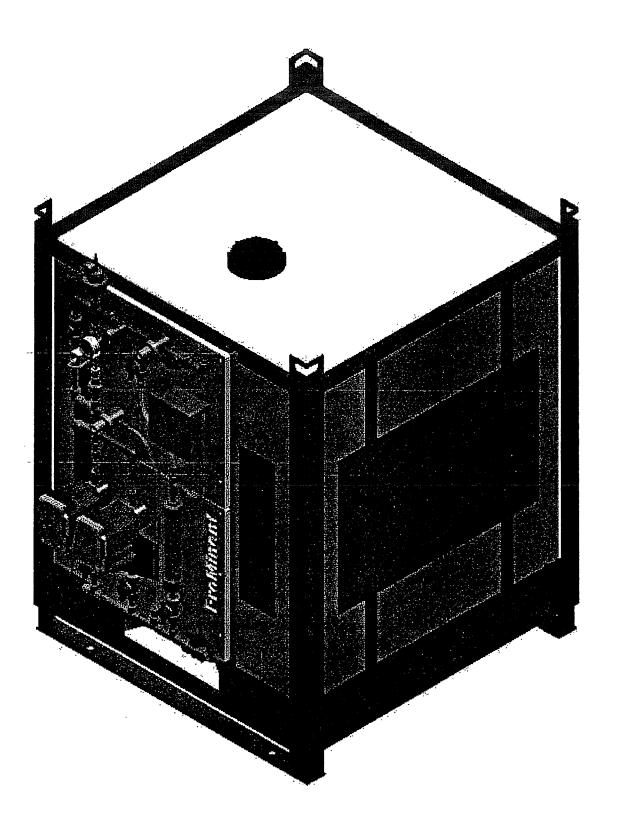
2029978 Corrosion Rack, Black Iron, 1" NPT, w/ 4 coupon holders & 10 gpm flow control valve.

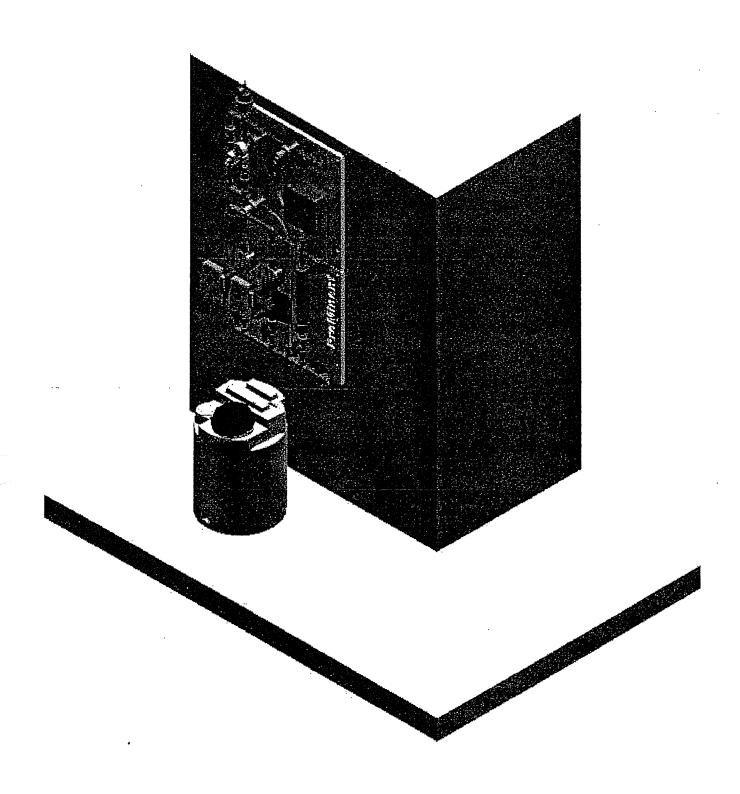
2032806 Corrosion Rack, 304 SS, 1" NPT, w/ 4 coupon holders.

2015850 Replacement Coupon Holder, 1" PVC w/ 6" stem.

2041977 Replacement Coupon Holder, 1" Black Iron w/ 6" Teflon™ Stem and Teflon nut & Screw

Corrosion test coupons and mounting screws are not supplied with the corrosion rack and must be ordered separately from the BetzDearborn Woodlands, TX laboratory.





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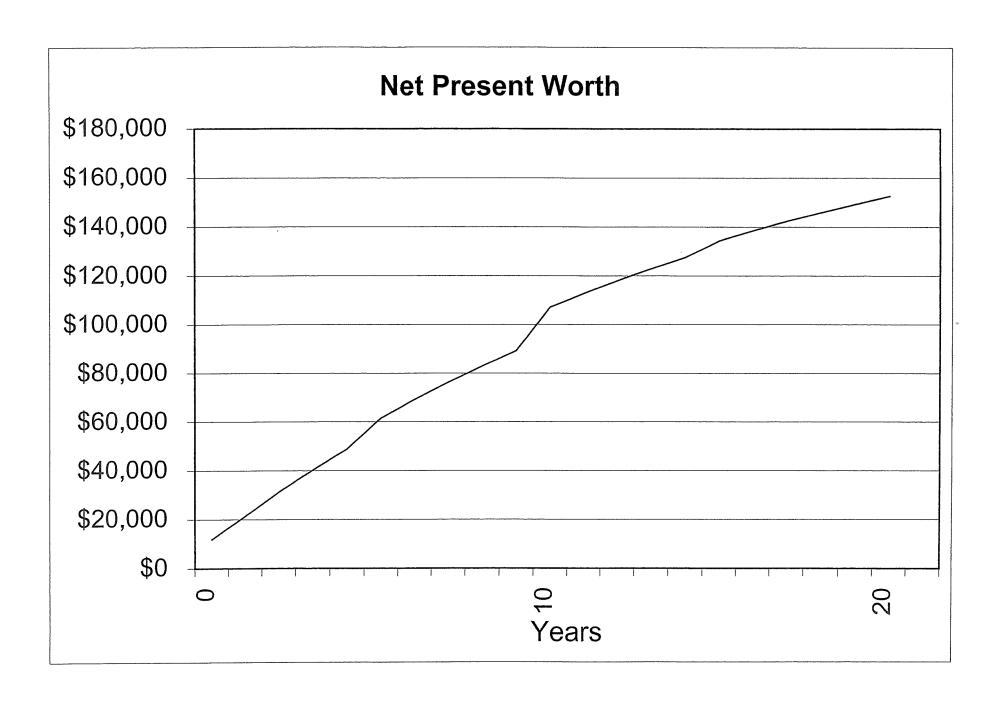
APPENDIX D

DO NOTHING

Capital Cost		
Total		0

Operating Cost		
Pump consumption (49 weeks)	\$11,936	
Clean SAC (10 yr)	\$5,743	
Clean SAC Piping (10 yr)	\$4,627	
Clean L Gen Brg Coolers (5 yr)	\$6,759	
Clean L Gen Brg Cooler Piping (10	\$3,508	
Clean U Gen Brg Cooler Piping (10	\$3,508	

	Year	Cash Flow	NPW
0	2002	\$11,936	\$11,936
1	2003	\$12,175	\$21,344
2	2004	\$12,419	\$31,066
3	2005	\$12,667	\$40,206
4	2006	\$12,920	\$48,799
5	2007	\$20,641	\$61,451
6	2008	\$13,442	\$69,045
7	2009	\$13,711	\$76,184
8	2010	\$13,985	\$82,895
9	2011	\$14,265	\$89,204
10	2012	\$43,983	\$107,133
11	2013	\$14,841	\$112,709
12	2014	\$15,138	\$117,951
13	2015	\$15,441	\$122,879
14	2016	\$15,750	\$127,512
15	2017	\$25,161	\$134,333
16	2018	\$16,386	\$138,427
17	2019	\$16,714	\$142,276
18	2020	\$17,048	\$145,894
19	2021	\$17,389	\$149,296
20	2022	\$17,737	\$152,494

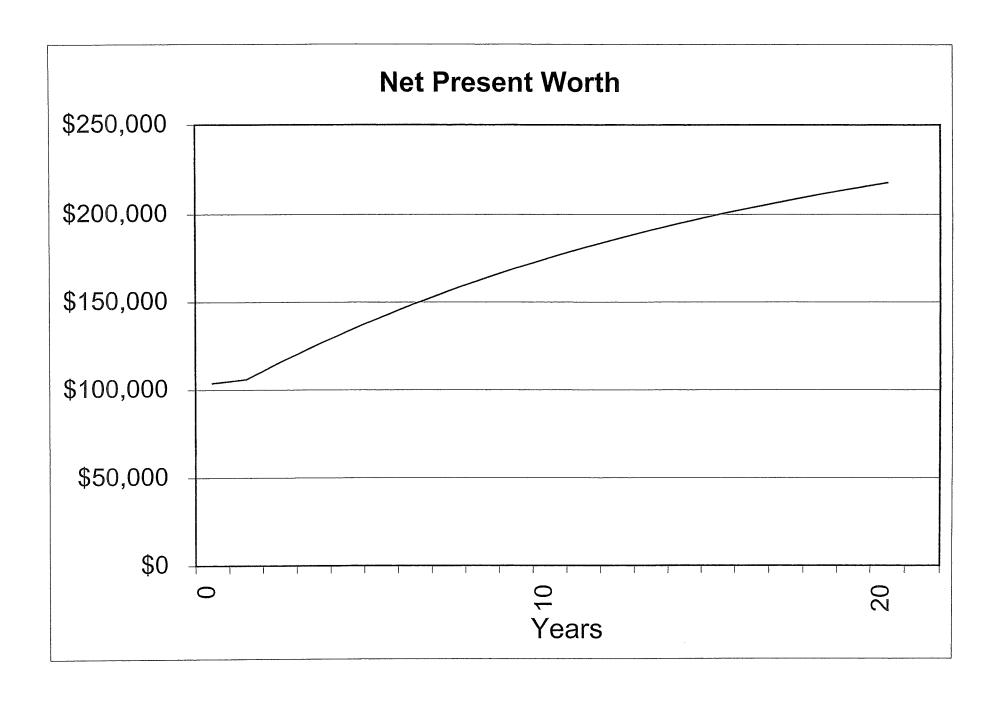


REPLACE PIPING

Capital Cost		
SAC Piping (Parts & Installation)	\$27,491	
Gen U Brg Piping (Parts & Installation)	\$5,623	
Gen L Brg Piping (Parts & Installation)	\$27,547	
Inlet Piping (Parts & Installation)	\$15,060	
Discharge Piping (Parts & Installation)	\$16,079	
Total	\$91,800	

Operating Cost	
Pump consumption (49 weeks)	\$11,936

	Year	Cash Flow	NPW
0	2002	\$103,737	\$103,737
1	2003	\$12,175	\$105,952
2	2004	\$12,419	\$115,675
3	2005	\$12,667	\$124,815
4	2006	\$12,920	\$133,407
5	2007	\$13,179	\$141,485
6	2008	\$13,442	\$149,079
7	2009	\$13,711	\$156,218
8	2010	\$13,985	\$162,930
9	2011	\$14,265	\$169,239
10	2012	\$14,550	\$175,170
11	2013	\$14,841	\$180,746
12	2014	\$15,138	\$185,988
13	2015	\$15,441	\$190,916
14	2016	\$15,750	\$195,548
15	2017	\$16,065	\$199,904
16	2018	\$16,386	\$203,998
17	2019	\$16,714	\$207,847
18	2020	\$17,048	\$211,465
19	2021	\$17,389	\$214,867
20	2022	\$17,737	\$218,064

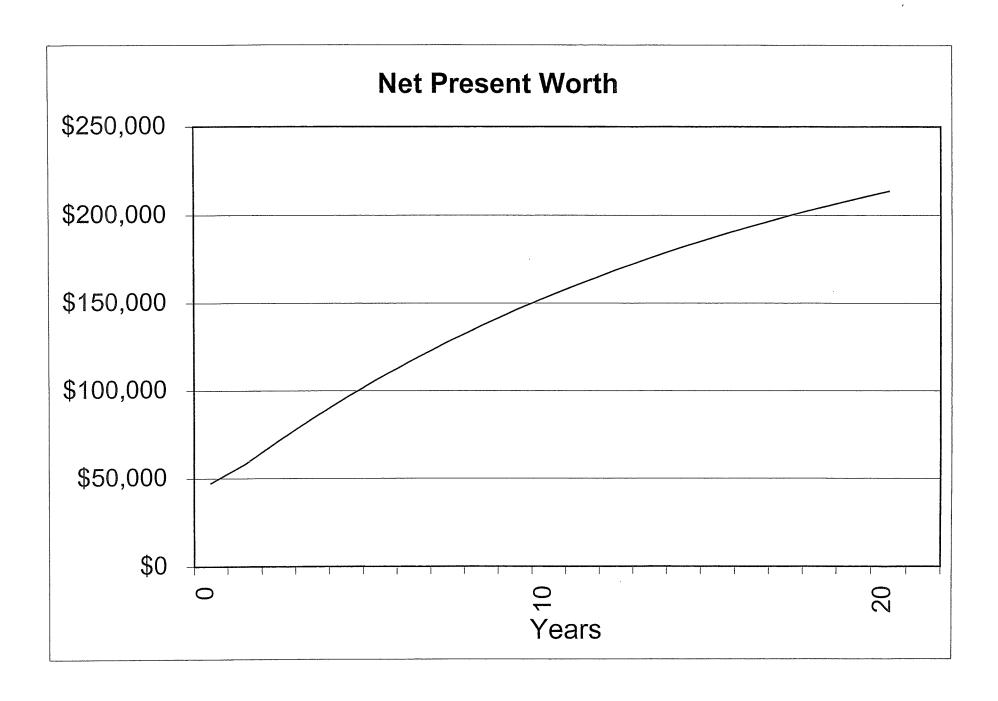


CLOSED LOOP SYSTEM

Capital Cost	
Pump	\$5,345
Heat Exchanger	\$17,500
Installation Piping & Hardware	\$8,000
Total	\$30,845

Operating Cost	
Pump consumption (49 weeks)	\$11,936
Recir Pump Consumption (49 weeks)	\$4,610

	Year	Cash Flow	NPW
0	2002	\$47,391	\$47,391
1	2003	\$16,877	\$58,015
2	2004	\$17,215	\$71,493
3	2005	\$17,559	\$84,163
4	2006	\$17,910	\$96,074
5	2007	\$18,269	\$107,272
6	2008	\$18,634	\$117,799
7	2009	\$19,007	\$127,695
8	2010	\$19,387	\$136,998
9	2011	\$19,774	\$145,744
10	2012	\$20,170	\$153,966
11	2013	\$20,573	\$161,696
12	2014	\$20,985	\$168,962
13	2015	\$21,405	\$175,793
14	2016	\$21,833	\$182,215
15	2017	\$22,269	\$188,252
16	2018	\$22,715	\$193,928
17	2019	\$23,169	\$199,263
18	2020	\$23,632	\$204,279
19	2021	\$24,105	\$208,994
20	2022	\$24,587	\$213,427

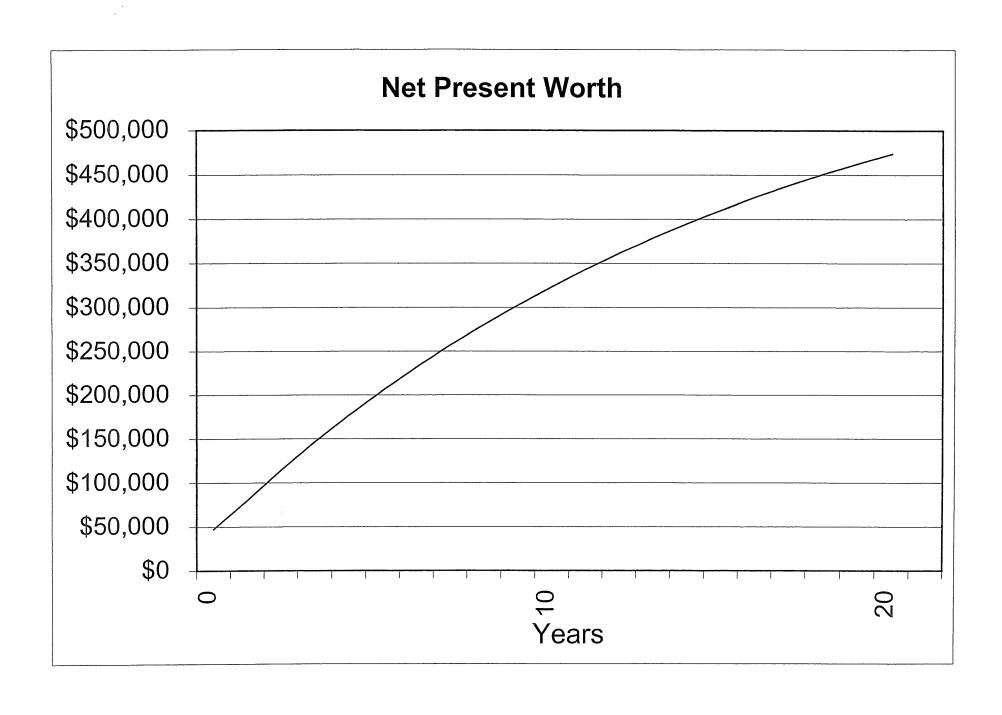


CHEMICAL INJECTION

Capital Cost	
Injection System	\$5,000
Test Coupon Rack	\$515
Total	\$5,515

Operating Cost	
Pump consumption (49 weeks)	\$11,936
Chemical (49 weeks)	\$30,000

	Year	Cash Flow	NPW
0	2002	\$47,451	\$47,451
1	2003	\$42,775	\$80,070
2	2004	\$43,631	\$114,228
3	2005	\$44,503	\$146,341
4	2006	\$45,393	\$176,529
5	2007	\$46,301	\$204,909
6	2008	\$47,227	\$231,589
7	2009	\$48,172	\$256,671
8	2010	\$49,135	\$280,250
9	2011	\$50,118	\$302,416
10	2012	\$51,120	\$323,255
11	2013	\$52,143	\$342,845
12	2014	\$53,185	\$361,261
13	2015	\$54,249	\$378,574
14	2016	\$55,334	\$394,850
15	2017	\$56,441	\$410,151
16	2018	\$57,570	\$424,536
17	2019	\$58,721	\$438,058
18	2020	\$59,896	\$450,771
19	2021	\$61,093	\$462,722
20	2022	\$62,315	\$473,956

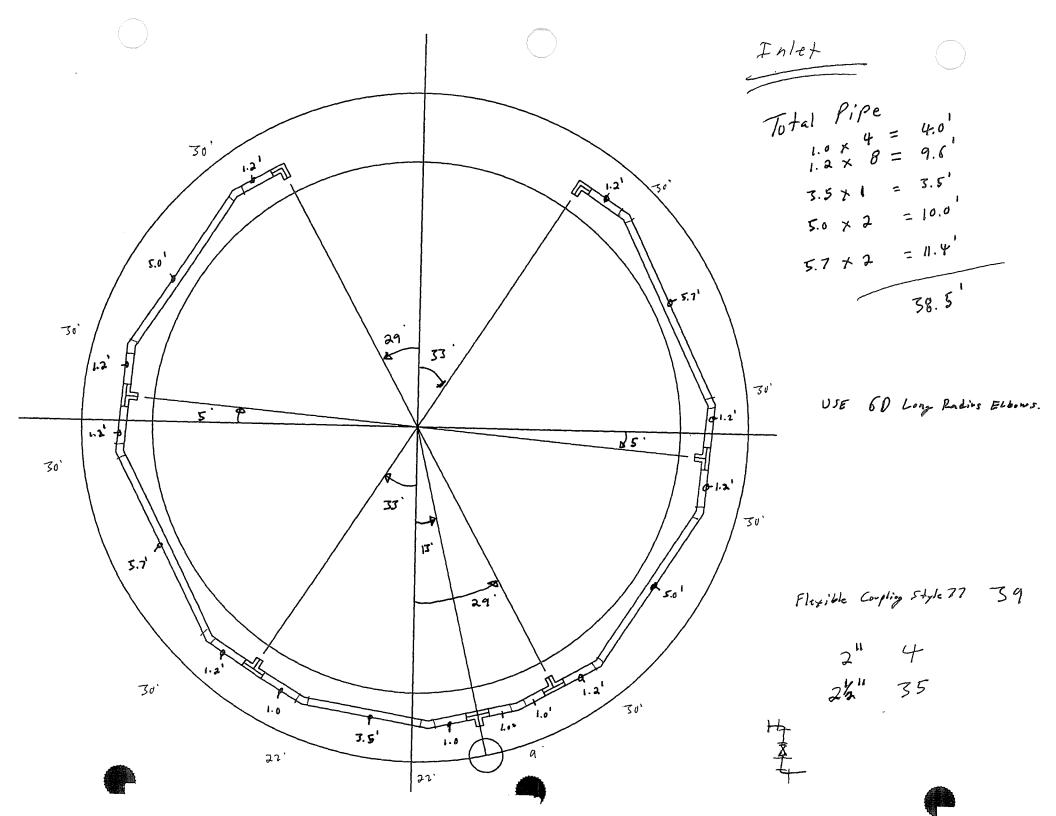


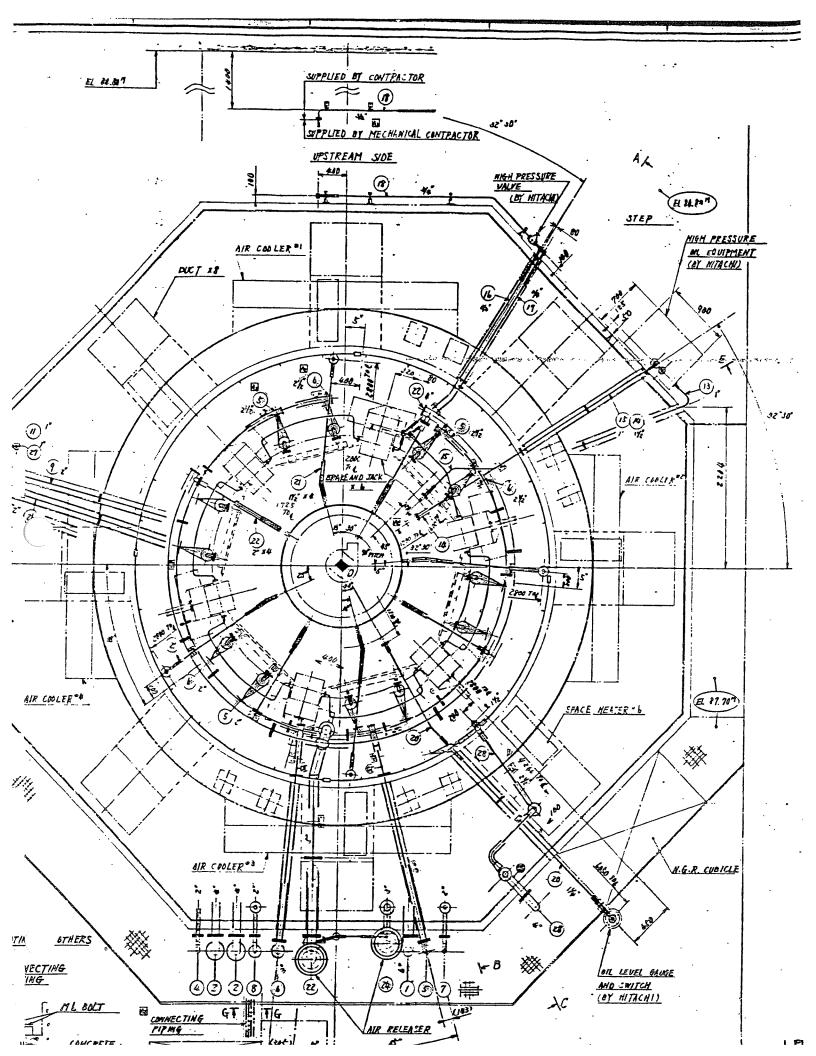
APPENDIX E

Labour Costs, 1					
Upper Gen Pip	ing (2")				
Estimate			actu	ial	
	Clen	days	Quantity	days	THE STATE OF THE S
50 h 10, black, 2"	1960m	43'	60'	1.40	
70° \$45° ELLONE 2"	IPLUM	25	16	0.84	
Corpling, 2"	IPLUA	50	21	0.56	
lanze, 2"	IPLUM	23	2	0,09	and the second s
11 Greve, 2"	QI	11 6	21	0.24	
Fine required for Add Additional Lab	I Plum z	line by 25%	2.19 × 0.75 =	2.02 days	·
Time required for	I Plum z	line by 25%		2.02 = Jays	
Time required for Add Additional Las	I Plum z bour reducer t al Cren =	0.24 days	, 2.19 × 0.75 =	days	
Time required for Add Additional Las	I Plum z bour reducer t al Cren =	0.24 days	, 2.19 × 0.75 =	days	
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Fine required for Add Additional Lad Time required for a Total time for Total time for	1 PUM Z Lour seducer + Qlaren = Qlatours =	o. 24 days 2. 26 da The pipings	2.19 x 0.75 =	0,34 days	
ine required for Add Addition Laboration to the for total time for	1 PUM Z Lour seducer + Qlaren = Qlatours =	o. 24 days 2. 26 da The pipings	2.19 x 0.75 =	0,34 days	bes)
ine required for Add Additional Lad Time required for a Total time for Statistica time toguin	1 PUM Z Lour seducer + Qlaren = Qlatours =	o. 24 days 2. 26 da The pipings	2.19 x 0.75 =	0,34 days	

abour Costs, Hik a:= IPUM. + 1 App. (3", 2", + 2") Estimate Artual days Quantity Cron 55' 0.36 52410, black, 3" 20' Q. 61' 80' 1.31 ch 10, dach, 2"2" 2, 40' 43' 0.93 Seg10, 6/42, 2" 1 PLum 170 4224 Elber 24" 0.60 -24 40 QI 0.96 1 Elbor 2" 24 25 Phum : 24" 0.07 2. 27 Ω 2/2"x 2" 28 0.29 Q1 pling 3" 0.03 67 (= 21/2" 0.8751 80 70 Q_1 -pling 2" 80 1.6 PLUM 50 100 24"x2" 0.05 82 4 Q i ducor 3"x 24" 0.03 74 2 Q. ye 3" 0.06 Q_{1} 31 ruse 2" 0.52 23 IPLUM 0.32 12 2" 12 38 1 PL van 1 Grove 34 Q. 4 0.04 100 Grove 24" 84 0.76 110 æι 0.41 ai 48 Frove 7" 116 Time Reguired for IPLVa = 4.33 days Add Additional Labour reduces time by 258 : 4.33 x 0.75 = 3.25 days Regulared for 10 crein = 4.89 days (65.1 hr) = 4,89 +3,25 = 8.14 days

Total Time for 2 Labours





SAC Piping	(4" 43")	Oleren = IPLus	and the additional and a West World with a substantial and the same an	
Estimate	and the state of t		Actua	<u>l</u>	مهرسته و در این از ۱۰ در ۱۵ در ۱۵ در ۱۵ در ۱۵ در ۱۵ در ۱۵ در ۱۸ در از ۱۸ در از ۱۸ در از ۱۸ در از ۱۸ در از ۱۸ در از ۱۸ در از ۱۸ در از ۱۸ در از از ۱۸ در از از از از از از از از از از
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godys Elbons, 4"	Q ₁	25	17	0.52	grant mannes sherin a ra mannang (Ser Philipson adam)
90° 445' ELbons, 3"	QI	33	33	0.67	Sin Tiber 3 Singing
Tee, 4"	Q1 ·	17		0.06	يرود والمراجعة والمراجعة والمراجعة والمراجعة والمراجعة والمراجعة والمراجعة والمراجعة والمراجعة والمراجعة والمر
Tee, 4"x3"	QI	18	4	0.22	Andread and project of the fourth of the project of the fourth of the fo
Coupling Flea, 311	QI	67	64	0.96	
Coupling flex, 4"	Q)	30	64	1. 28	
	Q1	31	8	0.26	
Flange, T"	Q I	23	3	0.13	
Valve, 3"	Q I	50	9	0.16	
Roll Graving, 3"	Q I	100	34	0.34	معادة والمعادد والمعا
Roll Groving, 4"	Q I	96	53	0.62	
Total Time := 10.85 days	reguired for (86.8 pr	r Q, c	ren.z		
	·				
				The second secon	
·					بمراهبتها والمراد مرادر مستدونين دور و مصابعتن

	15	100 Building Services Piping										
				DAILY	LABOR-	27.5	The second secon	2000 BAR	E COSTS		TOTAL	- 5
	151	07 Metal Pipe & Fittings	CREW	OUTPUT		UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P	1
<i>i</i> 60	9342	4" to:8" pipe, 6" stem	1 Plum	14	.571	Ea.	38.50	19		57.50	71 🐕	680
***	9343	8" pipe and larger, 6" stem	,	13	.615		38.50	20.50		59	73.50	
	9400	Mechanical joint ends for plain end pipe	 -	 -							·	
	9410	Malleable iron, black	•								.:	
	9420	90° Elbows, 1-1/4"	Q-1	29	.552	Ea.	9.30	16.50		25.80	35.50	
	9430	1-1/2"	Ĭ	27	.593	Ī	10.20	17.75		27.95	38	1
	9440		$\vdash \bot$	24	.667		12.05	19.95		32	43.50	
	9490	Tee, reducing outlet	V		,,,,,	٧	12.00	25,50		J	15	3
	9510	1-1/4" x 1/2"	Q-1	18	.889	Ea.	7.45	26.50		. 33.95	48.50	
	9520	1-1/4" x 3/4"	Ĭ	18	.889	Ī	7.45	26.50		33.95	48.50	1.00
	9530	1-1/4 × 0/4 1-1/4" x 1"		18	.889	 	7.45	26.50		33.95	48.50	
	9540	1-1/4 × 1 1-1/2" x 1/2"		17	.941		7.90	28		35.90	51 😅	. 10
	9550	1-1/2" x 3/4"	-	17	.941		7.90	28		35.90	51 %	
	9560	1-1/2" x 1"		17	.941		7.90	28		35.90	51 ·*·	
	9570	2" x 1/2"	\vdash	15	1.067		9.65	32		41.65	59 0 %	
	9580	2" x 3/4"		15	1.067		9.65	32		41.65	59 🦠	
	9590	2" x 1"		15	1.067		9.65	32		41.65	59 3	
	9640	Tee, reducing run and outlet	*			'		1			25	
	9660	1-1/4" x 1" x 1/2"	Q-1	18	.889	Ea.	7.95	26.50		34.45	49.50	
	9670	1-1/4" x 1" x 3/4"	Ì	18	.889		7.95	26.50		34.45	49.50	1 2
	9680	1-1/4" x 1" x 1"	H	18	.889		7.95	26.50		34.45	49.50	
	9690	1-1/2" x 1-1/4" x 1/2"		17	.941		8.45	28		36.45	52	A.
	9700	1-1/2" x 1-1/4" x 3/4"		17	.941		. 8.45	28		36.45	52	13
	9710	1-1/2" x 1-1/4" x 1"		17	941		8.45	28		36.45	52	
1	9720	2" x 1-1/2" x 1/2"		15	1.067		10.25	32		42.25	60 - 7	
	9730	2" x 1-1/2" x 3/4"		15	1.067		10.25	32		42.25	60	
-	9740	2" x 1-1/2" x 1"	\	15	1.067	+	10.25	32		42.25	60	
	9790	Tee, outlet			<u> </u>						1.0	
	9810	3" x 1-1/4"	Q-1	29	.552	Ea.	18.05	16.50		34.55	45	/ 海
	9820	3" x 1-1/2"		28	.571	L	18.05	17.10		35.15	46:01	
	9830	3" x 2"		26	.615		20	18.40		38.40	50 :	
10	9840	4" x İ-1/4"	$oldsymbol{\sqcup}$	28	.571	lacksquare	22.50	17.10		39.60	50.50	
	9850	4" x 1-1/2"		26	.615		23.50	18.40		41.90	54.34	
	9860	4" x 2"	*	24	.667	*	23.50	19.95		43.45	56	
	9940	For galvanized fittings for plain end pipe, add	į	1		l	20%				17 W 18 R	
690	0010	PIPE, GROOVED JOINT STEEL FITTINGS & VALVES	├	 	 	-						64
090	0020	Pipe includes coupling & clevis type hanger 10' O.C.	İ	1							- <u>}</u>	
	0500	Schedule 10, black	 	┼──	1	1	 				ارني	
	0550	2" diameter	1 Plum	43	.186	L.F.	3.02	6.20		9.22	12.65	
	0560	2-1/2" diameter	Q1	61	.262		3.65	7.85		11.50	15:90	
	0570	3" diameter		55	.291		4.18	8.70		12.88	17.75	
	0580	3-1/2" diameter		53	.302		5.35	9.05		14.40	19.55	10.65
	0590	4" diameter		49	.327		5.65	9.75		15.40	21%	1,000
	0600	5" diameter	1	40	.400		8.95	11.95		20.90	28:	
	0610	6" diameter	Q2	46	.522		9.60	16.20		25.80	35	
	0620	8" diameter	7	41	.585	1	18.45	18.15		36.60	48	
•	0700	To delete couplings & hangers, subtract									ं	
	0710	2" diam. to 5" diam.					25%	20%	1			
	0720	6" diam. to 8" diam.	<u> </u>			<u> </u>	27%	15%		<u> </u>	14: 12:	1
•	1000	Schedule 40, black							ŀ			11763
	1040	3/4" diameter	1 Plurr		.113	L.F.	2.04	3.75	ļ	5.79	7.90 8.80	
	1050	1" diameter		63	.127		2.17	4.22		6.39		· 103
	1060	1-1/4" diameter	11	58	.138	↓ ↓	2.64	4.59		7.23	9.85 11.15	
	1070	1-1/2" diameter		51	.157		2.97	5.20 6.65	į.	10.11	13.85	
	1080	2" diameter	1 🔻	40	.200	<u> </u>	3,46	0.00	L	10.11	13,00	1 2

7		Building Services Pi			DAILA	LABOR-			10 to 160 XIV 100	2000 BAR	F COSTS		TOTAL
	5107	Metal Pipe & Fittings	CRE			HOURS	UN	$_{f}$	MAT.	LABOR	EQUIP.	TOTAL	INCL O&P
Ú 1090)	2-1/2" diameter	Q·1		57	.281	L.F	_	4.68	8.40		13.08	17.85 6
1100)	3" diameter			50	.320		-	5.70	9.60		15.30	21
1110		4" diameter		7	45	.356	\vdash	\top	8.05	10.65		18.70	25 .
1120		5" diameter	↓	ł	37	.432			12.40	12.95		25.35	33
1130		6" diameter	Q-2	:	42	.571		\dashv	15.90	17.75		33.65	44.50
1140		8" diameter	1	1	37	.649			23.50	20		43.50	56.50
1150		10" diameter		十	31	.774		7	36	24		60	76
1160		12" diameter			27	.889			47.50	27.50		75	93.50
1170		14" diameter			20	1.200			56	37		93	118
1180		16" diameter	1		17	1.412			79.50	44		123.50	154
1190		18" diameter		\top	14	1.714			142	53		195	237
1200)	20" diameter		-	12	2			108	62		170	. 213
1210		24" diameter	₩	T	10	2.400	4	,	128	74.50		202.50	254
1/40		To delete coupling & hanger, subtract	l `				Ì						1
1/50		3/4" diam. to 2" diam.		T				\exists	35%	27%	·		
1760	I	2-1/2" diam. to 5" diam.							18%	18%			
1770		6" diam. to 12" diam.	1.					\top	14%	13%			
1800	1	Galvanized											
1840		3/4" diameter	1 Plu	m	71	.113	L.f	F.	2.27	3.75		6.02	8.15
1850	1	1" diameter			63	.127			2.34	4.22		6.56	9
1860	ı	1-1/4" diameter			58	.138			2.85	4.59		7.44	10.10
1870		1-1/2" diameter			51	.157			3.23	5.20		8.43	11.45
1880	(2" diameter] +		40	.200			3.81	6.65		10.46	14.25
1890		2-1/2" diameter	Q-1	_ _	57	.281		_ _	5.25	8.40		13.65	18.45
1900	1	3" diameter			50	.320			6.40	9.60		. 16	21.50
1910		4" diameter		_	45	.356		4	9.10	10.65		19.75	26
1920		5" diameter	★		37	.432		\perp	15.25	12.95		28.20	36.50
1930		6" diameter	Q-2	_	42	.571	$\vdash \vdash$	_	19.80	17.75		37.55	49
1940	1	8" diameter			37	.649			29.50	20		49.50	63 es
1950	1	10" diameter		4	31	.774	\vdash		44	24		68	85
1960		12" diameter	★	1	27	.889	₩	'	58	27.50		85.50	106
2540 2550	1	To delete coupling & hanger, subtract 3/4" diam, to 2" diam.		+				\dashv	36%	27%			
./550	1	2-1/2" diam. to 5" diam.							19%	18%			
7500 7570	1	6" diam. to 12" diam.		+				\dashv	14%	13%			
2600	1	dule 80, black	·						1470	13/4			
2610		3/4" diameter	1 Plu	<u>_</u>	65	.123	L.F	_	2.31	4.09		6.40	8.75
:1650	1	1" diameter		"	61	.131	ij		2.50	4.36		6.86	9.35
7660	1	1-1/4" diameter	-	+	55	.145	\vdash	\dashv	3.12	4.84		7.96	10.75
2670		1-1/2" diameter			49	.163			3.57	5.45		9.02	12.15
2680	1	2" diameter		+	38	.211	$\vdash \vdash$	\dashv	4.35	7		11.35	15.40
2690	ł	2-1/2" diameter	Q1		54	.296			5.95	8.85		14.80	. 19.90
2700		3" diameter		+	48	.333	1	_	7.45	10		17.45	23.50
2710	1	4" diameter	1	ļ	44	.364		-	10.75	10.90		21.65	28.50
2720		5" diameter		+	35	,457	$\vdash \vdash$	\dashv	12.55	13.70		26.25	34.50
2730		6" diameter	Q-2		40	.600			20.50	18.60		39.10	50.50
2740		8" diameter		+	35	.686	+	\dashv	47.50	21.50		69	84.50
2750	ĺ	10" diameter			29	.828			75.50	25.50		101	122
2760		12" diameter		+	24	1	4	.	83.50	31		114.50	139
.3240	ĺ	To delete coupling & hanger, subtract					*						
3250	1	3/4" diam, to 2" diam.		+				\dashv	30%	25%		1	
3260		2-1/2" diam. to 5" diam.						1	14%	17%			
3270		6" diam, to 12" diam,		+				\dashv	12%	12%		1	
3300	G	alvanized											
3310		3/4" diameter	1 Plur	n l	65	.123	L.F	: +	2.01	4.09		6.10	8.40
3350		1" diameter	1-1		61	.131	Ī		2.06	4.36		6.42	

	OT Malel Dies o Piulisses	1	DAILY	LABOR-			2000 BAF	E COSTS		TOTA
151	07 Metal Pipe & Fittings	CREW	OUTPUT	,	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL
360	1-1/4" diameter	1 Plun	n 55	.145	L.F.	2.51	4.84		7.35	
370	1-1/2" diameter		46	.174		2.83	5.80		8.63	·
380	2" diameter	*	38	.211		3.26	7		10.26	
390	2-1/2" diameter	Q-1	54	.296		4.25	8.85		13.10	
400	3" diameter		48	.333		5.25	10		15.25	
410	4" diameter		44	.364		7.55	10.90		18.45	
420	5" diameter	+	35	.457		15.45	13.70		29.15	
430	6" diameter	Q-2	40	.600		26.50	18.60		45.10	
140	8" diameter		35	.686		46	21.50		67.50	
450	10" diameter		29	.828		73	25.50		98.50	
160	12" diameter	\ \	24	1	*	81	31		112	
920	To delete coupling & hanger, subtract		ļ							
930	3/4" diam. to 2" diam.	l				30%	25%			
940	2-1/2" diam. to 5" diam.	 	-			15%	17%			
950	6" diam. to 12" diam.	l				11%	12%			
990	Fittings: cplg. & labor required at joints not incl. in fitting	<u> </u>	 				· · · · · · · · · · · · · · · · · · ·			
994	price. Add 1 per joint for installed price. Elbow, 90° or 45°, painted	l								
030	3/4" diameter	1 Plun	n 50	.160	Ea.	12.10	5.30		17.40	
)40	1" djameter	1 1 1	50	.160	La.	12.10	5.30	'	17.40 17.40	
50	1-1/4" diameter		40	.200		12.10	6.65		18.75	
60	. 1-1/2" diameter		33	.242		12.10	8.05		20.15	
70	2" diameter		25	.320		12.10	10.65		22.75	
80	2-1/2" diameter	Q-1	40	.400		12.10	11.95		24.05	
90	3" diameter		33	.485		21.50	14.50		36	i
100	4" diameter		25	.640		23.50	19.15		42.65	
.10	5" diameter	1	20	.800		56.50	24		80.50	
20	6" diameter	Q-2	25	.960		66.50	30		96.50	
30	8" diameter		21	1.143		139	35.50		174.50	
140	10" diameter		18	1.333		254	41.50		295.50	
50	12" diameter		15	1.600		405	49.50		454.50	
70	14" diameter	-	12	2		725	62		787	
80	16" diameter	*	11	2.182 2.133		945	67.50 67.50		1,012.50	1,
90	18" diameter 20" diameter	Q-3	15	2.133		1,200 1,575	78		1,267.50 1,653	1,
200	24" diameter		11	2.909		2,300	92.50		2,392.50	2
250	For galvanized elbows, add		+	1		26% .	32.50		2,002.00	
90	Tee, painted			,	▼:		,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,			
700	3/4" diameter	1 Plun	n 38	.211	Ea.	18.65	7		25.65	
740	1" diameter		33	.242		18.65	8.05		26.70	
50	1-1/4" diameter		27	.296		18.65	9.85		28.50	
60	1-1/2" diameter		22	.364		18.65	12.10		30.75	
770	2" diameter	+	17	.471		18.65	15.65		34.30	
80	2-1/2" diameter	Q-1	27	.593		18.65	17.75		36.40	
90	3" diameter		22	.727		26	22		48	
100	4" diameter		17	.941		40	28		68	
10	5" diameter	♦	13	1.231		93.50	37		130.50	
320	6" diameter	Q2	17	1.412		108	44		152	
330	8" diameter		14	1.714		238	53		291	
40.	10" diameter	oxdot	12	2	$\sqcup \sqcup$	495	62		557	
50	12" diameter		10	2.400		690	74.50		764.50	
51	14" diameter	-	9	2.667	$\vdash \vdash \vdash$	730 825	83 93		813 918	1
j2	16" diameter	\\ \\	8	3 2.909		825 1,025	92.50		1,117.50	1
53	18" diameter	Q3	10	3.200	$\vdash \vdash \vdash \vdash$	1,025	101		1,117.50	1
54	20" diameter 24" diameter		8	3.200		2,250	127		2,377	
JJ }	LT Quilletti .	1 A	1	1 7 1	• * ● {	_,	· · · · · ·	1	1 -,0//	

name adams	Building Services Pipi		igen en		Alle (18 bg)	Live State		รับเกล้าเหมือนที่	ariabata e salah		
15107	Metal Pipe & Fittings		- 1		LABOR-			2000 BAI	RE COSTS		TOTAL
	metal ripe & rinings	CRE	W O	UTPUT	HOURS	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL O&P
900	For galvanized tees, add		-			Ea.	24%				
O06 Cou	plings, rigid style, painted	•									
08	1" diameter	1 Pk	um	100	.080	Ea.	8.80	2.66		11.46	13.65
009	1-1/4" diameter			100	.080		8.80	2.66		11.46	13.65
10	1-1/2" diameter		\dashv	67	.119		8.80	3.97		12.77	15.65
12	2" diameter		, -	50	.160		9	5.30		14.30	17.95
)14	2-1/2" diameter	0	\mathbf{i}^{\dagger}	80	.200		. 10.40	6		16.40	20.50
16	3" diameter			67	.239		12.15	7.15		19.30	24
18	4" diameter		\dashv	50	.320		17.20	9.60		26.80	33.50
20	5" diameter		,	40	.400		22.50	11.95		34.45	42.50
22	6" diameter	0	2	50	.480		30	14.90		44.90	55.50
24	8" diameter	Ì		42	.571		47	17.75		64.75	78.50
26	10" diameter		\dashv	35	.686	\vdash	84	21.50		105.50	125
28	12" diameter			32	.750		94.50	23.50		118	139
30	14" diameter		\dashv	24	1	\vdash	123	31	·	154	182
31	16" diameter	1		20	1.200		161	37		198	234
32	18" diameter		\dashv	18	1.333	$\vdash \vdash \vdash$	186	41.50		227.50	267
33	20" diameter		,	16	1.500		221	46.50		267.50	315
34	24" diameter	Q	9	13	1.231		325	36		361	415
9	Flexible, standard, painted	'				'					,55
50	3/4" diameter	1 PI	um	100	.080	Ea.	6.30	2.66		. 8.96	10.95
50	1" diameter	11		100	.080		6.30	2.66		8.96	10.95
70	1-1/4" diameter	8 ₂	7	80	.100		8.40	3.33		11.73	14.30
30	1-1/2" diameter			67	.119		9.20	3.97		13.17	16.10
90	2" diameter		,	50	.160		9.70	5.30		15	18.70
00	2-1/2" diameter			80	.200		11.60	6		17.60	22
10	3" diameter			67	.239		12.80	7.15		19.95	25
20	3-1/2" diameter		-	57	.281		18.70	8.40		27.10	33
30	4" diameter			50	.320		18.70	9.60		28.30	35
40	5" diameter		.	40	.400		28.50	11.95		40.45	49.50
50	6" diameter	Q.	2	50	.480		34	14.90		48.90	60
70	8" diameter			42	.571		55.50	17.75		73.25	88
90	10" diameter			35	.686		92	21.50		113.50	133
10	12" diameter	· .		32	.750		105	23.50		128.50	150
20	14" diameter			24	1		127	31		158	187
30	. 16" diameter		\perp	20	1.200		167	37		204	240
40	18" diameter			18	1.333		195	41.50		236.50	278
50	20" diameter			16	1.500		305	46.50		351.50	410
50	24" diameter	+	'	13	1.846	♦	335	57.50		392.50	455
76	Lightweight style, painted		\dashv		110	-		2.03		11.03	1100
78	1-1/2" diameter	1 Pl	um	67	.119	Ea.	8	3.97		11.97	14.80
30	2" diameter	 - ,	+	50	.160	- -	8.20	5.30	ļ	13.50	17.05
32	2-1/2" diameter	Q:	1	80 67	.200		9,50	6 715		15.50	19.50
34	3" diameter		-	67	.239 .281		11.05	7.15 8.40	<u> </u>	18.20 24.05	23 30.
86	3-1/2" diameter			57 50	1 1		15.65	9.60		i	
38	4" diameter		4	50	.320		15.65			25.25	31.50 43
90	5" diameter	*		40	.400		22.50	11.95		34.45 41.90	
92	6" diameter	Q:	4	50	.480 .571		27 42.50	14.90 17.75		60.25	52.50 74
94	8" diameter	·		42	1		1			1	1
96	10" diameter		\perp	35	.686	- -	115	21.50		136.50	158 176
98	12" diameter	. 4		32	.750		128	23.50		151.50	1/6
)0 T	For galvanized couplings, add	-	-			<u> </u>	33%			<u> </u>	
1	reducing, painted			20	421	Г-	40 50	10.60		53.10	53.50
25	2" x 1-1/2" diarneter	Q-I	4	38	.421	Ea.	40.50	12.60 17.10		53.10	63.50 70.50
26	2-1/2" x 2" diameter			28	.571		40.50			l i	ì
27	3" x 2-1/2" diameter	· \	.	23	.696	*	35.50	21		56.50	70.50

161	107 Metal Pipe & Fittings	, ·		LABOR-			2000 BAR	E COSTS	- 3	TOTAL
	107 Meiul Fipe & Fiffings	CREW	OUTPUT	HOURS	UNIT	MAT.	LÄBOR	EQUIP.	TOTAL	INCL O
5228	4" x 3" diameter	01	18	.889	Ea.	48	26.50		. 74.50	9.
5229	5" x 4" diameter	↓	15	1.067		103	32		135	16
5230	6" x 4" diameter	Q-2	18	1.333		114	41.50		155.50	18
5231	8" x 6" diameter		15	1.600		238	49.50		287.50	33
5232	10" x 8" diameter		13	1.846		310	57.50		367.50	43
5233	12" x 10" diameter		11	2.182		475	67.50		542.50	62
5234	14" x 12" diameter		10	2.400		530	74.50		604.50	7(
5235	16" x 12" diameter	↓	9	2.667		660	83		743	8
5236	18" x 12" diameter	Q-3	12	2.667		790	84.50		874.50	1,0
5237	18" x 16" diameter	Ĭ	l ii .	2.909		1,000	92.50		1,092.50	1,2
5238	20" x 16" diameter	╂┼	10	3.200		1,300	101		1,401	1,5
5239	24" x 20" diameter		9	3.556	L	2,050	113		2,163	2,4
5240	Reducer, concentric, painted	Y		3.330		2,030	113		2,103	2,4
5241	2-1/2" x 2" diameter	Q-1	43	.372	Ea.	14.10	11.15		25.25	
5242	3" x 2-1/2" diameter	1	35	.457	1	17.05	13.70		30.75	ļ
5243	4" x 3" diameter		29	.552		20.50	1			
5244	5" x 4" diameter	\vdash	22	.552	- -	20.50	16.50 22		37 51	
5245	6" x 4" diameter	♦ 0-2	26	.923		33.50			i I	l .
5246	8" x 6" diameter	Ψ2 1	23	1.043	<u> </u>	87.50	28.50		62	
1			1			1	32.50		120	1
5247 5248	10" x 8" diameter		20	1.200	<u> </u>	178	37		215	2
	12" x 10" diameter	*	16	1.500	▼	320	46.50		366.50	4
5255	Eccentric, painted	1	40	201		ļ	- 11 40		47. 46	
5256 5257	2-1/2" x 2" diameter	Q-1	42 34	.381	Ea.	30	11.40		41.40	ſ
	3" x 2-1/2" diameter	├		.471 .571		34	14.10		48.10	<u> </u>
5258	4" x 3" diameter		28			42 57	17.10		59.10	
5259	5" x 4" diameter 6" x 4" diameter	▼ Q-2	21	.762 .960		66.50	23 30		80	ļ
5260	8" x 6" diameter	١	22	1.091		135	30 34		96.50	1
5261 5262	10" x 8" diameter	-	19	1.263	╟╌	II	39		169 409	1
5263	10" x 8" diameter		15	1.600		370 510	49.50		559.50	4
5270	Coupling, reducing, painted	-	13	1.000		310	49.00		203.50	6
5272	2" x 1-1/2" diameter	1 Plum	52	.154	Ea.	14.20	5.10		19.30	
5274	2-1/2" x 2" diameter	Q-1	82	.195		18.55	5.85		24.40	
5276	3" x 2" diameter	Α,	69	.232		21	6.95		27.95	
5278	4" x 2" diameter	\vdash	52	.308	\vdash	34	9.20		43.20	
5280	5" x 4" diameter		42	.381		38.50	11.40		49.90	
5282	6" x 4" diameter	Q-2	52	.462		58	14.30		72.30	
5284	8" x 6" diameter	٧2	44	545		87	16.95		103.95	
5290	· · · · · · · · · · · · · · · · · · ·		44	.545		0/	10,50		103.53	1
5290 5294	Outlet coupling, painted 1-1/2" x 1" pipe size	1 Plum	65	.123	Ea.	17.70	4.09		21.79	
5294	2" x 1" pipe size	I PAUN	48	.123	La.	17.70	5.55		21.79	
1	, ,	1	78	.205		1 5	1			
5298	2-1/2" x 1" pipe size	Q-I	70	.205		28	6.15	•	34.15	
5300	2-1/2" x 1" pipe size	1 Plum	í			32	3.80		35.80 34.35	
5302	3" x 1" pipe size	Q1	65	.246		27	7.35		34.35	
5304	4" x 3/4" pipe size		48	.333		40	10		50	
5306	4" x 1-1/2" pipe size	*	.46	.348	 	57	10.40		67.40	
5308	6" x 1-1/2" pipe size	Q-2	44	.545	*	81	16.95		97.95	1
5750	Flange, w/groove gasket, black steel (see 15107-660-0620, bolt sets)			<u> </u>	L					
5760	ANSI class 125 and 150, painted				١.					
5780	2" pipe size	1 Plum	23	.348	Ea.	41.50	11.55		53.05	
5790	2-1/2" pipe size	Q-I	37	.432		50	12.95		62.95	
5800	3" pipe size		31	.516		54	15.45		69.45	
5820	4" pipe size		23	.696		72.50	21		93.50	ì
5830	5" pipe size		. 19	.842		84	25		109	1
5840	6" pipe size	Q-2	23	1.043		92	32.50		124.50	1
5850	8" pipe size		17.	1.412		104	44		148	1

PER.	51 6	00 Building Services Piping	and A	, 100 (100 (100 (100 (100 (100 (100 (100	aciysissa 3		and the second s	ના કુલ્લાના કુલ્લા ત્રિક તે જેફિલાઇન કેટ		Visitario de Salado Saladores de Salado Saladores de Salado	engang dipagan at a	y god G
	tir.			DAILY	LABOR-			2000 BAR	COSTS		TOTAL	Г
	1510	7 Metal Pipe & Fittings	CREW	OUTPUT		UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL O&P	1
m	5860	10" pipe size	Q-2	14	1.714	Ea,	164	53	- 1 - 1 - 1	217	262	690
	5870	12" pipe size		12	2		215	62		277	330	
	5880	14" pipe size		10	2.400	-	495	74.50		569.50	660	1 (
∞ .	5890	16" pipe size		9	2.667		575	83		658	755	
Y	5900	18" pipe size		6	4		705	124		829	965	1
	5910	20" pipe size		5	4.800		850	149		999	1,150	Ï
	5920	24" pipe size	+	4.50	5.333		1,075	165		1,240	1,450	1
	5940	ANSI class 350, painted	٧			٧				,		
	5946	2" pipe size	1 Plum	23	.348	Ea.	50.50	11.55		62.05	73	1
	5948	2-1/2" pipe size	Q-1	37	,432	Ī	58.50	12.95		71.45	84	
ij	5950	3" pipe size	+	31	.516		80	15.45		95.45	112	1
: :	5952	4" pipe size		23	.696		107	21		128	150	1
	5954	5" pipe size	4	19	.842		121	25		145	172	1
	5956	6" pipe size	Q-2	23	1.043	11	141	32.50		173.50	205	1
	5958	8" pipe size		17	1.412		162	44		206	246	1
	5960	10" pipe size	. ↓	14	1.714		259	53		312	365	
· ·	5962	12" pipe size	1 Plum	12	.667	+	276	22		298	340	1
	1	Coupling, for PVC plastic pipe				•					ĺ	İ
	6110	2" diameter	1 Plum	50	.160	Ea.	10.80	5.30		16.10	19.95	1
	6112	2-1/2" diameter	Q-1	80	.200		15.20	6		21.20	26	
	6114	3" diameter	-	67	.239		18.45	7.15		25.60	31.50	
5	6116	4" diameter	↓	50	.320		24	9.60		33.60	41	
	6118	6" diameter	Q-2	50	.480		40	14.90		54.90	66.50	7
	6120	8" diameter		42	.571		65.50	17.75		83.25	99 .	
	6122	10" diameter		35	.686		108	21.50		129.50	150	1
	6124	12" diameter	↓	32	.750	↓	136	23.50		159.50	185	
	7400	Suction diffuser										
	7402	Grooved-end-inlet-x flanged outlet	-									
	7410	3" x 3"	Q-1	50	.320	Ea.	425	9.60		434,60	485	1
	7412	4" x 4"		38	.421		620	12.60		632.60	705	1
	7414	5" x 5"	₩	30	.533		675	15.95		690.95	765	Ì
	7416	6" x 6"	Q2	38	.632		850	19.60		869.60	965	4
	7418	8" x 8"		27	.889		1,575	27.50		1,602.50	1	ı
	7420	10" x 10"		20	1.200		2,150	37		2,187	2,425 3,975	4
	7422	12" x 12"		16	1.500	1	3,550	46.50		3,596.50 4,524.50	4	l
	7424	14" x 14"	-	15	1.600	-	4,475 4,600	49.50 53		4,653	5,000	4
	7426	16" x 14"	▼	14	1.714	*	4,000	33		4,000	3,130	1
	7500	Strainer, tee type, painted	1 Plum	38	.211	Ea.	265	7		272	300	4
	7506	2" pipe size		i .	.211	ca.	278	7.70		285.70	8	l
١	7508	2-1/2" pipe size	Q-1	62 50	.258	+	315	9.60		324.60	1	\dashv
	7510	3" pipe size		38	.421		355	12.60		367.60	1	
-	7512	4" pipe size	╂╌	30	.533	+	515	15.95		530.95		-
	7514	5" pipe size	▼ Q-2	38	.632		555	19.60		574.60	1	1
	7516	6" pipe size	\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	27	.889	\vdash	855	27.50		882.50		-
۱	7518	8" pipe size	1	20	1.200		1,250	37		1,287	1,425	
	7520	10" pipe size	╂┼┼	16	1.500	╂┼	1,625	46.50		1,671.50		1
	7522	12" pipe size		15	1.600		5,750	49.50		5,799.50		
١	7524	14" pipe size	╂╁	14	1.714		7,150	53		7,203	7,925	\dashv
	7526	16" pipe size	▼	"	1./14	*	7,150	33		,,,500	1,500	
١	7570	Expansion joint, max. 3" travel	1 Plum	38	.211	Ea.	218	7	<u> </u>	225	250	-
- 1	7572	2" diameter	Q-1	50	.320]	255	9.60	'	264.60		1
	7574	3" diameter	<u>"</u>	38	.421	\blacksquare	320	12.60		332.60		-
4	7576	4" diameter	Q-2	38	.632		555	19.60	1	574.60	8	and a second
	7578	6" diameter Ball valve w/handle, carbon steel trim	٧٠	1 30	.032	╅	-	13.00	 	1	 	-
	7800	•	1 Plum	50	.160	Ea.	64.50	5.30		69.80	79	
	7810	1-1/2" pipe size	2 1 1011	1 30	100	1	01.50	1	L	1	1	

	Building Services Pipi		74					500579349		
15107	Metal Pipe & Fittings		1	LABOR-			2000 BAS			TOTAL
				HOURS	UNIT	MAT:	LABOR	EQUIP.	TOTAL	INCL 0&P
7812	2" pipe size	1 Plum	38	.211	Ea.	89	7		96	109
814	2-1/2" pipe size	Q·1	62	.258		184	7.70		191.70	214
816	3" pipe size	i 1	50	.320		290	9.60		299.60	335
818	4" pipe size		38	.421		445	12.60		457.60	510
820	6" pipe size	Q-2	30	.800	*	1,300	25		1,325	1,500
7830	With gear operator									
7834	2-1/2" pipe size	Q1	62	.258	Ea.	325	7.70		332.70	365
836	3" pipe size		50	.320	Ш	430	9.60		439.60	485
838	4" pipe size	+	38	.421		575	12.60		587.60	655
840	6" pipe size	Q2	30	.800	*	1,475	25		1,500	1,675
1	ck valve									
874	2-1/2" pipe size	Q-1	62	.258	Ea.	116	7.70		123.70	140
876	3" pipe size		50	.320		137	9.60		146.60	166
878	4" pipe size	_ _	38	.421		145	12.60	-	157.60	178
880	5" pipe size	♦	30	.533		241	15.95		256.95	289
882	6" pipe size	Q2	38	.632	└-	286	19.60		305.60	345
884	8" pipe size	1	27	.889		390	27.50		417.50	470
886	10" pipe size		20	1.200		1,125	37		1,162	1,300
888	12" pipe size	🗡	16	1.500	\	1,350	46.50		1,396.50	1,550
900 Plug 906	g valve, balancing, w/lever operator		E0.	200		220	0.50		047.60	
908	3" pipe size	Q-1	50 38	.320	Ea.	238	9.60		247.60	277
909	4" pipe size 6" pipe size	Q-2	30	.421 .800	-	262 470	12.60 25		274.60 495	305
1	With gear operator	ŲΖ	30	.000	*	4/0	20		490	555
920	3" pipe size	Q-1	50	.320	Ea.	430	9.60		439.60	490
922	4" pipe size	, v	38	.421	[]	455	12.60		459.60 467.60	520
924	6" pipe size	Q-2	38	.632		660	19.60		679.60	760
926	8" pipe size	١	27	.889		885	27.50		912.50	1,025
928	10" pipe size		20	1.200	+	1,400	37		1,437	1,575
930	12" pipe size		16	1.500	1	2,025	46.50		2,071.50	2,300
	erfly valve, 2 position handle, with standard trim				Y				90.000	2,000
010	1-1/2" pipe size	1 Plum	50	.160	Ea.	103	5.30		108.30	121
020	2" pipe size	*	38	.211	1	103	7		110	124
030	3" pipe size	Q1	50	.320		147	9.60		156.60	177
050	4" pipe size	н	38	.421		162	12.60		174.60	197
070	6" pipe size	Q-2	38	.632		355	19.60		374.60	420
080	8" pipe size		27	.889	\top	540	27.50		567.50	635
090	10" pipe size		20	1.200	\	775	37		812	910
200	With stainless steel trim									
240	1-1/2" pipe size	1 Płum	50	.160	Ea.	130	5.30		135.30	151
250	2" pipe size	•	38	.211		130	7		137	154
270	3" pipe size	Q-1	50	.320		175	9.60		184.60	207
80	4" pipe size	*	38	.421		190	12.60		202.60	228
900	6" pipe size	Q-2	38	.632		355	19.60		374.60	420
10	8" pipe size		27	.889		605	27.50		632.50	705
20	10" pipe size		20	1.200		960	37		997	1,100
322	12" pipe size		16	1.500		1,225	46.50		1,271.50	1,425
24	14" pipe size		15	1.600		1,600	49.50		1,649.50	1,850
126	16" pipe size	V	14	1.714		2,200	53		2,253	2,500
28	18" pipe size	Q-3	12	2.667		2,700	84.50		2,784.50	3,100
30	20" pipe size		11	2.909		3,675	92.50		3,767.50	4,175
32	24" pipe size	\	10	3.200	\	4,675	101		4,776	5,275
36	Note: sizes 12" up w/manual gear operator									
00 Cut o	one groove, labor			- 1						
10	3/4" pipe size	Q1	152	.105	Ea.		3.15		3.15	4.7
120	1" pipe size	1 1	140	.114	1		3.42		3.42	5.1

15	107 Metal Pipe & Fittings	- :		1	LABOR-			2000 BAR	i-		TOTAL
		_		ОИТРИТ	_	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P
9030	1-1/4" pipe size	()-1 -	124	.129	Ea.	1	3.86		3.86	5.85
9040	1-1/2" pipe size		_	114	.140			4.20		4.20	6.35
9050	2" pipe size			104	.154			4.60		4.60	6.95
9060	2-1/2" pipe size		_	96	.167			4.99	***************************************	4,99	7.55
9070	3" pipe size	ł		88	.182			5.45		5.45	8.25
9080	3-1/2" pipe size		<u> </u>	83	.193			5.75		5.75	8.75
9090	4" pipe size	.		78	.205			6.15		6.15	9.30
9100	5" pipe size		\perp	72	.222			6.65		6.65	10.05
9110	6" pipe size	1		70	.229			6.85		6.85	10.35
9120	8" pipe size		 	54	.296	<u> </u>		8.85		8.85	13.40
9130	10" pipe size	1		38	.421			12.60		12.60	19.05
9140	12" pipe size		↓_	30	.533	\sqcup		15.95		15.95	24
9150	14" pipe size			20	.800			24		24	36
9160	16" pipe size		╁_	19	.842	 	ļ	25		25	38
9170	18" pipe size	ı		18	.889			26.50		26.50	40,50
9180	20" pipe size	- -	╄	17	.941		<u> </u>	28		28	42.50
9190	24" pipe size	'	A	15	1.067	*		32		32	48.50
9210	Roll one groove	+,) 1	266	.060	Ea.		1.80	·	1.00	0.70
9220 9230	3/4" pipe size	1	<u>ا</u> 1-7	228	.070	Ed.		2.10		1.80 2.10	2,72
9230	1" pipe size 1-1/4" pipe size		┼	200	.080	\vdash	 	2.39		2.10	3.18
9250	1-1/4 pipe size	İ		178	.090	1		2.69		2.59	4.07
9260	2" pipe size		╁╾	116	.138	┠╌	 	4.13		4.13	6.25
9270	2-1/2" pipe size	1		110	.145			4.35		4.15	6.60
9280	3" pipe size	╌╂╌	╁╴	100	.160		 	4.79		4.79	7.25
9290	3-1/2" pipe size	1	1	94	.170			5.10		5.10	7.7(
9300	4" pipe size	-	┼	86	.186		1	5.55		5.55	8.40
9310	·· ·· 5" pipe size	j		84	.190]		5.70		5.70	8.60
9320	6" pipe size	_	1	80	.200			6		6	9.0
9330	8" pipe size			66	.242			7.25		7.25	11
9340	10" pipe size		1	58	.276		 	8.25		8.25	12.50
9350	12" pipe size			46	.348			10.40		10.40	15.7
9360	14" pipe size		T	30	.533			15.95		15.95	24
9370	16" pipe size	ł		28	.571			17.10		17.10	26
9380	18" pipe size		1	27	.593			17.75		17.75	27
9390	20" pipe size			25	.640			19.15		19.15	29
9400	24" pipe size		*	23	.696	*		21		21	31.5
	•										
	PIPE, STAINLESS STEEL					ĺ					
0020	Welded, with clevis type hangers 10' O.C.								····		
0500	Schedule 5, type 304	١.									
0540	1/2" diameter	10	-15	128	.125	L.F.	3.91	3.74	.38	8.03	
0550	3/4" diameter	n		116	.138		4.46	4.13	.42	9.01	11.6
0560	1" diameter	ለፗ_	 	103	.155	lacksquare	5.35	4.65	.47	10.47	13.4
0570	1-1/4" diameter	א ו		93	.172		6.05	5.15	.52	,	15.1
0580	1-1/2" diameter	_	 	85	.188		6.95	5.65	.57		1
0590	2" diameter			69	.232		8.30	6.95	.71	l .	
0600	2-1/2" diameter	- -	1	53	.302		11.40	9.05	.92		
0610	3" diameter	J		48	.333		13.70	10	1.02	3	
0620	4" diameter		 	44	.364		17.45	10.90	1.11	29.46	
0630	5" diameter		12	36	.444		35	13.30	1.36		
0640	6" diameter	<u>_</u>	16	42	.571	 	32	17.75	1.16	A	H
0650	8" diameter			34	.706		49	22	1.43	1	B
0660	10" diameter		<u> </u>	26	.923		69	28.50	1.87	99.37	1
0670	12" diameter	7	₩ .	21	1.143	*	90.50	35.50	2.32	128.32	156
0700	To delete hangers, subtract			<u></u>		<u> </u>					<u> </u>

_				~~~~~			
	Inlet	Piping	(/ "	3"	2	12")
••							

Estimate		. Kinganiyas i Mi Makanasa in sa sanahin sa sa sa sa sa sa sa sa sa sa sa sa sa	1	Ictual	THE THE STATE OF T
"	Clew	days	Quantity	Days	uatta-vor-settivetaalistorio-usookiji tureettiis-tii-tii-tiivikkiikookij
, 1C Sch 80 6"	Q,	38'	.50'	1.33	and annual transfer and the second
16 5.480 3"	- Q.	50'	201	0.40	11
VC 50480 2"	Q.	55'	10'	0.18-	
c 5-480 12"	1 PLuz	34'	30'	0.88	
tys Erbors 6"	Q:	8	8.	1.0	for the state of t
45 Elbour 3"	Q,	16	5	0-31	<u>}</u>
Elbors 24	٥.,	23	3	0.13	
5 Ether, 1/2"	Q i	a7	14	0.52	
6"	\mathcal{O}_1	5		0,20	and the state of t
11/2"	Q,	20	3	0.15	
nge 6 4	Q,	16	3	0.125	3.73
147c 5"	Ø v	21		0,05	
nge 3"	Ø1	32	4	0.125	and the state of t
lange 2"	Q ₁	48	2	0.04	THE STATE OF THE S
20 /2 11	Q ₁	51	9+2	0,22	and the second s
lucer 6 X 5"	<i>a</i> ,	15	1	0.07	National substitution of the substitution of
2 3 X 1 4"	a.	24	2	0.08	
-Tee 6"x 3"	Q,	7	5	0.71	
eball Ku	# Ifcum	20	5	0.25 -	www.manager.com
"/e 2"1	1 PLum	17		0.06	
ive 34	A.	24	1	0.04	The state of the s
ve 6"	Ø ·	13	2	0.17)0	. 293
e we 64	Q,	12	1	0.083 /	ngan pagamangan mangangan mengangan semengan semengan pengangan pengangan pengangan pengangan pengangan pengan

	Building Services Pipir		: <u>.</u>	DAILY	LABOR-				TOTAL		
07	Metal Pipe & Fittings	• • • • •			HOURS	UNIT	MAT.	2000 BAF LABOR	EQUIP.	TOTAL	TOTAL INCL 0&P
-	2"	•	Q-1	9	1.778	Ea.	133	53	-4011	186	227
	For couplings and unions use 3000 lb., type 316			1						100	221
	3000 lb., type 304		 -								
	Coupling	•									
	1/8"		I Plum	19	.421	Ea.	2.41	14		16.41	23.5
	1/4"	•		19	.421	1	2.53	14			
	3/8"	<u> </u>	╂┼┼╌	19	.421	\vdash	3.04	14		16.53	24
	1/2"			19	.421		4.84			17.04	24.5
	3/4"		 	18		-		14		18.84	26.5
				15	.444		7.30	14.80	٠.	22.10	30.5
	1"		*	i	.533	$\vdash \vdash \vdash$	12.40	17.75		30.15	40.5
	1-1/4"		Q-1	26	.615		28	18.40		46.40	58.5
	1-1/2"	:	 	24	.667		32	19.95		51.95	65.5
•	2"		*	21	.762	▼	46	23		69	85.5
	Union.	<u>:</u> •									
•	1/8"	9	1 Plum	12	.667	Ea.	25.50	22		47.50	61.5
	1/4"			12	.667		25.50	22		47.50	61.5
	3/8"			12	.667		27.50	22		49.50	63.5
	. 1/2"			11	.727		27.50	24		51.50	66.5
·	: 3/4"	f		10	.800		33.50	26.50		60	77
	. 1"		*	9	.889		56	29.50		85.50	106
;	1-1/4"		Q-1	16	1		78.50	30		108.50	132
	1-1/2"			15	1.067		88	32		120	146
	2" .		*	13	1.231	V	123	37		160	192
3	3000 lb., type 316									1	
ul	Coupling										
	1/8"		1 Plum	19	.421	Ea.	2.95	14		16.95	24.5
	1/4"			19	.421		3.25	14		17.25	24.5
	3/8"			19	.421		3.46	14		17.46	25 -
	1/2"			19	.421		5.60	14		19.60	27
•	3/4"			18	.444		8.25	14.80		23.05	31.5
	1"		V	15	.533		13.95	17.75		31.70	42.5
	1-1/4"	·	Q-1	26	.615		32	18.40		50.40	63:5
	1-1/2"			24	.667		36.50	19.95		56.45	70
	2"	,	 	21	.7,62	1	53	23		76	93
	Union										* * * * * * * * * * * * * * * * * * * *
	1/8"		1 Plum	12	.667	Ea.	26	22		48	62.5
	1/4"			12 -	.667		26	22		48	62.5
	. 3/8".			12	.667		32	22		54	69 -
	1/2"		11	11	.727	$\top \!$	32	24		56	72
•	3/4"			10	.800		36.50	26.50		63	80
	1" *	7.7	+	9	.889	$\dashv \vdash$	63	29.50		92.50	114
	1-1/4"		Q-1	16	i		94	30		124	149
	1-1/2"		7+	15	1.067		118	32		150	178
	2"	:			1.231	1	154	37	l	191	225.
'n						-					
D8	Plastic Pipe & Fittings				.				. [
PE, PL	ASTIC		-+		\dashv					+	
	glass reinforced, couplings 10' O.C., hangers 3 per 10	1	-	.[3					1	
	General service									<u> </u> -	
. 4	2" diameter		Q-1	59	.271	L.F.	9.65	8.10		1775	23 :
			Λī	52	.308	L-1'-	13			17.75	
	3" diameter	:		- 1			·	9.20		22.20	28.5
	4" diameter		\dashv	48	.333	44	15.85	10		25.85	32.5
	6" diameter	: 1	V	39	.410		23	12.30		35.30	43.5
	8" diameter		Q-2	49	.490	11	36.50	15.20		51.70	63
	10" diameter			41	.585		53.50	18.15		71.65	86.5
	12" diameter		1 1	36	.667	1 1	65.50	20.50	3	86	104

0240 0260 0280 0390 0340 0350 0350 0350 0550 0560 0570 0600 0 PVC, high ir 020 0600 01000 01000 01100 01110 01120 01130 01140 0150 01170 01180 0190 01770 01770 01770	strength 2" diameter 3" diameter 4" diameter 6" diameter 8" diameter 10" diameter 12" diameter To delete coupling & hangers, subtract 2" diam. to 6" diam. 8" diam. to 12" diam. h impact/pressure, cplgs. 10' O.C., hangers 3 per 10'	Q-1 Q-2	58 51 47 38 48 40	.276 .314 .340 .421 .500	L.F.	10.75 14.65 17.65 26	8.25 9.40 10.20	EQUIP.	19 24:05 27.85	24.50.
0260 0280 0300 0300 0340 0360 0350 0550 0560 0570 0600 0PVC, high in 020 0500 0100 0100 0100 01100 01100 01110 01120 01300 01140 01300 01400 01500 01500 01600 01700 01800 01700 01800 01700 01800 01900	3" diameter 4" diameter 6" diameter 8" diameter 10" diameter 12" diameter 70 delete coupling & hangers, subtract 2" diam. to 6" diam. 8" diam. to 12" diam. h impact/pressure, cplgs. 10' 0.C., hangers 3 per 10'		51 47 38 48 40	.314 .340 .421	L.F.	14.65 17.65	9.40 10.20		24:05	l /
0280 0300 03	4" diameter 6" diameter 8" diameter 10" diameter 12" diameter 2" diam. to 6" diam. 8" diam. to 12" diam. h impact/pressure, cplgs. 10' 0.C., hangers 3 per 10'		47. 38 48 - 40	.340 .421		17.65	10.20			30(
3300 3320 3320 3320 3320 3340 3360 33	6" diameter 8" diameter 10' diameter 12" diameter To delete coupling & hangers, subtract 2" diam. to 6" diam. 8" diam. to 12" diam. h impact/pressure, cplgs. 10' 0.C., hangers 3 per 10'		38 48 . 40	.421				1	27.85	
0320 0340 0360 0360 0360 0550 0560 0570 0600 0PVC, high ir 0200 0600 01070 01080 01090 01100 01110 01120 01130 01140 01550 01660 01770 01880 01990 01770 01880 01990	8" diameter 10" diameter 12" diameter To delete coupling & hangers, subtract 2" diam. to 6" diam. 8" diam. to 12" diam. h impact/pressure, cplgs. 10' 0.C., hangers 3 per 10'		48			26 I	10 00 1			35
0340 0360 03	10" diameter 12" diameter To delete coupling & hangers, subtract 2" diam. to 6" diam. 8" diam. to 12" diam. h impact/pressure, cplgs. 10' 0.C., hangers 3 per 10'	Q-2	- 40	.500			12.60	•	38.60	47.50
3360 3550 To	12" diameter To delete coupling & hangers, subtract 2" diam. to 6" diam. 8" diam. to 12" diam. h impact/pressure, cplgs. 10' 0.C., hangers 3 per 10'					41	15.50		56.50	68.50
10550 To 10560 PVC, high in 1020 Schedu 1040 Schedu 1040 Schedu 1070 Schedu	To delete coupling & hangers, subtract 2" diam. to 6" diam. 8" diam. to 12" diam. h impact/pressure, cplgs. 10' 0.C., hangers 3 per 10'	+	1 00	.600		60	18.60		78.60	94
0560 0570 0600 PVC, high in 1020 Schedu 1040 1060 1070 1080 1090 1110 1120 1130 1140 1150 1160 1170 1180 1190 1200 1730 To 1740 1750 1760 1880 PVC, coupli 1820 Schedu 1880 PVC, coupli 1820 Schedu 1880 1870 1880 1890 1990 1910 1920 1930 1950	2" diam. to 6" diam. 8" diam. to 12" diam. h impact/pressure, cplgs. 10' 0.C., hangers 3 per 10'		36	.667	₩	73.50	20.50		94	113
0570 PVC, high in 1020 Schedu 1040 1060 PVC, high in 1020 Schedu 1060 1070 1080 1090 1090 1090 1090 1090 1090 109	8" diam. to 12" diam. h impact/pressure, cplgs. 10' 0.C., hangers 3 per 10'			٠.						
0600 PVC, high in 1020 Schedu 1040 1050 1070 1080 1090 1110 1110 1110 1110 1110 111	h impact/pressure, cplgs. 10' O.C., hangers 3 per 10'	1				33%	56%			
1020 Schedu 1040 1060 1070 1080 1090 1090 1090 1090 1090 1090 109		1				31%	52%			9.75
1020 Schedu 1040 1060 1070 1080 1090 1090 1090 1090 1090 1090 109										
1040 1060 1070 1080 1090 1110 1110 1120 1130 1140 1150 1160 1170 1180 1190 1200 1770 1880 PVC, coupling 1820 Schedut 1840 Schedut 1870 1880 Schedut 1870 1880 Schedut 1870 1880 Schedut 1870 1880 Schedut 1870 1880 1890 199	edule 80	1								
1060 1070 1080 1090 1110 1120 1130 1140 1150 1160 1170 1180 1190 1200 1770 1880 PVC, coupling 1820 Schedut 1880 Schedut 1880 Schedut 1890 1890 1900 1900 1900 1900 1900 1900 1900 1900	. 1/4" diameter	1 Plum	58	.138	L.F.	. 2.17	4.59		6.76	9.35
1070 1080 1090 1110 1120 1130 1140 1150 1160 1170 1180 1190 1200 1750 1760 1770 1880 PVC, coupli 1820 Schedu 1880 1870 1880 1890 1990 1910 1920 1930 1940 1950 1950 1960 1970 1980 1970 1980 1970 1980 1970 1980 1970 1980 10970 1980 10970 1980 1000 10	3/8" diameter		55	.145		2.26	4.84		7.10	9.80
1080 1090 1110 1110 1120 1130 1140 1150 1160 1170 1180 1190 1200 1730 To 1760 1770 1880 PVC, coupli 1820 Schedu 1860 1870 1880 1890 1990 1910 1920 1930 1940 1950 1960 1970 1980	1/2" diameter		50	.160		2	5.30		7.30	10.25
1090 1100 1110 11	3/4" diameter		47	.170		2.20	5.65	-	7.85	10.95
1100 1110 1120 1130 1140 1150 1150 1160 1170 1180 1190 11	1" diameter		43	.186		2.68	6.20			12.30
1110 1120 1130 1140 1150 1160 1170 1180 1190 1190 1170 1180 1190 1170 1180 1190 11	1-1/4" diameter	1	39	.205	\dashv	2.80	6.80		9.60	13,40
1120 1130 1140 1150 1150 1160 1170 1180 1190 1200 1730 1760 1770 1880 1880 1880 1880 1880 1890 1990 1910 1920 1930 1940 1950 1960 1970 1980	1-1/2" diameter		34	.235		3.01	7.80		10.81	15.15
1130 1140 1150 1160 1170 1180 1190 11	· 2" diameter	Q-1	55	.291	-	3.19	8.70		11.89	16.65
1140 1150 1160 1170 1180 1190 1200 1730 1760 1770 1880 1770 1880 1880 1880 1880 1890 1990 1910 1920 1930 1940 1950 1970	2-1/2" diameter		52	.308		3.30	9.20		12.50	17.55
1150 1160 1170 1180 1190 1200 1730 To 1750 1760 1770 1880 PVC, coupli 1820 Schedu 1860 1870 1880 1890 1990 1910 1920 1930 1940 1950 1960 1970 1980 1970 1980	3" diameter	+	50	.320	-	4.56	9.60	· · · · · ·	14.16	19.50
1160 1170 1180 1190 1200 1730	4" diameter		46	.348		6.05	10.40		16.45	22.50
1170 1180 1190 1200 1730 1760 1770 1800 1770 18800 1870 1880 1880 18	5" diameter	++-	42	.381	-	10.35	11.40		21.75	28.50
1180 1190 1200 170	6" diameter	11.	38	.421		9.30	12.60		21.90	29.50
1190 1200 1730 To 1740 1750 1750 1760 1770 1880 PVC, coupling 1820 Schedul 1820 Schedul 1840 Schedul 1840 1840 1840 1850	8" diameter	Q-2	47	.511		14.95	15.85		30.80	40.50
1200 To To To To To To To	10" diameter	l ï	42	.571	.	23.50	17.75		41.25	53
1730 To 1740 1750 1760 1770 18800 PVC, coupli 1820 Schedu 1860 1870 1880 1890 1990 1910 1920 1930 1940 1950 1970 1980	12" diameter	1 🗼	38	.632	\pm	30	19.60		49.60	62.
1740 1750 1760 1770 1880 1820 Schedu 1870 1880 1870 1880 1990 1910 1920 1930 1940 1950 1960 1970 1980	To delete coupling & hangers, subtract		"		•	50	15.00		15.00	1
1750 1760 1770 1800 PVC, coupli 1820 Schedu 1860 1870 1880 1890 1900 1910 1920 1930 1940 1950 1960 1970 1980	1/4" diam. to 1/2" diam.	+	 			62%	80%			:
1760 1770 1800 PVC, coupli 1820 Schedu 1870 1880 1880 1990 1910 1920 1930 1940 1950 1970 1970	3/4" diam. to 1-1/4" diam.		1			58%	73%			1
1770 PVC, coupli 1820 Schedu 1860 Schedu 1870 Schedu 1870 Schedu 1880 Schedu 1890 Schedu 1990 Schedu 1	1-1/2" diam. to 6" diam.	 	 			40%	57%			·
1800 PVC, coupli 1820 Schedu 1860 1870 1880 1890 1990 1990 1910 1950 1950 1960 1970	8" diam. to 12" diam.					34%	50%	Ì		1. 1
1820 Schedu 1860 1870 1880 1890 1900 1910 1920 1930 1940 1950 1970	uplings 10' O.C., hangers 3 per 10'	 	 			57.0	50%			
1860 1870 1880 1890 1900 1910 1920 1930 1940 1950 1960 1970	• •	1								i l
1870 1880 1890 1900 1910 1920 1930 1940 1950 1960 1970	1/2" diarneter	1 Plum	54	.148	L.F.	1.90	4.93		6.83	9.55
1880 1890 1900 1910 1920 1930 1940 1950 1960 1970	3/4" diameter		51	.157		2.06	5.20		7.26	10.15
1890 1900 1910 1920 1930 1940 1950 1960 1970	1" diameter	++	46	.174		2.57	5.80		8.37	11.60
1900 1910 1920 1930 1940 1950 1960 1970	1-1/4" diameter		42	.190		2.61	6.35		8.96	12.45
1910 1920 1930 1940 1950 1960 1970	1-1/2" diameter	11	36	.222		2.81	7.40		10.21	14.30
1920 1930 1940 1950 1960 1970	2" diameter	Q-I	59	.271		2.83	8.10		10.93	15.40
1930 1940 1950 1960 1970	2-1/2" diameter	1 1	56	.286	1	3.52	8.55		12.07	16.80
1940 1950 1960 1970 1980	3" diameter		53	.302		4.05	9.05		13.10	18.10
1950 1960 1970 1980	4" diameter	1-	48	.333	\vdash	5.50	10		15.50	21
1960 1970 1980			43	.372		7.50	11.15		18.65	25
1970 1980	5" diameter	+-	39	.410		8.30	12.30		20.60	27.50
1980	6" diameter	02	48	.500		13.15	15.50		28.65	
J	8" diameter	Q-2		.558	-	27.50	17.30		44.80	56.50
19901	10" diameter		43				17.30		52.75	
	12" diameter	1	42	.571		35	24		132	156
2000	14" diameter		31	.774		108		`	1	1 1
2010	16" diameter	_ ▼	23	1.043	*	136	32.50		168.50	198
	- 1 1 1									
2360	To delete coupling & hangers, subtract		 	ļ		65%	74%			
2370	1/2" diam. to 1-1/4" diam.	ı				44%	57%	.		1
2380	1/2" diam. to 1-1/4" diam. 1-1/2" diam. to 6" diam.	1			l	41%	53%			
	1/2" diam. to 1-1/4" diam.			<u> </u>		71/0	L			
	1/2" diam. to 1-1/4" diam. 1-1/2" diam. to 6" diam.]				- 170	5570			

) Building Services Pip		N. 1. 1.	DAILY	LABOR-	60 March 274-0150			TOTAL		
108	Plastic Pipe & Fittings			OUTPUT		UNIT	MAT.	2000 BAR LABOR	EQUIP.	TOTAL	TOTAL INCL 0&P
<i>-</i>	14" diam. to 16" diam.		GILLI	0011 01	·;	OHII	48%	45%	EQUIF.	TOTAL	INCL USE
	Schedule 80		. :		, , ,		70/1	45/0		ĺ	ı
 	1/4" diameter		1 Plum	58	.138	L.F.	1.91	4.59		6.50	9.05
1	3/8" diameter	• :		55	.145		1.91	4.84		6.75	
 				50	.160	\dashv	2.08	5.30			9.40
	1/2" diameter			47	.170		I			7.38	10.35
<u></u>	3/4" diameter	*	<u> </u>				2.31	5.65		7.96	41.10
1	1" diameter			43	.186 .205		2.84	6.20	,	9.04	12.50
1	1-1/4" diameter		<u> </u>	39	1		3.02	6.80	· · · · · · · · · · · · · · · · · · ·	9.82	13.60
£.	1-1/2" diameter		*	34	.235		3.27	7.80	•	11.07	15.49
1	Z" diameter	. ,	Q-1	55	.291		3.57	8.70		12.27	17.10
i	2-1/2" diameter			52	.308		3.86	9.20	•	13.06	18.20
	3" diameter		$oxed{oxed}$	50	.320		5.30	9.60		14.90	20.50
	4" diameter			46	.348		7.15	10.40		17.55	23.50
	5" diameter			42	.381		9.75	11.40		21.15	28
	6" diameter		\ \	38	.421		11.35	12.60	•	23.95	31:50
	8" diameter	•	Q-2	47	.511		18.10	15.85		33.95	44
	. 10" diameter			42	.571		28	17.75		45.75	57.50
) .	. 12" djameter		<u> </u>	38	.632	\rightarrow	36	19.60		55.60	69
1	To delete coupling & hangers, subtract				,				•		
1	1/4" diam. to 1/2" diam.						66%	80%		,	
	3/4" diam. to 1-1/4" diam.	-	•				61%	73%			
	1-1/2" diam. to 6" diam.				- 1		41%	57%			
	8" diam. to 12" diam.			,			31%	50%	•		
1	Schedule 120				;						
	1/2" diameter		1 Plum	50	.160	L.F.	2.63	5.30		7.93	10.9
	3/4" diameter			47	.170		3.03	5.65		8.68	11.9
	1" diameter			43	.186		3.89	6.20		10.09	13.6
	1-1/4" diameter			39	.205		4.50	6.80		11.30	15.2
	1-1/2" diarneter		+	33	242		5.05	8.05		13.10	17.7
1	2" diameter	:	Q-1	54 -	.296		6.10	8.85		14.95	20
	2-1/2" diameter			52	.308		8.30	9.20		17.50	23.
	3" diameter			49	.327		10.45	. 9.75		20.20	26.5
1	4" diameter			45	.356		15.70	10.65		26.35	33.50
	6" diameter		[↓ !	37	.432		27.50	12.95		40.45	50
1	To delete coupling & hangers, subtract				÷						
	1/2" diam. to 1-1/4" diam.				, A.		52%	74%			
†	1-1/2" diam. to 4" diam.						30%	57%			
	6" diam.						17%	50%			
PV	C, pressure, couplings 10' O.C., hangers 3 per 10'	•									
	SDR 26, 160 psi										ı
1	1-1/4" diameter		.1 Plum	42	.190	L.F.	2.44	. 6.35		8.79	12.3
,	1-1/2" diameter		"	36 .	.222		2.62	7.40		10.02	14.1
1	2" diameter		Q-1	59	.271		2.80	8.10		10.90	15.4
	2-1/2" diameter			56	.286		3.15	8.55		11.70	16.4
 	3" diameter			53	.302		3.65	9.05		12.70	17.6
	4" diameter	: 1		48	.333		5.10	10		15.10	20.5
 	6" diameter			. 39	.410		8.05	12.30		20.35	27:5
	8" diameter		Q2	48	.500	 	13.15	15.50		28.65	38
-	To delete coupling & hangers, subtract					-				 	
	· 1-1/4" diam.	•					63%	68%]	
+	the state of the s	<u> </u>	 				- 48%	57%		ļ .	,
	1-1/2" diam. to 4" diam. 6" diam. to 8" diam.						60%	54%		j .	i
	SDR 21, 200 psi, 1/2" diameter		1 Plum	54	.148	L.F.	2.01	4,93		6.94	9.6
`r'			1 3 10/11	51	.157]	2.18	5.20		7.38	10.3
1	3/4" diameter			46.	.174		2.63	5.80		8.43	11.6
 	1" diameter		, , ,	/in	1 110 -		7 54 7 1	n xii	,	× // * =	

	Plastic Pipe & Fittings	13		DAILY	LABOR-			2000 BAR	E.COSTS.	. <u> </u>	TOTAL
15108	Plastic Pipe & Fittings	~ (CREW	OUTPUT	HOURS	UNIT	MAT.	LABOR	EQUIP.	TOTAL	NC CO
3770	1-1/2" diameter	1	Plum	36	.222	L.F.	2.96	7.40	يمان د بي	10.36	
3780	2" diameter		Q-1	59	.271		3.17	8.10	٠.	11.27	
	2-1/2" diameter	<u> </u>	id	56	.286	_	4.15	8.55		12.70	
3800	3" diameter		11	53	.302		4.58	9.05		13.63	
	4" diameter		\dashv	48	.333		6.25	10		16.25	- 1
3810	•	1		39	.410	/.	10.05	12.30		22.35	
3830	6" diameter		Q-2	48	.500		16.70	15.50		32.20	- 1 m
3840	8" diameter		ŲΖ	40	.500	*	10.70	15.50	•	32.20	
4000	To delete coupling & hangers, subtract				:		730/	770/			
4010	1/2" diam. to 3/4" diam.	· /	İ	:			71%	77%	• •		
4020	1" diam. to 1-1/4" diam.				· ·		63%	70%	. •		
4030	1-1/2" diam. to 6" diam.		-		-		44%	57%			
4040	8" diam.		.		1.		46%	54%			- 4
4100 DV	WV type, schedule 40, couplings 10' O.C., hangers 3 per 10'							İ			
4120	ABS	1									
4140	1-1/4" diameter		l Plum	42	.190	L.F.	2.58	6.35		8.93	
4150	1-1/2" diameter	. 1	п :	36	.222		2.56	7.40		9.96	
4160	2" diameter		Q-1	59	.271		2.66	8.10		10.76	
4170	3" diameter	.	Ì	53	.302		3.28	9.05		12.33	
	4" diameter			48	.333	\vdash	4.44	10	9.55	14.44	7.0
4190	6" diameter		1	39	.410		7.10	12.30		19.40	
	To delete coupling & hangers, subtract		<u>.</u>		,,,20						200
4360		1			٠.		64%	68%	. `		
4370	1-1/4" diam.				<u> </u>		54%	57%		 	- Sec. 1975
4380	1-1/2" diam. to 6" diam.						3476	3/76			
4400	PVC			:40	100		2.55	C 25		0.01	1 1
4410	1-1/4" diameter		1 Plum	'42	.190	L.F.	2.66	6.35		9.01	
4420	1-1/2" diameter			36	.222		2.73	7.40		10.13	732
4460	2" diameter		01	59	.271		2.91	8.10	ļ	11.01	
4470	3" diameter	·		53	.302		3.79	9.05		12.84	
4480	4" diameter	- 1		48	.333		5.10	10		15.10	9 400
4490.	6" diameter	·	\forall	39	.410		7.40	12.30		19.70	
4500.	8" diameter		Q-2	48	.500	\ \	16.35	15.50		31.85	41
4750	To delete coupling & hangers, subtract	•									1
4760	1-1/4" diam. to 1-1/2" diam.						71%	64%			1
4770	2" diam. to 8" diam.	.a					60%	57%			
	VC, clear pipe, cplgs. 10' O.C., hangers 3 per 10', Sched. 40	· ·	-		·					,	《禮
4840	1/4" diameter		1 Plum	59	.136	. L.F.	2.32	4.51		6.83	
4850	3/8" diameter		\top	56	.143		2.51	4.75		7.26	
4860	1/2" diameter	- 1		54	.148		2.87	4.93		7.80	
4870	3/4" diameter		-	51	.157		3.36	5.20		8.56	
4880	1" diameter	- 1		46	.174		4.51	5.80		10:31	
	1-1/4" diameter			42	.190	\vdash	5.25	6.35	 	11.60	
4890	-	ĺ	1	36	.222		5.95	7.40		13.35	1 7778
4900	1-1/2" diameter		V Q-1	59	.271		7.25	8.10		15.35	
4910	2" diameter	1	ÅΤ	i	.271		10.20	8.55		18.75	14.57.55
4920	2-1/2" diameter		\dashv	56	·	\vdash		9.05		21.80	
4930	3" diameter	:		53	.302		12.75	1		1	
4940	3-1/2" diameter			50	320		15.65	9.60	<u> </u>	25.25	
4950	4" diameter	· .	\forall	48	.333	+	16.40	10		26.40) 3
5250	To delete coupling & hangers, subtract				<u> </u>		<u> </u>		ļ <u>.</u>	1	多物
5260	1/4" diam. to 3/8" diam.				'		60%	81%		1	
5270	1/2" diam. to 3/4" diam.	- <u> </u>				1	41%	77%			展
5280	1" diam. to 1-1/2" diam.						26%	67%			
5290	· 2" diam. to 4" diam.				'		16%	58%		-	
5360 C	CPVC, couplings 10' O.C., hangers 3 per 10'	.		 	1	1				·	78 H
1	Schedule 40	[
5380.			1 Plum	54	.148	L.F.	2.63	4.93	<u> </u>	7.5	51
5460	1/2" diameter	. 1	TEIMH	J4	.157	1	3.04	3		8.2	1297

	00 Building Services Pi			DAILY	LABOR-	·		2000 BAF	E COSTS	1987-1013 S. (1987)	TOTAL
Ø	Plastic Pipe & Fittings	544	CDEM	OUTPUT		UNIT	MAT,	LABOR	EQUIP.	TOTAL	INCL 0&P
j	1" diameter		1 Plum	46	.174	L.F.	3.98	5.80	cooir.	· 9.78	13.15
	1-1/4" diameter		. [42	.190	[4.57	6.35	•	10.92	14.65
_	1-1/2" diameter		1	36	.222	-	5.20	7.40		12.60	16.90
	2" diameter	•	0-1	59	.271		6.05	8.10	•	14.15	19
-			1.7	56	.286	-	, 8.85	8.55		17.40	22.50
(T	2-1/2" diameter			53	.302		10.55	9.05		: .	25.50
	3" diameter			48	.333		14.50	10		19.60	31
. — 1	4" diameter	•		ł			1 1			24.50	
<u>]</u> :	6" diameter		*	43	.372	*	26	. 11.15		37.15	45.50
	To delete coupling & hangers, subtract							77.			
	: 1/2" diam. to 3/4" diam.						37%	77%			
	1" diam. to 1-1/4" diam.						27%	70%			
· ';	1-1/2" diam. to 3" diam.				<u> </u>		21%	57%			
	4" diam. to 6" diam.	,:					16%	57%			
1	; Schedule 80			·							
)Ţ	1/2" diameter		1 Plum	50	.160	L.F.	2.74	5.30		· 8.04	11.05
	3/4" diameter			47	.170		3.22	5.65		8.87	12.10
1	1" diameter	•		43	.186		4.24	6.20		10.44	14
)	· 1-1/4" diameter			39	.205		4.96	6.80		11.76	15.7
i	1-1/2" diameter	:	*	34	.235		5.70	7.80		13.50	18.1
	2" diameter		Q1	55	.291	l l'	6,85	8.70		15.55	20.5
o i —	2-1/2" diameter			52	.308		9.90	9.20		19.10	25
\ \	3" diameter			50	.320		12.10	9.60	1	21.70	28 :
	4" diameter			46	.348		17	10.40		27.40	34.5
-	6" diameter		[↓	38	.421		31.50	12.60		44.10	53.5
	· 8" diameter		Q-2 .	47	.511	V	68.50	15.85		84.35	99.5
	To delete couplings & hangers, subtract			ļ		•					
\-	1/2" diam. to 3/4" diam.						44%	. 77%		1.	
0	1" diam. to 1-1/4" diam.		ŀ	·	· .		32%	71%			
1	1-1/2" diam. to 4" diam.		· ·				25%	58%			
	6" diam. to 8" diam.		[· : :		20%	53%			
ا إن	CTS, 1/2" diameter		1 Plum	54	.148	L.F.	2.08	4.93		7.01	9.7
0	3/4" diameter			51	.157		2.80	5.20		8	Ħ
+	: 1" diameter			46	.174		3.58	5.80		9.38	12.7
از	1 1/4"			42	.190		4.22	6.35		10.57	14.2
0	1 1/2" diameter			. 36	.222		5.05	7.40		- 12.45	16.7
	2" diameter	,	Q:1	59	.271	↓	7.10	8.10		15.20	20
+	To delete coupling & hangers, subtract		<u> </u>			<u> </u>					
J	: 1/2" diam.					1	51%	79%			
n)	3/4" diam.			 	+-	 	40%	76%			.:
"	1" thru 2" diam.	:					72%	68%	ł		
1	Polyethylene, flexible, no couplings or hangers		 	<u> </u>		<u> </u>	7270				
١.	Note: For labor costs add 25% to the couplings and fitting	.c lahar tatal		1	1 :						
2	· · · · · · · · · · · · · · · · · · ·	S labor total.	 		 	ļ.—			<u> </u>		
1	SDR 15, 100 psi			ľ	ļ	L.F.	17			.17	.1
)	3/4" diameter		 	 	 	L.F.	.17		 	.22	
01-	1" diameter	:	ŀ	ľ			1		1	1	
0	1-1/4" diameter		<u> </u>	 	-	-	.40		<u> </u>	.40	
)[1-1/2" diameter		j .		-		.50		}	.50	
υ	2" diameter		<u> </u>	<u> </u>	i .	<u> </u>	.80			.80	
0	SIDR 9, 160 psi		l:		1	I					
0	1/2" diameter				<u> </u>	L.F.	.23			23	
h 	3/4" diameter						,23			.23	
	1" diameter	•	[LÍ	.36			.36	
ο̃Ι	1-1/4" diameter	······································			1:		.60			.60	
ol	1-1/2" diameter		1				.84			.84	
0	2" diameter	:	<u> </u>	1.	1	1	1.38	·		1.38	1,
0	SDR 9, 200 psi	•	l	}	1	1 '.	-	}		1	

15	108 Plastic Pipe & Fittings	. 24%		DAILY			, 1.	2000 BAR		12 . rd.	TOTAL
		Maj Aja	CREW	ОИТРИТ	-	UNIT L.F.	MAT. .20	LABOR	EQUIP.	TOTAL .20	INCL 0&P .22
3150	3/4" diameter 1" diameter				- 4	,L.I.	.33		7.1	.20	
3160	1						.49		: .	.33	 (
3170			٠.		, ; }	*	١ د٦.			.43	- 74
3420				-		L.F.	.29			.29	32
3440					,	L.F.	1			1	
3450	1		· · ·	· .	<u> </u>	_ _	.46			.46	: :51
8460		;				4	.79	Ì		.79	:87.
8800		gr.		·	· .				**		1. V.a.
8840	3" diameter	*				L.F.	.32	: '	- ÷ ; + +	.32	.35
8850		<u>:</u>					.40			.40	.44
8860	6" diameter	:	1			₩ .	.89			.89	.98
9000	Perforated ·	†	Ŀ								: प्रस्कृ
9040	4" diameter				1	L.F.	.42		•	.42	.46
	· ·	•		İ	. "					ta 19 a i	1.384
0010	PIPE, PLASTIC, FITTINGS										188
0030	1	•			,			.			. (1)
0090	En 006 011		Q-1	23	.696	Ea.	45.50	21		66.50	81.50
0100	4 4 19			16	1		64.50	30	•.	94.50	116
0110	The state of the s	1		13	1.231		104	37		141	170 ≥ 8
0120	· ·	:	↓	8	2		156	60		216	263
0130			Q-2	. 9	2.667		260	83		. 343	4105kg
0140	N .	:		7	3.429		360	106		· 466	555
0150			 	5	4.800	+	500	149		: 649	775-3
0160	1	•	'			ľ					.>₫
0170	l										· joint
0172	i ·		⁻ Q-1	23	.696	Ea.	91	21		112	132 😘
0173			1	16	i		105	.30		135	162 ⊝∮
0174	` l ·			13	1.231		138	37		175	2
0174	1		╂╁╴	8	2	\vdash	249	60		309	3b
	1 .		Q-2	9	2.667		450	83		533	615
0177	<u> </u>		1	7	3.429		615	106		721	835/33
0178			1 1	5	4.800		835	149	,	984	1,150 39
0179			 	+	11000	<u> </u>					- 04i
0186	i .		Q-1	23	.696	Ea.	91.50	21-		112.50	133
0188											
0189	. 3			13	1.231		137	37		174	207
0190	0 4"		$+\pm$	13 R	2	$\vdash \vdash$	251	60		311	365
0192	0"		0.2	۵	2 667		450	83		533	620
0193	8"		\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	1 7	2.007		615	106		721	835
0194	10"		1	5	J.423		835	149		984	1 150 -0
0195	12"	-	01	17	0/1		61	20	-	90- F	11089
0290	Tee, 2" 2.5" 13		l Åī	10	1 600	'	71 50	40.		110 50	151: 67
0300	0 3"		+	10	1.000	1	0r	40		1/5	19/
0310	0 4"			6	2 200		220	مد مد		324	205 F
0320	0 6"		1 *	1 2	3.200	-	760	124	<u> </u>	207	175 · :
0330	0 8"		ŲΖ	0	4 000		400	140		307	505
0340	0 10"		 	1 5	4.800		420	149		200	000 /
0350	0 12"		🔻	4	6	🗡	510	186		סצס	04U\<.:
0352	Tee, flanged		1		1:		<u> </u>				170
0354	4 2"	•	Q-1	17	.941	Ea.	124	28		152	1/9
0355	5 3"	:		10	1.600		166	48		214	256
0356	6 4"	:		8	2		185	60		245	294 "
0358	8 6"	•	4	5 ·	3.200		365	96		461	545
0359	9 8"		Q-2	6	4		625	124		749	875
0360	0 10"	٠.		·5	4.800		905	149		1,054	1(
0361	1 12"	····	14	4	6		1,150	186	1	1,336	1,550
0365	5 Wye, flanged	3	'	ļ .	1	1.					
0300	V Try manbad		<u>. L.</u>						d		
	3" 4" 2 6" 3 8" 4 10" 5 12"										

	Building Services										
08	Plastic Pipe & Fittings	27.2	7. I		LABOR-			2000 BAR			TOTAL
ine I	Plasne Pipe of Fillings		CREW	OUTPUT	HOURS	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL O&P
	2"	:	Q1	17	.941	Ea.	. 320	28		348	395
	3"			10	1.600		355	48		403	465
	4"			8	2		440	60		500	575.
!	6"	•		5	3.200		530	96		626	725
· · · · ·	8"		Q-2	6 .	4		690	124		814	945
١,	10"			5	4.800		1,175	149		1,324	1,500
	12"		+	4	6		1,425	186		1,611	1,825
	Couplings		'			'					.:.
	2"		Q-1	28	.571	Ea.	10.90	17.10		28	38
	3″		Ì	20	.800		18.85	24		42.85	56.5
ı'	4"			17	.941	\vdash	20	28		48	64.5
	4 6″			12	1.333		38	40		78	103
·	8″		0-2	15	1.600		58	49.50		107.50	139
:	.10*	:	Ĭ	11	2.182		87.50	67.50		155	198
_	12"		$\vdash \bot$	10	2.400		117	74.50		191.50	242
	High corrosion resistant couplings, add		!	1.0	2.,00	▼	30%	,			
		<u> </u>	 							 	
1	Reducer, concentric, flanged	:	Q1	30	.533	Ea.	132	15.95		147.95	169
ļ	2" x 1-1/2" 3" x 2"		├	24	.667	 -	150	19.95		169.95	195
	•	>		19	.842		158	25		183	212
<u>, </u>	4" x 3"			15	1.067		206	32		238	276
	6" x 4"	· 2	Q ² 2	16	1.500		289	46.50		335.50	390:
<u> </u>	8" x 6"		\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	13	1.846		385	57.50		442.50	510×
١ .	10" x 8"	•		11	2.182		555	67.50		622.50	710 °
	12" x 10"		. Y	11	2.102		333	07.30		022,30	- 10
	Adapter, bell x male or female		01	28	.571	Ea.	19.65	17.10		36,75	47.5
·	2"		41	20	.800	La.	25	24		49	63.5
	3"			17	.941		34.50	28		62.50	80.5
·	4"		-	12	1.333		68.50	40		108.50	136
	6"	1	*	1	1		95.50	49.50		145	180
<u></u>	8"		Q-2	1 <u>5</u>	1.600 2.182	-	168	67.50		235.50	287
	10"	-		11	2.102	♥	100	07.50		255.50	**:
	Flange		0.1	10		F	17.40	10.40		27.80	35
ŀ	2" 2.5" 39		Q-1	46	.348	Ea.	17.40	10.40 14.95		35.95	
<u> </u>	3"		<u> </u>	32	1		21	18.40		47.90	60.5
,	4"	٠.		26	.615		29.50	30		80	101;
	6"		*	16.	1 1 222		50 82	41.50		123.50	153
	8"		Q-2	18	1.333			(167	207.
	10"	·		14	1.714		114	53		235.50	207.
	12"		🗡	10	2.400	*	161	74.50		233.30	250
	PVC schedule 80			<u> </u>	1			14.00		15.00	23:
. ·	· · · · · · · · · · · · · · · · · · ·	•	1 Plum	18	444	Ea.	.89	14.80		15.69	1
1	3/4"			17	.471		1.14	15.65		16.79	
1	1"			15	.533		1.83	17.75		19.58	l .
	1-1/4"			14	.571		2.44	L		21.44	
)[1-1/2"		\	13	.615		2.62	1		23.12	34
	. 2"	<u> </u>	Q-1	22	.727		3.16		·	25.16	
	3"	*		14	1.143		8.30	1		42.30	4
	4 ۳			12 -	1.333		12.65	1		52.65	
	6"	;	1	7	2.286		42.50		1	111	151
1	. 8"	:	Q-2	8	3		117	93		210	270 ⁻
 	45° elbow, 1/2"		1 Plum	18	.444		1.68	14.80		16.48	1
J	3/4"	*		17	.471		2.54	i .		18.19	26.
) }	. 1"	:	1	15	.533		3.84			21.59	31
	•	•		14	.571		4.87	1		23.87	1
}	1-1/4"		11	13	.615	 -	5.75		 	26.25	
.61	1-1/2"	-	i ▼	1 -5	.727	I i	7.45	1	1	29.45	8

46 304 314 314	75	100	Building Services Piping	j								richtender Karlichersberg	TEST STATE		
1989				7.		DAILY	LABOR-				2000 BARI	COSTS		TOTAL	100
	151	08	Plastic Pipe & Fittings			OUTPUT		UNIT	MA	IT.	LABOR	EQUIP.	TOTAL	INCL 0&P	
560	2320		. 3"	· Q	1	14	.1.143	Ea.		19.05	34		53.05	73%	7
	2330		4"			12	1.333			34.50	40		74.50	JO .,	100
	2340		6"	٦,	7	7	2.286			43	68.50		111.50	152	
	2350		8"		2	8	3.			83	93		176	232:	
	2400		Tee, 1/2"	1 F	lum	12	.667			2.50	22		24.50	36.50	1.00
	2420		3/4"			11	.727			2.62	24		26.62	39.50	
	2430		1"			10 -	.800			3.27	26.50		29.77	43.50	1.5
	2440		1-1/4"	_		9	.889	<u> </u>		9	29.50		38.50	54.50 60.50	1000
	2450		1-1/2"		V	8	1			9	33.50		42.50		350
	2460	,	2"		-1	14	1.143	ĻĻ	<u> </u>	11.25	34		45.25	64.50 97.50	
	2470		3"	1		9	1.778			15.30	53		68.30 77.70	110	
	2480		4"		1-1	8	<u>2</u> 3.200	\vdash	<u> </u>	17.70 60.50	60 96		156.50	212	-
	2490		6"	1	*	5 6	3.200			85.50	124		209.50	282	
	2500		8")-2 Plum	34	.235			4.84	7.80		12.64	17.15	- 3
	2510		Flange, socket, 150 lb., 1/2"	1''	1011	32	.250			5.20	8.30		13.50	18.25	
	2514		3/ 4 "		+	28	.286	\vdash	+-	5.80	9.50		15.30	20.50	
	2518	*	1" 1-1/2"	ŀ	\perp	24	.333			6.10	11.10		17.20	23.50	7.72
	2522 2526		2")-1	42	.381		+	8.10	11.40		19.50	26	1
	2530	•	2. 4"		ï	30	.533			17.45	15.95		33.40	43 🖑	
	2534		6"			22	.727		-	27.50	22		49.50	63 🗡	
	2538		8"		22	26	.923			50	28.50		78.50	.98.50	
	2550		Coupling, 1/2"	1	Plum	18	.444			1.61	14.80		16.41	24.50	20
	2570		3/4"			17	.471			2.17	15.65		17.82	26 -	100
	2580		1"		П	15	.533			2.23	17.75		19.98	29.50) [灣
•	2590		1-1/4"			14	.571			3.39	19	·	22.39	32 -	一 類
	2600		1-1/2"		₩	13	.615			3.66	20.50		24.16	35	
	2610		2"		Q-1	22	.727			3.92	22		25.92 36.10	37.5 50	(
	2620		3"			19	.842			11.10	25 30		43.90	61 ±	Ì
	2630		· 4"		-	16	1.333	\vdash		13.90 30	40		70	93.50	
•	2640		6"		▼	12 14	1.714			54	53		. 107	140	
	2650		8"		Q-2 1	13	1.846	+		84	57.50		141.50	1	-
	2660		10" 12"		1	12	2			112	62		174	217	
	2670 2700	DVO	(white), schedule 40, socket joints		*	 	+-	┰							1
	2760	rvu	90° elbow, 1/2"	1	Plum	22	.364	Ea	.	.23	12.10		12.33	18.5	5
	2770		3/4"		\top	21	.381	I		.25			12.90	19.4	5
	2780		1"	1		18	.444			.45	14.80		15.25		
	2790		1-1/4"		1.	17	.471			.80	1		16.45	1	
	2800		1-1/2"	.	\downarrow	16	.500			.85	1		17.50		
	2810		2"		Q-1	28	.571			1.34	1		18.44	•	
	2820		2-1/2"		_	22	.727		4	4.06	1		26.06		0
	2830		3"			17	.941			4.86			32.86		
	2840		4" .		\perp	14	1.143	1		8.70			42.70 62.50		
•	2850		5"	1		12	1.333			22.50	I .		87.50		
	2860		6"		<u>*</u>	8	2	1		27.50	1		151.50		-
	2870		8"		Q-2	10	2.400			77	74.50 12.10		12.4		70
	2980		45° elbow, 1/2"		Plum		.364	+		.37			13.2		
	2990		3/4"	1		21	.381			.c. 86.	[1	15.4	1	1
	3000		1"			18	.444			.00			16.6	_1	
	3010		1-1/4"			16	.500			1.20	1	1	17.8		
	3020		1-1/2"		<u>▼</u> Q-1	28	.571			1.5			18.6		
	3030		2"		Ĭ	22	.727		.	4.0	1		26.0	1	/
	3040		2-1/2" 3"		+÷	17	.941			6.30		 	34.3		
	3050 3060		4" ·	1		14	1.143		,	11.3	l .		45.3	5 . 64.	50
	2000		T		<u> </u>	حضيك			<u></u>						:

	00 Building Services P		4	DAILY	LABOR			2000 RAI	RE COSTS		7074
08	Plastic Pipe & Fittings		CREW	1	HOURS		MAT.	LABOR	EQUIP.	TOTAL	TOTAL INCL 0&P
	5"		Q-1	12	1.333		22.50	40	EQUIF.	62.50	85 .
	6″			8	2	Ī	28	60		88	122· 、
	8"		Q-2	10	2.400	┢┈	93	74.50		167.50	215
	Tee, 1/2"	•	1 Plum	Į.	.571		.28	19		19.28	213 \
	3/4"			13	.615	H -	.32	20.50	<u> </u>	20.82	<u> </u>
	1"			12	.667		.59	22		22.59	31.50
	1-1/4"	1,,	1-	11	.727	┢┵	.94	24			34 .
	1-1/2"			10	.800]	1.13	26.50		24.94	37.50
	. 2"	:	Q·1	17	.941	\vdash	1.13	28.30		27.63	41
	2-1/2"		Y.	14	1.143		5.45	34		29.65	44.50
	3"		╂┼╌	11	1.455	++	7.15	43.50		39.45	58
	4"			9	1.778		12.90	43.30 53	-	50.65	74
	5"			8	2	$\vdash \vdash$	31	60		65.90	94.50
	-	:		5	1					91	125
	6" 8"		V Q-2	6.	3.200		43.50	96 124		139.50	193
	Coupling, 1/2"	·*	. Q-2 1 Plum	22	.364		.18		,	177	246
	3/4"		1 1 10111	21	.381		.18	12.10		12.28	18.50
	5/ 4 . 1″	•		. 18	.301		.41	14.80		12.89	19.40
-3	1 1 /An		 - -	17.	.471		.57	15.65		15.21 16.22	23 24
ı	1-1/4"	.,		16	.500		.61	16.65		17.26	
	2"		0-1	28	.571		.95	17.10		18.05	25.50 · 27
	2-1/2"		Ĭ	. 20	.800		2.08	24		26.08	38.50
	3"	· · · · · · · · · · · · · · · · · · ·	-	19	.842		3.27	25		28.27	41.50
,	4"		Ì	. 16	1		4.72	30		34.72	50.50
	5"			14	1.143		8.65	34		42.65	61:50
·	6"			. 12	1.333		14.90	40		54.90	77
	8"		Q-2	14	1.714		28	53		81	111
· Marian	Reducing insert, schedule 40, socket weld	÷				'				0.	111 1
	3/4"		1 Plum	20	.400	Ea.	70	13.30		· 14	21.
٠.	1"			18	.444	1 1	1.19	14.80		15.99	24
 	1-1/2"		•	16	.500		1.25	16.65		17.90	26.50
	2"	٠.	Q1	31	.516		1.59	15.45		17.04	25.50
:	4"			22	.727		7.05	22		29.05	41 :
	6"		↓ .	: 14	1.143		17.45	34		51.45	71
	8"		Q-2	18	1.333	V	61	41.50		102.50	130
	Reducing insert, socket weld x female/male threa	ad '	. (i				
	1/2"		1 Plum	24	.333	Ea.	1.41	11.10	٠.	12.51	18.30
	3/4"			23	.348		.87	11.55		12.42	18.45
	. 1"			20	.400	. •	1.22	13.30		14.52	21.50
	1-1/2"		₩.	16	.500		2.20	16.65		18.85	27.50
	· 2"		Q-I	26	.615		1.17	18.40		19.57	29.50
	4"		"	14	1.143	*	4.61	34		38.61	57
	Male adapter, socket weld x male thread				1		-	.			•
	1/2"		1 Plum	24	.333	Ea.	.27	11.10		11.37	17.05
	3/4"	1	-11	23	.348		.30	11.55		11.85	17.85
	· 1"			20	.400		.53	13.30		13.83	· 20.50
	1-1/2"		₩.	16	.500	.	.87	16.65		17.52	26
	2"		Q-1	26	.615		1.14	18.40		19.54	29.50
	4 *		. "	14	1.143	₩	6.30	34		40.30	59
	Female adapter, socket weld x female thread	<u> </u>			3						
	1/2"	1 g	1 Plum	24	.333	Ea.	33	· · 11:10		·11.43	17.10
	3/4"			23	.348		.42	11.55		11.97	17.95
	1"	į,	T	20	.400		.49	13.30		13.79	20.50
	1-1/2"		V	16	.500		.87	16.65		17.52	26:
***************************************	2"	7.1	Q-1	26	.615		1.17	18.40	•	19.57	29.50
	. 4 "	, ,		14	1.143	1 1	6.60	34		40.60	59.50

9 2 3 00	Plastic Pipe & Fittings	3. T.		DAILY	LABOR-			2000 BAF	RE COSTS	100	TOTAL
15108	Plastic Pipe & Fittings	CR	EW		HOURS	UNIT	MAT,	LABOR	EQUIP.	TOTAL	INCL 08
3800	PVC, schedule 80, socket joints							D.O.V.	270111	10112	1102.00
3810	Reducing insert										
3812	3/4"	10	lum.	23	.348	Ea.	.67	11 65		10.00	<u> </u>
	*	1.,	IUIII		1 1	Ca.	1 1	11.55		12.22	1
	. ' 1"			20	.400	<u> </u>	1.91	13.30		15.21	2
3815	1-1/2"		7	16	.500		4.09	16.65		20.74	2
3816	2"	Q	1 .	28	.571		5.35	17.10		22.45	3
3817	4"			16	1,		22	30		52	7
3818	6"	1	- 1	12	1.333		31	40		71	9
3819	8"	Q	-2	14	1.714	V	22.50	53		75.50	10
3830	Reducing insert, socket weld x female/male thread		1		. : }	'					
3832	1/2"	1 1	1um	24	.333	Ea.	1.78	11.10		12.88	
3833	3/4"	117	ı''''	23	.348	La.	1 1			1 '1	1
1.	1"						1.11	11.55		12:66	1
3834				20	.400		1.92	13.30		15.22.	. 2
3836	1-1/2"	- 1		16 ·	.500		3.22	16.65		19.87	2
3837	2"	Q	-1	28	.571		4.66	17.10		21.76	3
3838	4"	1 '	"	16 -	1	₩	41	30		71	g
3844	Adapter, male socket x male thread							······································			:
3846	1/2"	1 P	tum	24	.333	Ea.	1.01	11.10		12.11	1
3847	3/4"	-		23	.348		1.11	11.55	 	12.66	1
3848	1"			20	.400		1 1			1	
					L		1.92	13.30		15.22	2
3850	1-1/2"	- 13		16	.500	•	3.22	16.65		.19.87	.2
3851	2"	. Q		28	.571		4.66	17.10		21.76	
3852	4"	1	'	16	1	\ ₩	10.45	30		40.45	- 5
3860	Adapter, female socket x female thread		1		. :	١.		1			
3862	1/2"	1 P	lum	24	.333	Ea.	.81	11.10		11.91	1
3863	3/4"	· •		23	.348		2.88	11.55		14.43	2
3864			-	20	.400	\vdash	4.25	13.30		17.55	2
3866	1-1/2"			16	.500	1 1	8.45	16.65		25.10	,
3867	. 2"	Q	,	28 .	.571	├-	14.75	17.10		31.85	
3868	4"	, Y	,	16			1 1				`.
	·		_	10	1	*	45	30		75	9
3872	Union, socket joints	. [. 1		1		1				i.
3874	1/2"	1 P	lum	19	.421	Ea.	4.25	14		18.25	2
3875	. 3/4"			18	.444		5.40	14.80		20.20	2
3876	1"	.1 1	1	15	.533		6.15	17.75		23.90	. 3
3878	1-1/2"			13	.615		13.85	20.50		34.35	7
3879	2"	Q	1	27	.593		18.80	17.75		36.55	4
3888	Cap	- `					20.00	17.70	 	30,00	
3890	1/2"	1 PI	lum	36	.222	Ea.	202	7.40		0.43	1
\$	3/4"	1 1	unti	34	, ,	⊏a,	2.03	7.40		9,43	1
3891	3/4" 1"		- 1		.235		2.13	7.80		9.93	1
3892		-	4	30	.267		3.80	8.85		12.65	• 1
3894	1-1/2"] 4	,	. 26 -	.308		4.58	10.25		14.83	2
3895	2"	Q	1	44	.364	4	9.05	10.90		19.95	2
3896	4"		1	32	.500		36.50	14.95		51,45	. 6
3897	6"		, 1	24.	.667		83	19.95		102.95	12
3898	8"	Q	2	28	.857		107	26.50		133,50	15
	V, ABS, non pressure, socket joints			~~	.00,	,▼			}	.55,55	1
1	1/4 Bend, 1-1/4"	1 Pi	_	17	471	Fa		1F CF		10.04	 ,
1540	· · · · · · · · · · · · · · · · · · ·	117	uiii			Ea.	.99	15.65		16.64	Ş
1560	1-1/2"			16	.500		.53	16.65	<u> </u>	17.18	- 3
1570	2"	0	1	28	.571		.87	17.10		17.97	7
1580	3"		1	17	.941		2.05	28 · ·		30.05	1
1590	4 ^r		1	14	1.143		3.57	34		37.57	1
1600	6"	.]]	,	8	2		22.50	60		82.50	15
1650	1/8 Bend, same as 1/4 Bend		-		-	V	- L.30		 	- 02.00	1.3
1	•		Í	•			[.			1.	
1800			1						<u> </u>	ļ	
1820	1-1/4"	. 1 PI	nm	11	.727	Ea.	. 1.25	24	1	25.25	1 2
830	1-1/2"		4	10	.800		.77	26.50		27.27	à

	00 Building Services Piping			12000			0000 000	C COSTO		
08	8 Plastic Pipe & Fittings	ODEN!	,	LABOR-	Unior	1447		RE COSTS	le Torn	TOTAL
Ĭ	2"	CREW Q-1	17	HOURS .941	UNIT Ea,	MAT. 1.10	LABOR 28	EQUIP.	TOTAL 29.10	INCL 0&P 43.50
ľ	2 3"	1.9	11	1,455	[[a,	2.79	43.50		46.29	43.50 69 T
	Δ" .		9	1.778	┝┼╌	6.90	53		59.90	88
	Tee, sanitary, reducing, 2" x 1-1/2"	[]	17	.941		1.63	28		29.63	44.50
	3" x 2"		11	1.455	$\vdash \vdash$	2.36	43.50		45.86	68.50
	4" x 3"		10	1.600		7.70	48		55.70	81
	Combination Y and 1/8 bend	-+	 	1						
	1-1/2"	· 1 Plum	10	.800	Ea.	2.34	26.50		28.84	42.5
	2"	Q1	17	.941		2.84	28		30.84	45.5
	3"		11	1.455		5	43.50		48.50	71.50
	4"		9	1.778	\Box	9.85	53		62.85	91.5
	3" x 1-1/2"		11	1.455		5.85	43.50		49.35	72.5
	4" x 3"	1	10	1.600		8.80	48		56.80	82 -
	Wye, 1-1/4"	1 Pluп	11	.727	•	1.44	· 24		25.44	38 ·
	1-1/2"	. "	. 10	.800		1.47	26.50		27.97	41.5
	2"	Q1	17	.941		1.51	28		29.51	44.
	3"	•	11	1.455		3.47	43,50		46.97	70
	· 4"		9	1.778		8.20	53 ·		61.20	89,5
	6"		5	3,200		31	96		127	180:
· .	3" x 1-1/2"		11	1.455	<u> </u>	3,43	43,50	 	46,93	. 70.
	4" x 3"		10	1.600		5.70	48		53.70	79
	. 6" x 4"	1.0	6	2.667	<u> </u>	25.50	80		105.50	150
	Double Wye, 1-1/2"	1 Plum 0-1	8	1.333		3.12 4.01	33,50		36.62 44.01	54 65
	2"	1	8	2	 	10.35	40 60	<u> </u>	70.35	102
١.	4"	: 1	6	2.667		21	80		. 101	144
- }-	2" x 1-1/2"	-1	11	1.455	$\vdash \vdash$	4.01	43.50		47.51	70.5
	3" x 2"		8	2		7.70	• 60		67.70	. 99 :
 	4" x 3"		1.7	2.286	\vdash	16.65	68.50		85.15	122
i i	6" x 4"		5	3.200		34.50	96		130.50	183
7.	Reducer bushing, 2" x 1-1/2"		30	.533		.51	15.95		16.46	24.5
1	3" x 1-1/2" (3" x 2" 22)	11	24	.667		1.85	19.95		21.80	32.
-	4" x 2"		20 .	.800		4.27	24		28.27	40.5
	6" x 4"	1 🔻	17	.941		11.40	28		39.40	554
	Couplings, 1-1/2"	1 Plum	1	.500		.56	16.65		17.21	25,5
_	2".	Q-1	28	.571		.33	17.10		17.43	26.5
	3"		22	.727		1.15	22		23.15	34.5
_	4"		. 17 -	.941	<u> </u>	1.77	28		29.77.	.44.5
	6"		: 12	1.333		11.85	40		51.85	73.5
	2" x 1-1/2"		30	.533	 	1.15	15.95 19.95		16,29 21.10	24.5 31.5
	3" x 1-1/2" 4" x 3"		19	.842		4.53	25		29.53	43
-	4" X 3" Closet flange, 4"	1 Plum		.250	$\vdash\vdash$	4.55	8.30	<u> </u>	12.99	17.7
	4" x 3"	, , , ,	34	.235		4.02	7.80		11.82	16.2
1	DWV, PVC, schedule 40, socket joints		+	 	├ ▼			 		10.1
1	1 /4 1 1 1 1 /4"	1.Plum	17	.471	Eą.	.93	15.65		16.58	24.5
			16	.500	H	.41	16.65	 	17.06	25.5
[:	2"	0-1	28	.571		.63	17.10		17.73	26.5
1	3*	:	17	.941		1.57	28		29.57	44
	4"		14	1.143		2.82	34		36.82	55 ·
-	6"	1	8	2		17.15	60	· · · · ·	77.15	109
۱ :	. 8"	Q2	10	2.400		34.50	74.50		109 :	151
1	10"	"	7	3,429		37.50	106		143.50	202
	1/4 bend, long sweep, 1-1/2"	. 1 Pluri		.500		1.28	16.65		17.93	26.9
ξ;	2"	Q1	28	.571		1,05	17.10		18.15	27
12	3"	* 1 \	17	.941	↓	2.73	28		30.73	45.5

	0 Building Services P						indicated (1986). J		discontinuos.	pelijakszentjanski.	Making Sign
15108	Plastic Pipe & Fittings		CREW	DAJLY	LABOR HOURS	•	MAT.	2000 BA	RE COSTS	ا مخمد	TOTAL
5116	^ 4"		Q-1	. 14	1.143	Ea.	5.40	34	EQUIP.	TOTAL 39.40	INCL OF
5150	1/8 bend, 1-1/4"		1 Plum	17	.471	1	.82	15.65	Ì	16.47	
5170	1-1/2"		1 110111	16	.500	 	.46	16.65	 		24. 25.
5180	2"		Q-1	28	.571		ş	1		17.11	. 744
5190	3"		141	17	.941	} }-	.66	17.10	ļ ·	17.76	26
5200				1	1		1.35	28		29.35	44
	. 4"		1	14	1.143	 	2.25	34		36.25	54
5210	6"		A	8	2		15.70	60 -		75.70	108
5215	. 8"		Q-2	10	2.400		41	74.50		115.50	158
5216	10"			7	3.429		62	106		168	230
5217	12"		₩	6	4		99.50	124		223.50	297
5250	Tee, sanitary 1-1/4"		1 Plum	11	.727		1.45	24		25.45	38
5254	1-1/2"			10	.800		.61	26,50		27.11	40
5255	2"		Q-1	17	.941		.83	28		28.83	43
5256	3"			11	1.455		2.29	43.50		. 45.79	68.
5257	4"			9	1.778		4.38	53		57.38	85
5259	6"		₩	. 5	3.200		25.50	96	l ·	121.50	173
5261	. 8"		Q-2	6	4		76	124		200	272
5264	2" x 1-1/2"		Q1	17	.941]	2.05	28		30.05	15
5266	3" x 1-1/2"			12	1.333		1.76	40		41.76	62
5268	4" x 3"			12	1.333		8.05	40		48.05	69
5271	6" x 4"	. ,	-	8	-2	*	25	60		85 .	148
5276	Tee, sanitary, reducing			ļ							
5281	2" x 1-1/2" x 1-1/2"		Q-1	17	.941	Ea.	.87	28		. 28.87	43
5282	2" x 1-1/2" x 2"	·		17	.941		1.63	28		29.63	44
5283	2" x 2" x 1-1/2"			16	1		1.03	30		31.03	46
5284	3" x 3" x 1-1/2"	•		12	1.333		2.13	40		42.13	63
5285	3" x 3" x 2"			11	1.455		. 2.36	43.50		45.86	68
5286	4" x 4" x 1-1/2"			11	1.455		6.15	43.50	-	49.65	73
5287	4" x 4" x 2"			10	1.600		5.90	48		53.90	79
5288	4" x 4" x 3"			· 9	1.778		8.05	- 53		61.05	89
5291	6" x 6" x 4"		V	6	2.667	\	24.50	80		104.50	140
5294	Tee, double sanitary					ľ					
5295	1-1/2"		1 Plum	8	1	Ea.	1.57	33.50		35.07	52
5296	2"		01	12	1.333		2.66	40		42.66	
5297	3"			8	2		7.45	60		67.45	63 98
5298			↓	6	2.667	4	12	80		92	134
5303	Wye, reducing					<u> </u>				 	W.
304	2" x 1-1/2" x 1-1/2"		Q1	17	.941	Ea.	2.25	28		. 30.25	4
305	2" x 2" x 1-1/2"			15	1.067		2.13	32	L	34.13	- 51
306	3" x 3" x 2"			12	1.333		4.40	40		44.40	64
307	4" x 4" x 2"			11	1.455		4.10	43.50		47.60	1
309	4" x 4" x 3"		↓	10	1.600		4.79	48	•	52.79	.71
314	Combination Y & 1/8 bend, 1-1/2"		1 Plum	10	.800		1.88	26.50		28.38	4
315	2"		Q1	. 17	.941		2.50	28		30.50	Ų,
317	3".		1"	11	1.455		4.12	43.50		47.62	70
318	4" .	•		9	1.778		8.10	53		61.10	89
319	6"		. 🔻	5	3.200		62.50	96		158.50	214
320	8"	•	Q-2	6 .	4		100	124		· 224	290
324	Combination Y & 1/8 bend, reducing	***************************************				▼.		-L r			: 886
325	2" x 2" x 1-1/2"	:	Q1	17	:941	Ea.	3.64	28		31.64	4
327	3" x 3" x 1-1/2"	•	4,	13	1.231		4.80	37		41.80	6
328	3" x 3" x 2"			12	1.231		3.01	40		43.01	
329	4" x 4" x 2"		\vdash	11	1.455		6.70	43.50		50.20	64 73
331			1 Plum	11 -						a a	
1	Wye, 1-1/4"	·	1 Plum		.727		1.39	24		25.39°	38
332 333	1-1/2"			10	.800		1.21	26.50		27.71	11
5551	2".		Q1	17	.941	4	1.21	28		29.21	¥

100 Building Services Pipi			DAILA	LABOR-			2000 DAI	RE COSTS	2,50157658152154581	7071
108 Plastic Pipe & Fittings	1	CREW	OUTPUT	1		MAT.	LABOR	EQUIP.	TOTAL	TOTAL
3"		Q-1	11	1:455	Ea.	2.79	43.50	EQUIP.		INCL 0&P
	- 1	Į.	9	1.778	La.	f t			46.29	69 ↔
6"		-				5.10	53		58.10	86 ¿
-		▼	5	3.200		33 · .	96		129	182
8"		Q-2	5	4.800		37.50	149		186.50	267
10"			4	6		58.50	186		244.50	345
12"		<u> </u>	3	8		86.50	248		334.50	470
2" x 1-1/2"	l	Q-1	17	.941		2.13	28		30.13	45
3" x 1-1/2"			12	1.333		2.82	40		42.82	63.50
al 4" x 3"	. 1		10	1.600		4.79	48		52.79	78
6" x 4"		<u> </u>	6	2.667		18.80	80		98.80	142
8" x 6"		Q-2	8	3	1	45	93		138	191
Double wye, 1-1/2"	· 1	1 Plum	8	1		2.57	33.50		36.07	53.50
2"	·	Q-1	12	1.333		3.30	40		43.30	64 :
3"	. [8	2		8.50	60		68.50	100
4 ^ñ	7		6	2.667		17.25	80		97.25	140 -
2" x 1-1/2"	·		11	1.455		3.02	43.50		46.52	69:50
. 3" x 2"			8	2		6.35	60		66.35	97.50
4" x 3"			7	2.286		13.70	68.50		82,20	119
6" x 4"		+	5	3.200		28.50	96		124.50	177
Coupling, 1-1/4"	1	Plum	17	.471		.78	15.65		16.43	24.50
1-1/2"			16	.500		.26	16.65		16.91	25.50
2"		Q-1	28	.571		.27	17.10		17.37	26.50
. 3"	— 	Ì	22	.727	\vdash	.78	22		22.78	347
4"	Ì		17	.941		1.28	28		29.28	44
6"		\downarrow	12	1.333	\vdash	6.85	40		46.85	68
8"		Q2	14	1.714		15.45	53		68.45	97.50
2" x 1-1/2"		Q1	30	.533	\vdash	.68	15.95		16.63	25.
3" x 1-1/2"		i l	25	.640		2.15	19.15		21.30	
4" x 3"	- : :		18	.889		3.73	26.50		30.23	31.50 44.50
Reducer bushing, 2" x 1-1/4"			. 31	.516		.46	15.45		1 5	
2" x 1-1/2"		+-1	30	.533		.46	15.45		15.91	24 🖖
			1			1	i		16.41	24.50
3" x 1-1/2"			25	.640	\dashv	2.01	19.15		21.16	31
 	:		. 24	.667		.93	19.95		20.88	31
4" x 2"		\bot	22.	.727		3.51	22		25.51	37
4" x 3"	- 1		20	.800		1.94	24		25.94	38
6" x 4"		*	14	1.143		10.05	34		44.05	63
8" x 6"		Q2	. 18	1.333		20	41.50		61.50	84.50
Closet flange 4"		Q-1	32 -	.500		4.73	14.95		19.68	27.50
4" x 3" Solvent comput for PVC industrial grade per quart			34	.471	*	3.55	14.10		17.65	25.50
Solvent Centent for 1 vo, moust fair Brade, per quart				, ž	Qt.	10.80			10.80	11.90
CPVC, Schedule 80, threaded joints	ŀ									, .
90° Elbow, 1/4"	1	Plum	20	.400	Ea.	5.35	13.30		18.65	26
1 1/2"			18	.444		2.09	14.80		16.89	25
3/4"		1 1	17	.471		2.67	15.65		18.32	26:50
I"		11	15	.533		4.24	17.75		21.99	31.50
1-1/4"			14	.571		9.20	19		28.20	38.50
1-1/2"		+	13	.615	$\dashv \dashv$	10.25	20.50		30.75	42:50
2"		Q-1	22	.727		12.40	22		34.40	46.50
The state of the s	<u> </u>	++	18	.889	++	28.50	26.50		55	72
2-1/2″ 1. 3″			1	1.143		32	34		66 ·	87.50
4"		+		1.143	+	58	40		98	125.
•						1	(
6" 45° Elbow same as 90° Elbow		*	7	2.286	*	117	68.50		185.50	232 16
	1.	_	_		_					
Tee, 1/4"	11	Plum	14	.571	Ea.	6.55	.19		· 25.55	35.50
1/2"		1	1,2	.667	\prod	6.55	22		28.55	40.50
3/4"		1	11	.727		6.65	24		30.65	44

ur i / P	151	00 Building Services Piping												Be.
	C12531 - 411		'n	i		LABOR-		·		2000 BARE		1	TOTAL	
١	1510	8 Plastic Pipe & Fittings	CRE	W O	UTPUT	HOURS	UNIT	-	MAT.	LABOR	EQUIP.	TOTAL	INCL OU	
60 5	890	1"	1 Plu	ım ,	10	.800	Ea.	.	8.15	26.50		34.65	58.1	SE P. 19 12
	900	1-1/4"			9	.889	Ŀ		12.90	29.50		42.40 48.30	67	
	910	1-1/2"	. 🔻		8	1			14.80	33.50		50.45	70	24 B 27
	920	2"	Q-1	1	14	1.143			16.45	. 34		82	107	-
8	930	2-1/2"			12	1.333			42	40		95	127	200 24 124
8	5940	3"			9	1,778			42	53		116	152	4 77 7 3
- 8	5950	4"			8	2		1.	56	60		241	305	
	5960	6"	4	,	5	3.200		\perp	145	96	· · · ·	19	26	
L	5000	Coupling, 1/4"	1 Pl	lum	20	.400			5.70	13.30		1	25	100
	5020	1/2"			18	.444			2.21	14.80		17.01	27	
	6030	3/4"			17	.471		1	3.09	15.65		18.74		
	6040	. 1"			15	.533			4.16	17.75		21.91	31	
	6050	1-1/4"			14	.571			6.25	19		25.25	1	1.77
- 1	1	1-1/2"	١,		13	.615			7.85	20.50		28.35		
ŀ	6060	2"	Q	ŀI	22	.727		I	9.15	22		31.15	147	100
	6070	2-1/2"	1		20	.800	.1		20.50	24		44.50		
	6080	3"	1		19	.842			22	25		47		27.0
ı	6090	4"			16	1	1		29	30		. 59	1 7	
	6100	6"	1	+	12	1.33	3	\sqcap	68	40		. 108	2	
	6110	· 6") -2	14	1.71	4 4	↓	126	53		. 179		0.2
	6120	CTS, 100 psi at 180°F, hot and cold water	+		1	1	1		, , , , , , , , , , , , , , , , , , , ,				13	
	6200	·	1	Plum	20	.400) E	a.	.07	13.30		13.3		0
.	6230	90° Elbow, 1/2"	╁	1	19	.42			.16	14		14.1		圖影
	6250	3/4"			16	.500			.52	16.65		17.1		
٠. ا	6251	1"	╁	+	15	.53			.89	17.75		18.6		200
	6252	1-1/4"	1	Ţ	14	.57	1		1.43	19		20.4		30 製
	6253	1-1/2"	十	V Q1	23		1	1	3.08	21		24.0		35
	6254	2"		Plun	li .	1 3			12	13.30		. 13.4		20
	6260	45° Elbow, 1/2"	╁	1	19			+	.18	· 14		14.1		21
	6280	3/4"		1	16	- 1			.48	16.65		17.		25
	6281	1"	╁	╫	15			+	.94	17.75		18.		28
•	6282	1-1/4"		1	14	1 .			1.49	19		20.		30
٠,	6283	1-1/2"	+	Q-1	23			+	3.14	21		24.		35
	6284	2"		. Plui	i	1	- 4	1.	.10	20.50		20.	60	31
	6290	Tee, 1/2"	+	1	12			Ť	.23	22		22.	23	34 38 4 42
	6310	3/4"		-	11				1.18	24		25.	18	38
	6311	1"	\dashv	+	10			1	1.80			4		
	6312	I		1	10	i			2.34	26.50) .	- 28		42.00
	6313		+	0-1			41	+	3.80	28		1		46 4
	6314	1		ı Plu	- 1		64		.0:			1		18 N
	6320		+	-	2		81	十	1.1	12.6	5		.75	192
	6340		.				44		.4		0	I	.25	23
	6341			\dashv	$+\frac{1}{1}$		71	+-	 		5		5.21	24 2
	6342	1	١	1		- 1	00		.7		5		7,44	26
	6343	<u></u>		Q:			571	+	1.5		0	1	3.68	27.50
	6344	t optoaraid grade per quart	.	Ą,	. ['	- 1		▼ Qt.	7.3	1			7.30	8
	6360	Solvent cement for CPVC, commercial grade, per quart		<u> </u>	\dashv				-		1			
	·7990													
	8000	Compression type, PVC, 160 psi cold water		1 Pl	um '	21 .	381	Ea.	1.9	90 12.6	55	1	4.55	21
	8010				- 1	- 1	444	<u> </u>	2.3		30	i	7.14	25
	8020		\dashv	\vdash			471	+	3.			1	8.92	27
	803		<u> </u>				4/1 500			50 16.		2	1.15	30
	804	0 1-1/2" CTS () 3 (S)	3) 4		1		533	$\vdash +$	1	30 17.			4.05	34
	805	0 2" CTS	7		t t	i i			3	01 11.	1	1	4.56	213
	806	1 2 4 5 5 6 4 5 EDT 2 4 5 CTC	: .		· I		348	$\vdash \vdash$		50 12.	1		7.15	
	807	1 070			l ł		381		1	53 13.	- 1	l l	17.83	2/ 25
	808			نــــــــــــــــــــــــــــــــــــــ	<u> </u>	20 :	.400	*	4.	10 10.	~			4
	1 000													

	ces Piping				8585			DE COSTO		
Plastic Pipe & Fittings	(4.5) (4.4)	CDEM	DAILY OUTPUT	LABOR-		MAT.	2000 BAI LABOR	RE COSTS	TOTAL	TOTAL
1-1/4" FPT x 1-1/4" CTS		1 Plum	. 18	.444	Ea.	. 5.95	14.80	EQUIP.	TOTAL 20.75	INCL 0&P 29
1-1/2" FPT x 1-1/2" CTS			16	.500	Ī	6.95	16.65	1	23.60	32,50
2" FPT x 2" CTS	(v) //is/-	H +	13	.615	┢┿	10.30	20.50			
Male adapter, 3/4" MPT x 3/4" CTS		1	23	.348		2,71	11.55		30.80	42.50
3/4" MPT x 1" CTS		╂┼	21	.381	├ ─├			 	14.26	20.50
						3.34	12.65	ĺ	15.99	23
1" MPT x 1" CTS		 	20	.400	<u> </u>	3,42	13.30		16.72	24.
1-1/4" MPT x 1-1/4" CTS			- 18	.444		5,25	14.80		20.05	28:50
1-1/2" MPT x 1-1/2" CTS	(() <u> </u> ()	<u> </u>	16	.500		.6.05.	. 16.65		22.70	-31.50
2" MPT x 2" CTS			13	.615		9.70	20.50		30.20	41.50
Spigot adapter, 3/4" IPS x 3/4" CTS			. 23	.348		2.71	11.55	<u> </u>	14.26	20.50
3/4" IPS x 1" CTS			21	.381		2.71	12,65		15.36	22
1" IPS x 1" CTS			20	.400		2.94	13.30		16.24	23
1-1/4" IPS x 1-1/4" CTS		!	18	.444		5.25	14.80		20.05	28.50
1-1/2" IPS x 1-1/2" CTS			16	.500		6.05	16.65		22.70	31.50
2" IPS x 2" CTS	:	▼	13	.615	+	9.70	20.50		30.20	41:50
Price includes insert stiffeners	· ' :				L]	İ		
250 psi is same price as 160 psi		·		-						: , ,
Insert type, nylon, 160 & 250 psi, cold w	ater			,	ĺ	1			1	
Clamp ring stainless steel, 3/4" IPS	2000	1 Plum	115	.070	Ea.	.62	2.31		2.93	4;18
1" IPS	4000		107	.075		.63	2.49		3.12	4.4
1-1/4" IPS			101 .	.079		.63	2.63		3.26	4.6
1-1/2" IPS			95	.084		.64	. 2.80		3,44	4.9
2" IPS			85	.094		.64	. 3.13		3.77	5.4
Coupling, 3/4" IPS			22	.364		.56	12.10	ŀ	12.66	18.90
1-1/4" IPS	,		18	.444	 -	1.34	14.80		16.14	24
1-1/2" IPS			. 17 .	.471		1,74	15.65	· · · · · ·	17.39	25.50
2" IPS			16	.500		2.09	16,65		18.74	27.5
Elbow, 90°, 3/4" IPS			22	.364		.82	12.10		12.92	19.20
1" IPS			19	.421		.90	14		14.90	22
1-1/4" IPS			18	.444	1 1	1.01	14.80		15.81	23:5
1-1/2" IPS		\vdash	17	.471		1.19	15.65		16.84	25.3
2" IPS			16	.500		1.67	16.65		18.32	27
Male adapter, 3/4" IPS x 3/4" MPT		-+-	25	.320		.57	10.65		11.22	16.7
1" IPS x 1" MPT			21	.381		.74	12.65	i	13.39	19.9
1-1/4" IPS x 1-1/4" MPT		\vdash	20	.400		1.23	13.30		14.53	21:5
1-1/2" IPS x 1-1/2" MPT			18	.444		1.63	14.80	~ -		24.5
2" IPS x 2" MPT		-	15	.533		2.09	17.75		16.43	L
Tee, 3/4" IPS			14	.553		1.07	17.73		19.84	29.5
1" IPS	- []	\vdash	13	.615			20.50	·	20.07	29:5
•			12	.667		1.75	(22.25	33.
1-1/4" IPS	╶Ѿ╼┖╼╌╌╟╌╢╣					3.14	22		25.14	37
1-1/2" IPS			11	.727		3.95	24		27.95	41
2" IPS		*	10	.800		5.35	26.50		31.85	46
Insert type, PVC, 100 psi @ 180°F, hot & o	cold water :	1	}	.:]		1 . 1	.]	٠.]	1.0
Coupler, male, 3/8" CTS x 3/8" MPT	<u>}</u> • • .	1 Plum	29	.276	Ea.	.96	9.15		. 10.11	14.9
3/8" CTS x 1/2" MPT			28	.286		.96	9.50		10.46	15.4
1/2" CTS x 1/2" MPT			27	.296		.30	.9.85		10.15	15.2
1/2" CTS x 3/4" MPT			26	.308		.86	10.25	٧,٠	11.11	16.4
3/4" CTS x 1/2" MPT			25	.320		.86	10.65.	i ja	11.51	17.0
3/4" CTS x 3/4" MPT		77	25	.320		4.11	10.65		. 14.76	20.5
Coupling, 3/8" CTS x 1/2" CTS		.	25	.320		2.15	10.65		12.80	18.4
1/2" CTS			23	.348	- -	2.50	11.55		14.05	20.5
1/2" CTS x stub			23	.348		1.96	11.55	· .	13.51	19.6
3/4" CTS	U	-++	22	.364		3.96	12.10		16.06	22.50
Elbow 90°, 3/8" CTS			25	.320		.65	10.65		11.30	16.8
1/2" CTS		++	23	.348	┵	.65	11.55	· · · · · · · · · · · · · · · · · · ·		18.20
•	<u> </u>					í	5		12.20	
3/4" CTS	1	*	22	.364	V	.82	12.10	1.0	12.92	19:20

1510	8 Plastic Pipe & Fittings	1	-DAILY	LABOR-		[2000 BAI	RE COSTS		TOTA
1510		CREW	OUTPU	HOURS	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL 0
8800	Rings, crimp, copper, 3/8" CTS	1 Plum	1 120	.067	Ea.	.11	2.22		2.33	7,0
8810	1/2" CTS		117	.068		.12	2.27		2.39	
8820	3/4" CTS	1	115	.070		.15	2.31		2.46	<u> </u>
8850.	Reducer tee, 3/8" x 3/8" x 1/2" CTS		17	.471		1.46	15.65		17.11	
8860	1/2" x 3/8" x 1/2" CTS	1-	15	.533		1.25	17.75		19	
8870	3/4" x 1/2" x 1/2" CTS		. 14	.571		1.31	17.73			1
8890		-	14	.571		1.31	19		20.31	
8900	3/4" x 3/4" x 1/2" CTS 3/4" x 1/2" x 3/8" CTS		14	.571					20.24	
8930	Tee, 3/8" CTS		17	.471		1.09	19		20.09	
8940	1/2" CTS		1	}		1.05	15.65		16.70	
8950	3/4" CTS	I - I -	15	.533		1.19	17.75		18.94	
L	7 7 5	▼	14	.571	♥	1.29	19		20.29	
8960	Copper rings included in fitting price	1	1							
9000	Flare type, assembled, acetal, hot & cold water									
9010	Coupling, 1/4" & 3/8" CTS	1 Plum		.333	Ea.	2.14	11.10		13.24	
9020	1/2" CTS	11	22	.364		2.45	12.10		14.55	
9030	3/4" CTS		21	.381		3.61	12.65		16.26	
9040	1" CTS	1.	18	.444		4.61	14.80		19,41	
9050	Elbow 90°, 1/4" CTS		26	.308		2.38	10.25		12.63	
9060	3/8" CTS	\Box	24	.333		2.55	11.10		. 13.65	12
9070	1/2" CTS		22	.364		3.01	12.10		15.11	
9080	. 3/4" CTS		21	.381		4.61	12.65	•	17.26	.;
9090	1" CTS		18	.444		5.80	14.80		20,60	×
9110	Tee ,1/4" & 3/8" CTS		15	.533		2.62	17.75		20.37	
9120	1/2" CTS		14	.571	. ()	3.44	19		22.44	
9130	3/4" CTS		13	.615		5.25	20.50		25.75	
9140	1" CTS		12	.667		. 7	22		29	
9550	For plastic hangers see 15060-300-8000		 	-	-	·				
9560	For copper/brass fittings see 15107-460-7000	. ·					.			
0010 PIP	E, HIGH DENSITY POLYETHYLENE PLASTIC (HDPE)									
	Not incl. hangers, trenching, backfill, hoisting or digging equipment.									٠,
0030	Standard length is 40', add a weld for each joint.		\vdash							
0050	Straight									
0054	1" diameter DR 11	 	 		L.F.	.28			.28	
0058	1-1/2" diameter DR 11	ŀ				.62			.62	
0062	2" diameter DR 11			· · ·		.79			.02	
0066	3" diameter DR 11								.79	\$. 1.4
0070	3" diameter DR 17		 			1.72			1.72	
	4" diameter DR 11					1.15			1.15	
0074			<u> </u>	·	$\sqcup \sqcup$	2.84			2.84	4
0078	4" diameter DR 17					1.91			1.91	10.7
082.	6" diameter DR 11	ļ				6.15			6.15	1
086	6" diameter DR 17	l				4.13			4.13	
090	8" diameter DR 11			*		10.40			10.40	
094	8" diameter DR 26			:		4.69			4.69	***
098	10" diameter DR 11					16.20			16.20	
102	10" diameter DR 26					7.25			7.25	2
106	12" diameter DR 11			<u>.</u>		23	-		23	
110	12" diameter DR 26					10.25			10.25	-
114	16" diameter DR 11				.	34			``34	
118	16" diameter DR 26			· .		15.20		,	15.20	
122	· 18" diameter DR 11					43 ·			43	1
126	18" diameter DR 26				-	19.20			19.20	
130	20" diameter DR 11				. •	53			53	
134	20" diameter DR 26					23.50			23.50	1.3
138	20' diameter DR 11			.:		I	1			
				<u> </u>		64			64	(
142	22" diameter DR 26			3		28.50			28.50	l `
146	24" diameter DR 11			a. 🛊		76			7.6	

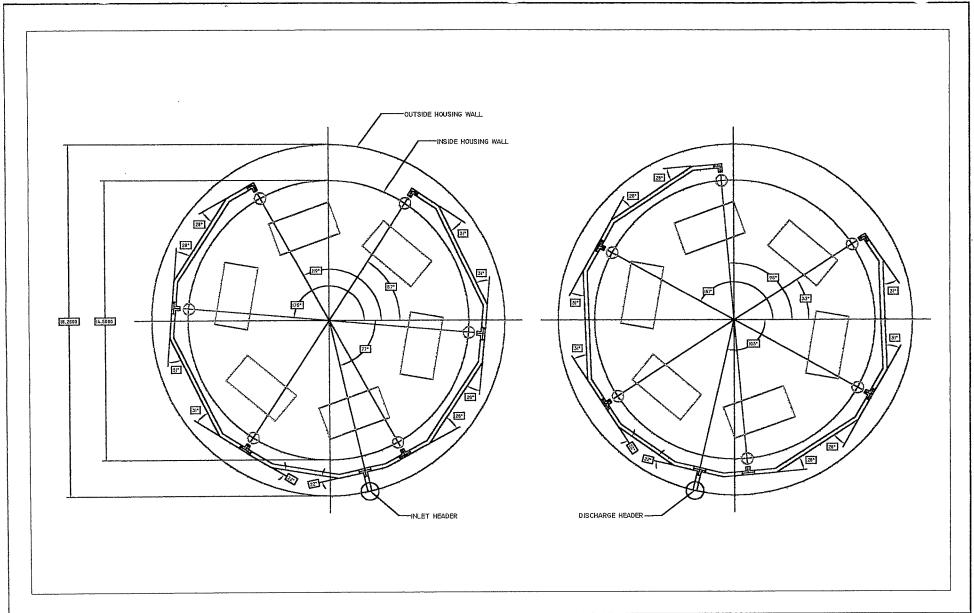
00 Building Services Piping					land Herri					
· · · · · · · · · · · · · · · · · · ·	77 h			LABOR-			2000 BARE			TOTAL
Valves	C	REW	OUTPUT	HOURS	UNIT	MAT.	LABOR	EQUIP.	TOTAL	INCL O&P
1-1/2" size	1	Stpi	11	.727·	Ea.	274	24.50		. 298.50	335
2" size	\perp	*	8	1		330	33.50		363.50	415
2-1/2" size		Q-5	5	3.200		360	96.50		456.50	540
3" size			4.50	3.556	*	380	107		487	580
Flanged	ı									
3" size	\perp	Q5	4.20	3.810	Ea.	415	115		530	630
4" size		"	. 3	5.333		835	161		996	1,175
5" size		Q6	3.80	6.316		990	197		1,187	1,400
6" size	1		3	8		1,200	250		1,450	1,700
8" size			2.50	9.600		1,775	300		2,075	2,400
10" size	T		2.20	10.909		2,525	340		2,865	3,300
12" size	-		2.10	11.429		7,075	355		7,430	8,350
14" size		V	2	12.	*	10,100	375		10,475	11,700
			,							
VES, PLASTIC R1510	<u> </u>						Ì			
Angle, PVC, threaded	41									
1/4" size	1	Plum	26	.308	Ea.	47.50	10.25		57.75	. 67:50
1/2" size	Ш		26	.308	:	47.50	10.25		57.75	67.50
3/4" size	\top		25	.320		55.50	10.65		66.15	77
1" size	Ш	₩	23	.348	V	66.50	11.55		78.05	90.50
Ball, PVC, socket or threaded, single union	11.			<i>i</i> .				•		,
1/4" size	1	Plum	26	.308	Ea.	22	10.25		32.25	39.5
3/8" size	П		26	.308		22	10.25		32.25	39.5
1/2" size			26	.308		22	10.25		32.25	39.5
3/4" size			25	.320		26.50	10.65	٠.	37.15	45
1" size			23	.348		31 、	11.55	-	42.55	51.5
1-1/4" size	Ш		21	.381		41.50	12.65		54.15	65 ·
1-1/2" size	Ш		20	.400		52	13.30	:	65.30	. 77
2" size	Ш	\downarrow	17	.471		. 74.50	15.65		90.15	105
2-1/2" size		Q-I	. 26	.615	L.L.	185	18.40		203.40	232 /
3" size	- 11		24	.667		185	19.95		204.95	234-:
4" size	Ш	<u> </u>	20	.800		320	24		344	385
For PVC, flanged, add	.					100%	15%		25.05	12
Double union 1/2" size		Plum		.308		25	10.25		35.25	43 46.5
3/4" size		•	25	.320		28	10.65		38.65	
1" size	Ш		23	.348	$\sqcup \bot$	35	11.55		46.55	83
1-1/4" size			21	.381		58	12.65		70.65	1
1-1/2" size	4		20	.400		58	13.30		71.30	111
2" size	Ш	₩	17	.471	♦	79.50	15.65		95.15	111
CPVC, socket or threaded, single union	Щ.				<u> </u>	25.50	10.05		AC 75	55.
1/2" size	: 	l Plum	I .	.308	Ea. 1	36.50	10.25		46.75 54.15	
: . 3/4" size	11	-	25	.320	1	43.50	10.65		62.55	1
1 5126	?. 1		23	.348		51	11.55		100.65	
1-1/4" size	Щ		. 21	.381	!	88	12.65 13.30		100.65	
1-1/2" size	, -	. . '	20	.400		88	15.65		133.65	1
2" size	1	<u></u>	17	.471	 -	118	19.95		267.95	<u> </u>
3" size	: []	Q-1	24	.667		. 248	1	-	207.93	303
101 01 10, nungeo, uou	Ш			1	1	65%	15%	 	· · · · · · · · · · · · · · · · · · ·	
For true union, socket or threaded, add					₩	50%	5%]	<u> </u>	
Polypropylene, threaded					1		<u></u>			1
1/4" size	\prod	1 Plum	1	.308	Ea.	30	10.25		40.25	
3/8" size	_]-[26	.308		30	10.25		40.25	
1/2" size		T	26	.308		30	10.25		40.25	
			25	.320		. 37.50		1	48.15	
1" size	\Box		23	.348		44.50	i	1	56.05	•
		\perp	2:1	.381	1 1	64.50	12.65	1	77.15	90

	100 Building Services P		: .	DAHV	LABOR-	(September 1999)		2000 BAR	COSTS		TOTAL
151	10 Valves		CREW			דואט	MAT.	LABOR	EQUIP.	TOTAL	INCL 0&P
			1 Plum	20	.400	. Ea.	74	13.30	EQUIF,	87.30	102
2170	1-1/2" size	R15100 -090	1 10111			. Ed.	1		`.	116.65	135
2180	2" size		▼	17	.471	<u> </u>	101	15.65			
2190	3" size	·	Q-1	24	.667		266	19.95	ļ	285.95	325
2200	4" size		" .	20	.800	▼	445	24		469	525
2550	PVC, three way, socket or threaded	. [1.5	
2600	1/2" size		1 Plum	26	.308	Ea.	56.50	10.25		- 66.75	77.5
2640	3/4" size			25	.320		64	10.65		74.65	86.5
1 1	1" size			23	.348		69.50	11.55		81.05	94
2650	1 -1/2" size		H - H	20	.400		140	13.30		153.30	174
2660	•			17	.471		188	15.65		203.65	231:
.2670	2" size		Q.1	24	.667	\vdash	455	19.95		474.95	530
2680	3" size		Á÷1	24	.007		1			777.55	330.
2740	For flanged, add		1			▼	60%	15%	·		•
3150	Ball check, PVC, socket or threaded									05.05	•
3200	1/4" size		1 Plum	. 26	.308	Ea.	25	10.25		35.25	43
3220	3/8" size		1 "	26	.308		25	10.25		35.25	43
3240	1/2" size			26	.308		25	10.25		35.25	43
3250	3/4" size	· · · · · · · · · · · · · · · · · · ·		25	.320		28	10.65	-	38.65	,46.
3260	1" size			23	.348		35	11.55		46.55	56
3270	1-1/4" size			21	.381		58	12.65		70.65	83
3280	1-1/2" size			20	.400		58	13.30		71.30	84
3290	2" size		$\dagger \downarrow$	17	.471		79	.15.65	• :	94.65	s ³ 111
1 1	3" size		Q1	24	.667		183	19.95		202.95	231
3310	4" size		+ **	20	.800		259	. 24		283	320
3320				-	,,,,,,		50%	15%			-4,7
3360	For PVC, flanged, add			<u> </u>	 	 •	3070	1570			ļ
3750	CPVC, socket or threaded	,	1,	00	200	٠,	20.50	10.25		46.75	55
3800	1/2" size		1 Plum	·	.308	Ea.	36.50	10.25		54.15	63
3840	3/4" size		1.	25	.320		43.50	1		62.55	1
3850	1" size			23	.348	1	51	11.55		l	1
3860	1-1/2" size			20	.400		88	13.30		101.30	E .
3870	2" size		♦	17	.471		118	15.65		133.65	·
3880	3" size	,	Q-1	24	.667		249	19.95		268.95	2
3920	4" size			20	.800		335	24		359	400
3930	For CPVC, flanged, add	:				\	40%	15%		. ',	
4340	Polypropylene, threaded									85.15.5	
4360	1/2" size		1 Plum	26	.308	Ea.	25	10.25	`.	35.25	
4400	3/4" size			25	.320		29	10.65		39.65	
4440	1" size			23	.348		37.50	11.55		49.05	
4450	1-1/2" size	*		20	.400		72.50	1		85.80	. 100
· I	2" size			17	.471	 -	91	15.65		106.65	
4460				-			200%	15%			
4500	For polypropylene flanged, add	·	H	+	+	╁┸	 	1		1	1
4850	Foot valve, PVC, socket or threaded		1 Plum	34	.235	Ea.	36.50	7.80		44.30	5.5
4900			I Fight	32	.250	1 -1	41.50			49.80	
4930	3/4" size	:		28	.286		54	9.50		63.50	1
4940		<u> </u>	╂┷┼╌			+	104	9.85	· ·	113.85	
4950	1-1/4" size	•		27	.296		1	1		114.25	8 .
4960			\coprod	26	.308	1	104.	10.25	<u> </u>	1	
4970	2" size	· ·	-	24	.333		120	11.10	l .	131.10	
4980	3" size			20	.400		287	13.30		300.30	
4990			₩	18	.444		505	14.80	1	519.80	•
5000	ì	•	`		1	₩	25%	10%			
5050			1	1	1.	1					:
	1		· 1 Plum	34	.235	Ea.	64.50	7.80	1	72.3	0 . 8
5060			H	32	.250		78	8.30		86.3	0 . 9
5070	1			28	.286	`	92	9.50	1	101.5	8
5080			H +	27	.296		129	9.85		. 138.8	_
5090	1	1		Į.			1	1	ı	160.2	
5100	1-1/2" size		∀ I	26	.308	♦	150	10.25		1 . 100,2	J 10

	00 Building Services Pi		I	DAILA	14000			2000 ወለ፡	ር ሶስየተየ		
_	O Valves		CREW	1	LABOR- T HOURS	2	MAT.	LABOR	RE COSTS EQUIP.	TOTAL	TOTAL INCL 0&P
	2" size	[1 1 Plum		.333	Ea.	193	11.10	LQUIT.	204.10	230
	3" size	R15100 -090		20	.400	Ī	365	13.30		1	
	4" size		+	18	.444	├	790	14.80		378.30	420
	For flanged, add		 V	10	.,,,,,		25%	14.80		804.80	890
┝	Needle valve, PVC, threaded		 	 	┼		23/0	10%			
	1/4" size		1 Plum	26	.308	Ea.	32	10.25		40.05	50.5
-	3/8" size		1 (1011	26	.308	Ca.	37			42.25	50.5
	1/2" size			Į.	1		ł	10.25		47.25	56
_			*	26	.308	 	37	10.25		47.25	56
	For polypropylene, add		İ			₩	10%			1	
-	Y check, PVC, socket or threaded		4	 							
	1/2" sìze		1 Plum	26	.308	Ea.	52.50	10.25		62.75	73
L	. 3/4" size			25	.320		56.50	10.65		67.15	78
	1" size	٥.		23	.348		62	11.55		73.55	85.5
L	1-1/4" size			21	.381		97	12.65		109.65	126
	1-1/2" size	1		20	400		105	13.30		118.30	136
	2" size		1	17	.471		131	15.65		146.65	169
	2-1/2" size		V	15	.533		277	17.75		294.75	330
_	3" size		Q-1	24	.667		260	19.95		279.95	315
	4" size	j	"	20	.800		455	24		479	535
	For PVC flanged, add		<u> </u>			*	45%	15%			
	Y sediment strainer, PVC, socket or threaded										
	1/2" size		1 Plum	26	.308	Ea.	29.50	10.25		39.75	48
-	3/4" size			24	.333		32	11.10	***************************************	43,10	52.5
	l" size		1	23	.348		39	11.55		50.55	60.5
	1-1/4" size			21	.381		64.50	12.65		77.15	. 90
	1-1/2" size	-{		. 20	.400		67.50	13.30		80.80	94.5
	2" size			17	.471		78.50	15.65		94.15	110
	2-1/2" size		↓	15	.533		192	17.75		209.75	238
	3" size		Q1	24	.667		192	19.95		211.95	241
;	4" size		"	20	.800		320	24		344	385
!	For PVC, flanged, add	*				*	55%	15%			
V	ALVES, SEMI-STEEL	R15100	-								
	Lubricated plug valve, threaded, 200 psi	-090			l						
	1/2" pipe size		1 Plum	18	.444	Ea.	61.50	14.80		76.30	90
	3/4" pipe size			16	.500	11	61.50	16.65	}	78.15	92.5
•	l" pipe size			14	.571	$\dashv \dashv$	79	19		98	116
	1-1/4" pipe size			12	.667		95	22	}	117	139
•	1-1/2" pipe size			11	.727		102	24		126	149
	2" pipe size			8	1		120	33.50		153.50	183
	2-1/2" pipe size		Q-1	5	3.200	$\dashv \dashv$	186	96		282	350
	3" pipe size		"	4.50	3.556	11	228	106	1	334	410
	Flanged, 200 psi			7.00	3.330		220	100		334	. 410
	2" pipe size		1 Plum	8	1	Ea.	145	22 50	1	170 50	013
	2-1/2" pipe size		Q-1	5	3.200	La.	218	33.50 96		178.50	211
	3" pipe size		1	4.50	3.556		1	ľ		314	385
						-+-+	264	106		370	450
	4" pipe size			3	5.333		335	160	1	495	610
	5" pipe size		▼	2.50	6.400		500	192		692	840
	6" pipe size		Q2	3	8		655	248		903	1,100
	8" pipe size			2.50	9.600		1,125	298		1,423	1,700
	10" pipe size]]		,	10.909		1,725	340	T	2,065	2,400
	12" pipe size	<u>+</u>	*	1.70	14.118	V	2,975	440		3,415	3,925
11	NI VES, STEEL	R15100 -090									
	ાત્તી	1-020		1	- 1	1	1	ļ		1	ł
	Check valve, swing type, 150 lb., flanged		1								

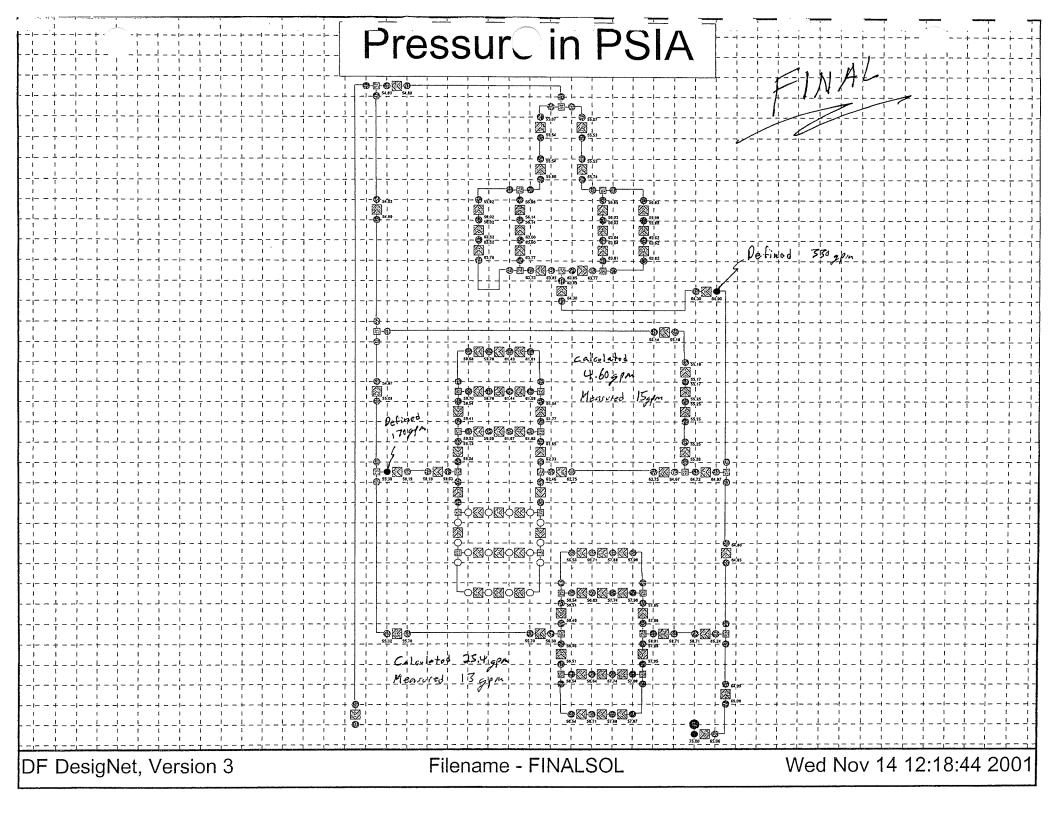
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APPENDIX F



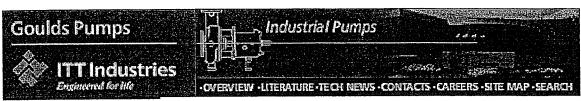
MA HADEO	NEWFOUNDLAND AND LABRA	ADOR HYDRO	
SCALE: N/A DRAWN: S.WHITE CHECKED: APPROVED:	HINDS LAKE LOWER GEN COOLER PIPING	DATE: 9/09/0 W.D# DWG# REV. 0	

APPENDIX G

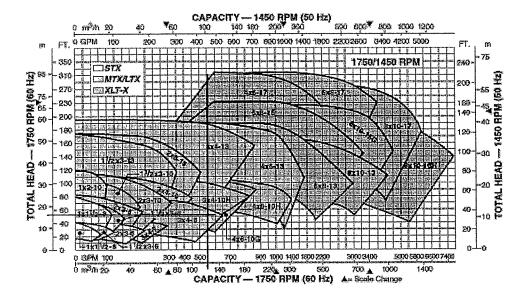


APPENDIX H

HLK



Previous Page



50 Hz	60 Hz
1480 RPM	1780 RPM
1X1.5-6-Alloy	1X1.5-6-Alloy
1x1.5-6-Iron	1X1.5-6-Iron
1.5X3-6	1.5X3-6
2x3-6-Alloy	2x3-6-Alloy
2x3-6-lron	2x3-6-Iron
1x1.5-8-Alloy	1x1.5-8-Alloy
1x1.5-8-Iron	1X1.5-8-Iron
	1.5Y3-8-Alloy
1.5X3-8-Alloy	1.5X3-8-Alloy 1.5X3-8-Iron
1.5X3-8-Iron	1.3/3-0-11011
2X3-8-Alloy 2X3-8-Iron	2X3-8-Alloy
2X3-8-Iron	2X3-8-Iron
3x4-7	3x4-7
3X4-8	3X4-8
3X4-8G	3X4-8G
1X2-10-Alloy	1X2-10-Alloy
1X2-10-Iron	1X2-10-Iron
1.5X3-10-Alloy	1.5X3-10-Alloy
1.5X3-10-Iron	1.5X3-10-lron
2X3-10	2X3-10
3x4-10	3X4-10
3X4-10H	3X4-10H
4X6-10	4X6-10
4X6-10H-Alloy	4x6-10H-Alloy
4x6-10H-Iron	4x6-10H-Iron
4X6-10G	4X6-10G
1.5x3-13-Alloy	1.5x3-13-Allov
1.5x3-13-Iron	1.5x3-13-Alloy 1.5x3-13-Iron
2X3-13	2X3-13
2/3-13	3x4-13
3x4-13	10 10 10 10 10
4X6-13 6X8-13	4X6-13 6X8-13
0.40.40	1000-13
8x10-13	8x10-13
6X8-15	6X8-15
8X10-15	8X10-15G
8X10-15G	8x10-16H
Н	H

